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Direct degradation of methylene blue by unactivated peroxymonosulfate:

Reaction parameters, kinetics, and mechanism

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Abstract: Advanced oxidation processes (AOPs) are efficient methods for water purification. However, there are few studies on direct oxidation with inactive peroxymonosulfate (PMS) to remove pollutants. In this study, methylene blue (MB) was oxidised efficiently by PMS. MB was decomposed through a non-radical pathway, as verified by the scavengers and electron paramagnetic resonance experiments. Although singlet oxygen was formed, the possibility of it degrading MB was ruled out via kinetics calculations. Therefore, the obvious conclusion was that PMS reacted directly with MB. Additionally, the operating parameters, including PMS dosage, MB dosage, temperature, and initial pH, were investigated. MB degradation followed pseudo-first-order kinetics, with rate constants ranging from 0.0082 to 0.3912 min⁻¹. The second-order rate constant ($k_{\text{PMS,MB}}$) for the reaction of MB with PMS was 0.08 M⁻¹s⁻¹ at pH 3–6, but $k_{\text{PMS,MB}}$ increased dramatically to 4.68 M⁻¹s⁻¹ with increasing solution pH. Chloride in the PMS/MB system reacted with PMS to form HClO, which was catalysed by PMS to rapidly decompose MB. Interestingly, MB is effectively mineralised by PMS in the presence of chlorine. In addition, humic acid, a common scavenger, did not inhibit MB degradation. In an alkaline environment, the removal rate of TOC reached 16%, but PMS caused almost no mineralisation of MB in an acidic environment. This study provides new insights into pollutant removal based on AOPs and an additional strategy for water purification.

34 1. Introduction

35 With the development of industry, environmental pollution has become a progressively larger concern, and
36 emerging synthetic compounds with refractory biodegradability have become important for pollutant removal
37 technologies. Advanced oxidation technology could play an important role in water treatment by efficiently
38 destroying various kinds of pollutants, such as aromatic ring substances and azo dyes, among others. However,
39 the mechanisms underlying pollutant degradation have not been fully elucidated (Chen et al., 2019a; Chen et
40 al., 2018). Peroxymonosulfate (PMS), peroxydisulfate (PDS), and hydrogen peroxide (H_2O_2) are often used to
41 generate strong oxidative species, and many methods have been developed to activate these oxidants,
42 including the use of transition metals (Zhou et al., 2020a), UV light (He et al., 2014), a base (Qi et al., 2016),
43 heat (Tan et al., 2015), microwaves (Monteagudo et al., 2018), carbon-based materials (Wang et al., 2020),
44 inorganic ions (Yang et al., 2018), and organic materials (Ahamd et al., 2013). Although the activation
45 methods are conducive to the removal of target pollutants, the energy required and heavy metals leached from
46 catalysts increase the costs and cause secondary pollution. Furthermore, degradation efficiency is
47 unsatisfactory because the radicals generated have poor selectivity for target pollutants when other impurities
48 exist in the system (Long et al., 2021; Huang et al., 2019).

49 Due to their differences from the adjacent O–O structure, PDS, PMS, and H_2O_2 have redox potential (E^0)
50 values of 2.01, 1.82, and 1.78 V, respectively (Qi et al., 2017; Ding et al., 2017). Furthermore, the asymmetric
51 structure of PMS makes it unstable. In comparison with $HClO$ (1.48 V), the redox potential of PMS enables it
52 to thermodynamically oxidize pollutants directly. Zhou et al. (2020b) reported that PMS could degrade
53 tetracyclines effectively in the presence of radical scavengers (methanol and tert-butyl alcohol) and a singlet
54 oxygen scavenger (sodium azide). Ding et al. (2017) found that PDS could directly decolourize methylene
55 blue (MB). However, the unactivated PDS could damage the structure of MB, but not rhodamine B (Yang et
56 al., 2021a). The degradation of several sulphonamides by non-activated PMS has been compared, and aniline
57 and dimethylisoxazole ring moieties rich in electrons were inferred to be the reactive sites (Ji et al., 2018).
58 Recently, Yang et al. (2021b) found that oxidation by PMS was responsible for trimethoprim degradation in
59 the trimethoprim/PMS direct system, despite the existence of singlet oxygen. The oxidation rate of
60 chlorophenols for PMS alone was shown to increase with increased solution pH, which was attributed to the
61 difference in degree of dissociation among several chlorophenols (Li et al., 2019). As an oxidant, PMS
62 directly participates in the oxidation of pollutants. However, the reaction kinetics, related mechanisms, and
63 influence of reaction parameters (PMS dosage, pollutant concentration, solution pH, temperature, and water

64 matrix) in the PMS oxidation system have not been studied systematically due to the complexity of the
65 reaction environment. For example, with the exception that p-benzoquinone, a PMS oxidation by-product,
66 activates PMS (Zhou et al., 2017), the reaction mechanisms between PMS and other pollutants have not been
67 clarified. Moreover, research on the effects of environmental parameters on the degradation of various
68 pollutants by PMS remains highly insufficient.

69 MB, a type of cationic dye and redox indicator, is used widely in the textile and dyeing industries, and
70 for pharmaceutical processes. MB wastewater has a deep blue colour and does not readily biodegrade. Based
71 on previous studies, this work used MB as a model pollutant to study the reaction mechanism, kinetics, and
72 reaction parameters in the MB/PMS system. The study aimed to provide more information about direct
73 oxidation of pollutants by PMS, which has been overlooked in previous research.

74 **2. Materials and methods**

75 *2.1. Chemicals and reagents*

76 The chemicals used in this study were of analytical grade and used as received without further purification.
77 Detailed information about the chemicals is included in Text S1 of the Supporting Information. Each solution
78 was prepared with ultrapure water (18 M Ω cm). Detailed information about the preparation of the humic acid
79 stock solution is described in Text S1 in the Supporting Information.

80 *2.2. Experimental procedures*

81 The MB degradation experiments were conducted in 150-mL conical flasks placed on a magnetic stirrer
82 (CJJ-2S; Jintan Instrument Factory, Changzhou, China). The reaction temperature was controlled via heating
83 in a water bath. A certain amount of MB stock solution was added to 100 mL of ultrapure water with constant
84 stirring, and 1 mL of MB solution was withdrawn for detection of the initial MB concentration. Then, a
85 predetermined volume of PMS stock solution was injected into the mixture to initiate MB degradation. At
86 regular intervals, 1 mL of the mixture was sampled for detection within 1 minute. The solution pH was
87 adjusted to the desired value with 0.1 M NaOH and H₂SO₄. A series of MB degradation experiments was
88 evaluated under varying PMS dosage (0–4.5 mM), MB dosage (5–40 mg/L), temperature (25–45°C), initial
89 pH (3.14–10.50), Cl⁻ (0–100 mM), HCO₃⁻ (0–100 mM), and humic acid (0–10 mg/L) conditions.

90 To investigate the effect of different water matrices on the decomposition of MB, 100 mL of sea water (or
91 tap water) was used as the background solution. In addition, the pseudo-first-order kinetics were analysed as
92 follows:

93

94
$$\ln\left(\frac{C}{C_0}\right) = -k_{\text{obs}} t. \quad (1)$$

95 In this model, C and C₀ are the MB concentration at time t and the initial concentration, respectively, and k_{obs}
96 is the pseudo-first-order kinetic rate constant (min⁻¹).

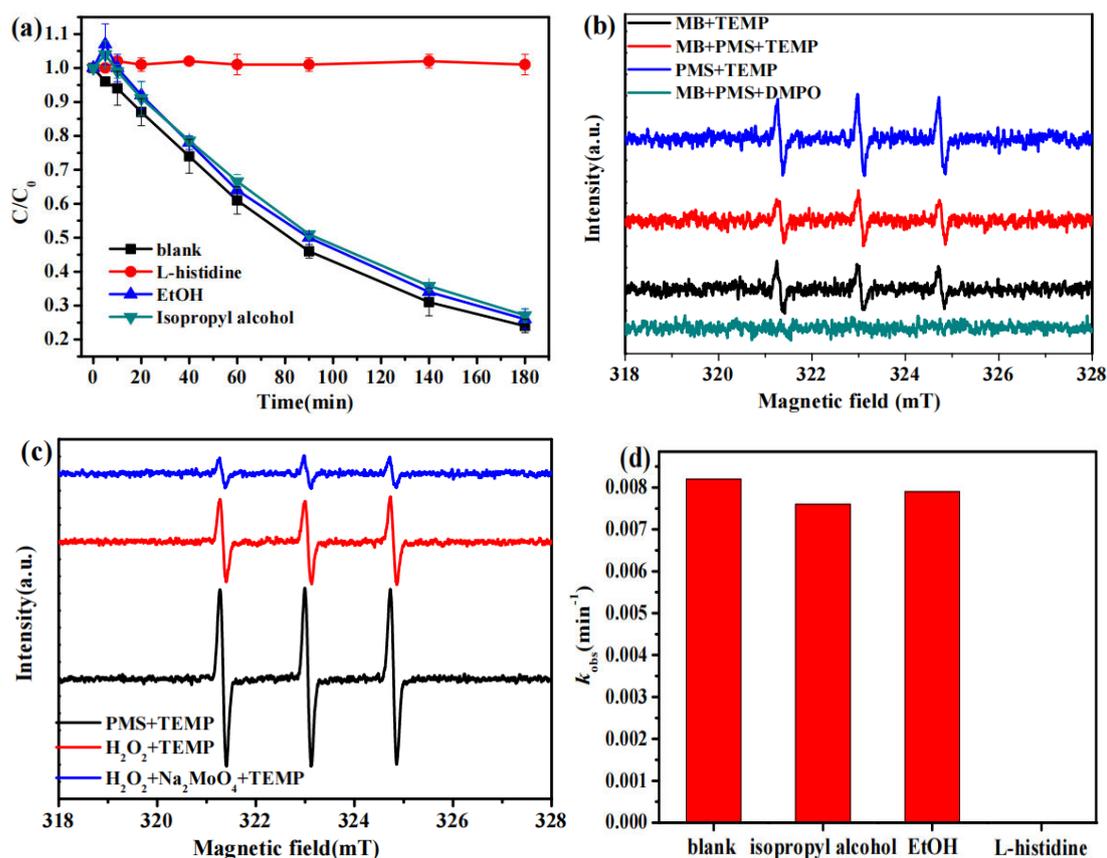
97 2.3. Analytical methods

98 An ultraviolet spectrophotometer (TU-1810; Beijing Purkinje General Instrument Co., Ltd., Beijing, China)
99 was used to detect MB, methyl orange (MO), and malachite green (MG) concentrations, with detection
100 wavelengths set at 664, 465, and 612 nm, respectively. N,N-dimethylaniline (NN) was detected using
101 high-performance liquid chromatography (G4212-6007; Agilent, Santa Clara, CA, USA) with a UV detector
102 (detection wavelength = 240 nm) and C₁₈ column (size, 250 × 4.6 mm). The mobile phase consisted of water
103 and acetonitrile (25/75, v/v). The flow rate was set at 1 mL/min, and the injection volume was 100 µL. The
104 reaction solution pH was monitored using a PHS-3G pH meter with an E-201F composite electrode (Shanghai
105 LEICI CHUANGYI Instrument & apparatus Co. Ltd., Shanghai, China). The mineralisation of MB under the
106 different conditions was determined using a TOC analyzer (Sievers M9 Portable TOC Analyzer; SUEZ Water
107 Technologies & Solutions, Feasterville-Trevose, PA, USA). Reactive oxygen species, such as sulphate radicals
108 and hydroxyl radicals, were captured by 5,5-dimethylpyrroline N-oxide (DMPO) and the singlet oxygen
109 reacted with 2,5,5-trimethyl-1-pyrroline N-oxide (TMPO). Then, the DMPO and TMPO adducts were
110 detected via in situ electron paramagnetic resonance (EPR) analysis (EMXplus-10/12; Bruker, Karlsruhe,
111 Germany). The detection parameters of the EPR were as follows: modulation frequency, 100 kHz; microwave
112 frequency, 9.066 GHz; microwave power, 0.998 mW; and scanning range: 317.989–327.989 mT.

113 3. Results and discussion

114 3.1. Reaction mechanism

115 PMS has a higher redox potential (1.82 V) than HClO (1.48 V) and KMnO₄ (1.68 V) (Feng et al., 2019).
116 PMS can be catalysed to generate sulphate and hydroxyl radicals, which degrade pollutants efficiently;
117 however, in these systems, direct oxidation by PMS is usually ignored. The results shown in Fig. 1a and d
118 suggest that PMS can decolourise MB by 75% within 180 min without the addition of a catalyst. The k_{obs}
119 value calculated was 0.0082 min⁻¹, indicating that PMS has a greater capability to degrade MB than
120 trimethoprim oxidation by PMS (k_{obs} = (5.13 ± 0.07) × 10⁻⁵ s⁻¹) (Yang et al., 2021b).



121

122

123 **Fig. 1.** (a) Degradation of methylene blue (MB) by PMS in the presence of different scavengers. (b) Electron
 124 paramagnetic resonance (EPR) spectra of TEMP-¹O₂ adducts formed in different cases. (c) EPR spectra of
 125 5,5-dimethylpyrroline N-oxide (DMPO) adducts and 2,5,5-trimethyl-1-pyrroline N-oxide (TEMP) adducts in
 126 different cases. (d) k_{obs} values calculated in the presence of different scavengers. Experimental conditions:
 127 [MB] = 10 mg/L, [PMS] = 1.5 mM, [EtOH] = [isopropyl alcohol] = 150 mM, [TEMP] = [DMPO] = 100 mM,
 128 [H₂O₂] = 10 mM, [Na₂MoO₄] = 1 mM, reaction temperature = 25°C, pH unadjusted.

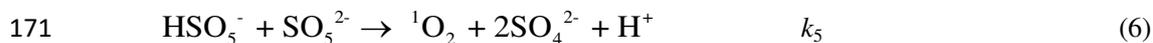
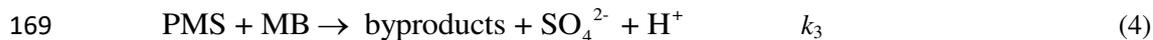
129 A series of experiments were conducted to study the reactive substances and explore the degradation
 130 mechanism. Ethanol reacts with both sulphate and hydroxyl radicals with high second-order kinetic rate
 131 constants, and can be used as a scavenger, whereas isopropyl alcohol reacts rapidly with hydroxyl radicals but
 132 not with sulphate radicals (Sun et al., 2021; Sun et al., 2019). Thus, these two alcohols were employed to
 133 determine whether radicals are involved in the degradation of MB. L-histidine is usually used to capture
 134 singlet oxygen. The data in Fig. 1a and d show that the removal rate of MB was as high as 75%, and that it
 135 only dropped by 2% and 3.1% in the presence of ethanol and isopropyl alcohol, respectively. k_{obs} values
 136 declined only slightly. from 0.0082 to 0.0079 and 0.0076 min^{-1} , respectively, indicating that radicals played
 137 only a minor role in damaging MB. Furthermore, the MB degradation rate was 58% and 52.5%, and k_{obs} was
 138 0.005 and 0.0045 min^{-1} , in the presence of 1.5 M ethanol and isopropyl alcohol, respectively (Fig. S1).

139 Notably, the reduction in degradation rate and k_{obs} might be attributable to the increase of solution viscosity
140 under the high doses of alcohol, which prevented PMS and MB from diffusing and prevented decolourisation
141 (Guan et al., 2014). On the other hand, the complete inhibition of MB removal by addition of L-histidine may
142 be an indication of singlet oxygen in the PMS/MB system.

143 EPR spectroscopy was performed to confirm reactive species in the system directly. As shown in Fig. 1b,
144 there was no signal of DMPO–SO₄ or DMPO–OH in the system, consistent with the results of the radical
145 scavenging experiments. On the contrary, a three-peak, equal-strength signal provided evidence of singlet
146 oxygen. It is well known that self-decomposition of PMS can generate singlet oxygen at an extremely low rate.
147 Notably, the intensity of singlet oxygen is weak in Fig. 1c because it survived for only 4.2 μs in the H₂O and
148 was scavenged rapidly by H₂O ($k = 2.5 \times 10^5 \text{s}^{-1}$) (Yang et al., 2018; Bohme et al., 1992). MB, an excellent
149 photosensitised organic material (Yao et al., 2019), can produce singlet oxygen under light illumination, which
150 was verified by the result in Fig. 1c. Yang et al. (2018) stated that L-histidine reacted directly with PMS, and
151 that the PMS was consumed completely within a few minutes. Additionally, Liao et al. (2021) observed that
152 the suppression of methyl parathion by PMS oxidation with addition of furfuryl alcohol was attributable to the
153 furfuryl alcohol reacting with PMS. Therefore, although L-histidine captures singlet oxygen efficiently, it can
154 be inferred that it may consume PMS in a largely spontaneously manner and thus suppress MB degradation.
155 To verify this hypothesis, singlet oxygen was generated in situ according to a previous report (Bohme et al.,
156 1992), and the degradation of MB by singlet oxygen in the H₂O₂/Na₂MoO₄/MB system was assessed. The
157 generation rate of singlet oxygen was as high as ~30 μM s⁻¹ at pH 9.30, comparable to the rate of MB under
158 light (Bohme et al., 1992). Figure 1c shows that the characteristic signal of singlet oxygen in the
159 H₂O₂/Na₂MoO₄ system was stronger than that of PMS alone, in agreement with prior research (Bohme et al.,
160 1992). Nevertheless, the removal rate of MB in Fig. S2, even at a high concentration of singlet oxygen, was
161 only 13%, and the k_{obs} value was about $1.06 \times 10^{-3} \text{min}^{-1}$. This result indicated that singlet oxygen was not
162 responsible for the MB removal. Moreover, Lu et al. (2021) found the same interesting phenomenon: although
163 singlet oxygen existed in the system, it barely degraded isoproturon.

164 To further evaluate the effect of singlet oxygen on the degradation of MB, the dynamic calculation method
165 was employed. The second-order rate constant of PMS self-decomposition is $k_5 = (7.32 \pm 0.43) \times 10^{-3} \text{M}^{-1} \text{s}^{-1}$,
166 as listed in a previous paper (Yang et al., 2021b). The reaction equations follow:





172 In the $\text{H}_2\text{O}_2/\text{Na}_2\text{MoO}_4/\text{MB}$ system, k'_{obs} was calculated to be $1.06 \times 10^{-3} \text{ min}^{-1} = 1.77 \times 10^{-5} \text{ s}^{-1}$. In Eq. (5),
 173 $k_4 \approx 0$ because H_2O_2 could not decompose MB (discussed below). In the other systems, $[{}^1\text{O}_2]_{\text{ss}}$ represents the
 174 steady state concentration of ${}^1\text{O}_2$, and $R = 35.2 \times 10^{-6} \text{ M s}^{-1}$ was inferred to be the generation rate of ${}^1\text{O}_2$
 175 (Bohme et al., 1992). Assuming that the generation and consumption rates of singlet oxygen were equal
 176 during the reaction process, k_2 and $[{}^1\text{O}_2]_{\text{ss}}$ could be calculated by the following equations:

177 $k'_{\text{obs}} = k_2 [{}^1\text{O}_2]_{\text{ss}} + k_4 [\text{H}_2\text{O}_2] \approx k_2 [{}^1\text{O}_2]_{\text{ss}}$

178 $R = (k_1 + k_2) [{}^1\text{O}_2]_{\text{ss}}$

179 As calculated above, $k_2 = 1.26 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ and $[{}^1\text{O}_2]_{\text{ss}} = 1.4 \times 10^{-10} \text{ M}$. These are similar to the values
 180 reported by Yang et al. (2018). Therefore, the second-order reaction rate constant of ${}^1\text{O}_2$ reacting with MB was
 181 lower than the rate constant of ${}^1\text{O}_2$ reacting with H_2O .

182 The maximum degradation rate of MB by ${}^1\text{O}_2$ in the PMS/MB system was calculated as follows:

183 $k_5[\text{PMS}]^2 = (k_2[\text{MB}] + k_1)[{}^1\text{O}_2]_{\text{ss}}$

184 $d[\text{MB}]/dt = k_2 [\text{MB}] \times k_5[\text{PMS}]^2 / (k_2[\text{MB}] + k_1)$

185 $f = k_2[\text{MB}] / (k_1 + k_2 [\text{MB}])$, where f represents the fraction of ${}^1\text{O}_2$ reacting with MB (Yang et al., 2018).

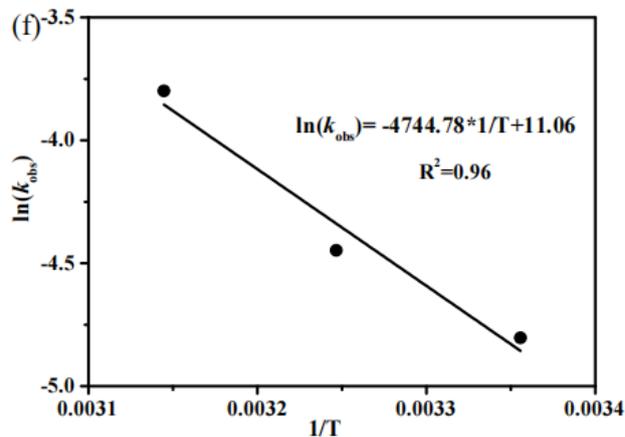
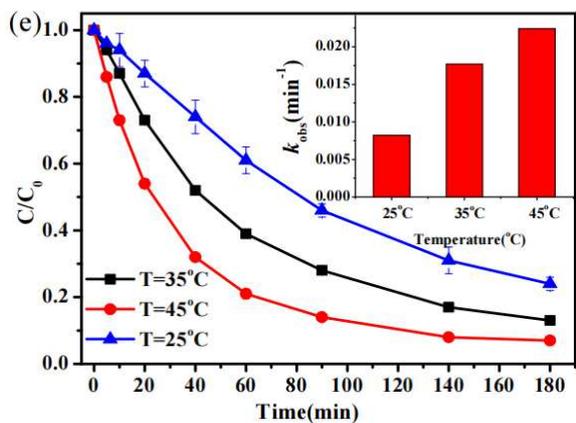
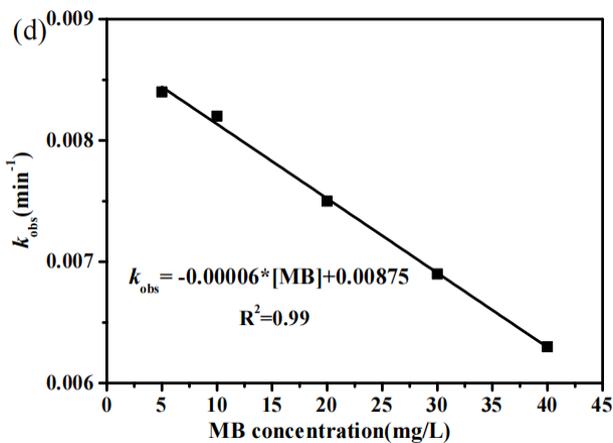
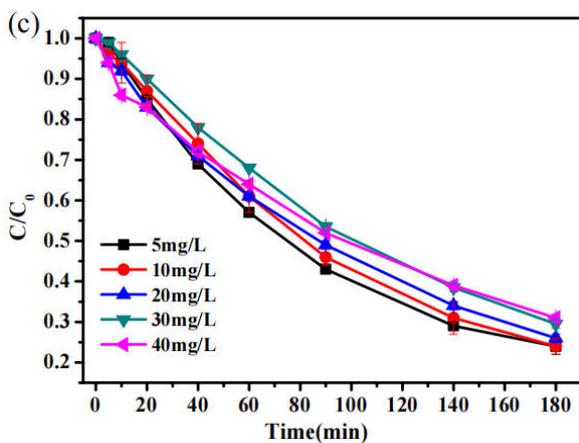
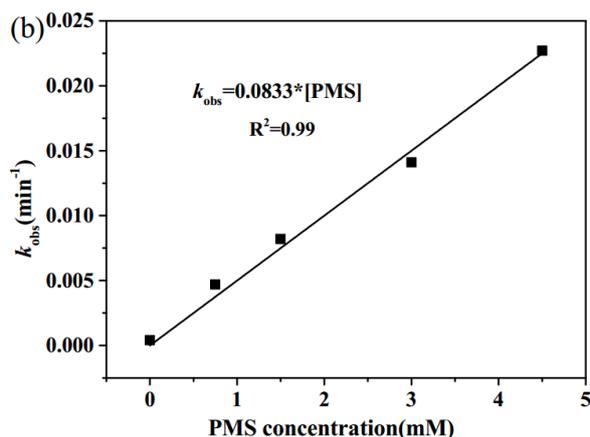
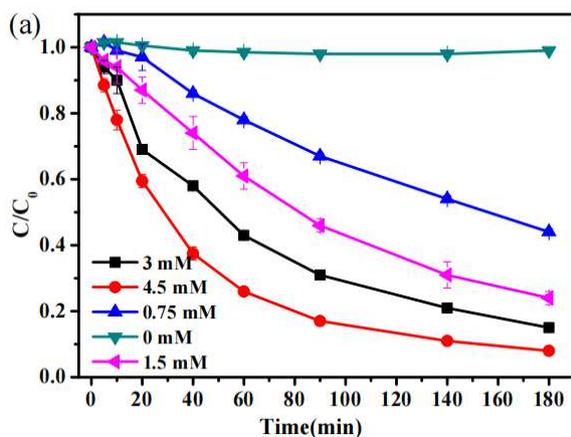
186 Therefore, the calculated removal rate of MB was only $2.6 \times 10^{-13} \text{ M s}^{-1}$; however, in this experiment, the
 187 measured value was $2.2 \times 10^{-9} \text{ M s}^{-1}$. Moreover, $f < 0.1\%$ was extremely low, implying that ${}^1\text{O}_2$ barely contributed
 188 to MB degradation. The above results suggest that MB degradation did not depend on ${}^1\text{O}_2$, because of the low
 189 second-order rate reaction constant, but rather on direct oxidation by PMS through a non-radical pathway.

190 3.2 Effect of reaction parameters on MB degradation

191 3.2.1 PMS dosage

192 The correlation between PMS and pollutant degradation could be obtained by adjusting the PMS dosage. As
 193 shown in Fig. 2a, the removal rates of MB with increasing PMS concentration (from 0 to 0.75, 1.5, 3, and 4.5 mM)
 194 were improved to 1%, 56%, 85% and 92%, respectively. The reaction of PMS and MB was first order with the MB
 195 concentration. As presented in Fig. 2b, the k_{obs} of MB was positively proportional to the PMS concentration and the

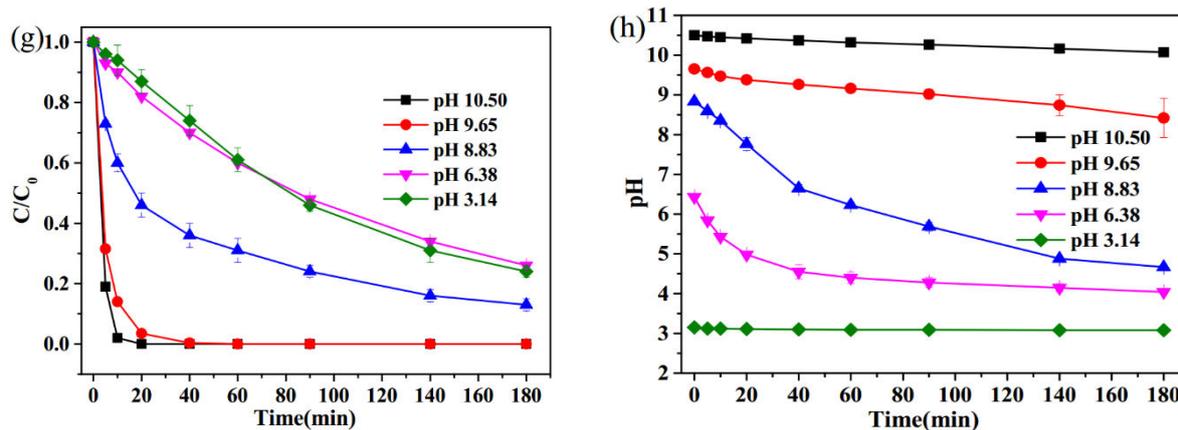
196 correlation was $k_{\text{obs}} = 0.0833 [\text{PMS}] (\text{s}^{-1})$, implying that MB degradation was also first order with respect to PMS
 197 dosage. Furthermore, the second-order reaction rate constant of MB and PMS was estimated to be $0.0833 \text{ M}^{-1}\text{s}^{-1}$,
 198 which was much lower than the rate constant of PMS reacting with sulfamethoxazole ($k_{\text{obs}} = 0.23 \text{ M}^{-1}\text{s}^{-1}$), but
 199 higher than the rate constant of PMS with trimethoprim ($k_{\text{obs}} = 0.043 \text{ M}^{-1}\text{s}^{-1}$) (Ji et al., 2018; Yang et al., 2021b).
 200 This difference may be associated with the structure of the different pollutants. Ji et al. (2018) deduced that
 201 aniline and the dimethylisoxazole moiety within sulfisoxazole are the main reactive sites. This suggests that PMS
 202 selectively oxidises pollutants with electron-rich moieties because of its weak oxidative capacity.



203

204

205



206

207 **Fig. 2.** Effect of (a) PMS dosage, (c) MB dosage, (e) reaction temperature, and (g) initial pH on the direct
 208 degradation by PMS, and fitting curve for the (b) PMS concentration, (d) MB concentration versus k_{obs} , and (f)
 209 $\ln(k_{obs})$ versus $1/T$. (h) Variation of solution pH during the reaction process.

210 3.2.2 MB dosage

211 To understand the potential PMS oxidation ability of this system, decomposition of different MB concentrations
 212 by PMS was performed. k_{obs} decreased gradually from 0.0082 to 0.0063 min^{-1} with MB concentration change from
 213 5 to 40 mg/L (Fig. 2c). The plot of k_{obs} versus MB dosage obtained via linear regression analysis revealed an
 214 equation of $k_{obs} = -0.00006 [\text{MB}] + 0.0087 (\text{min}^{-1})$ (Fig. 2d). The relationship $G = (C_0 - C_{180}) V / ([\text{PMS}]V)$ (Text
 215 S2) was used to depict the amount of MB degraded (mg) per mmol PMS. The calculated G values were 5.1, 5.0,
 216 4.87, 4.67, and 4.60 mg/mmol with an increase of MB from 5 to 40 mg/L. Greater MB input resulted in a reduction
 217 of PMS oxidation efficiency, possibly because of the extra consumption of PMS by MB by-products.

218 3.2.3 Reaction temperature

219 Temperature played an important role in the reaction process, and high temperature generally increased the
 220 reaction rate. The MB removal rate increased with reaction temperature (25, 35, 45°C), and the k_{obs} values were
 221 0.0082, 0.0177, and 0.0224 min^{-1} , respectively. The removal rates were in line with k_{obs} (Fig. 2e). As shown in Fig.
 222 2f, the activation energy was calculated based on the Arrhenius equation ($\ln k_{obs} = \ln A - E_a/RT$). The obtained E_a
 223 was approximately 43 kJ/mol, which was higher than the values (30 and 32 kJ/mol) of phenol degradation achieved
 224 by PMS activated by cobalt-functionalised activated carbon, but lower than the value (62.3 kJ/mol) in the
 225 PMS/sulfuron-methyl/chloride system (Espinosa et al., 2019; Javier et al., 2018). Peng et al. (2018) reported that
 226 the E_a in the PMS/norfloxacin system was approximately 40.3 kJ/mol. The above results implied that the
 227 degradation of MB by PMS was an endothermic reaction process, which could reduce the energy barrier for
 228 reaction of PMS with MB. Although catalysts are usually used to reduce the activation energy, the E_a value

229 obtained in this experiment suggests the potential for direct oxidation of MB by PMS.

230 3.2.4 Initial pH

231 The species of PMS and MB were influenced by the pH of the system according to protonation and
232 deprotonation processes, and these PMS and MB species could affect the reaction process. Therefore, the
233 degradation of MB was investigated in solutions with various pH. As shown in Fig. 2g, an alkaline environment
234 was beneficial for MB degradation by PMS. The degradation of MB showed higher removal rates (Fig. 2g) and k_{obs}
235 values with increasing pH (Fig. S3). Furthermore, the pH of the solution gradually declined due to the release of H^+
236 during the PMS oxidation process (Fig. 2h) (Qi et al., 2016). Shimizu et al. (2007) reported that MB is unstable and
237 easily decolourised at $\text{pH} > 10$. The adjacent structure of PMS causes it to be activated easily to decolourise MB at
238 high pH (Yang et al., 2015). Kinetics analysis was conducted using the equations below:



241 PMS had three species ($\text{pK}_{\text{a}1} < 0$, $\text{pK}_{\text{a}2} = 9.4$). In this experiment, pH values ranging from 3.14–10.50 were
242 employed. As a cationic dye, MB had only one species, while the PMS species varied with solution pH. The result
243 follows:

244 $[\text{PMS}]_{\text{total}} = \alpha_6[\text{PMS}]_0 + \alpha_7[\text{PMS}]_0 + \alpha_8[\text{PMS}]_0$ (α_6 and α_7 , α_8 indicate the percentages of HSO_5^- , SO_5^{2-} , and
245 H_2SO_5 under different pH)

$$246 \quad \alpha_6 = [\text{H}^+]/([\text{H}^+] + \text{K}_{\text{a}2})$$

$$247 \quad \alpha_7 = \text{K}_{\text{a}2}/([\text{H}^+] + \text{K}_{\text{a}2})$$

$$248 \quad \alpha_8 \approx 0$$

249 The reaction rate of MB with PMS can be described by the following equation:

$$250 \quad \text{d}[\text{MB}]/\text{dt} = \sum k_i \alpha_i [\text{PMS}]_0 [\text{MB}]_0 \quad (i = 6, 7, k_i \text{ represents the corresponding reaction rate})$$

$$251 \quad = (k_6 \alpha_6 + k_7 \alpha_7) [\text{PMS}]_0 [\text{MB}]_0 = k_{\text{PMS,MB}} [\text{PMS}]_0 [\text{MB}]_0$$

$$252 \quad k_{\text{PMS,MB}} = k_6 \alpha_6 + k_7 \alpha_7$$

253 As illustrated in Table 1, k_6 was estimated as $0.0865 \text{ M}^{-1}\text{s}^{-1}$, which was close to $0.0833 \text{ M}^{-1}\text{s}^{-1}$, suggesting that
254 HSO_5^- was the main species of PMS under low solution pH ($\text{pH} < 7$). However, as the pH value of the solution
255 increased, SO_5^{2-} became the main species, and k_7 increased dramatically (10-fold) when the solution became
256 alkaline. Liao et al. (2021) found that the transformation of methyl parathion by PMS was also complex under
257 different pH values. This change was attributed to three aspects: the high reactivity and electrostatic attraction

258 between SO_5^{2-} and MB, easy decolourisation of MB under an alkaline environment (Shimizu et al., 2007), and
 259 enhanced alkalinity promoting activation of PMS for generation of $^1\text{O}_2$ and superoxide anion radicals (Qi et al.,
 260 2016).

261

262

Table 1 The reaction kinetics parameters at different initial pH

Initial pH	k_{obs} (min^{-1})	HSO_5^- percentage	k_6 ($\text{M}^{-1}\text{s}^{-1}$)	k_7 ($\text{M}^{-1}\text{s}^{-1}$)
3.14	0.0082	99.99%	0.091	— ^a
6.38	0.0074	99.90%	0.082	— ^a
8.83	0.011	78.79%	0.0865 ^b	0.254
9.65	0.1406	34.94%	0.0865 ^b	2.354
10.50	0.3912	7.36%	0.0865 ^b	4.68

263 a: The percentage of SO_5^{2-} was below 0.1% and the contribution of k_{obs} was ignored.

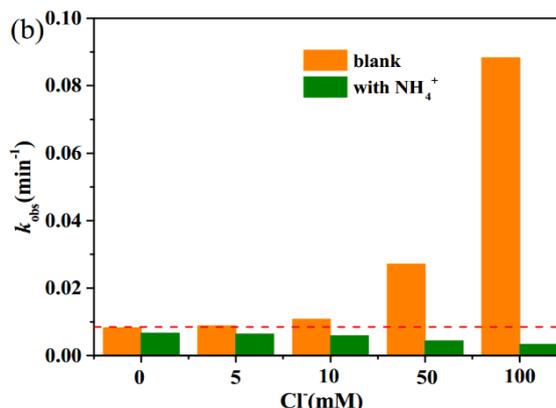
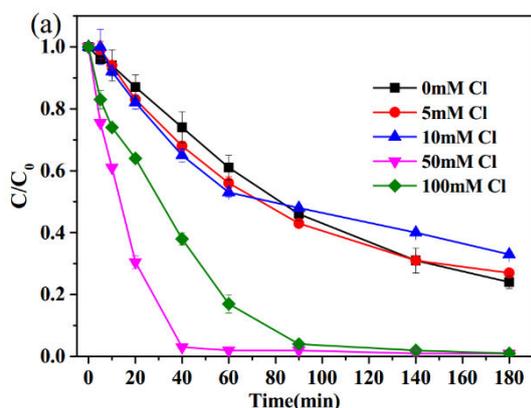
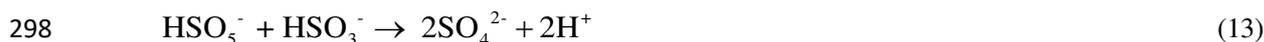
264 b: The value was obtained via $(0.091 + 0.082)/2$. The difference of k_6 between pH 3.14 and 6.38 was about 10%.

265 3.3 Effect of coexisting ions and humic acid

266 The chloride content in a natural body of water or wastewater treatment plant ranges from tens to hundreds of
 267 mg/L, and the drainage usually amounts to thousands of mg/L. In particular, higher concentrations of chloride are
 268 released by the metal smelting industry. Chloride can be oxidised by strong oxidants to generate HClO, which is
 269 used widely as an oxidant and bleaching agent, via the loss of an electron. As depicted in Fig. 3a, chloride
 270 accelerated degradation of MB, and the promotion effect increased with increased chloride concentration. However,
 271 the addition of NH_4^+ inhibited the degradation of MB in the presence of chlorine (Fig. S4). NH_4^+ can be
 272 deprotonated into NH_3 , which can react with HClO to induce the formation of chloramines (Deborde et al., 2008).
 273 The k_{obs} in the chloride system with NH_4^+ addition was obviously lower than the value in the system without NH_4^+ ,
 274 suggesting that Cl^- competes with MB for PMS (Fig. 3b) (Eqs. 9–11). Bromide can also be oxidised by PMS to
 275 generate HBrO, which was shown to accelerate the oxidation of tetrabromobisphenol S (Xu et al., 2021). Moreover,
 276 although PMS was consumed to generate HClO, the residual portion could still oxidise the majority of the MB
 277 when HClO was scavenged by NH_3 , and the k_{obs} dropped only slightly in comparison to the value in the PMS/MB
 278 system (Fig. 3b). This result indicated that the degradation of MB by PMS in the presence of chlorine was
 279 relatively low, and that the main factor leading to the degradation of MB may be the catalysis of PMS on chlorine.
 280 Ding et al. (2021) found that PMS did not react with chlorine but could be catalysed by chlorine to react with

281 acetaminophen. Therefore, the high reaction rate in the presence of chloride might occur through three steps:
 282 chloride reacting with PMS to generate HClO as the rate-limiting reaction (a determined step); decomposition of
 283 MB by HClO catalysed by PMS (main step); direct degradation of MB by PMS (minor step).

284 S(IV) can also scavenge radicals. Therefore, the effect of a reducing agent (NaHSO₃) on MB degradation by
 285 PMS was investigated. As shown in Fig. S5, MB decolourisation was almost inhibited with PMS alone.
 286 Nevertheless, with the addition of 10 and 50 mM chloride, the MB removal rate increased up to 32% and 76%,
 287 respectively. Connick et al. (1995) reported that PMS reacted with HSO₃⁻ in two ways: (1) via the formation of
 288 sulphate radicals, with an extremely slow reaction rate (Eq. (12)); and (2) via the production of a sulphate ion and
 289 proton with a fast reaction rate in comparison to (1) (Eq. (13)). PMS was consumed by HSO₃⁻, so the removal rate
 290 of MB diminished significantly. The chloride ion was able to react with the residual PMS (about 0.5 mM PMS) to
 291 form HClO, and the HClO was catalysed by PMS to accelerate the oxidation of MB. Hence, when a reducing agent
 292 was present in the PMS system, the diminished removal of organic matter could be compensated by the addition of
 293 chloride.



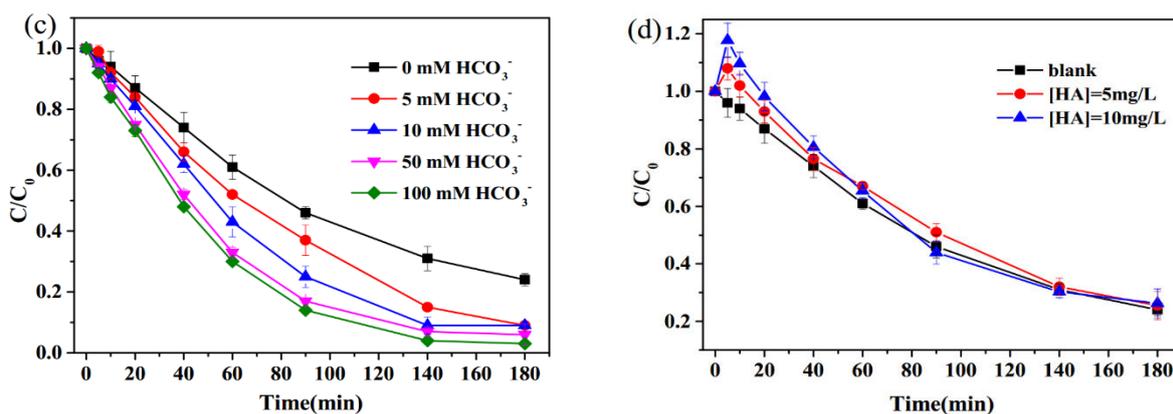


Fig. 3. Effect of (a) chloride, (c) bicarbonate, and (d) humic acid on MB degradation by PMS, and (b) k_{obs} of MB degradation in the presence of chloride and NH_4^+ . Experimental conditions: $[\text{MB}] = 10 \text{ mg/L}$, $[\text{PMS}] = 1.5 \text{ mM}$, $[\text{NH}_4^+] = 150 \text{ mM}$, reaction temperature = 25°C , pH unadjusted.

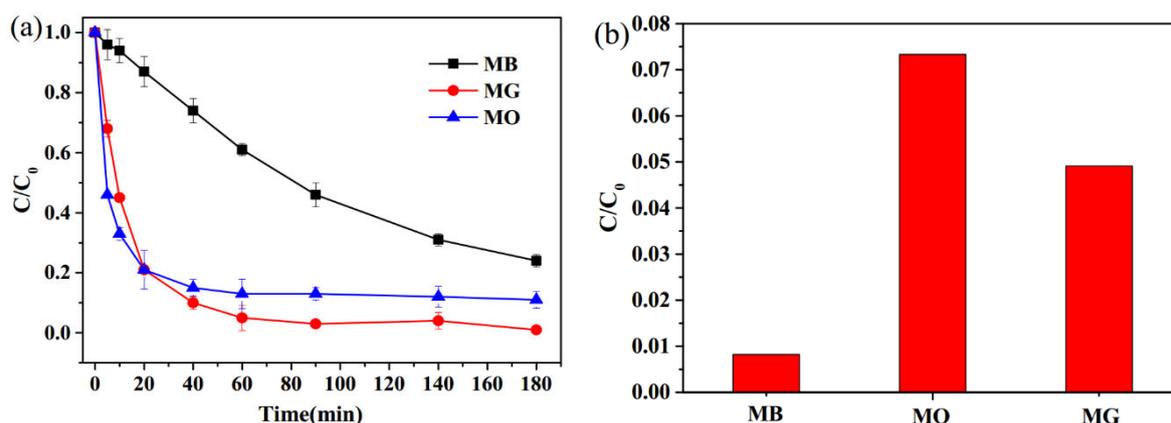
Bicarbonate is a common substance in surface bodies of water. Therefore, it is essential to investigate the effect of bicarbonate on the degradation of MB from the viewpoint of practical application (Song et al., 2019; Chen et al., 2019b). As illustrated in Fig. 3c, bicarbonate improved the removal rate of MB by PMS. The reaction rate was also accelerated from 0.0082 to 0.021 min^{-1} (Fig. S4). The addition of bicarbonate increased the solution pH (higher than 8.0 during the reaction process), and the alkaline environment was beneficial for the decomposition of MB. Furthermore, Yang et al. (2018) found that PMS could be catalysed by bicarbonate to form singlet oxygen. The effect of bicarbonate on MB removal was consistent with the results showing that the degradation of the azo dye Acid Orange 7 by PMS oxidation was activated by bicarbonate (Yang et al., 2010).

The dissolved organic matter in a natural body of water is composed of a carbon skeleton with abundant oxygen-containing functional groups at the surface, and the effect of humic acid on MB degradation can be ignored (Fig. 3d). For removal rates of 76%, 74.5%, and 77%, the k_{obs} values of MB degradation were 0.0082 , 0.0081 , and 0.0087 min^{-1} , respectively (Fig. S4). Humic acid reacted with sulphate radicals and hydroxyl radicals with second-order rate constants of 2.35×10^7 and $3 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$, respectively (Xie et al., 2015; Pang et al., 2018), further suggesting that the MB oxidation by PMS was a radical reaction process.

3.4 Universal degradation of other typical dyes

Different structures and physical and chemical properties can significantly affect the reaction between pollutants and oxidants. Three common dyes (MB, MO, and MG) were selected to investigate the capacity for PMS oxidation. MO is a typical azo dye, MB is a commonly used cationic dye, and MG is a type of toxic triphenylmethane dye. The k_{obs} values of MO, MB, and MG were 0.0733 , 0.0082 , and 0.0491 min^{-1} , respectively (Fig. 4b), and the removal rates were 89%, 76%, and 99%, respectively, indicating that PMS could decompose the

324 three dyes efficiently (Fig. 4a). Different from the cases of MB and MG, the NN moiety in MO is an
 325 electron-donating group and the sulfonic acid group is an electron-withdrawing group. The interaction of the two
 326 groups induced the electron clouds to be attracted to the side of the azo bond that was easily attacked by the
 327 electrophilic reagent PMS. This result agrees with previous studies (Guo et al., 2021; Chen et al., 2019c; Nie et al.,
 328 2019; Liu et al. 2015) reporting that decolourisation took precedence over degradation of the benzene ring. The NN
 329 moiety is the common sub-structure among the three dyes, and NN was degraded by more than 90% within 5 min
 330 by direct oxidation by PMS (Fig. S6). The higher reaction rate of NN compared to other parent dyes may indicate
 331 that NN was the reactive site of the three dyes. The lower reaction rates than the rate of NN might be attributable to
 332 an effect of other sub-structures on the parent dyes (Ji et al. 2018). The formation of the conjugated system in the
 333 three parent dyes prompted the rearrangement of electron clouds. However, the introduction of strong
 334 electron-withdrawing groups induced a reduction of the energy barrier and electrons could escape easily (Titov et
 335 al., 2015). Further research is needed to understand the details of the mechanism.

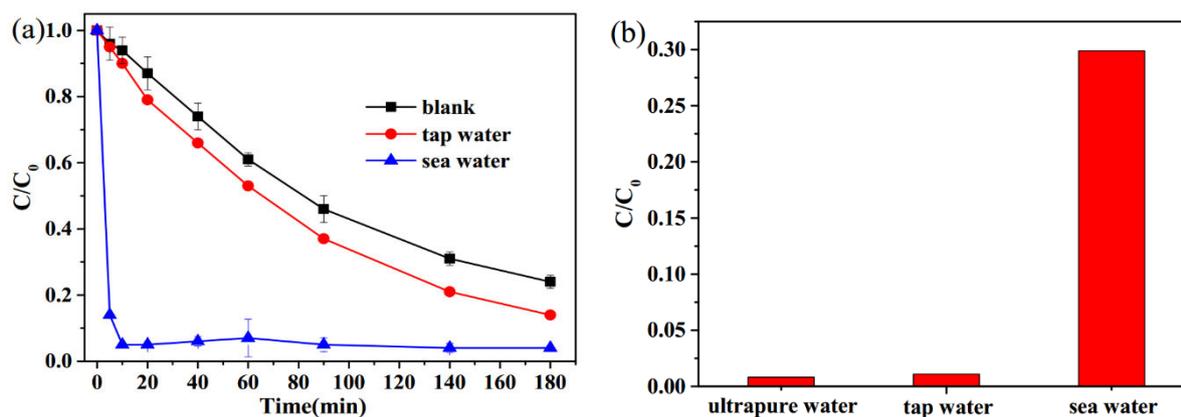


336 **Fig. 4.** (a) Direct degradation of MB, MG, and MO by PMS and (b) k_{obs} of the MB, MG, and MO degradation.
 337 Experimental conditions: [MB] = [MO] = [MG] = 10 mg/L, [PMS] = 1.5 mM, reaction temperature = 25°C, pH
 338 unadjusted.

340 3.5 Effect of water matrix

341 To understand the MB degradation performance of advanced oxidation processes (AOPs) more completely, two
 342 types of water (sea water and tap water) were employed. Sea water was collected from the South China Sea and tap
 343 water was obtained from Shanghai, China. The water quality of the two samples is described in Table S1. The MB
 344 removal and reaction rates in the above waters were better than those in ultrapure water (Fig. 5). Especially, the
 345 high chloride content of sea water promoted MB degradation. Although the two water matrices contained dissolved
 346 organic matter, which competed with MB for radicals, PMS reacted with MB directly without generating radicals.
 347 The results from the application of the two water types suggest that PMS is an efficient choice for real water

348 sample purification.



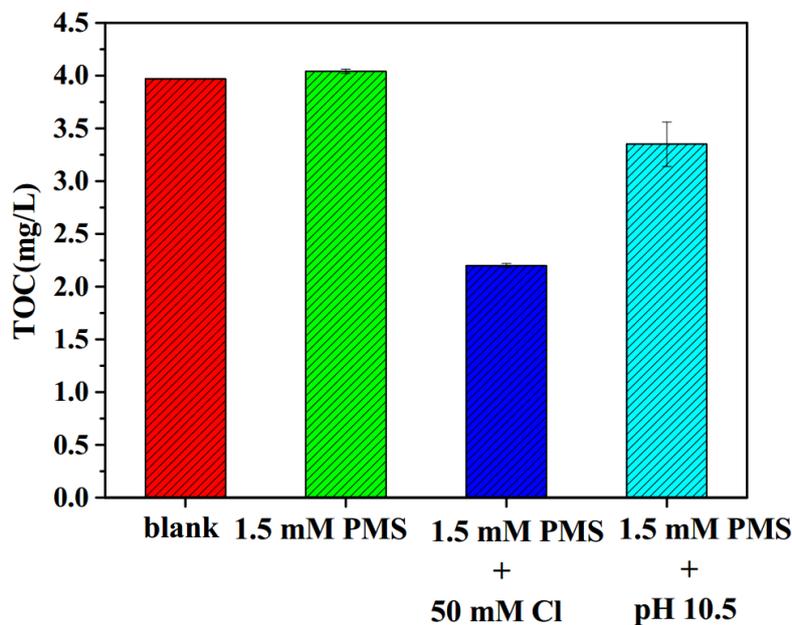
349

350 **Fig. 5.** (a) Effect of different water matrices on the degradation of MB by unactivated PMS. (b) k_{obs} of MB
351 degradation under different water matrices. Experimental conditions: [MB] = 10 mg/L, [PMS] = 1.5 mM, reaction
352 temperature = 25°C, pH unadjusted.

353 3.6 TOC removal in different reaction conditions

354 Total organic carbon (TOC) is an important indicator of the mineralising capacity of pollutants in a system. In
355 this study, the pollutants were first decomposed into small molecular substances and then oxidised into carbon
356 dioxide and water. The results of the TOC removal are shown in Fig. 6. The TOC removal rate was near zero at pH
357 3.14. However, it increased to 16% at pH 10.5. In the presence of 50 mM chloride, the TOC removal rate was 45%.
358 These results suggest that PMS alone can barely mineralise MB and only damaged the chromogenic group of the
359 MB. Zhou et al. (2020b) found that MB oxidation by PMS proceeded through oxygenation, demethylation, and
360 deamination processes, but the main structure of MB remained unchanged. The TOC removal rate of AO7 by PMS
361 alone was only 19.2%, suggesting that the mineralisation capacity in the PMS system was low (Chen et al., 2021).
362 Under the highly alkaline environment, SO_5^{2-} was the main species of PMS, and it reacted with MB rapidly
363 through the mineralisation process. Additionally, the formation of singlet oxygen and superoxide anion radicals via
364 PMS self-decomposition selectively degraded pollutants with electron-rich moieties. Therefore, more recalcitrant
365 by-products were formed in the reaction process and could barely be mineralised. In the presence of chloride, the
366 HClO that formed had a strong capacity to oxidise the chromogenic group and further mineralise MB with catalysis
367 by PMS. Wang et al. (2011) pointed out that the TOC removal rate of azo dyes in the Co/PMS/Cl system was lower
368 than 5% within 450 s, indicating that chloride could improve the decolourisation ability but not the TOC removal
369 rate. Yuan et al. (2011) reported that although the sulphate and hydroxyl radicals formed in the Co/PMS system had
370 strong redox potential, the oxidation ability of chlorine radicals generated by the reaction of other radicals with
371 chlorine was low in comparison to the sulphate and hydroxyl radicals. Additionally, the chlorine radicals reacted

372 with azo dyes or by-products to form refractory organic halogen compounds, which are difficult to mineralise.
373 However, on the contrary, the addition of chloride enhanced the TOC removal rate in this study, which may be
374 attributable to HClO replacing, and being catalysed by, PMS. However, with the generation of organic halogen
375 compounds and the consumption of PMS, mineralisation gradually ceased.



376 **Fig. 6.** Variation of TOC under different circumstances. Experimental conditions: [MB] = 10 mg/L, reaction
377 temperature = 25°C, pH unadjusted (except where specified).
378

379 4. Conclusion

380 AOPs based on radicals have strong oxidation abilities, allowing the removal of a broad range of organic
381 micropollutants. However, direct oxidation by PMS for water purification has been overlooked. The reaction
382 mechanism, kinetics, and parameters of PMS reacting with MB found in this study can be summarized as follows:

383 (1) PMS reacted with MB via a non-radical pathway. Additionally, the second-order rate constant of MB
384 reacting with singlet oxygen was estimated to be approximately $1.25 \times 10^5 \text{ M}^{-1}\text{s}^{-1}$.

385 (2) The pseudo-first-order rate constant of MB transformation showed a negative linear correlation with the MB
386 concentration and a positive linear correlation with the PMS concentration.

387 (3) Increasing the solution pH favoured MB degradation by PMS, which was attributed to the high reaction rate
388 between SO_5^{2-} and MB.

389 (4) The addition of chloride accelerated MB transformation and mineralisation by PMS due to the formation of
390 HClO and catalysis by PMS.

391 (5) In real water matrices (sea water and tap water), MB degradation was promoted. Even in water with added
392 humic acid, MB degradation was not affected, suggesting an advantage of the PMS oxidation system.

393 Above all, this study aimed to provide deeper insight into AOPs based on the PMS oxidation system and thus
394 provide an alternative solution for the treatment of environmental pollution.

395 **Ethical approval**

396 Not applicable.

397 **Consent to participate**

398 The authors all agree to participate in the paper.

399 **Consent to publish**

400 The authors all agree that the paper is published in the journal.

401 **Credit author statement**

402 **Xu Zuo:** Conceptualization, Investigation, Writing - original draft. **Jianxin Nie:** Writing - review & editing. **Beier**

403 **Jiang:** Editing. **Aijun Jiang:** Methodology. **Shiyang Zou:** Editing & Supervision. **Junrong Wu:** Supervision.

404 **Bingquan Ding:** Investigation. **Xuehui Wang:** Validation. **Yang Liu:** Investigation.

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407 **Declaration of competing interest**

408 The authors report no declarations of interest.

409 **Availability of data**

410 All data generated or analyzed during this study are included in this published article.

411

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