

Research and Application of Precision Fertilizer Application Algorithm Based on PSO Optimized Fuzzy PID Control

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1 Research and application of precision
 2 fertilizer application algorithm based on PSO
 3 optimized fuzzy PID control

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12 **Abstract**

13 In irrigation's process and fertilizer application in production of agri-
 14 culture, the accuracy of fertilizer application and water maintains at a
 15 relatively low level, which results in waste of soil slabbing and resources.
 16 In this research, a fuzzy PID algorithm based on PSO optimization
 17 is designed to control the fertilizer application process and irrigation
 18 of the fertilizer applicator. Firstly, a mathematical model of the fer-
 19 tilizer applicator is established according to the relevant modules and
 20 corresponding parameters. Based on the MATLAB/Simulink platform,
 21 the PID controller, the fuzzy PID controller and the controller pro-
 22 posed in this article are constructed respectively, which can be applied
 23 to the established transfer functions. The simulation outcomes demon-
 24 strate that the response time of the control algorithm proposed in this
 25 research is shortened to 30s, compared to fuzzy PID and PID, which
 26 is 62.5% and 50% shorter respectively, and the overshoot of the control
 27 algorithm in this article is nearly 0 of apart from the early oscillation.
 28 In order to verify the algorithm's reliability in practical application, this
 29 research designs groups of different pressure for the accuracy control
 30 test , the test consequences illustrate that the fuzzy PID control based
 31 on PSO optimization has excellent control effect under each pressure.
 32 The control accuracy is concentrated at around 2%, while PID con-
 33 trol maintains around 20% and fuzzy PID control distributed at 10%.

The results show that the control algorithm proposed in this research enhances the irrigation accuracy in the practical application process.

Keywords: Precision fertilizer application,Fuzzy PID control,PSO algorithm,Performance analysis,experimental validation

1 Introduction

Agriculture accounts for more than 65% of total water consumption, and 95% of water application of agriculture is applied for irrigation of large zones of farmland, where water is severely scarce[1]-[5].Variable fertiliser application is an important area of research in the development of precision that farms, and this technology is a excellent solution to the high labour intensity, low efficiency of fertiliser application operations and the unevenness of manual fertiliser application. Most of the current fertiliser application models are still based on ready approach and a rough, with water's concentration proportion to fertiliser being ignored in the fertiliser application process and irrigation, leading to depressed fertiliser uptake by crops and plenty of wasted water and labour[6][7]. Although the increased application of water and fertiliser measures can achieve higher yields, the relatively high water and fertiliser inputs not only increase the risk of groundwater pollution, but also have a negative impact on plant growth and the greenhouse environment.

Research on the waste of fertilizer resources and water has been done by a large number of scholars. Literature[8] designs and realization of water, fertilizer and pesticide integrated automatic control device, the paper discusses selection and application of fertilizer pesticides, use procedure, water, fertilizer and pesticide saving effect and receptive crowd in the application process of modern planting industry. In view of the application status of irrigation and fertilizer system control, cloud computing is applied in Literature[9].Two new control algorithms based on MSP430 microcomputer unit(MCU)are developed in Literature[10] to improve the performance of a fustigation system controlled by the electrical conductivity(EC)value of an irrigation nutrient solution in a greenhouse. In view of the phenomenon of heavy workload, time-consuming, labor-consuming and error leakage by manual statistics in the process of large-scale cultivation of maize in Ningxia, different nitrogen treatment experiments are designed Literature[11].An integrated experiment system of water and fertilizer control based on PLC was in designed Literature[12],which can monitor EC value of water and fertilizer.In view of the large hysteresis, large inertia and uncertain mathematical model of the water and fertilizer integrated in Literature[13] machine to adjust the pH value of water and fertilizer, this paper applies fuzzy control to water and fertilizer integrated equipment, and designs a fuzzy control system to adjust the pH value of water and fertilizer. In general,

73 there are fewer control algorithms focusing on precision fertilization in the fol-
74 lowing work, the drawbacks and advantages of some of the control algorithms
75 are analysed.

76 Traditional PID control, to a great extent dependent on the model's accu-
77 racy, which will cause the corresponding costs in modelling's process [14][15],
78 in addition, since conventional PID is not straightforward to on-line rectifica-
79 tion parameters, can not adapt to the complex parameters of the environment
80 for on-line adjustment, fast response requirements, so the conventional con-
81 trol algorithm has not been able to meet liquid fertilizer variable control's
82 necessities. A precise mathematical model is not required by Fuzzy PID
83 control [16]-[20], to a certain extent to puzzle out the control police problem's
84 model, only need to summarize the human control experience, is a sort of
85 human behavior's imitation, convenient to be accepted by the operator con-
86 trol technology. The fuzzy PID controller, nonetheless, is less delicate in its
87 control on account of the blind spot near the balance point. In production of
88 agriculture of today, there are frequently problems with fertiliser application
89 accuracy being difficult to grasp and timing not being easily controlled.

90 Overall, this paper proposes to analyse the variable control section's com-
91 position, solve for the relevant parameters and derive the electric proportional
92 valve's transfer function, and simulate the transfer function applying the PID
93 control algorithm. The control algorithm is selected as study's object with
94 three control algorithms, PID, fuzzy PID and PSO fuzzy PID, and the MAT-
95 LAB software is used as the simulation platform for simulation and the quality
96 parameters are analysed for the simulation consequences. In order to verify the
97 algorithms' superiority proposed in this research in the actual operation pro-
98 cess, different control algorithms' accuracy is compared by the accuracy test
99 designed in this article in the irrigation process.

100 2 Mathematical modelling of fertilizer 101 application systems

102 This system's flow adjustment device is an electric proportional valve which
103 comprises a valve body and a drive motor, the motor drives the transmission
104 part through rotation so as to control the valve spool and thus realise the
105 control of the valve body's opening. The opening degree's control is realised
106 by the electric proportional control valve and thus the flow's control rate.
107 And it comprises the following parts: DC Motor Speed Reducer Voltage Drive
108 Module Sensing Module and Data Acquisition Module.

109 A closed-loop control strategy where the controller forms a decision signal
110 through the position input signal, adjusts the voltage output and drives the
111 motor for start-stop, forward and reverse action is used by the electric propor-
112 tional valve's control, and the spool is driven by the motor to change the valve
113 opening's size. The position sensor's function is to detect the valve that opens
114 information and transmit it to the controller to form a closed loop control.
115 The principle block diagram is shown in Fig.1.

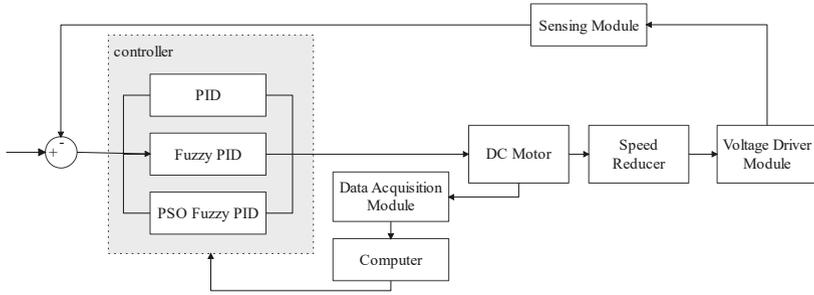


Fig. 1 Control structure diagram of fertilizer application system.

116 Through the analysis of the liquid fertilizer spraying variable control system control part of the electric proportional control valve's composition, the transfer function by the DC motor, reduction device, the electric proportional valve that opens control transfer function is constituted by voltage drive.

117
118
119
120 DC motors are the driving device in electric proportional valves. DC motors are widely applied in regions that require speed control and forward and reverse rotation owing to the ease and high precision of control. The stroke control and speed of the motor are associated with the valve control's precise operation. The voltage's transfer function and stroke of the DC motor is derived as follows.

121
122
123
124
125
126 The equilibrium equation for the motor drive voltage is shown in Eq(1).

$$U_d(t) = RI_d + L \frac{dI_d(t)}{dt} + E(t) \quad (1)$$

127 Where $U_d(t)$ is the DC motor's drive voltage, R is the internal resistance, $I_d(t)$ is the armature current and $E(t)$ is the electric potential. The equation for the output torque can be expressed as:

$$M(t) = KI_d(t) \quad (2)$$

130 where $M(t)$ is the output torque of the DC motor and K is the DC motor torque factor. The DC motor torque expression is given in Eq.

$$M(t) - M_1(t) = J \frac{dw(t)}{dt} \quad (3)$$

132 where $(M)t$ is the torque of the load, J is the amount of rotational inertia of the DC motor and $w(t)$ is the speed of the DC motor.

$$M_1(t) = f\ddot{\theta}(t) \quad (4)$$

134 where f is the coefficient of friction and θ is the angle of rotation of the motor output.

135
136 Combining the above equations yields.

$$I_d(t) = \frac{1}{K_m} [J\dot{\theta}(t) + f\ddot{\theta}(t)] \quad (5)$$

137 Bringing the above equation into the voltage balance equation gives.

$$LJ\ddot{\theta}(t) + (Lf + RJ)\dot{\theta}(t) + Rf\ddot{\theta}(t) + K_m E_m(t) = K_m U(t) \quad (6)$$

138 where K_m is the inverse electric potential coefficient. The transfer function
139 between the DC motor's output angle and the input voltage is obtainable after
140 the Laplace inverse transformation as:

$$G_1(s) = \frac{\theta(s)}{U(s)} = \frac{K_m}{L_a f s^3 + (Rf + L_a J)s^2 + RJs} \quad (7)$$

141 By the series relationship between the parts, the output angle is used as the
142 reduction device's input reference, which increases the output torque by reduc-
143 ing the motor speed, and its expression is the ratio of the reduction device's
144 torque to the DC motor's output torque, without generality's loss, equating the
145 link to the proportional relationship between the two angles, the part's transfer
146 function is the proportional relationship between the two angles, reflected
147 in the relationship between the reduction device's output displacement and
148 the input angle, which can be listed and written as follows.

$$G_2(2) = \frac{X(s)}{\theta(s)} = \frac{L}{2\pi} \quad (8)$$

149 where L denotes the lead of the guide rod and X is the output displacement.

150 Through the modelling of the above two connections, the transfer function
151 of the driving part of the fertiliser can be determined by the output voltage and
152 the input voltage to, in addition, the existence of a certain delay in this trans-
153 mission module, the delay time can be neglected compared to the switching
154 frequency, in summary, this voltage driving module's transfer function is:

$$G_3(3) = \frac{U_{out}(s)}{U_{in}(s)} = K_s e^{\tau s} \approx K_s \quad (9)$$

155 The modules are connected in parallel with each other and K_s is the con-
156 verter amplification factor. The transfer you function of the system can be
157 obtained as:

$$G(s) = G_1(s)G_2(s)G_3(s) = \frac{K_m K_s L}{(L_a f s^3 + (Rf + L_a J)s^2 + RJs)2\pi} \quad (10)$$

158 The fertiliser application system parameters are listed in the table 1.

159 Bringing the parameters into the mathematical model yields the transfer
160 function for this study as

$$G(s) = \frac{0.048}{9.9 \times 10^{-5} s^3 + 4.65 \times 10^{-4} s^2 + 2.87 \times 10^{-4} s} \quad (11)$$

Table 1 Table of relevant parameters of the fertilizer application device

Symbol	Parameters	Value
K_m	Counter-electromotive force constant	0.048V/rad
K_s	Magnification factor	2
L	Guide bar movement distance	5mm
L_a	Stator inductor	3.94mH
f	Friction coefficient	$3 \cdot 10^{-6}$ mm
R	Stator resistance	2.74 Ω
J	Rotational inertia	$1.67 \cdot 10^{-5}$ kg/m ²

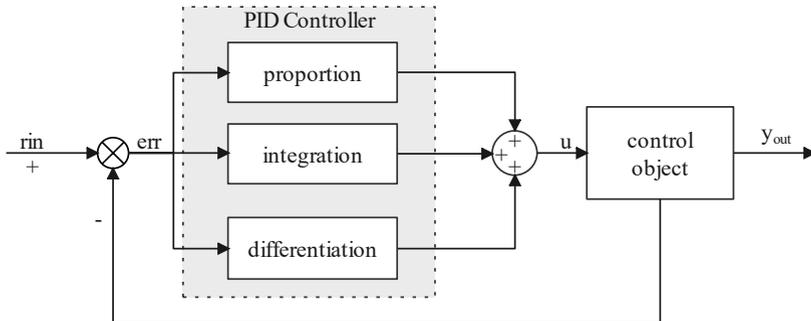
3 Design of the control algorithm

3.1 Design of a fuzzy PID controller

In order to compare and analyse different controllers' performance indicators, an algorithmic control system that is based on PID control is first constructed starting from the traditional classical control PID algorithm[21]-[25], which can compensate for a blind's lack spot near the controller's balance point. Determining the k_p , k_i and k_d of the PID, either continuous control or analogue control can be done by the PID controller, and its expression is:

$$u(t) = k_p[e(t) + \frac{1}{T_1} \int_0^t e(t)dt + T_d \frac{de(t)}{dt}] \quad (12)$$

The control structure is schematically shown in Fig.2.

**Fig. 2** Schematic diagram of PID controller.

The fuzzy adaptive PID algorithm comprises a combination of a PID controller and a fuzzy controller mainly, with the error (e) and the rate of change of the error (ec) as controller inputs and the control parameters of the PID proportional link (K_p), integral link (K_i) and differential link (K_d) adaptively adjusted according to fuzzy rules. The fuzzy adaptive PID structure is demonstrated in Fig.3 as follows[26]-[30].

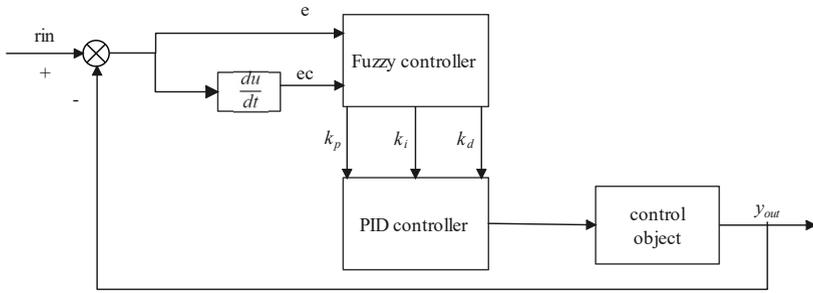


Fig. 3 Schematic diagram of Fuzzy PID controller.

176 The deviation e and the rate of change of deviation ec are selected as the
 177 two input variables of the fuzzy controller for water and fertilizer flow, and the
 178 three parameters k_p, k_i, k_d are selected as the output variables of the fuzzy
 179 controller for optimisation, and the corresponding fuzzy variables were E, EC
 180 and u_p, u_i, u_d . The quantization factor of the deviation of flow value, the
 181 quantization factor of the rate of change of deviation and the scaling factor
 182 were denoted by k_e, k_{ec} and respectively.

$$e_n = b_n - b_0 \quad (13)$$

$$e_{n-1} = b_{n-1} - b_0 \quad (14)$$

$$c_n = \frac{e_n - e_{n-1}}{T} = \frac{b_n}{b_{n-1}} \quad (15)$$

183 where b_0 is the fertilizer flow rate value and set water. b_{n-1} and b_n are
 184 the flow rate values that are detected by the flow sensor for the n_{th} times and
 185 $n-1$ st, respectively. e_{n-1} and e_n are the deviations between the $n-1$ st and n_{th}
 186 detected fertilizer flow values and the set value, respectively. c_n is the rate of
 187 change of the deviation of the fertiliser flow value and n_{th} detected water. T
 188 is the sampling period.

189 The deviation input, deviation rate of change input and parameter optimi-
 190 sation output of the designed water and fertiliser flow value fuzzy controller
 191 all use a triangular type of affiliation function, and the area centre of gravity
 192 method is chosen as the clarification method for the water and fertiliser flow
 193 value fuzzy controller. The number of fuzzy subsets covering the whole fuzzy
 194 domain is generally 3 10, which can avoid the excessive number of fuzzy rules
 195 and ensure a certain control accuracy.

196 In this article, the linguistic values of the deviation e and the rate of change
 197 of the flow values' deviation ec are selected as [NB, NM, NS, ZO, PS, PM, PB]
 198 , and the fuzzy domains are taken as the characteristic points [- 3,- 2,- 1, 0, 1,
 199 2, 3]. where NB, NM, NS, ZO PS, PB and PM denote negative large, negative
 200 medium, negative small, 0, positive small, positive medium and positive large,
 201 respectively. For instance, when E is PB means that the current measured
 202 water and fertiliser flow is much larger than the set value; when EC is PB,

203 it means that the next time the fertiliser flow and water will be much larger
 204 than the current that was measured flow. The linguistic values of the selected
 205 optimisation parameters k_p k_i k_d are [NB, NM, NS, ZO, PS, PM, PB] and
 206 the fuzzy domain's characteristic points are [- 3,- 2,- 1, 0, 1, 2, 3]. Where NB,
 207 NS, ZO, PS and PB denote the parameter values for the fertilizer application
 208 system's different operation modes.

209 Through literature review and field research to summarise the expert experi-
 210 ence of flow values, the fuzzy control statement was chosen in the form of
 211 "If E and EC then k_p k_i k_d ", and the fuzzy control rules were written in the
 212 form of $7 \times 7 = 49$ statements, and the control rule table is shown in Table 2.
 213 The affiliation relationship between the two inputs and the output affiliation
 214 relationship between the three optimised parameters is shown in Fig.4. The
 215 fuzzy surface diagram of the optimised parameters is shown in Fig.5- Fig.7.

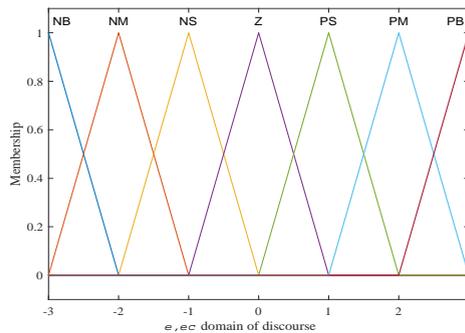


Fig. 4 Affiliation function of fuzzy input & fuzzy output.

216 3.2 Design of a fuzzy PID controller based on particle 217 swarm optimization

218 PSO (particle swarm algorithm) has a strong ability to deal with continuous
 219 problems, and is therefore suitable for parameter optimisation, while the PID
 220 controller consists of three parameters: k_p, k_i, k_d .

221 The PID controller is treated as a "black box", with these three parameters
 222 as inputs and the response curve as output, and all we have to do is optimise
 223 this response curve. A good PID controller should have a fast response, small
 224 overshoot and steady-state error for different types of inputs. Therefore, the
 225 classical three input signals: step, ramp and parabolic are used to measure the
 226 PID control effectiveness. The topology of the PSO optimisation based fuzzy
 227 PID controller designed in this study is shown in Fig.8 .

228 The flow of the basic particle swarm algorithm is as follows, Which can be
 229 shown in Fig.9.

230 (1) Particle swarm hyperparameters as well as random solutions are
 231 initialised.

Table 2 Fuzzy rule table for fuzzy control.

E	EC						
	NB	NM	NS	Z	PS	PM	PB
NB	PB,NB,PB	PB,NB,PB	PM,NM,PM	PM,NM,PM	PM,NM,PM	PB,NB,PB	PB,NB,PB
NM	PB,NB,PB	PB,NB,PM	PM,NM,PS	PM,NM,PS	PM,NM,PS	PB,NB,PM	PB,NB,PB
NS	PM,NM,PM	PS,NM,PS	PS,NS,Z	Z,NS,Z	PS,NS,Z	PM,NM,PS	PB,NB,PB
O	PM,NM,PM	PM,NM,PS	PS,NS,Z	Z,NS,Z	PS,NS,Z	PM,NM,PS	PM,NM,PM
PS	PM,NM,PM	PM,NM,PS	PS,NS,Z	PS,NS,Z	PS,NS,Z	PM,NM,PS	PM,NM,PM
PM	PB,NB,PB	PB,NB,PM	PM,NM,PS	PM,NM,PS	PM,NM,PM	PM,NB,PM	PB,NB,PB
PB	PB,NB,PB	PB,NB,PB	PM,NM,PM	PM,NM,PM	PM,NM,PM	PB,NB,PB	PB,NB,PB

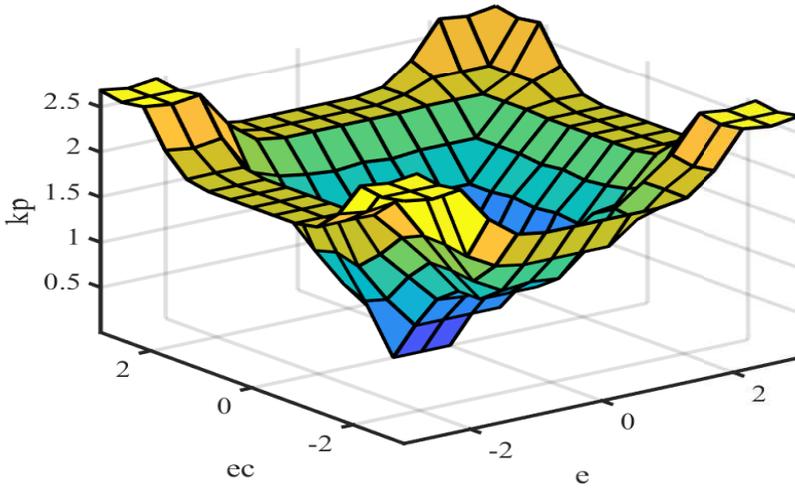


Fig. 5 Fuzzy surface diagram of k_p .

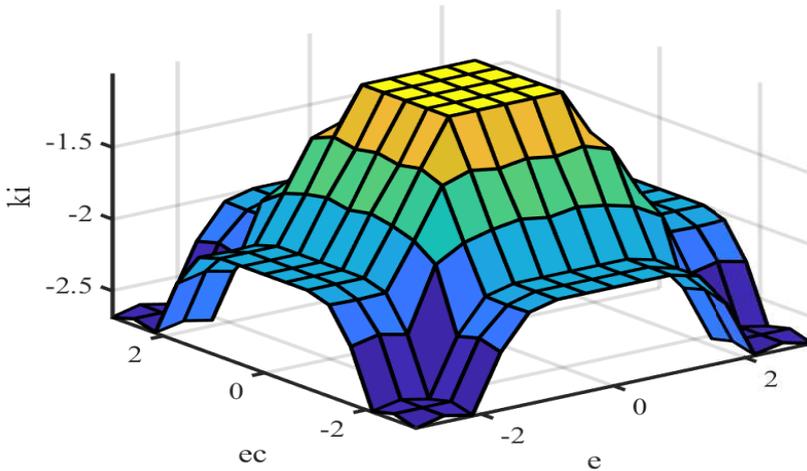


Fig. 6 Fuzzy surface diagram of k_i .

232 (2) Set the values of the PID control parameters, run the system and judge
 233 whether the system performance indicators meet the requirements.

234 (3) If the particle adaptation value at the current time is higher than all
 235 previous ones, the optimal value is updated.

236 (4) Iterate each particle, if the current particle is better than the best
 237 position adaptation value in the swarm, then its as the population optimum.

238 (5) The velocity and position of the particle are updated.

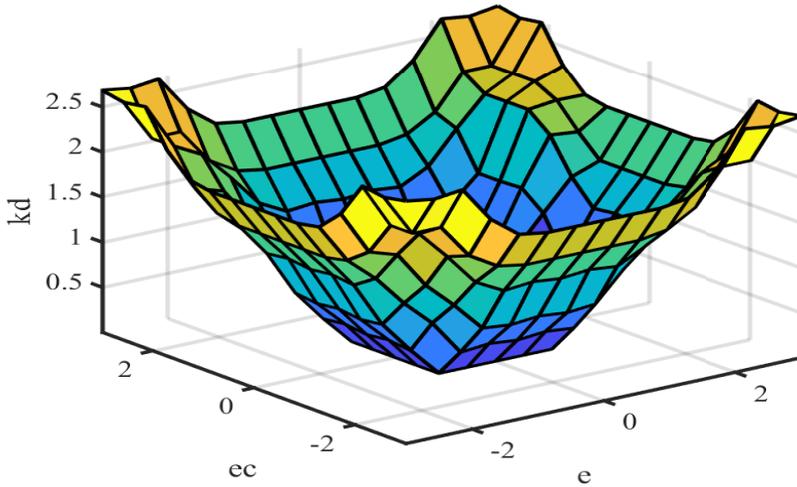


Fig. 7 Fuzzy surface diagram of k_d .

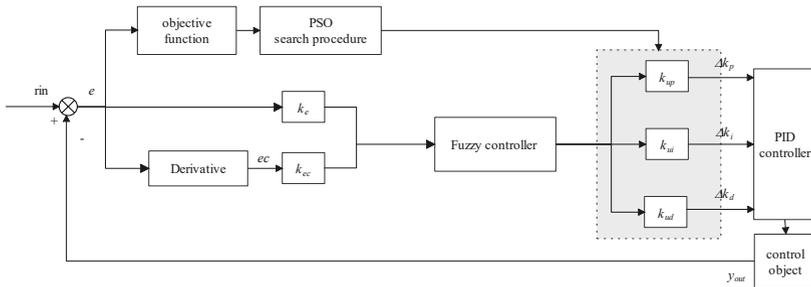


Fig. 8 Schematic diagram of fuzzy PID control based on PSO optimization.

239 (6) If the global adaptation value is satisfied to be sufficiently good or the
 240 run reaches the maximum number of iterations), then end, otherwise go to
 241 step (1).

242 The control schematic and control flow diagram of particle swarm optimi-
 243 zation algorithm are Fig 8 and Fig 9 respectively.

244 4 Simulation of flow value control for fertilizer 245 application systems

246 For the designed variable fertiliser control model, a conventional PID control
 247 simulation model of the liquid fertiliser variable fertiliser control system was set
 248 up using the simulink simulation module in MATLAB software, the input step
 249 signal amplitude was set to 10, the PID controller parameters were adjusted
 250 and the output waveforms were analysed. The PID control model's simulation

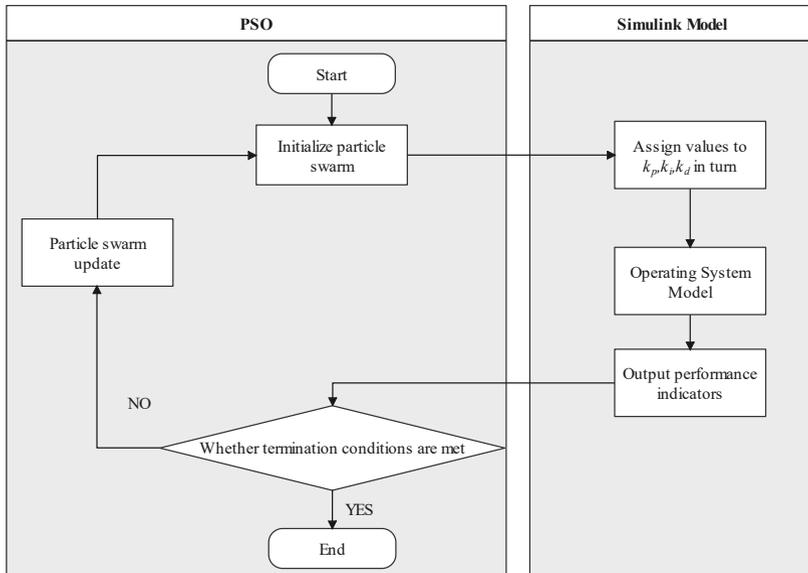


Fig. 9 Control flow chart of particle swarm algorithm.

251 process is as follows: a step signal of amplitude 10 is input at $t = 0$, the
 252 simulation time is set to 100 s, and k_i , k_d and the k_p of the PID controller are
 253 adapted, the waveform is then output to the oscilloscope

254 According to the graph(Fig.10), the model response time is 80 s, the over-
 255 shoot is 0.229 and there is some oscillation before the system operation reaches
 256 stability. According to the empirical trial and error method, $k_p=6.5$, $k_i=1.2$
 257 and $k_d=1$ are finally chosen.

258 The simulation model of the fuzzy PID control system is set up in the
 259 simulink simulation module, and the input signal is also a step signal with an
 260 amplitude of 10. The simulation process is to input a step signal of amplitude
 261 10 at $t = 0$ and set the simulation time to 100 s. The input variables of the
 262 fuzzy controller are the fuzzified error $e(k)$ and the rate of change of the
 263 error $ec(k)$, and the fuzzy controller outputs the compensation value of the
 264 defuzzified PID parameters, and the compensation value is used to optimise
 265 the initial parameters, and then the simulation waveform of the control system
 266 is obtained. The control curve of the optimised system is shown in Fig 10. As
 267 can be seen from the graph, the model response time of the fuzzy PID control
 268 is 40 s, the overshoot is 0.18 and there is some oscillation before the system
 269 operation reaches stability.

270 The model developed for the variable fertiliser control system was pro-
 271 grammed with MATLAB software to implement a genetic algorithm for the
 272 optimisation of fuzzy control rules. The absolute error integration criterion is
 273 used to judge the performance index of each generation of individuals opti-
 274 mised by the genetic algorithm, and the optimisation process ends when the
 275 population iterations reach the required performance index, and if the required

276 index is not reached, the best individual of the last generation of the population
277 is taken as the result for the control model simulation.

278 The system inputs a step signal with an amplitude of 10, then the fuzzy
279 language values corresponding to the compensation values k_p , k_i and k_d from
280 the fuzzy controller are formed into individuals, and the initial population is
281 randomly generated, and the population is optimised by the particle swarm
282 operator, and the population is iterated to the maximum genetic generation.
283 The particle swarm algorithm optimal individual iterative search process is
284 shown in Fig. The optimised parameters are shown in Fig. The control curve
285 of the optimised system is shown in Fig 10. As can be seen from the graph, the
286 model response time for the particle swarm optimised fuzzy PID control is 27
287 s with an overshoot of 0.03, which is a substantial reduction in overshoot com-
288 pared to the other controls, with some oscillations before the system operation
289 reaches stability.

290 Simulation examinations are carried out with the electric proportional valve
291 opening transfer function as the control object, applying fuzzy adaptive PID,
292 PSO fuzzy PID and conventional PID. The fuzzy PID control based on PSO
293 optimisation possesses a short time from disturbance's occurrence to equilib-
294 rium's establishment again for the control quantity, and the overshoot process
295 is an important indicator of the system's rapid response. The control algo-
296 rithm proposed in this study outperforms the other two algorithms in terms of
297 overshoot, indicating that the control proposed in this study has a small dif-
298 ference in deviation from the set value. Further, the algorithm is substantially
299 reduced compared to the other two algorithms, indicating a short overshoot
300 high system accuracy and process time with small deviations from the set
301 value. In summary, the control algorithm that is proposed in this study pos-
302 sesses the advantage of fast convergence of control parameters, strong adaptive
303 capability, high control accuracy and on-line self-tuning of the adaptive vari-
304 able control algorithm when this variable control system is used as the control
305 object.

306 5 Experimental design and analysis

307 A fuzzy PID is used by the liquid fertiliser variable control system based on
308 PSO optimisation as the control algorithm for the variable control system.
309 The system is tested indoors by setting target quantities through the control
310 terminal to respectively verify the relationship between flow rate and system
311 pressure, and the operational accuracy of the system. These results are applied
312 to measure the liquid fertiliser variable control system's liquid fertiliser con-
313 trollability and are also important indicators to test whether this system meets
314 the variable operation. The system pressure relates to the pressure that is
315 obtained by changing the regulating valve's opening when the pressure sup-
316 plied by the pump is constant. The system pressure during the experiment
317 is the pressure value demonstrated after adapting the proportional regulating
318 valve. The platform for the precision fertiliser system is shown in Fig.11.

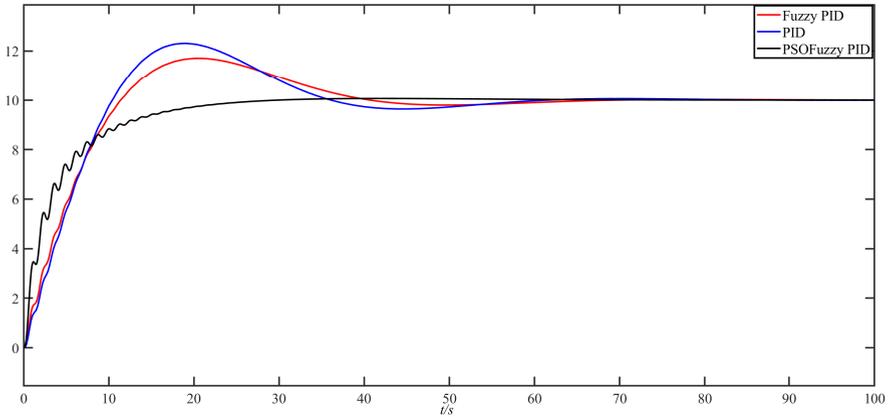


Fig. 10 Simulation comparison graph of the three control methods.



Fig. 11 Precision fertilization physical platform.

319 Accuracy is one of the significant indicators for evaluating variable control
 320 systems. By setting the target flow rate, i.e. the theoretical flow rate, the
 321 actual flow rate in actual operation is measured, thus verifying the operational
 322 accuracy of the liquid fertiliser variable control system. Five sets of different
 323 pressure values were set to quantify the fertiliser application system's fertiliser
 324 application accuracy under different control algorithms, five sets of actual flow
 325 data are measured and the average value was taken as the actual flow rate's
 326 measured value. The accuracy test diagram is as follows.

327 As is visible from the Fig.12- Fig. 14, three target spray volumes are set
 328 at different pressure levels, and the actual spray volumes were collected. At
 329 a theoretical fertilizer application volume of 20L, the PID control's accuracy
 330 ranged from 8.5% to 20%, the fuzzy PID control's accuracy ranged from 4.5%
 331 to 8.5%, and the accuracy of the fuzzy PID control based on PSO optimization
 332 ranged from 1% to 3.5%; at a theoretical flow rate of for a theoretical flow rate
 333 of 40L, the control accuracy of the three control algorithms that are ranged

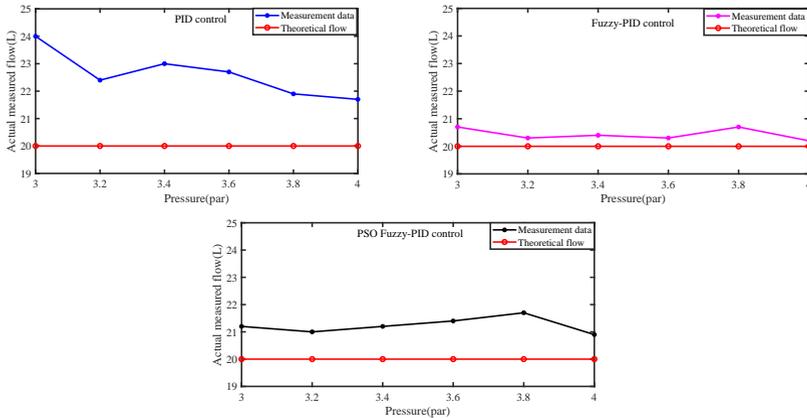


Fig. 12 Comparison of the accuracy of the three different controls at a pressure of 20 *par*.

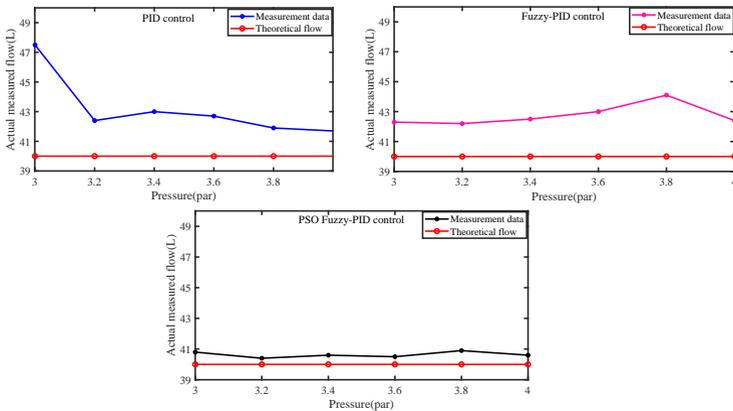


Fig. 13 Comparison of the accuracy of the three different controls at a pressure of 40 *par*.

334 from, respectively, 5.5%-10.25%, 1%-2.25% and 10%-18.75%; for a theoretical
 335 flow rate of 60L, the control accuracy of the three similarly control algorithms
 336 that are ranged from, respectively, 5.3%-8.3%, 1.25%-1.5% and 6.7%-16.7%.
 337 Regularity was not shown by the variation in accuracy at each pressure, but
 338 compared to fuzzy PID control and PID control, significant results is achieved
 339 by the control algorithms proposed in this study in flow rate's regulation at
 340 each pressure.

341 6 Conclusion

342 In this research, liquid fertilizer variable fertilizer control system's control accu-
 343 racy is studied, a control model is constructed, and the liquid fertilizer flow
 344 control under traditional PID, fuzzy PID and fuzzy PID control based on PSO

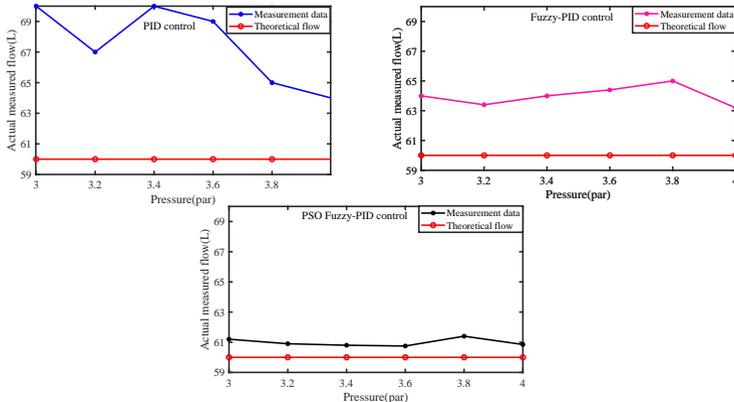


Fig. 14 Comparison of the accuracy of the three different controls at a pressure of 60 *par*.

algorithm is simulated and examined, and the following principal conclusions
 are obtained.

By constructing a mathematical model of the system, combined with MAT-
 LAB/Simulink system, PID control, fuzzy PID control and fuzzy PID control
 based on PSO optimization, the comparison consequences illustrate that PID
 control's response time is 80s with 23% overshoot, and fuzzy PID control
 division's response time is 60s with 17.1% overshoot, compared with the first two
 control algorithm, the regulation time is 30s and there is no overshoot. The
 stability and rapidity of the algorithm can be proven.

In order to verify the of algorithms, the research designs a fertiliser appli-
 cation accuracy examination, devising five fertiliser application tests under
 different pressure values, each group is brought in to verify the three algorithms
 in five measurements, and the average value is taken as the measurement data.
 The test outcomes reveal that PID control's fertiliser application accuracy is
 in adequate, causing an error of 20% and wasting water resources in practical
 applications; fuzzy PID control's accuracy fluctuates around 5%-10%, which
 is a certain improvement compared to PID control; the control algorithm pro-
 posed in this research possesses an accuracy of 3.5% apart from when the
 pressure is 4*par*, and is fundamentally controlled within 2%. It is concluded
 that the control method in this research can save water effectively in the
 fertiliser application process.

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