

Implementing Circular Economy Concept by Converting Cassava Pulp and Wastewater to Biogas for Sustainable Production in Starch Industry

Ruenrom Lerdlattaporn

The Joint Graduate School of Energy and Environment, King Mongkut's University of Technology Thonburi

Chantaraporn Phalakornkule

King Mongkut's University of Technology North Bangkok Faculty of Chemical Engineering

Sivalee Trakulvichean

Pilot Plant Development and Training Institute, King Mongkut's University of Technology Thonburi

Warinthorn Songkasiri (✉ warinthorn@biotec.or.th)

National Center for Genetic Engineering and Biotechnology <https://orcid.org/0000-0002-7730-6388>

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1 **Implementing Circular Economy Concept by Converting Cassava Pulp and Wastewater**
2 **to Biogas for Sustainable Production in Starch Industry**

3 Ruenrom Lerdlattaporn¹, Chantaraporn Phalakornkule^{1,2}, Sivalee Trakulvichean³, Warinthorn
4 Songkasiri^{3,4,*}

5 ¹*The Joint Graduate School of Energy and Environment, King Mongkut's University of*
6 *Technology Thonburi, Bangkok, Thailand.*

7 ²*Department of Chemical Engineering, Faculty of Engineering, King Mongkut's University of*
8 *Technology North Bangkok, Thailand.*

9 ³*Pilot Plant Development and Training Institute, King Mongkut's University of Technology*
10 *Thonburi, Bangkok, Thailand.*

11 ⁴*National Center for Genetic Engineering and Biotechnology (BIOTEC), National Science*
12 *and Technology Development Agency (NSTDA), Bangkok, Thailand.*

13 * *Corresponding author: warinthorn@biotec.or.th*

14 **Highlights**

- 15 • Converting cassava pulp and wastewater to biogas is one way to apply CE concept.
16 • 77% of GHG emission reduction comes from using cassava pulp and wastewater to
17 biogas production.
18 • The advantages of CE concept adaption in cassava starch industry are increase energy
19 security and resource efficiency.
20 • Regulatory and social responsibility are the key drivers for CE concept implementation
21 in cassava starch industry.

22 **Abstract**

23 This research integrated the circular economy (CE) concept in the cassava starch industry in
24 Thailand, and revealed the benefits of biogas generation from both the wastewater and waste
25 cassava pulp with a focus on the identification and analysis of the key drivers and challenges
26 to increase the efficiency of the biogas system. The research methodology applied the CE
27 concept for scenarios of cassava pulp utilization for biogas production, compared to the no
28 waste treatment and anaerobic wastewater treatment scenarios, in terms of an economic
29 assessment, resource efficiency, water recovery, land use, and global warming potential.
30 Proposed options mainly involved the conservation of energy, water, land use, and reduction

31 of greenhouse gases emissions. These included the reuse and recycling of water and use of
32 biogas to substitute for fuel oil for burners and electricity in the cassava starch production
33 process.

34 **Keywords:** anaerobic digestion, GHG emission, biogas, tapioca starch

35 **1. Introduction**

36 The circular economy (CE) concept, or simply circularity, is an increasingly popular
37 concept in the effort to maximize resources and minimize waste. It is an economic system
38 aimed at eliminating waste and continually using or recirculating resources. The CE concept
39 involves the reuse, sharing, repairing, refurbishing, remanufacturing, and recycling of materials
40 to create a closed-loop system. The advantages of the CE concept are reduced costs from the
41 efficient use of energy and resources and waste management costs, increased income from
42 waste utilization as a raw material in the process, and reduced emissions, pollution, and release
43 of chemical substances to the environment via soil, water, and air (Geissdoerfer et al., 2017;
44 Lieder and Rashid 2016; Murray et al., 2017; Morsetto, 2020).

45 Cassava is an economically important tuber crop in Thailand that is used in food, animal
46 feed, pharmaceuticals, production of bioethanol, and other industries. In 2017, Thailand was
47 the world's largest exporter of cassava starch with a 68% market share. Approximately 4.2
48 million tons (t) of native cassava starch were produced in Thailand and 75% of this was
49 exported (Chuasuan, 2018). The export value of native starch increased from US\$ 1.2 billion
50 in 2017 to US\$ 1.5 Billion in 2018 (Thai Customs Department, 2019).

51 The cassava starch production process (CSPP) generally has eight steps, which are
52 comprised of: receiving cassava roots from suppliers, screening out rocks and soil, washing the
53 roots, rasping them into smaller pieces, extracting the starch granules from the cassava pulp,
54 separating the impurity from the starch slurry, dewatering, and drying to obtain starch
55 (Songkasiri et al., 2014a), as shown in Figure 1. One ton of starch is produced from
56 approximately 4.4 t of cassava roots, using 10.9 m³ of water, 207.8 kWh of electricity, 1,898.2
57 MJ of fuel for drying the starch, 0.9 kg of chemicals, and 93.1 m³ of biogas for use in the boiler
58 and to generate electricity. Wastes from the CSPP typically consist of 0.6 t rhizomes, 0.17 t
59 sand, 0.1 t cassava peels, 2.5 t wet pulp, 8.4 m³ wastewater, and 4.0 kg of low-grade starch
60 (Trakulvichean et al., 2019).

61 The wastewater has a high chemical organic content, measured as an oxygen demand
62 (COD) level (4,800 – 70,000 mg/L), high total volatile solids (1,200 – 39,000 mg/L), and a
63 low pH (4.3 – 5.6) (Chavalparit and Ongwandee, 2009; Colin et al., 2007; Paixão et al., 2000;

81 can be applied to the CSPP to minimize the wastewater (Dakwala, 2011; Yesaswini and
82 Saravanathamizhan, 2018).

83 The reuse of wastewater exiting CSPP is proposed as follows: (i) wastewater from coarse
84 extraction and pulp dewatering unit are reused to chopping and rasping unit, (ii) wastewater
85 from the fine extraction, separating, and dewatering units are reused to coarse extraction unit,
86 (iii) wastewater from the separating unit reused to fine extraction unit, and (iv) wastewater
87 from dewatering unit reused to separating unit. Accumulation of contaminants, i.e., protein and
88 fiber is needed to be monitored (Songkasiri et al., 2014a).

89 For the water recycling, wastewater from the CSPP occurs in the separating unit
90 (Chavalparit and Ongwandee, 2009; Songkasiri et al., 2014b). The effluent stream consists of
91 starch, protein, fine fiber, and toxic chemicals and can be treated by both aerobic and anaerobic
92 treatments. However, aerobic treatment produces a bad odor and requires a large area so most
93 cassava starch factories use anaerobic treatment. The advantages of the anaerobic treatment are
94 (i) reduce the cyanide toxicity, (ii) reduce bad odors, and (iii) remove the organic matter to
95 produce biogas (Fukushima et al., 2016; Rajbhandari and Annachhatre, 2014; Oliveira, et al.,
96 2001).

97 Wastewater from the CSPP is used to produce biogas, which in turn is used to generate heat
98 and electricity for factories with surplus electricity being sold to the grid. According to the
99 updated Thai Alternative Energy Development Plan (AEDP) in 2018 under the concept of
100 energy security, there has been a tendency to increase strategies that promote biogas formation
101 from waste and wastewater, and this is predicted to increase from the current 546 MW to 928
102 MW by 2037, which would increase the proportion of electricity produced from renewable
103 energy (RE) in Thailand to 20% of the overall capacity in the country (DEDE, 2019).

104 Solid waste from the CSPP consists of pulp, peel, sand, and rhizomes. The adaptation of
105 CE concept by using the solid waste as the raw material to produce value added products is an
106 important option for the long-term sustainability of the CSPP. These valued added products
107 can be divided in three sectors: biofuels, biochemical, and biobased products for agriculture.

108 Peel, sand, and rhizomes are usually used as a soil conditioner. Moreover, other options for
109 peel utilization include to sell it as animal feed and to use to produce biofuel, such as biochar.
110 (Lounglawan et al., 2011; Sivamani et al., 2018). Rhizome utilization options are its use as an
111 adsorbant for metal ions from rivers (Jorgetto et al., 2014) and combusted to produce heat in
112 form of fuel pellets, briquettes, biochar, and bio-oil (Torii et al., 2011; Sivamani et al., 2018).

113 However, most of the solid waste is cassava pulp, with currently around six million tons being
114 produced annually in Thailand from the CSPP.

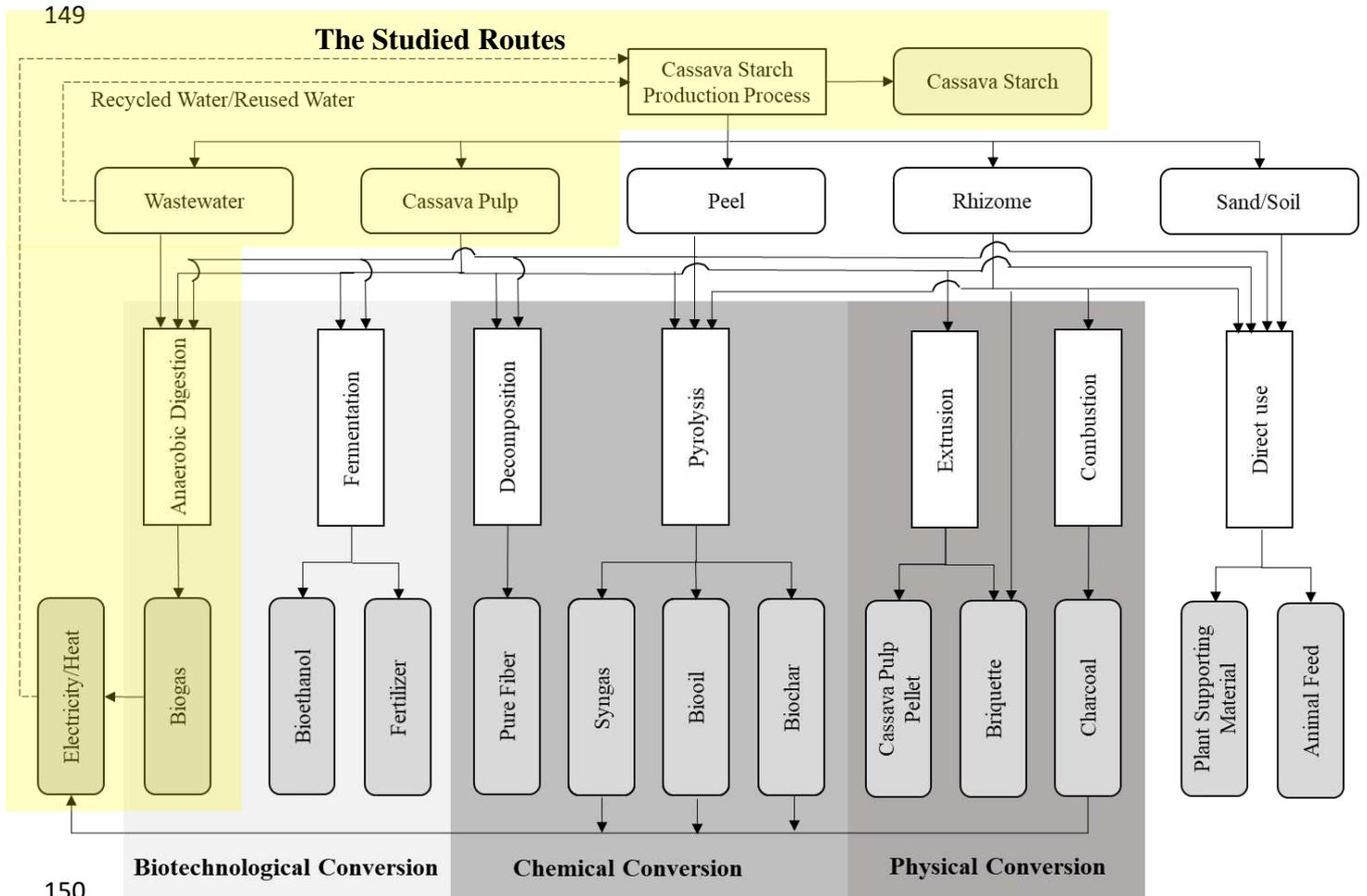
115 The current options for cassava pulp utilization are to sell it as raw material for animal feed,
116 produce cassava pellets, use as raw material for mushroom growing media, or it is sometimes
117 given to farmers for free (Trakulvichean et al., 2017; Sivamani et al., 2018). The retail prices
118 of wet and dried cassava pulp are 5.98 and 83.11 US\$/t, respectively. Nevertheless, disposing
119 of the cassava pulp in these options lead to the problem of a strong odor from its fermentation,
120 especially during the rainy season. Moreover, laws and regulations on waste management place
121 limits on the transport of cassava pulp. Cassava pulp has high organic content that has the
122 potential for use as a feedstock for biogas because it is mostly comprised of lignocellulose with
123 (by weight in dry basis) 60 – 75% starch, 13 – 28% crude fiber, 4 – 15% cellulose, 4 – 5%
124 hemicellulose, 1 – 3% lignin, 1 – 2% protein, 0.1 – 0.2% lipids, 2 – 12% ash, and 1 – 17% of
125 other materials (Chavalparit and Ongwandee, 2009; Rattanachomsri et al., 2009; Sriroth et al.,
126 2000; Virunanon et al., 2013; Yimmongkol and Jattupornpong, 2007) as well as an alternative
127 for waste reduction and environmental improvement due to reducing greenhouse gas (GHG)
128 emissions (Hansupalak et al., 2016). Dried cassava pulp is sold to pellet or fertilizer at 9.00 –
129 17.79 US\$/t. The pulp can instead be used to produce biogas as LPG which can be sold to
130 generate about 18.00 US\$/t of pulp. By using the biogas instead of fuel oil to produce the heat
131 and generate electricity, it can generate an equivalent value of 13.33 and 5.00 US\$/t of cassava
132 pulp, respectively.

133 However, the use of the lignocellulosic materials found in cassava pulp for biogas
134 production is limited because these substrates are very difficult to digest and resist microbial
135 hydrolysis in biogas production. Despite these limitations of the production biogas from
136 cassava pulp at a commercial level are the pretreatment technology, conversion technology,
137 and cost-effectiveness (Jeihanipour, 2011; DIW, 2010).

138 For resource efficiency, problems encountered in converting cassava pulp to biogas have
139 to be overcome in order that starch factories can be accredited for adaption the CE concept that
140 produces biogas from both the wastewater and cassava pulp for generation of heat and
141 electricity. For the industrial process, three scenarios are considered as follows: **scenario 1** is
142 without a biogas system in factory, **scenario 2** is with biogas generation from the wastewater
143 only, and **scenario 3** is with biogas generation from both the wastewater and cassava pulp.

144 Since **scenarios 1** and **2** above are well documented, this study, focus on investigating the
145 benefits of using **scenario 3**, that is using both the wastewater and cassava pulp for biogas
146 production in the cassava starch industry in Thailand as summarized schematically in Figure

147 2. In addition, this research also highlights the main drivers and barriers to implementing the
 148 CE concept in the CSPP in Thailand.



151 **Fig. 2** Implementation of CE concept in the Thai cassava starch industry

152 **2. Methodology**

153 In 2020, Thailand has 112 cassava starch factories in operation and they generate a total of
 154 10.5 million t/y of wet pulp, and 35.1 million m³/y of wastewater from the production process
 155 (Trakulvichean et al., 2019). The number includes both native and modified starch factories.
 156 Sixty-two (55.4%) of these factories have biogas generation systems from the wastewater only,
 157 six (5.4%) factories have biogas systems from both the wastewater and pulp and two (1.8%)
 158 currently only have biogas systems from the wastewater but biogas systems from cassava pulp
 159 are under construction. Fifty of these factories are considered small with a production capacity
 160 of less than 100 t/d, and so these factories do not qualify for the investment necessary to build
 161 a biogas system from wastewater and cassava pulp. Unless their production capacity increases,
 162 the use of biogas from wastewater in those 62 factories will likely not increase.

163 Data was collected from a native cassava starch factory in Northeastern Thailand in the
164 base period of January to December 2018. The starch production capacity was 500 t/d. A
165 systematic methodology to use wastewater and cassava pulp for biogas production in the starch
166 industry, in terms of the economics, resource efficiency, water recovery, reduction of the GHG
167 emission, and land use.

168 2.1 Data collection of biogas production in the cassava starch factory

169 *2.1.1 Data collection*

170 Primary data was obtained from a native cassava starch factory in the Northeastern region
171 of Thailand. The starch production capacity was 500 t/d with 196 working d/y. Wastewater
172 from the starch production process was 1,135,944 m³/y, while solid waste pulp generation from
173 the process was approximately 450 t/d. Biogas conversion technology for wastewater
174 comprised a covered lagoon with a wastewater receiving capacity of 165,970 m³, while the
175 biogas conversion technology of the solid cassava pulp used a thermophilic continuously
176 stirred tank reactor (CSTR) at 55°C with pulp utilization capacity of 450 t/d.

177 *2.1.2 Scope and system boundary*

178 The system boundary of this study was scoped gate-to-gate to compare with the three
179 studied scenarios (introduction). The economics, resource efficiency, water recovery, reduction
180 of GHG emissions, and land use of these three scenarios were analyzed with a 10-y operational
181 period base.

182 2.2 Resource efficiency and water recovery analysis

183 The study aims to minimize waste generation and emissions by incorporating resource use
184 efficiency in a closed-loop product. Resource and water consumption input to the process was
185 calculated using the life cycle inventory for the three studied scenarios (section 2.1.2), and the
186 resource efficiency and water recovery analysis was undertaken and compared between the
187 three studied scenarios.

188 As stated, one ton of starch is produced from approximately 4.4 t of cassava roots, using
189 16.7 m³ of water, 197.8 kWh of electricity, 1,644.4 MJ of fuel for drying the starch, 0.4 kg of
190 chemicals, and 59.3 m³ of biogas for use in the boiler and to generate electricity. Waste from
191 the production process consisted of 0.5, 0.4, 0.1, and 1.6 t dry basis of rhizomes, sand, peels,
192 and dried pulp, respectively, and 7 kg dry basis of low-grade starch, plus 19.6 m³ of wastewater.
193 The low-grade starch is the large particles and defect color that occurs during the production
194 process. The low-grade cassava starch is reprocessed to increase the production capacity by

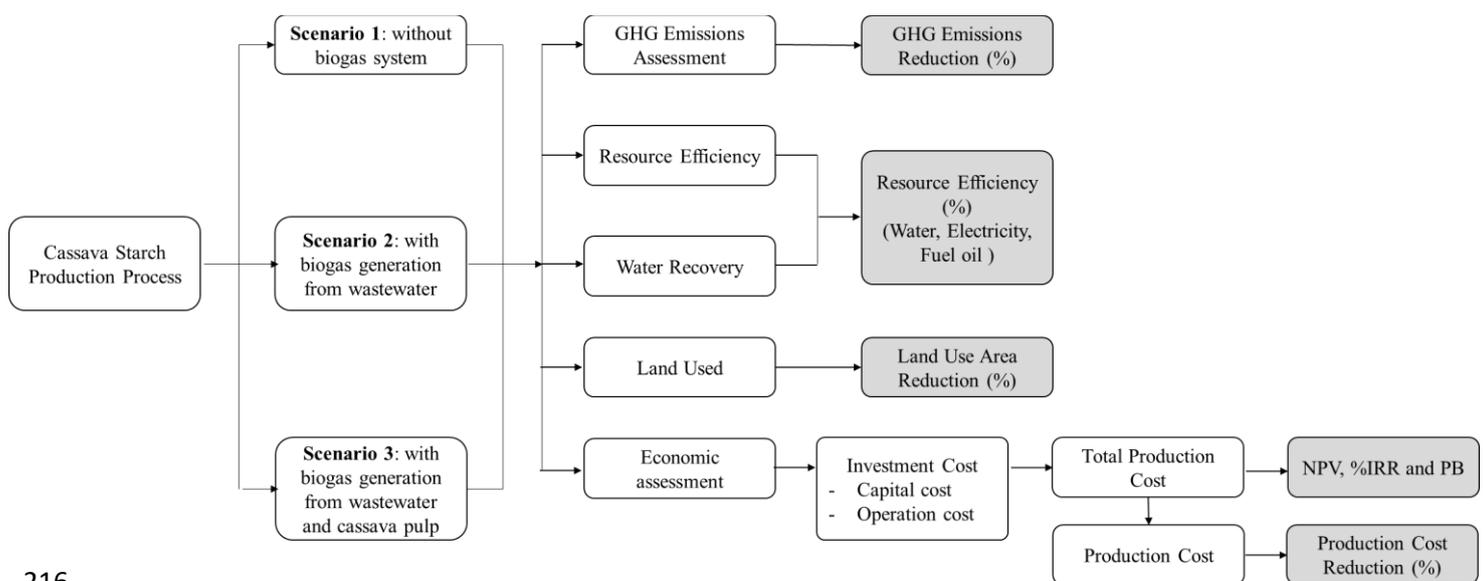
195 reducing the starch loss. Figure 3 presents a simplified input and output summary of the CSPP
 196 at the case study site in Thailand.

197 A case study was undertaken of a cassava factory that had a starch production capacity of
 198 500 t/d and generated 6,560 m³/d wastewater with a COD of 12,184 mg/L. The biogas
 199 production system was a covered lagoon for the wastewater treatment and a CSTR for biogas
 200 production from the cassava pulp. The covered lagoon was 165,970 m³ in size with a retention
 201 time of 15 d. The system yielded a COD removal efficiency of 92%, achieving a COD at the
 202 outlet of 1,037 mg/L and produced 41,000 m³ biogas/d with a CH₄ composition of 55% by
 203 volume.

204 In this same case study, the pulp was transported to the biogas plant in the starch factory,
 205 where the biogas production capacity from the pulp was 3.2 m³ biogas/m³ reactor • day using
 206 the thermophilic (55°C) CSTR technology with 15% (w/v) total solid (TS). The primary and
 207 secondary digesters were operated in series, with a buffer tank after the secondary digesters.
 208 The sediment from the buffer tank was recycled to the primary digesters, which contained the
 209 thermophilic anaerobic bacteria, to ensure the stable operation of the system and enhance the
 210 CH₄ content in the biogas. The average biogas production yield was 500 m³/t TS under a
 211 hydraulic retention time of 16 d, and yielded 22,500 m³ biogas/d.

212 2.3 Environmental and economic analysis

213 The benefits of applying the CE concept in the cassava starch industry were assessed in
 214 terms of an economic assessment, resource efficiency, water recovery, reduction in GHG
 215 emission and GHG emissions, and land use. The research framework is illustrated in Figure 3.



216

217 **Fig. 3** Research framework

250 the same amount of up-front investment, the project with the highest IRR would be considered
251 the best and undertaken first. The IRR was calculated from Eq. (2),

$$252 \quad 0 = \sum_{t=1}^T \frac{C_t}{(1+IRR)^t} \quad (2),$$

253 *(iii) Calculation of the PBP*

254 The PBP is the period of time required to recoup the funds expended in the investment,
255 and was calculated from Eq. (3);

$$256 \quad PBP = \frac{\text{Cost of investment}}{\text{Annual cash inflow}} \quad (3),$$

257 2.4 Drivers and barriers to applying the CE concept in the Thai CSPP

258 Data was collected from twelve cassava starch industries to determine the drivers and
259 barriers to implementation of the CE concept. The information was collected using surveys,
260 interviews, and questionnaires. Four of these factories applied biogas production from cassava
261 pulp under the CE concept.

262

263 3. Results and Discussion

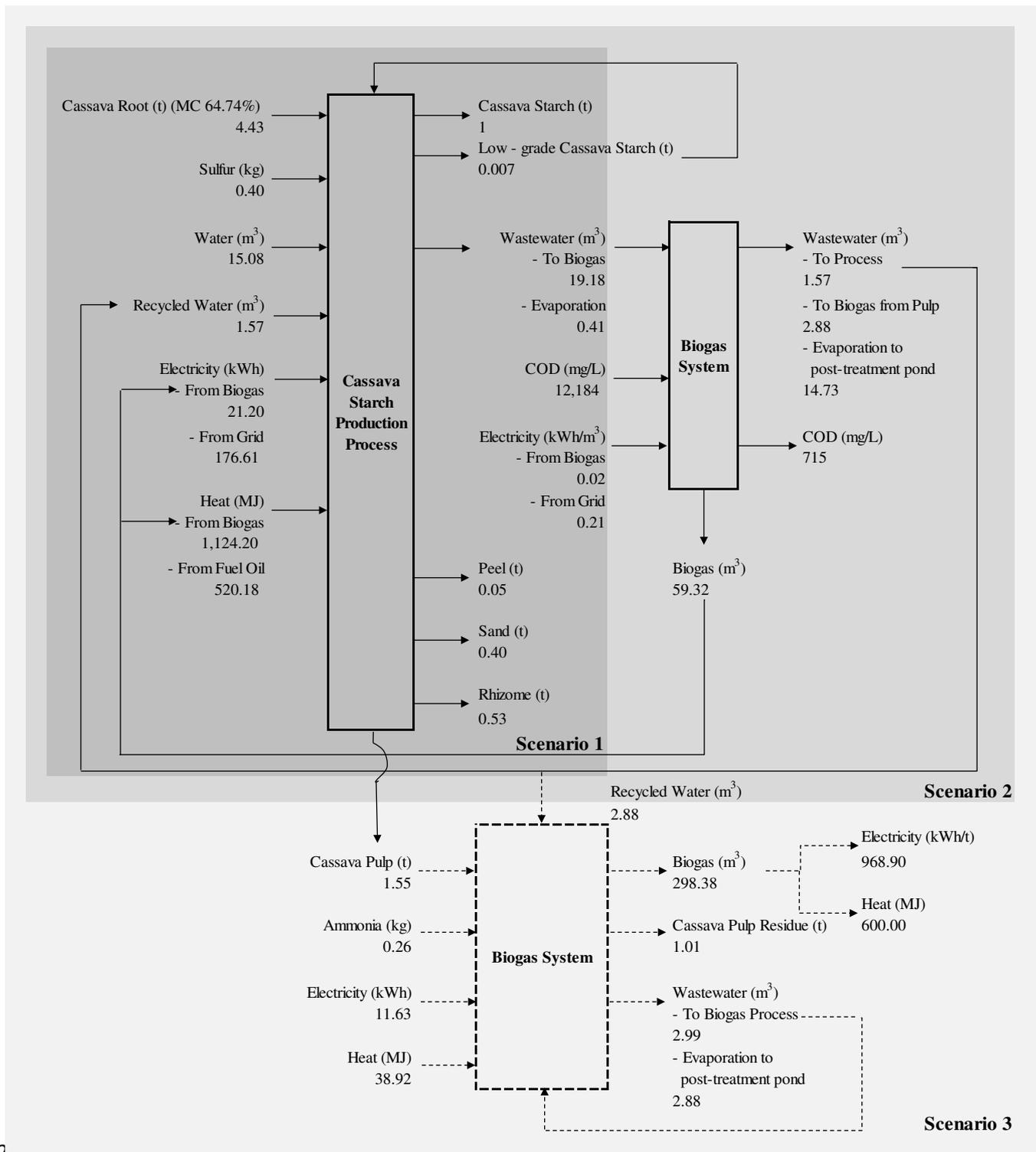
264 3.1 Resource efficiency analysis

265 3.1.1 Analysis of water consumption and waste generation

266 For each ton of cassava starch, the water consumption within the starch production
267 process in **Scenario 1** used 16.7 m³ of freshwater and generated 19.6 m³ of effluent as show in
268 table 1 and figure 4. The wastewater enters the open lagoon for evaporation. To minimize
269 wastewater sources, starch factories should recycle the water in the production process. In the
270 existing process, wastewater from the separating and dewatering units were reused to the
271 extracting and separating unit. The used water from the dewatering unit contained protein
272 impurities and so was not suitable to be reused in the other stages except for root washing.
273 However, the used water from the extracting unit can be returned to the chopping and rasping
274 unit because the water contained extracted starch (Sánchez et al., 2017).

275 For **Scenario 2**, the water consumption (per ton of cassava starch) was 15.1 m³ of
276 freshwater and 1.6 m³ of recycled water, generating 19.6 m³ of effluent. The wastewater entered
277 the covered lagoon to generate 59.3 m³ of biogas. For **Scenario 3**, the water consumption was
278 15.1 m³ of freshwater and 1.6 m³ of recycled water to generate 17.6 m³ of effluent. The
279 wastewater entered the covered lagoon to generate 357.8 m³ biogas as show in figure 4. The
280 biogas from **Scenario 2 and 3** used to producing heat and electricity in the CSPP. The treated
281 wastewater was discharged into the open lagoon and then evaporated. Rather than evaporation,

282 an alternative approach is to use the macronutrients dissolved within the effluent as liquid
 283 fertilizer (Sánchez et al., 2017; Songkasiri et al., 2014b).



285 **Fig. 4** Resource consumption and waste generation (per one ton of cassava starch produced)
 286 from CSPP. Three scenarios of starch production consist of (i) **scenario 1**, without biogas
 287 system in factory, (ii) **scenario 2**, with biogas generation from wastewater, and (iii) **scenario**
 288 **3**, with biogas generation from wastewater and cassava pulp.

289 *3.1.2 Analysis of energy consumptions*

290 The electricity consumption of the CSPP was calculated as 197.8 kWh/t of cassava starch.
291 For **Scenario 2**, 4.5 kWh/t cassava starch produced was required for the biogas system from
292 wastewater, whereas in **Scenario 3** this was almost 2.6-fold higher at 11.6 kWh/t the CSPP as
293 show in table 1. However, the biogas obtained from the wastewater produced 21.2 kWh of
294 electricity or 2.54 US\$/t of starch, while the biogas production from cassava pulp produced
295 968.9 kWh of electricity and then be used in the CSPP 176.6 kWh or 21.19 US\$/t of starch.
296 Therefore, a surplus of 738.4 kWh from **Scenario 3** was generated and could theoretically be
297 sold to the electricity grid as 88.60 US\$/t of starch as show in table 1 and figure 4.

298 The fuel oil used to supply process heat for the flash dryer was evaluated as 1,518.5 MJ.
299 Biogas recovery from the wastewater treatment system has shown great potential for cassava
300 starch factories. Since the price of fuel oil has increased significantly over the past decade,
301 cassava starch factories have been using biogas to replace the fuel oil for the burners to generate
302 hot air for drying the moist starch. The direct burning of the biogas obtained from the
303 wastewater can supply 1,124.2 MJ of energy. Moreover, the biogas from **Scenario 3** is able to
304 supply 1,724.2 MJ of energy as show in table 1. In conclusion, the fuel oil is unnecessary for
305 thermal energy in the CSPP. The recovered biogas from the wastewater and cassava pulp was
306 used to substitute fuel oil of 29.4 and 15.7 L/t of starch and this helped to reduce the fuel cost
307 by approximately 16.49 and 8.80 US\$/t of starch, respectively, based upon the cost of fuel oil
308 at 0.56 US\$/L as show in table 1 and figure 4.

309 *3.1.3 Cost reduction*

310 One of the starch factories that recently changed its pulp utilization options from dried
311 cassava pulp to biogas production has shown a significant saving on the fuel oil and electricity
312 used. However, the main production cost in the CSPP is the expenditure on purchasing cassava
313 roots, which makes up to 83 – 91% of the total costs. The other costs are electricity (3 – 9%),
314 fuel (4 – 5%), water (1%), chemicals (4%), and labor (2%) (Songkasiri et al., 2014b). The
315 reduction in the fuel oil and electricity from biogas in **Scenarios 2** and **3** reduced the total costs
316 by 4% and 11%, respectively as show in figure 5. A return to the government actively
317 promoting investment through incentives, as well as easing of conditions for sale to the grid
318 would see these figures improve dramatically through the additional income it would provide.

319 *3.2 Environmental impact assessment*

320 The CE concept focuses on reducing the landfill, GHG emission, and production energy
321 consumption, while increasing the resource use efficiency and so enabling a new life-cycle for

322 the otherwise end-of-life product. Regarding the minimization of the GHG emissions, the CO₂
 323 equivalent from the three scenarios was considered in this study to analyze the GHG emission.

324 In this study, the GHG emission was related to the emissions from electricity consumption,
 325 energy consumption, cassava pulp utilization options, and water treatment methods. Under
 326 **Scenario 3**, the cassava starch industry applied the CE concept, including a covered lagoon for
 327 biogas generation from wastewater and a CSTR for biogas generation from the cassava pulp,
 328 reducing the GHG emission by 77% as show in figure 5. This result was achieved by the
 329 reduced electricity consumption from the electricity grid and the reduced GHG emission from
 330 wastewater treatment using anaerobic technology.

331 **Table 1.** The resource usage, waste generation, GHG emission, and land use of the Thai CSPP
 332 (per one ton of cassava starch produced)

	Scenario 1	Scenario 2	Scenario 3
Resource usage			
Cassava root (t dry basis)	1.56	1.56	1.56
Fresh water (m ³)	16.65	15.08	15.08
Chemical (kg)	0.26	0.26	0.66
Recycled water (m ³)	0.00	1.57	4.45
Biogas production (m ³)	0.00	59.32	357.70
Electricity from grid (kWh)	197.8	176.6	0.0
Electricity from biogas (kWh)	0.0	21.2	197.8
			(Surplus:738.4)
Fuel oil consumption (L)	45.15	15.71	0.00
Biogas for drying (m ³)	0.00	64.45	98.84
Waste generation			
Wastewater to final open lagoons (m ³)	19.18	14.73	17.61
COD of wastewater to final open lagoons (mg/L)	12,184	715	715
Cassava pulp (t dry basis)	1.55	1.55	1.01
Peel (t dry basis)	0.05	0.05	0.05
Rhizome (t dry basis)	0.53	0.53	0.53
Sand/soil (t dry basis)	0.40	0.40	0.40
GHG emission (kg CO_{2eq})			

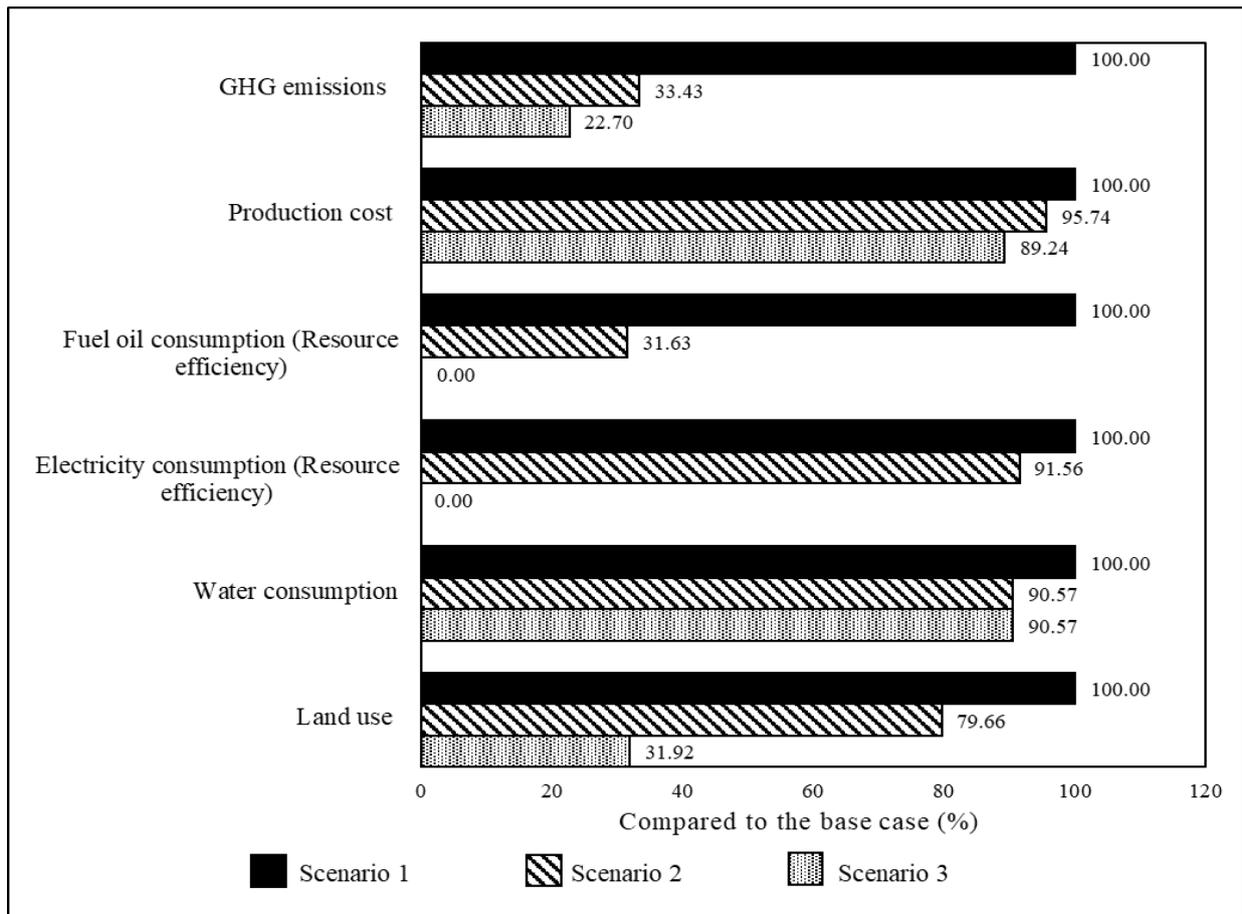
	Scenario 1	Scenario 2	Scenario 3
Wastewater	398.67	15.74	15.74
Cassava pulp fermentation	0.71	0.71	0.47
Electricity consumption in biogas system	-	0.15	19.93
Electricity consumption in cassava starch production	115.15	106.36	33.26
Thermal consumption in biogas system	-	-	0.00 (3×10^{-3})
Thermal consumption in cassava starch production	121.42	89.64	74.93
Total	635.95	212.62	144.33
Land use (ha)	59.22	47.18	18.90

333

334 3.3 Land use

335 The three scenarios were also examined for their effect on the land utilization. For a
336 cassava starch factory with a process capacity of 500 t/d, the land use options are the
337 construction of a 1.6 ha starch production plant, 14.5 ha wastewater treatment (covered lagoon),
338 1.8 ha CSTR for biogas production from cassava pulp, and 44.3 ha for drying the cassava pulp.
339 The total land use areas for **scenarios 1, 2, and 3** were 59.2, 47.2, and 18.9 ha, respectively as
340 show in table 1. The land needs are significantly reduced for **scenario 3** due to the reduction
341 of the cassava pulp drying area.

342



343

344 **Fig. 5** Overall reduction of GHG emission, production cost, resource use, and land use from
 345 the three scenarios of starch production. **Scenario 1** is without a biogas system in factory,
 346 **Scenario 2** is with biogas generation from the wastewater, and **Scenario 3** is with biogas
 347 generation from both the wastewater and cassava pulp.

348 3.4 Economic impact

349 The economic viability and the IRR are the main factors of concern to any entrepreneur,
 350 and the first stage that entrepreneurs will calculate is total investment cost. The investment cost
 351 of a biogas system depends on type of feedstock and biogas conversion technology. The
 352 relationship between the investment time and biogas conversion technology provides a
 353 measurement of the corresponding effect in terms of investment timing. For this, the NPV is
 354 the economic analysis method that best assesses the investment cost of a biogas system.

355 As outlined already, cassava pulp can be utilized in many ways, such as the animal feed,
 356 and a carbon source in an alcohol fermentation process. However, the factories are not entirely
 357 satisfied with the current cassava pulp utilization and disposal options because the cassava pulp
 358 still has high starch content, which they view as a loss to them, even though odor is a constant
 359 problem. Biogas generation from cassava pulp is one option to solve these problems (Thai

360 Customs Department, 2019; Trakulvichean, 2017, 2019; Yimmongkol and Jattupornpong,
 361 2007).

362 The investment cost varied with the size of reactor and the organic loading rate to the
 363 system (kg COD/m³ of digester/d). The investment and operation costs of the CSTR technology
 364 were 180 – 267 US\$/m³ biogas system and 0.07 – 0.17 US\$/m³ wastewater, respectively,
 365 (DIW, 2010). In this study, the investment cost of the biogas production system consisted of
 366 land (10 – 25%), reactor system (18 – 35%), piping (5 – 13%), purification system (8 – 12%),
 367 generator (15 – 29%), and other (e.g. insulation and equipment installation). The key economic
 368 indicators for a biogas system from wastewater and cassava pulp are presented in Table 2. For
 369 the biogas generation from **scenarios 2** and **3**, the total investment cost was 2.24 and 8.65
 370 million US\$, respectively. The PBP for biogas generation from **scenario 3** was the most
 371 economically attractive option due to the highest NPV of US\$ 6.15 million with a PBP of 4.37
 372 y.

373

374 **Table 2.** Key indicators of different biogas technologies

Key indicator	Unit	Biogas from wastewater	Biogas from wastewater and cassava pulp
Discount rate	%	10	10
Investment cost (First year)	Million US\$	2.24	8.65
NPV	Million US\$	1.98	6.14
IRR	%	18	31
PBP	Year	5.03	4.37

375

376 3.5 Drivers and barriers of CE concept implementation for the CSPP

377 This study determined which four main factors that were technical, economic, regulatory,
 378 and social responsibility as a driver or a barrier for CE concept implementation in the CSPP.
 379 A driver was defined as a supporting factor and a barrier was defined as an inhibiting factor to
 380 implementation of the CE concept using the wastewater and cassava pulp to produce biogas
 381 for producing heat and electricity in factories.

382 The results showed that the main driver and barrier for CE concept implementation in the
 383 CSPP were technical concerning. These results corresponded to the previous study about the
 384 implementation of CE concept in industry. The regulatory factors were the most important

385 concern to entrepreneurs (36%), followed closely by economic factors (35%) and then social
386 responsibility and technical support at 21 and 8%, respectively. For the barriers to CE concept
387 implementation technical problems were the most important factor that concerned
388 entrepreneurs (35%), followed by regulatory, economic, and social at 23%, 22%, and 20%,
389 respectively, (Sousa-Zomer et al., 2018; Vanner et al., 2014). The driver and barrier of CE
390 concept implementation are as show in table 3.

391 *3.5.1 Technology*

392 The technical barrier are outlined in turn below.

393 *(i) Limitations of pretreatment technology*

394 The application of biogas production from cassava pulp still has technical and cost-
395 effectiveness limitations. Technically, the cassava pulp has a high lignocelluloses so these are
396 difficult to convert into biogas. It requires both a long substrate retention time inside the reactor
397 and an equally large reactor size so the cassava pulp required the pretreatment process to
398 increasing surface area of cassava pulp, increasing microorganism accessibility, increasing
399 substrate digestibility, and increasing lignin and hemicellulose solubility. These are the reasons
400 for the high investment cost of a biogas system (Wang et al., 2011; Cannemi et al., 2014).
401 Currently, the total degradation time for the solid organic waste is approximately 30 d.
402 Consequently, various pretreatment methods have been used to improve the rate of the
403 hydrolysis of lignocelluloses for biogas production (Zhang et al., 2011; Zheng, 2014).

404 *(ii) Availability of cassava pulp*

405 The amount of energy produced from biogas varies with the volume of cassava pulp
406 generated by the factory, making it difficult to manage the energy. Cassava pulp is an
407 agricultural residue that is available only during the cassava root harvesting period (September
408 to April), is difficult to store, and so it is sometimes left on the biogas generation site for
409 mulching purposes (Cannemi et al., 2014). Biogas production systems that support a wide range
410 of raw materials and substrates would enhance the investment opportunities for biogas
411 production systems and satisfy the desire of the electricity utility for year-round generation.
412 More work needs to be done on developing such systems.

413 *(iii) Lack of a successful model for biogas production from cassava pulp*

414 A modified covered lagoon is the most popular system chosen by investors for
415 processing cassava pulp due to the stability of the system. Furthermore, the system is able to
416 support the fluctuation/variance of wastewater/solid waste in each production season, does not

417 have a very high investment cost and is relatively easy for operation and maintenance.
418 However, most starch factories are not confident in the efficiency of the high technology for
419 biogas system generation from cassava pulp, since the technology has not yet been established
420 at the commercial scale, nor shown to be cost-effective. Too few models of success to establish
421 the efficiency of this biogas technology are available to satisfy the doubts of potential investors.

422 *3.5.2 Economic*

423 Economic barriers to CE concept implementation for the CSPP are related to the cost-
424 effectiveness, uncertain return and profit, and lack of incentive.

425 *(i) Financial barriers*

426 The biogas investment and operation cost was approximately 6.00 – 1000.00 US\$/m³ and
427 0.02 – 2.67 US\$/m³ of wastewater respectively, ranging from a simple lagoon to high
428 technology biogas system with pretreatment technology. It can be seen that the more complex
429 the technology, the higher the operating cost. The cost depends not only on the chosen
430 technology, but also the type of feedstock (DIW, 2010; Zheng, 2014). Therefore, biogas
431 production from the cassava pulp requires a pretreatment step to adjust the physical and
432 chemical properties, which results in higher biogas production costs and investment costs.

433 Current benefit measures provided by the government, such as tax benefits and financial
434 support, are too little to motivate entrepreneurs to invest more in building biogas systems.
435 Added to this is the difficulty of paperwork when requesting funding for an extension of the
436 support limit, for permits, and for licenses, which often involve different agencies. Thus, the
437 associated bureaucracy needs to be made easier.

438 *(ii) Lack of incentive*

439 Government policies, especially the announcement to stop accepting claims and
440 proposals to sell electricity from very small power producers (VSPP) that generate electricity
441 from RE, is causing a slowdown in investment and is of great concern to the entrepreneurs who
442 have already invested in biogas power generation systems. In addition, the current electricity
443 purchase price is close to the production cost, making the PBP longer, and so far less attractive
444 for the private sector to invest in. This is because the Ministry of Energy estimates that current
445 electricity reserves are about 30% (DEDE, 2019). The termination of financial assistance,
446 especially for the cases of waste and wastewater without efficient technology, is a major
447 obstacle causing the private sector to cancel or delay the decision to invest in biogas production
448 systems. Although there is an overall policy to promote energy from renewable resources, the
449 denial of new feed-in tariff (FiT) approvals is possibly the greatest barrier to investment. It not

450 only denies an increase in the use of renewable resources, it runs counter to CE concept
451 implementation.

452 *3.5.3 Regulatory*

453 Environmental regulations are one of the drivers of CE concept implementation for the
454 CSPP related to the reduction of GHG emission. Since laws require expensive policing and
455 civil actions, voluntary compliance under social responsibility would be preferable (Carbon
456 Brief, 2018).

457 *(i) Agreement on GHG emissions in COP24*

458 From COP24, Thailand signed an agreement on the implementation of the guidelines
459 of the Paris Agreement to reduce its GHG emission by 20% below the 2010 emission levels by
460 2030. Environmental policies have been set up, such as the Environmentally Sustainable
461 Transport System Plan, a Waste Management Roadmap, FiT, and tax incentives, to promote
462 investment in RE (DEDE, 2019).

463 *(ii) Laws on waste and wastewater treatment*

464 Hazardous Waste Management laws define cassava pulp as a hazardous waste so it is
465 prohibited to transport it off-site. This results in the disturbing odors and the need for landfill
466 for drying the cassava pulp.

467 In terms of barriers, the primary disincentives are the high initial investment costs, lack
468 of a conducive legal system, limited government support, especially in power purchase and
469 production of RE, as well as a conflict in the laws on waste management and product lifecycle
470 management. These are outlined in turn below.

471 *(iii) Lack of a conducive legal system*

472 The government attaches great importance to the development of the country into the
473 CE. However, this top down policy has not been integrated into the actual production stream
474 with any unity. By way of example, investment in biogas systems still requires contacting
475 several departments, either sub-district administration organizations, provincial industry
476 authorities, Department of Industry, Department of Business Development, Department of
477 Alternative Energy Development and Energy Conservation, local power authorities, local
478 environment authorities, and the Energy Regulatory Office.

479 *(iv) Limited government support*

480 Policy/law/regulation in RE and the environment is unclear and highly changeable in
481 biogas production systems. Thailand has the policies and strategies in place associated with a

482 sustainable development, environment, and energy, including the implementation of the
483 Sustainable Development Agenda B.E. 2030, (Sustainable Development Goals: SDGs), the
484 AEDP was updated in 2018 to focus on BCG economy. However, the various promotional
485 measures focus on the economic returns and determination of the purchase price of RE is
486 mainly based on the lowest cost of energy.

487 *(v) Conflict of laws on waste management on product lifecycle management*

488 The Urban Planning Act stipulates that biogas projects are on a negative list and so
489 cannot be co-located with raw material production sources (e.g., cassava starch factories and
490 palm oil plants). Currently, the Ministry of Industry is in the process of listening to public
491 opinion to solve this issue of the urban plan problem as it is also associated with the request
492 for borrowing funds from the bank by the developer.

493 *3.5.4 Social responsibility*

494 Social responsibility is driven by CE concept implementation in the cassava starch industry
495 related to the area of the industry. These are discussed below

496 *(i) Expansion of communities close to industry*

497 With the high demand for living space, communities are expanding closer to the
498 cassava processing factories, which, when first established, were relatively isolated. This is
499 largely due to a lack of proper zoning from the outset. Communities are of course concerned
500 about the detrimental environmental effects of industry and are active in their surveillance and
501 reporting to the government. This result in an important driving force for investment in the CE
502 concept and minimization of emissions and waste.

503 The current barriers are associated with the lack of environmental concern from
504 entrepreneurs.

505 *(ii) Lack of environmental concern*

506 Thailand's environmental laws have only been set for sewage measures. Therefore,
507 entrepreneurs are not interested in investing in high-efficiency biogas production systems that
508 require a high investment. This is in contrast to foreign countries, such as Germany and Italy,
509 who have implemented measures to support/attract the use of more modern technology.

510 Therefore, Thailand should establish a network, including the enforcement of
511 environmental laws, and improve related laws to be in the same direction. Environmental crime
512 punishment, surveillance, and reporting are important driving forces for investment in biogas
513 production systems. This would include the establishment of an organization to disseminate

514 knowledge, including making policy recommendations that promote and support the
 515 construction of biogas production systems in accordance with space and industry limitations.
 516 In addition, for effective operations, the government needs to establish a mechanism for
 517 monitoring and disseminating biogas performance to the public.

518

519 **Table 3.** Drivers and barriers for the CE concept implementation of the Thai CSPP

	Technology	Economic	Regulatory	Social responsibility
Driver			- Agreement on COP24 for GHG emission reduction to 20% below the business as usual by 2030 - Laws on waste and wastewater treatment	Expansion of community close to industry
Barrier	- Limitations of pretreatment technology - Availability of cassava pulp (technology for flexible substrate) - Lack of a successful model for biogas production from cassava pulp	- Financial barriers from investment cost effectiveness - Lack of incentive	- Conflict of laws on waste management and product lifecycle management - Lack of a conducive legal system - Limited government support	Lack of environmental concern

520

521 **4. Conclusion**

522 The purpose of this study was to apply the CE concept implementation for the CSPP by
 523 using cassava pulp and wastewater to biogas production. The advantages of these
 524 implementation attempt to increase energy security and resource efficiency and decrease the
 525 problems of waste management including reduce disturbing odor, the waste entering landfills,
 526 GHG emissions, and land use. However, the barriers to biogas production from cassava pulp

527 are cost and technology for pretreatment of the cassava pulp. Supportive regulatory and
528 financial support mechanisms are needed for an investor to progress from the early business-
529 planning stages through to operations and commercial sustainability.

530

531 **5. Declarations**

532 5.1 Availability of data and materials

533 The datasets used and/or analyzed during the current study are available from the
534 corresponding author on reasonable request. The necessary data that generated and analyzed
535 during this study are included in this published article and its supplementary information file.

536 5.2 Competing interests

537 The authors declare that they have no competing interests.

538 5.3 Funding

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543 5.4 Authors' contributions

544 Songkasiri, W. designed, directed, and coordinated for this research. Songkasiri, W.
545 and Phalakornkule, C. provided conceptual and technical guidance for all aspect of the project.
546 Lerdlattaporn, R. and Trakulvichean, S. performed and analyzed the data of economic
547 assessment, resource efficiency, water recovery, land use, and global warming potential for
548 using wastewater and cassava pulp for biogas production in the cassava starch industry in
549 Thailand. Lerdlattaporn, R. wrote the manuscript. Songkasiri, W. and Phalakornkule, C.
550 commented, reviewed, and edited for its completion.

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561 **6. References**

562 Cannemi, M., García-Melón, M., Aragonés-Beltrán, P., Gómez-Navarro, T., 2014. Modeling
563 decision making as a support tool for policy making on renewable energy development. *Energy*
564 *Pol.*, 67, 127-137. <https://doi.org/10.1016/j.enpol.2013.12.011>.

565 Carbon Brief, 2018. COP24: Key outcomes agreed at the UN climate talks in Katowice. *Web*
566 *Page*. [https://www.carbonbrief.org/cop24-key-outcomes-agreed-at-the-un-climate-talks-in-](https://www.carbonbrief.org/cop24-key-outcomes-agreed-at-the-un-climate-talks-in-katowice)
567 [katowice](https://www.carbonbrief.org/cop24-key-outcomes-agreed-at-the-un-climate-talks-in-katowice). (Accessed January 18, 2020).

568 Chavalparit, O., Ongwandee, M., 2009. Clean technology for the tapioca starch industry in
569 Thailand. *J. Clean. Prod.*, 17(2), 105-110. <http://doi.org/10.1016/j.jclepro.2008.03.001>.

570 Chuasuwan, C., 2018. Cassava Industry. Krungsri Research. *Web Page*.
571 [https://www.krungsri.com/bank/getmedia/57ef4f9d-2dcc-4b12-](https://www.krungsri.com/bank/getmedia/57ef4f9d-2dcc-4b12-b3a2-3d0ae268471c/IO_Cassava_180807_EN_EX.aspx)
572 [b3a2-3d0ae268471c/IO_Cassava_180807_EN_EX.aspx](https://www.krungsri.com/bank/getmedia/57ef4f9d-2dcc-4b12-b3a2-3d0ae268471c/IO_Cassava_180807_EN_EX.aspx) (Accessed November 20, 2019).

573 Colin, X., Farinet, J. L., Rojas, O., Alazard, D., 2007. Anaerobic treatment of cassava starch
574 extraction wastewater using a horizontal flow filter with bamboo as support. *Bioresour.*
575 *Technol.*, 98(8), 1602-1607. <https://doi.org/10.1016/j.biortech.2006.06.020>.

576 Dakwala, M., Mohanty, B., Bhargava, R., 2011. Waste water minimization of starch industry
577 using water pinch technology. In 3th International Workshop for Advantages in Cleaner
578 Production. *Web Page*.
579 <http://citeseerx.ist.psu.edu/viewdoc/download?doi=10.1.1.663.1577&rep=rep1&type=pdf>.
580 (Accessed January 5, 2020).

581 Department of Alternative Energy Development and Efficiency [DEDE], 2014. Database for
582 Monitoring and Evaluation of Biogas Production in Thailand. *Web Page*.
583 http://biogas.dede.go.th/biogas/web_biogas/ (Accessed November 30, 2019).

584 Department of Alternative Energy Development and Efficiency [DEDE], 2019. Department of
585 Alternative Energy Development and Efficiency Plan 2018. *Web Page*.
586 [http://www.greennetworkthailand.com/%E0%B8%9E-](http://www.greennetworkthailand.com/%E0%B8%9E%E0%B8%9E-%E0%B8%AA%E0%B8%99%E0%B8%9E-aedp-2018)
587 [%E0%B8%9E-](http://www.greennetworkthailand.com/%E0%B8%9E%E0%B8%9E-%E0%B8%AA%E0%B8%99%E0%B8%9E-aedp-2018)
[%E0%B8%99%E0%B8%9E-aedp-2018](http://www.greennetworkthailand.com/%E0%B8%9E%E0%B8%9E-%E0%B8%AA%E0%B8%99%E0%B8%9E-aedp-2018) (Accessed November 3, 2019).

588 Department of Industrial Works [DIW], 2010. Manual on Process Design, Quality Control, and
589 Operation Process of Biogas System for Industrials. *Web Page*.
590 https://www.diw.go.th/km/safety/pdf/biogas_2.pdf (Accessed December 17, 2019).

591 Eggleston, S., Buendia, L., Miwa, K., Ngara, T., Tanabe, K. (Eds.), 2006. 2006 IPCC
592 guidelines for national greenhouse gas inventories (Vol. 5). Hayama, Japan: Institute for Global
593 Environmental Strategies.

594 Fukushima, A. R., Nicoletti, M. A., Rodrigues, A. J., Pressutti, C., Almeida, J., Brandão, T.,
595 Spinosa, H. D. S. et al., 2016. Cassava flour: quantification of cyanide content. *Food Nutr. Sci.*,
596 7(07), 592. [http:// dx.doi.org/10.4236/fns.2016.77060](http://dx.doi.org/10.4236/fns.2016.77060).

597 Geissdoerfer, M., Savaget, P., Bocken, N. M., Hultink, E. J. (2017). The Circular Economy—A
598 new sustainability paradigm? *J. Clean. Prod.*, 143, 757-768.
599 <https://doi.org/10.1016/j.jclepro.2016.12.048>.

600 Greenhouse Gas Management Organization. 2019. Emission Factor in Thailand. *Web Page*.
601 http://thaicarbonlabel.tgo.or.th/admin/uploadfiles/emission/ts_11335ee08a.pdf (Accessed
602 December 3, 2019).

603 Hansupalak, N., Piromkraipak, P., Tamthirat, P., Manitsorasak, A., Sriroth, K., Tran, T., 2016.
604 Biogas reduces the carbon footprint of cassava starch: a comparative assessment with fuel oil.
605 *J. Clean. Prod.*, 134, 539-546. <https://doi.org/10.1016/j.jclepro.2015.06.138>.

606 Jeyhanipour A., 2011. Waste textiles bioprocessing to ethanol and biogas. Sweden: Chalmers
607 University of Technology

608 Jorgetto, A. O., Silva, R. I. V., Saeki, M. J., Barbosa, R. C., Martines, M. A. U., Jorge, S. M.
609 A., Castro, G. R. et al., 2014. Cassava root husks powder as green adsorbent for the removal
610 of Cu (II) from natural river water. *Appl. Surf. Sci.*, 288, 356-362. [http://dx.doi.org/10.1016/](http://dx.doi.org/10.1016/j.apsusc.2013.10.032)
611 [j.apsusc.2013.10.032](http://dx.doi.org/10.1016/j.apsusc.2013.10.032).

612 Jovanović, P., 1999. Application of sensitivity analysis in investment project evaluation under
613 uncertainty and risk. *Int. J. Project Manag.* doi:10.1016/S0263-7863(98)000350

614 Liedler, M., Rashid, A., 2016. Towards circular economy implementation: a comprehensive
615 review in context of manufacturing industry. *J. Clean. Prod.*, 115, 36-51.
616 <https://doi.org/10.1016/j.jclepro.2015.12.042>.

617 Lounglawan, P., Khungaew, M., Suksombat, W., 2011. Silage production from cassava peel
618 and cassava pulp as energy source in cattle diets. *J. Anim. Vet. Adv*, 10, 1007-1011.
619 <http://dx.doi.org/10.3923/javaa.2011.1007.1011>.

620 Morseletto, P., 2020. Targets for a circular economy. *Resour. Conserv. Recycl.*, 153, 104553.
621 <https://doi.org/10.1016/j.resconrec.2019.104553>.

622 Murray, A., Skene, K., Haynes, K., 2017. The circular economy: an interdisciplinary
623 exploration of the concept and application in a global context. *J. Bus. Ethics*, 140(3), 369-380.
624 <https://doi.org/10.1007/s10551-015-2693-2>.

625 National Science and Technology Development Agency [NSTDA], 2018. BCG Economy.
626 *Web Page*. <http://nstdachannel.tv/20181009-bcg-economy> (Accessed November 2, 2019).

627 Oliveira, M. A., Reis, E. M., Nozaki, J., 2001. Biological treatment of wastewater from the
628 cassava meal industry. *Environ. Res.*, 85(2), 177-183. <https://doi.org/10.1006/enrs.2000.4118>.

629 Paixão, M. A., Tavares, C. R., Bergamasco, R., Bonifácio, A. L., Costa, R. T., 2000. Anaerobic
630 digestion from residue of industrial cassava industrialization with acidogenic and
631 methanogenic physical separation phases. In *Twenty-First Symposium on Biotechnology for
632 Fuels and Chemicals* (pp. 809-819). Humana Press, Totowa, NJ.

633 Rajbhandari, B. K., & Annachatre, A. P., 2004. Anaerobic ponds treatment of starch
634 wastewater: case study in Thailand. *Bioresour. Technol.*, 95(2), 135-143. [http://
635 dx.doi.org/10.1016/j.biortech.2004.01.017](http://dx.doi.org/10.1016/j.biortech.2004.01.017).

636 Rattanachomsri, U, Tanapongpipat, S, Eurwilaichitr, L., 2009. Simultaneous non-thermal
637 saccharification of cassava pulp by multi-enzyme activity and ethanol fermentation by *Candida
638 tropicalis*. *J. Biosci. Bioeng.*, 107: 488–493. <https://doi.org/10.1016/j.jbiosc.2008.12.024>.

639 Sánchez, A. S., Silva, Y. L., Kalid, R. A., Cohim, E., Torres, E. A., 2017. Waste bio-refineries
640 for the cassava starch industry: New trends and review of alternatives. *Renew. Sust. Energ.
641 Rev.*, 73, 1265-1275. <https://doi.org/10.1016/j.rser.2017.02.007>.

642 Sivamani, S., Chandrasekaran, A. P., Balajii, M., Shanmugaparakash, M., Hosseini-
643 Bandegharai, A., & Baskar, R., 2018. Evaluation of the potential of cassava-based residues
644 for biofuels production. *Rev. Environ. Sci. Biotechnol.*, 17(3), 553-570.
645 <https://doi.org/10.1007/s11157-018-9475-0>.

646 Songkasiri, W., Nopharatana, A., Seangchan, K., Ruttithiwapanich, T., Chayawattana. T.,
647 Lerdlattaporn, R. et al., 2014a. Productivity and Process Efficiency Improvement of Tapioca
648 Starch Industry. Department of Industrial Promotion, Ministry of Industry, *Web Page*.

649 <http://www.thailandtapiocastarch.net/download/download-th-55.pdf> (Accessed November 20,
650 2019).

651 Songkasiri, W., Seangchan, K., Lerdlattaporn, R., Lerdlattaporn, W., 2014b. Implementation
652 of Near Zero Waste Concept for Improvement of Process Efficiency in Cassava Starch
653 Industry. National Center for Genetic Engineering and Biotechnology (BIOTEC), Thailand.

654 Sousa-Zomer, T. T., Magalhães, L., Zancul, E., Cauchick-Miguel, P. A., 2018. Exploring the
655 challenges for circular business implementation in manufacturing companies: An empirical
656 investigation of a pay-per-use service provider. *Resour. Conserv. Recycl.*, 135, 3-13.
657 <https://doi.org/10.1016/j.resconrec.2017.10.033>.

658 Sriroth, K, Chollakup, R, Chotineeranat, S., 2000. Processing of cassava waste for improved
659 biomass utilization. *Bioresour. Technol.*, 71: 63– 69. [https://doi.org/10.1016/S0960-](https://doi.org/10.1016/S0960-8524(99)00051-6)
660 [8524\(99\)00051-6](https://doi.org/10.1016/S0960-8524(99)00051-6).

661 Sun, L., Wan, S., Yu, Z., Wang, Y., Wang, S., 2012. Anaerobic biological treatment of high
662 strength cassava starch wastewater in a new type up-flow multistage anaerobic reactor.
663 *Bioresour. Technol.*, 104, 280-288. <https://doi.org/10.1016/j.biortech.2011.11.070>.

664 Thai Customs Department, 2019. Export Tapioca Product. *Web Page*.
665 http://www.thaitapiocastarch.org/th/information/statistics/export_tapioca_products (Accessed
666 November 20, 2019).

667 Torii, S., Pambudi, N. A., Sudarwanto, S., Saptoadi, H., 2011. Combustion characteristics of
668 bio mass-based fuel using cassava husk. *Int. J. Earth Sci. Eng.*, 4(5), 896-9.

669 Trakulvichean, S., Chaiprasert, P., Otmakhova, J., Songkasiri, W., 2017. Comparison of
670 fermented animal feed and mushroom growth media as two value-added options for waste
671 cassava pulp management. *Waste Manag. Res.*, 35 (12) , 1210-1219.
672 <https://doi.org/10.1177/0734242X17730135>.

673 Trakulvichean, S., Chaiprasert, P., Otmakhova, J., Songkasiri, W., 2019. Integrated economic
674 and environmental assessment of biogas and bioethanol production from cassava cellulosic
675 waste. *Waste Biomass Valor.*, 10(3), 691-700. <https://doi.org/10.1007/s12649-017-0076-x>.

676 Vanner, R., Bicket, M., Withana, S., Ten Brink, P., Razzini, P., Van Dijk, E., Hudson, C., 2014.
677 Scoping study to identify potential circular economy actions, priority sectors, material flows
678 and value chains. Study prepared for the European Commission, DG Environment.

679 Virunanon, C, Ouephanit, C, Burapatana, V., 2013. Cassava pulp enzymatic hydrolysis process
680 as a preliminary step in bio-alcohols production from waste starchy resources. *J. Clean. Prod.*
681 39: 273–279. <https://doi.org/10.1016/j.jclepro.2012.07.055>.

682 Wang, W., Xie, L., Chen, J., Luo, G., Zhou, Q., 2011. Biohydrogen and methane production
683 by co-digestion of cassava stillage and excess sludge under thermophilic condition. *Bioresour.*
684 *Technol.*, 102(4), 3833-3839. <https://doi.org/10.1016/j.biortech.2010.12.012>.

685 Yesaswini, G., Saravanathamizhan, R., 2018. Wastewater Minimization of Starch Industry
686 using Water Pinch Analysis and Comparison with Water Design Software. *Web Page*.
687 [https://s3.amazonaws.com/academia.edu.documents/57028733/3806.pdf?response-content-](https://s3.amazonaws.com/academia.edu.documents/57028733/3806.pdf?response-content-disposition=inline%3B%20filename%3DWastewater_Minimization_of_Starch_Indust.pdf&X-Amz-Algorithm=AWS4-HMAC-SHA256&X-Amz-Credential=AKIAIWOWYYGZ2Y53UL3A%2F20200303%2Fus-east-1%2Fs3%2Faws4_request&X-Amz-Date=20200303T073937Z&X-Amz-Expires=3600&X-Amz-SignedHeaders=host&X-Amz-Signature=1bc2b65e5180aa20f0b3469c19912424a7912693cfab395cd64261ce4e85ddb9)
688 [disposition=inline%3B%20filename%3DWastewater_Minimization_of_Starch_Indust.pdf&](https://s3.amazonaws.com/academia.edu.documents/57028733/3806.pdf?response-content-disposition=inline%3B%20filename%3DWastewater_Minimization_of_Starch_Indust.pdf&X-Amz-Algorithm=AWS4-HMAC-SHA256&X-Amz-Credential=AKIAIWOWYYGZ2Y53UL3A%2F20200303%2Fus-east-1%2Fs3%2Faws4_request&X-Amz-Date=20200303T073937Z&X-Amz-Expires=3600&X-Amz-SignedHeaders=host&X-Amz-Signature=1bc2b65e5180aa20f0b3469c19912424a7912693cfab395cd64261ce4e85ddb9)
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693 [Signature=1bc2b65e5180aa20f0b3469c19912424a7912693cfab395cd64261ce4e85ddb9](https://s3.amazonaws.com/academia.edu.documents/57028733/3806.pdf?response-content-disposition=inline%3B%20filename%3DWastewater_Minimization_of_Starch_Indust.pdf&X-Amz-Algorithm=AWS4-HMAC-SHA256&X-Amz-Credential=AKIAIWOWYYGZ2Y53UL3A%2F20200303%2Fus-east-1%2Fs3%2Faws4_request&X-Amz-Date=20200303T073937Z&X-Amz-Expires=3600&X-Amz-SignedHeaders=host&X-Amz-Signature=1bc2b65e5180aa20f0b3469c19912424a7912693cfab395cd64261ce4e85ddb9)
694 (Accessed January 5, 2020).

695 Yimmongkol, S, Jattupornpong, S., 2007. Utilization of Dried Cassava Pulp for Animal Feed:
696 Fully Integrated Cassava Pulp Utilization. Suwanvajokkasikij Animal Research and
697 Development Institute, Thailand. *Web Page*.
698 http://www.rdi.ku.ac.th/kufair50/animal/11_2_animal/11_2animal.html (Accessed December
699 3, 2019).

700 Zhang, Q., He, J., Tian, M., Mao, Z., Tang, L., Zhang, J., Zhang, H., 2011. Enhancement of
701 methane production from cassava residues by biological pretreatment using a constructed
702 microbial consortium. *Bioresour. Technol.*, 102 (19) , 8899-8906.
703 <https://doi.org/10.1016/j.biortech.2011.06.061>.

704 Zheng, Y., Zhao, J., Xu, F., Li, Y., 2014. Pretreatment of lignocellulosic biomass for enhanced
705 biogas production. *PECS.*, 42, 35-53. <https://doi.org/10.1016/j.pecs.2014.01.001>.

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Figures

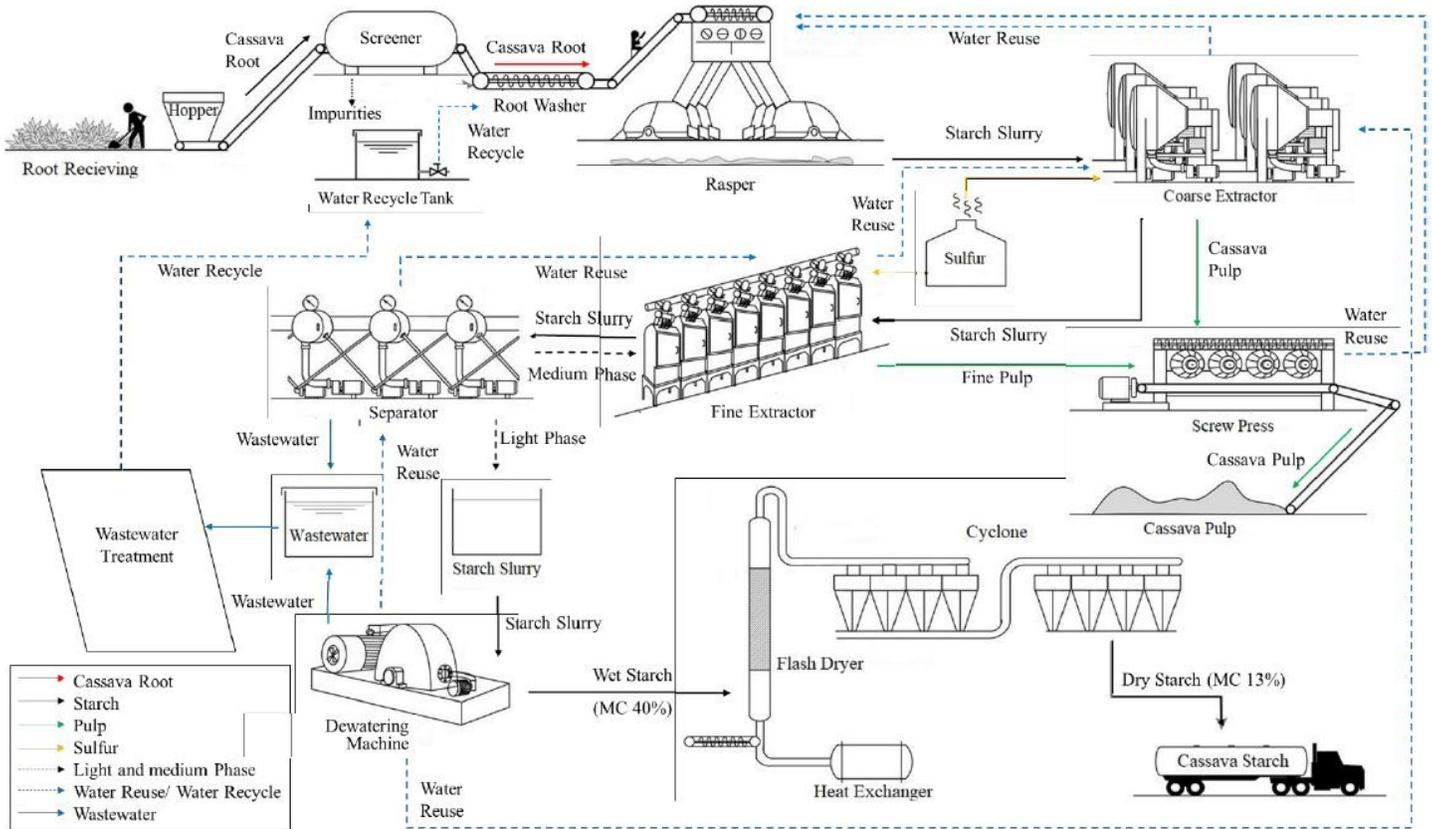


Figure 1

Schematic diagram summarizing the CSPP (Songkasiri et al., 2014a)

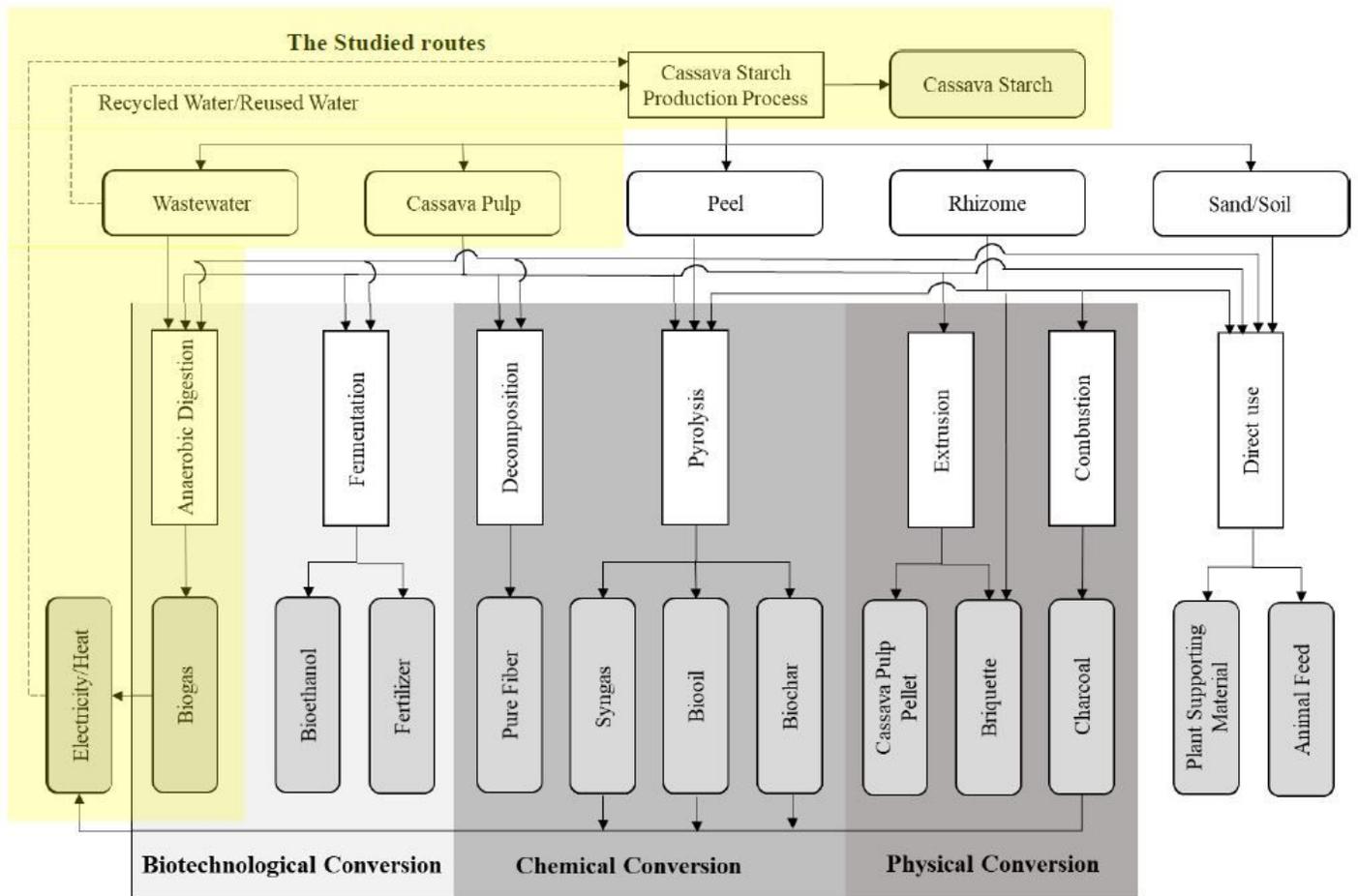


Figure 2

Implementation of CE concept in the Thai cassava starch industry

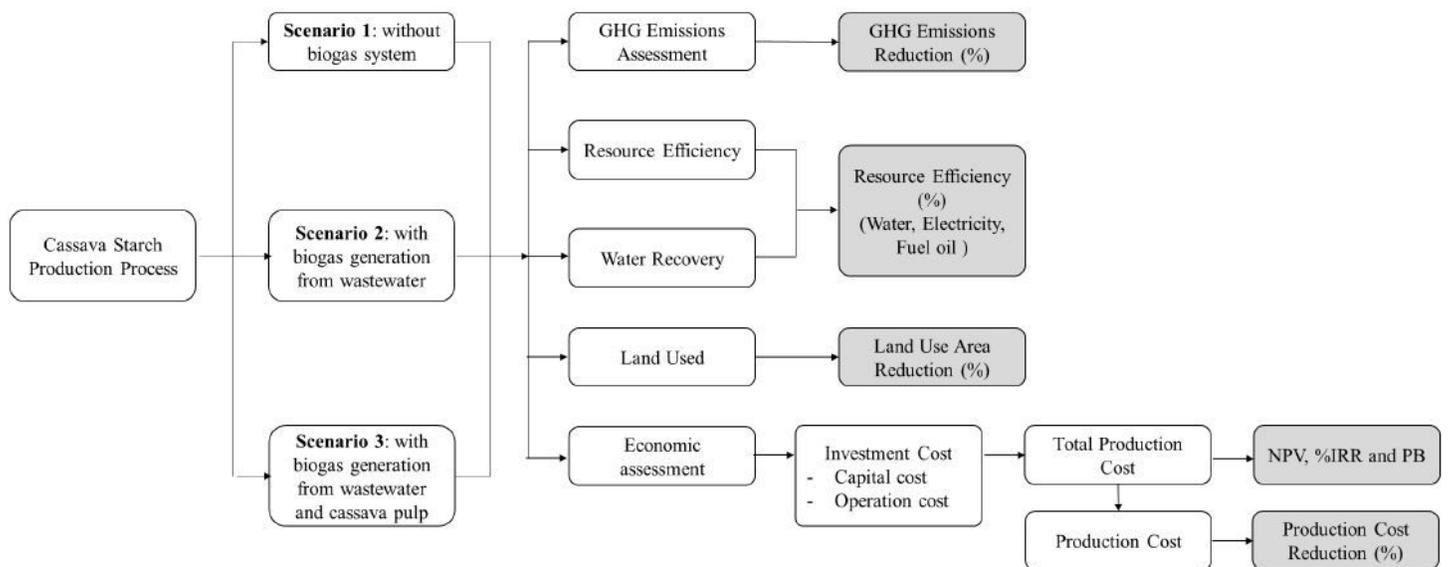


Figure 3

Research framework

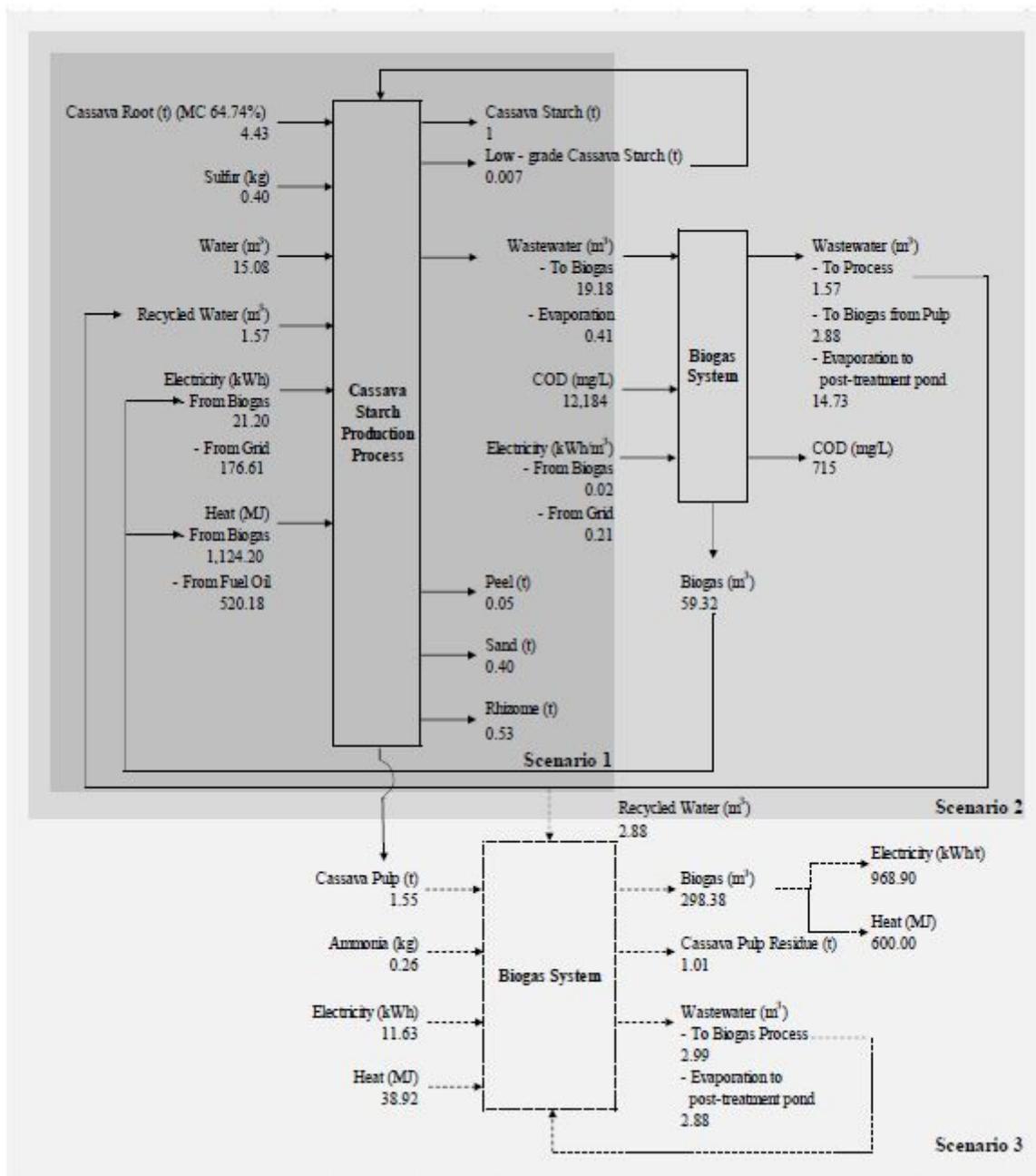


Figure 4

Resource consumption and waste generation (per one ton of cassava starch produced) from CSPP. Three scenarios of starch production consist of (i) scenario 1, without biogas system in factory, (ii) scenario 2, with biogas generation from wastewater, and (iii) scenario 3, with biogas generation from wastewater and cassava pulp.

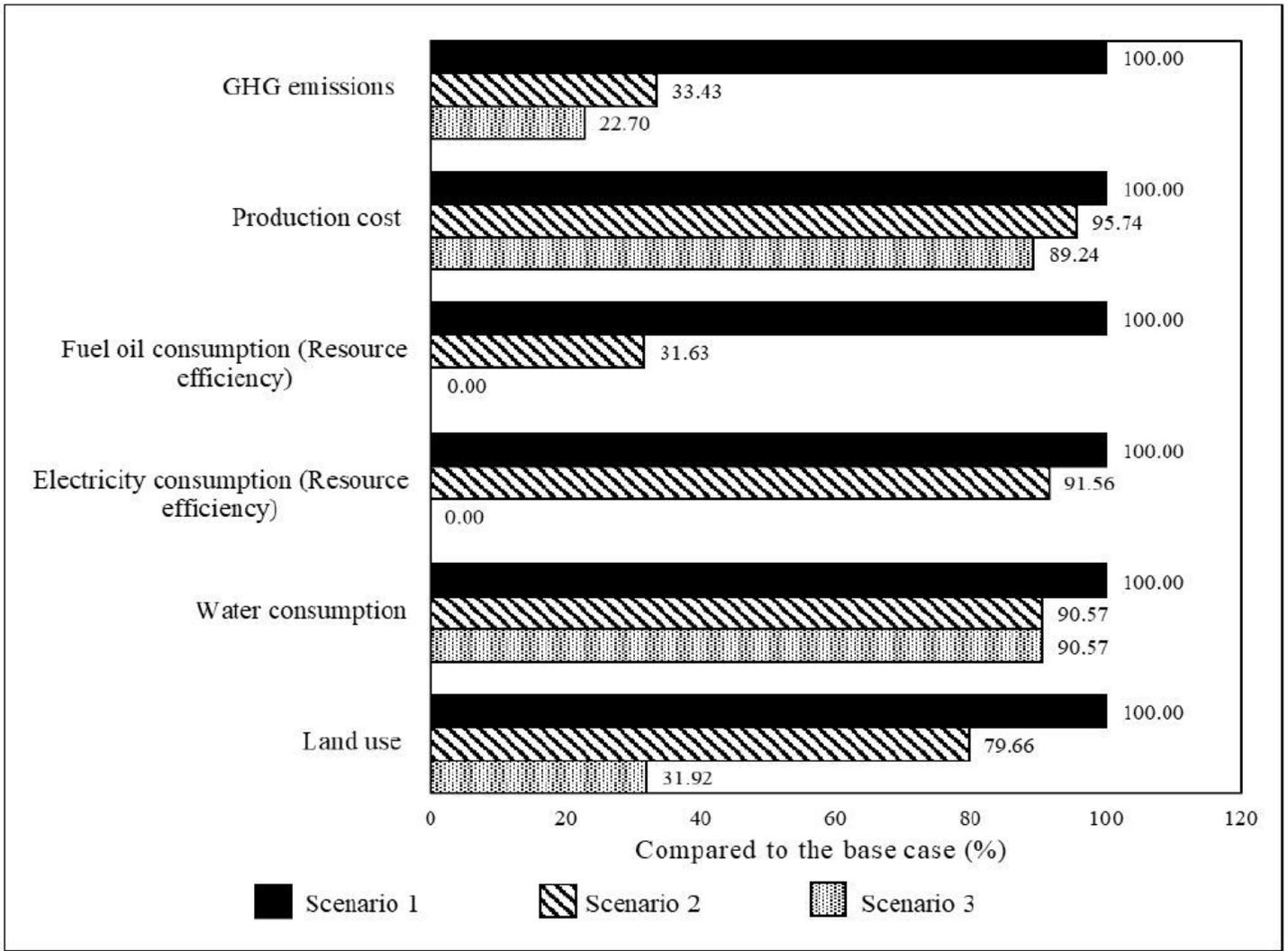


Figure 5

Overall reduction of GHG emission, production cost, resource use, and land use from the three scenarios of starch production. Scenario 1 is without a biogas system in factory, Scenario 2 is with biogas generation from the wastewater, and Scenario 3 is with biogas generation from both the wastewater and cassava pulp.