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1 Leveraging the polymer glass transition to access thermally- 2 switchable shear jamming suspensions

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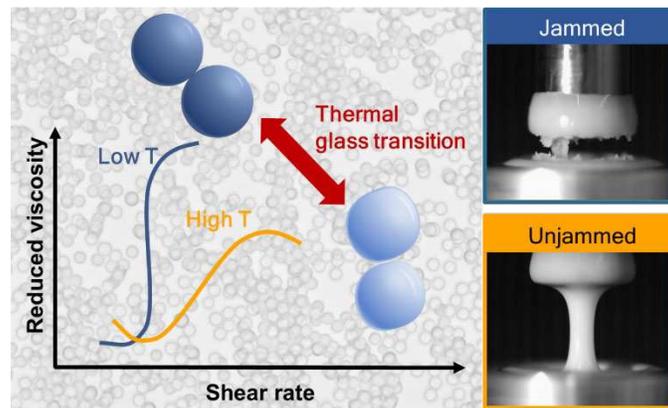
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10 **Abstract**



12 When sheared sufficiently strongly, suspensions having a large volume fraction of solid particles
13 can exhibit a dramatic increase in viscosity (shear thickening) and even solidify (shear jamming).
14 Investigations to date have almost exclusively focused on rigid, non-responsive particles, which
15 do not allow *in situ* tuning of shear thickening or jamming. Here we report suspensions of
16 polymeric micron-sized particles with accessible glass transition temperatures (T_g) designed to
17 control their non-Newtonian rheology. The underlying mechanical stiffness and interparticle
18 friction between particles change dramatically near T_g . We capitalize on these properties and
19 show that, in contrast to conventional systems, a dramatic and non-monotonic change in shear
20 thickening is observed as the suspensions transition through the particles' T_g . This behavior
21 enables the *in situ* turning on or off of shear jamming by varying the temperature relative to T_g ,
22 and lays the groundwork for thermally switchable jamming systems.

23 **Introduction**

24 Discontinuous shear thickening (DST) in dense suspensions is a phenomenon in which a sheared
25 fluid experiences a large, abrupt jump in viscosity (η), which potentially can lead to solid-like
26 shear-jamming (SJ) behavior¹⁻³. This shear-induced transformation from an easily flowing state
27 to a state of much enhanced viscosity is fully reversible, and has been leveraged in a range of
28 applications, including flexible stab-proof armor, smart speed bumps, and damping systems for
29 impact mitigation⁴⁻⁸. Although the phenomenon is well-known (e.g., corn starch and water⁹), an
30 understanding of the microscopic mechanism behind this transformation has only been
31 developed recently. Under shear, the particles (which typically occupy more than 50% of the
32 fluid volume, $\phi > 50\%$) are forced into sufficiently close proximity with neighbors that they
33 start to interact through direct frictional contacts^{1,3,10-13}, causing the emergence of an extended
34 network of frictional force chains that resist further deformation.

35 To date, most studies of suspensions exhibiting DST or SJ have been restricted to relatively
36 simple chemistries, in which the particles act as rigid, non-deformable objects in relation to the
37 applied shear stress. Typical materials for the particles include silica^{11,14}, glassy polymers like
38 poly(methyl methacrylate) (PMMA)^{6,15} or polystyrene (PS)^{16,17}, or rigid non-spherical granular
39 materials like cornstarch⁹. In such systems, key factors that determine DST and SJ include
40 applied stress (τ), volume fraction (ϕ), and interparticle friction^{3,14,15,17-23}.

41 For strong shear thickening and shear jamming, where ϕ is high and frictional contact forces are
42 crucial, recent studies have shown that the chemical composition and structure of the particle
43 surfaces can affect contact interactions and drastically influence the rheological behavior^{14,15,19,21}.
44 While these works and related studies^{12,24,25} have contributed towards a better understanding of
45 the structure-property relationship during DST and SJ, little is known about the roles of particle
46 and interfacial compliance.

47 A considerable amount of research has been aimed at characterizing polymeric interfaces,
48 including molecular mobility and friction, as a material goes through a glass transition. As a
49 polymeric material is heated above its glass transition temperature (T_g), within a span of just a
50 few degrees, molecular mobility increases by over ten orders of magnitude²⁶⁻²⁸, elastic moduli
51 drop dramatically^{28,29}, and friction exhibits a distinct temperature anomaly²⁹⁻³⁵. Building on that

52 body of work, this work considers the interplay between polymer glass formation/devitrification
53 and shear-jamming phenomena, and how that can be leveraged to arrive at suspensions with
54 adaptable shear-jamming characteristics. More specifically, we introduce a generally applicable
55 strategy that relies on design of suspensions of particles with targeted T_g , and we investigate the
56 impact of the T_g on their shear rheology. At temperatures below T_g the particles are rigid, with a
57 tensile storage modulus (E') on the order of 10^9 Pa (close to that of hard spheres). Above T_g , the
58 particles become rubbery and deformable, with E' decreasing to $\sim 10^6$ Pa. It is hypothesized that
59 such a pronounced change in stiffness around T_g will impact interparticle contact interactions and
60 force-chain rigidity, thereby providing a versatile platform for tunable shear thickening and shear
61 jamming.

62

63 **Results and Discussions**

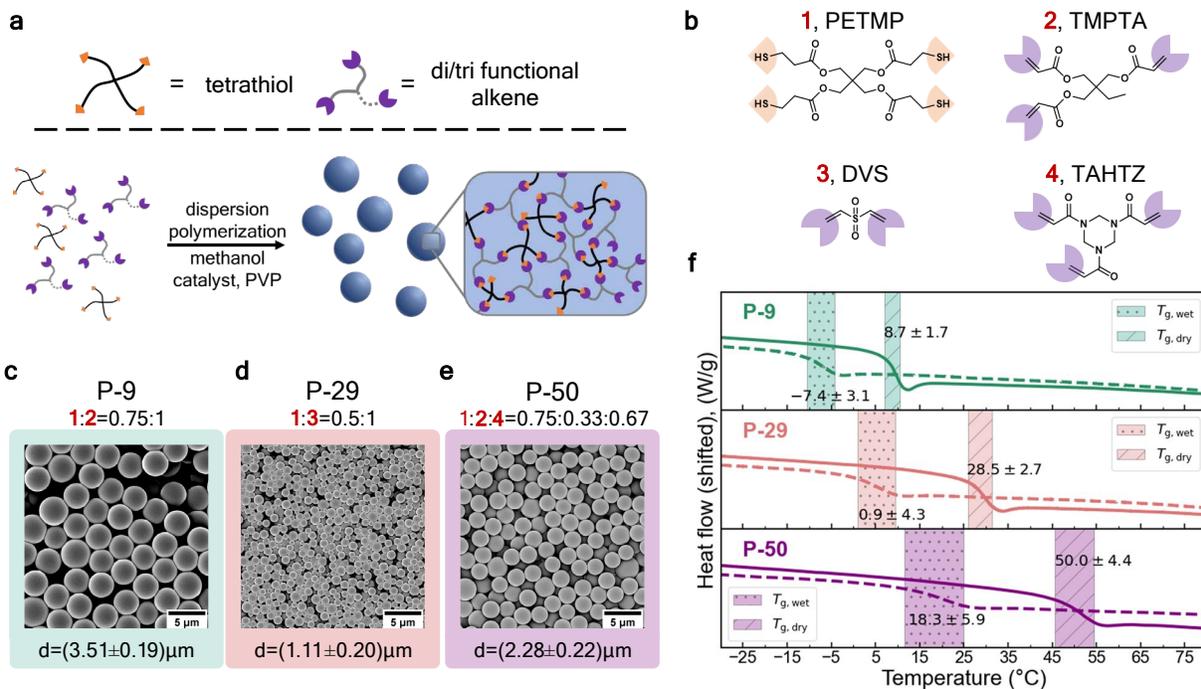
64 While there are many examples of polymeric particles reported in the dense suspension
65 literature, most are based on poly(styrene) (PS) or poly(methyl methacrylate) (PMMA), which
66 exhibit a glass transition temperature (T_g) that is well above ambient conditions ($T_g \sim 100^\circ\text{C}$) and
67 rarely accessed in rheological measurements^{6,15,16,36}. Furthermore, non-crosslinked PS or PMMA
68 particles can suffer from irreversible plastic deformations and dissolution above T_g ^{37,38}, and
69 randomly crosslinked polymers can exhibit broadened T_g 's that can be difficult to characterize³⁹⁻
70 ⁴¹. These and other features serve to underscore that studying the effect of T_g in suspension
71 rheology requires careful choice of the particles' chemistry.

72 To access a series of crosslinked particles with different and accessible T_g s, polymeric particles
73 were synthesized using thiol-Michael dispersion polymerization⁴²⁻⁴⁴ of small molecule
74 monomers (Fig. 1a,b). This technique offers several advantages: (1) the product is a polymer
75 network with high crosslinking density and minimal plastic deformation above T_g , (2) the glass
76 transition temperature range is narrow, (3) the T_g of the polymer can be precisely tuned by
77 varying the monomer structures, and (4) the reaction is facile and relatively insensitive to
78 moisture or air⁴²⁻⁴⁴. Three types of particles (referred to as **P-X**, where X is the dry T_g in $^\circ\text{C}$), **P-**
79 **9**, **P-29**, and **P-50** were synthesized by thiol-Michael dispersion polymerization at stoichiometric

80 thiol/vinyl ratio following general procedures reported by Bowman and coworkers^{42,43}. In each
81 case, a tetrathiol, pentaerythritol tetrakis(3-mercaptopropionate) (PETMP, **1**), was mixed with
82 monomer(s) containing multiple Michael acceptor functionalities, trimethylolpropane triacrylate
83 (TMPTA, **2**), divinyl sulfone (DVS, **3**), or 1,3,5-triacryloylhexahydro-1,3,5-triazine (TAHTZ, **4**),
84 at an alkene to thiol ratio of 1:1. By varying the type and ratio of the different Michael acceptor-
85 containing monomers it was possible to tailor the T_g of the particles (Fig. 1c-e). The reaction was
86 monitored by alkene/thiol conversion via FTIR spectroscopy (see Supplementary Fig. S1-S3).
87 Images from scanning electron microscopy (SEM) demonstrate that the particles were uniform in
88 size (Fig 1.c-e, and Supplementary Fig. S4).

89 To create suspensions, poly(ethylene glycol) of molecular weight 200 g/mol (PEG200) was used
90 as the carrier fluid for all the particle systems (in the case of the **P-29** particles, ~20 vol%
91 dimethyl sulfoxide was added as a cosolvent, see the Methods section for further details). The T_g
92 of the dry particles and the suspensions were determined by differential scanning calorimetry
93 (DSC) as shown in Fig. 1f. In all three cases, the T_g of the particles immersed in the carrier fluid
94 drops by 15~25°C from that of the dry particles, suggesting that the carrier fluid acts as a
95 plasticizer. Nevertheless, the particle size stays roughly the same in the dry or wet state on
96 account of their high crosslinking density (see Supplementary Fig. S5).

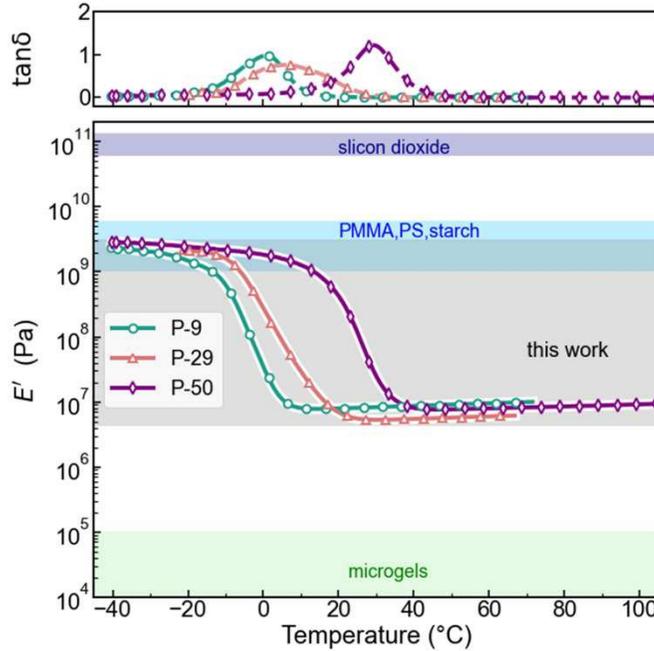
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99 **Fig. 1 | Particle synthesis scheme and characterization by SEM and DSC.** **a**, Schematic diagram of
 100 the Thiol-Michael dispersion reaction and the particle network structure. Detailed reactions and
 101 purification conditions are in the Methods section. **b**, Chemical structures of the monomers,
 102 pentaerythritol tetrakis(3-mercaptopropionate) (PETMP, **1**), trimethylolpropane triacrylate (TMPTA, **2**),
 103 divinyl sulfone (DVS, **3**), or 1,3,5-triacryloylhexahydro-1,3,5-triazine (TAHTZ, **4**), used to synthesize the
 104 different particles. **c-e**, The monomer composition and SEM micrographs of **P-9**, **P-29** and **P-50** particles,
 105 respectively. The mean size and the standard deviation are indicated below each image. **f**, DSC
 106 measurement results showing the normalized heat flow as a function of T for the dry particles (solid line)
 107 and particles suspended in their respective carrier fluid at around 56wt% (dashed lines). Shaded areas
 108 with (.) and (/) indicate the wet and dry T_g respectively. The first number is the half-height midpoint of
 109 the glass transition (T_g) range. The second value is the width of the T_g range.

110

111 As the thermomechanical properties of these networks represent a critical aspect of this work, we
 112 evaluated them by preparing **P-9**, **P-29** and **P-50** films, which were characterized by dynamic
 113 mechanical analysis (DMA) in both the dry (see Supplementary Fig. S6-S7) and carrier-fluid-
 114 swollen state (Fig. 2) for a better representation of the suspension environment. Consistent with
 115 the literature^{42,43}, the polymer networks synthesized using this chemistry exhibit a relatively
 116 narrow glass transition window. The thermomechanical T_g of the materials, designated by the
 117 peak in $\tan\delta$, are comparable to the DSC measurements (Fig. 1f) for the dry and immersed film
 118 (see Supplementary Fig. S6-S7). Importantly for these studies, the tensile storage modulus (E')
 119 changes by three orders of magnitude, from around 10^9Pa in the glassy state to 10^6Pa in the
 120 rubbery state for all three materials.



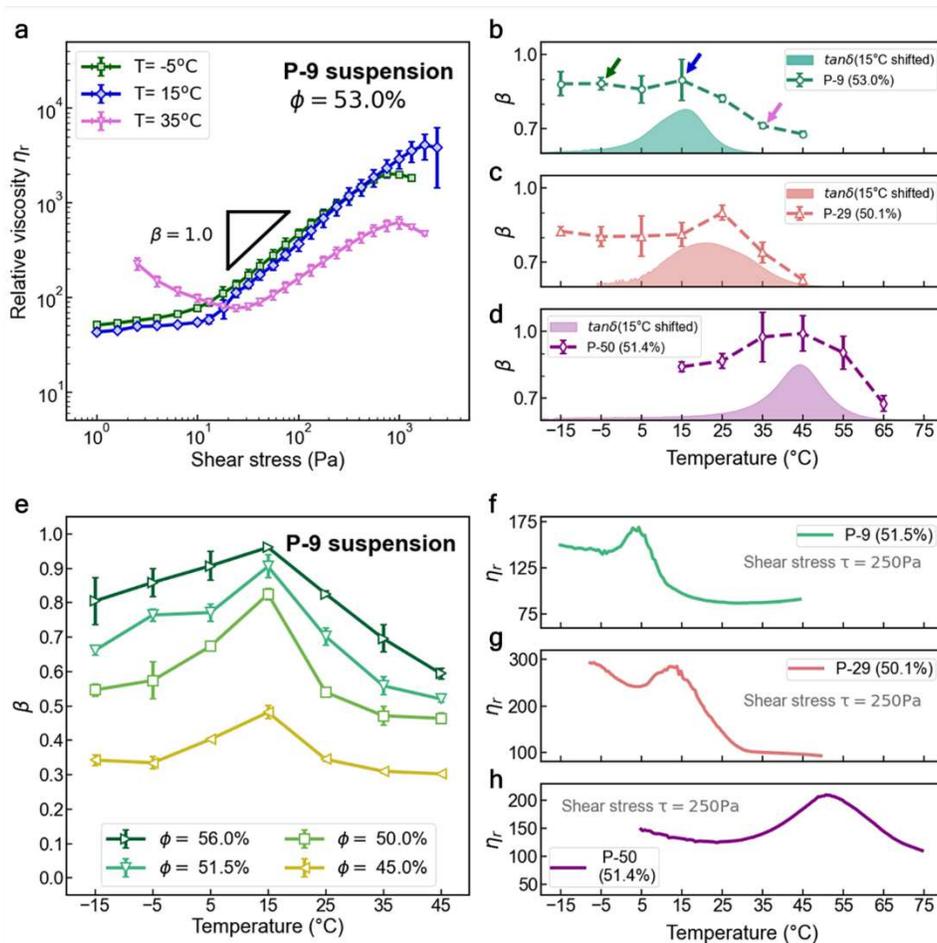
122 **Fig. 2| Mechanical stiffness characterization via DMA.** The storage modulus (E') and $\tan\delta = E''/E'$
 123 of the carrier fluid-swollen **P-9**, **P-29** and **P-50** polymer films were measured in an immersion setup,
 124 using an oscillation frequency of $f = 1\text{ Hz}$. See Supplementary Fig. S6 for plots including loss modulus
 125 (E''). Thermomechanical T_g is designated by the peak in $\tan\delta$. The values of E' for several other particle
 126 materials are indicated for comparison^{45–48}, PMMA: Poly (methyl methacrylate) and PS: polystyrene.

127

128 To examine the effect of temperature (T) on rheology, steady-state flow curves for particle
 129 suspensions with fixed particle volume fraction were measured at different temperatures as a
 130 function of stress (τ). The suspension viscosity η can be normalized by the viscosity $\eta_0(T)$ of
 131 the Newtonian carrier fluid to define a relative viscosity $\eta_r = \eta/\eta_0(T)$ (see Supplementary Fig.
 132 S8). Critically, the strength of shear thickening can be parameterized by the power law exponent
 133 β ($\eta_r \propto \tau^\beta$), which represents the slope of the curve during the shear thickening regime on a log-
 134 log plot, with $\beta = 0$ corresponding to a Newtonian fluid; and $\beta = 1.0$ signaling the occurrence
 135 of discontinuous shear thickening (DST), which is a precursor of shear jamming in steady-state
 136 rheological measurements^{1,9,24}.

137 In typical suspensions of hard spheres, such as silica particles, the η_r vs τ curves are independent
 138 of temperature, and for a given packing fraction β is roughly constant (with an estimated decline
 139 of less than 0.03 per 10°C)^{11,49}. In contrast to the behavior of these traditional suspensions, we
 140 find that the **P-9** particle suspension shows a strong sensitivity to temperature, as demonstrated

141 in Fig. 3a, where η_r for a volume fraction of $\phi = 53\%$ shows a significant change in shear
 142 thickening strength as T is varied from -15°C to 45°C . Here, a strong, nearly discontinuous
 143 thickening with $\beta \approx 0.9$ was observed below 15°C . This should be contrasted with
 144 measurements at higher temperatures, for example 35°C and 45°C , where the suspension shows
 145 comparatively mild thickening ($\beta < 0.7$) (Fig. 3b and Supplementary Fig. S9a). This change in
 146 β over a temperature range of $\sim 20^\circ\text{C}$ suggests that control of shear thickening should be possible
 147 simply by modulating temperature, thereby providing new avenues for engineering responsive
 148 fluids or for facilitating suspension processing.



150 **Fig. 3 | Dependence of rheological behavior on temperature.** **a**, Stress-controlled steady-state
 151 rheometry data for the **P-9** suspension with $\phi = 53.0$ vol% at -5°C (green), 15°C (blue) and 35°C (pink),
 152 demonstrating that the strength of shear thickening is highly temperature dependent. The black line has a
 153 slope of 1 corresponding to DST where the shear rate is constant. A plot of η_r vs shear rate can be found
 154 in the Supplementary Fig. S9. **b-d**, β as a function of 53.0% **P-9** suspension, 50.1% **P-29** suspension,
 155 51.4% **P-50** suspension. See Supplementary Fig. S9 for the flow curves. Shaded areas indicate the $\tan\delta$
 156 results from Fig. 2, here shifted up by 15°C . Arrows in **b** indicate β for the conditions measured in **a**. **e**,
 157 Plots of the shear thickening exponent β ($\eta_r \propto \tau^\beta$) as a function of temperature for all seven packing

158 fractions of **P-9** suspensions. See Supplementary Fig. S10 for the flow curve. Error bars represent the
159 standard deviation from three or more replicate measurements in **a-e. f-h**, Reduced viscosity η_r measured
160 as a function of temperature for 51.5% **P-9** suspension, 50.1% **P-29** suspension, 51.4% **P-50** suspension
161 at a shear stress of 250 Pa. Plots of η vs T for the cooling and heating steps can be found in
162 Supplementary Fig. S12.
163

164 To test whether this phenomenon is indeed related to the particles' T_g , further experiments were
165 carried out on suspensions of **P-29** and **P-50**. While the three types of particles have different
166 sizes (ranging from ca. 1 to 3.5 μm), the effect of particle size is well understood, and has been
167 shown to mainly affect the onset shear stress of thickening, but not the trend in β ^{3,50}. For these
168 higher T_g suspensions, the non-monotonic behavior in β is found to be similar for all particle
169 compositions. The peak, however, is shifted to higher temperatures, consistent with the changes
170 in T_g (Fig. 3b-d, see Supplementary Fig. S9 for the flow curves). Critically, in all three cases the
171 peak in β can be well aligned with $\tan\delta$ in Fig. 2 when the latter is shifted by the same amount
172 $\Delta T = 15^\circ\text{C}$, suggesting that the temperature dependence is directly related to the thermal glass
173 transition of the particles. An offset ΔT is consistent with literature data, where polymer
174 interfaces under confinement and, in particular, for different deformation rates, can exhibit
175 dynamics different from the bulk^{28,51}. This result motivates further research to quantify how
176 polymer stress relaxation at the interface can influence the constraints on particle relative
177 motions³. For the three materials considered here, the fact that the maximum observed β strongly
178 tracks with T_g offers a general, yet simple approach for controlling the shear thickening
179 characteristics of dense suspensions by simply tuning the T_g of the particles.

180 To explore how β vs. T varies for different volume fraction (ϕ), detailed studies were carried out
181 using **P-9** suspensions at four additional ϕ values that span weak to strong shear thickening
182 regimes (see Fig.3 e and Supplementary Fig. S10). In all cases, β is a non-monotonic function of
183 T , with a peak near 15°C for all volume fractions studied (Fig. 3e). Above 15°C , β drops
184 significantly as the temperature increases. At 45°C , β is smaller than 0.7 even at highest ϕ
185 studied, implying that DST has been suppressed. At this temperature, the elastic modulus is
186 around 3 orders of magnitude smaller than in the glassy state. In this rubbery regime, the
187 deformation caused by typical interparticle stress in shear experiments is estimated to be around
188 1~3% of the particle radius (see Supplementary Fig.S11 for experimental evidence of
189 deformability and additional calculation details). Although this number appears small in

190 magnitude, it is about 100 times larger compared to the deformation in the glassy state and may
191 affect the constraints on particle motions. We therefore speculate that the change in
192 deformability may lead to the observed attenuation in shear thickening at temperatures much
193 above T_g : as temperature increases, the particle surfaces become more compliant, discouraging
194 the formation of sample spanning rigid force chains under shear^{13,52}.

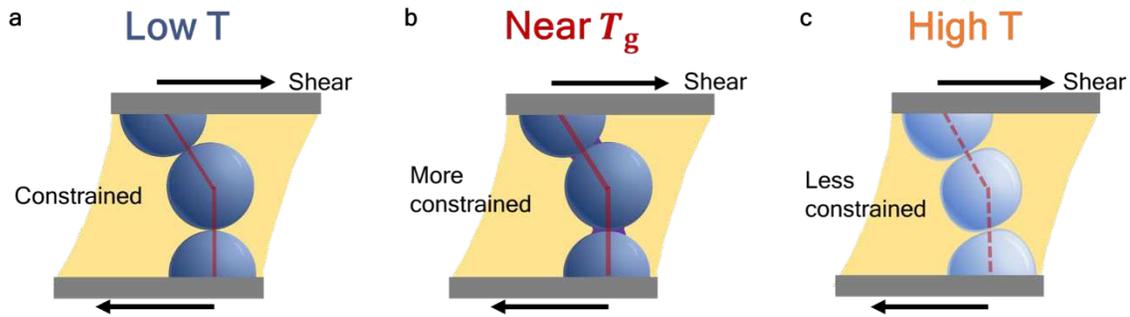
195 As an alternative to measuring β vs T , a common way to probe molecular dynamics in polymer
196 and molecular glass transition is to investigate how viscosity varies with temperature for a given
197 stress⁵³. A temperature ramp experiment under constant shear stress ($\tau = 250\text{Pa}$, heating/cooling
198 rate = $1.5^\circ\text{C}/\text{min}$) was conducted for **P-9**, **P-29** and **P-50** suspensions (Fig. 3f-h and
199 Supplementary Fig. S12). In all cases, particle volume fraction was held at $\phi \sim 50\%$, since
200 intermediate ϕ shows the most prominent peak in β in Fig. 3e. To normalize the temperature
201 dependency of carrier fluid viscosity (η_0), $\eta_r = \eta / \eta_0(T)$ is shown in Fig. 3f-h. The relative
202 viscosity η_r can be regarded as a measure of the additional resistance due to the presence of the
203 particles. For conventional hard sphere suspensions, the curve is expected to be approximately
204 flat with a slight decreasing trend with temperature^{11,49}. For all systems measured in this study, it
205 was found that the relative viscosity of the suspension clearly shows a local peak near each
206 particle's T_g , which further supports that the maximal shear thickening occurs around the glass
207 transition. Interestingly, the observed behavior in viscosity bears similarities to studies of
208 polymer dispersions that undergo microphase separation, such as in block copolymer solutions⁵⁴
209 and polymers around their lower critical solubility temperature (LCST)⁵⁵. In those studies, a peak
210 in η is observed at a temperature where the conformation of polymer chain is changing. Here, the
211 peak in η_r suggests maximal constraints on the suspension flow. It is worth noting that this peak
212 can be observed in both heating and cooling experiments (Supplementary Fig. S12), implying
213 reversibility in the interactions induced by T_g .

214 The observed non-monotonicity leads us to consider other effects of temperature on the
215 suspension. First, the thermal expansion coefficients (α) of the particle materials was evaluated
216 since if ϕ increases significantly near T_g then β should also increase^{11,24}. However, it was found
217 that α of the particles is comparable to that of the carrier fluid (see Supplementary Fig. S13). For
218 all suspensions, the calculated drift in ϕ is minimal ($\Delta\phi < 0.05\%$ for changing T by 10°C) and
219 therefore unlikely to be the main cause of the peak in β (see Supplementary Fig. S14).

220 Surface friction, which is of vital importance for constraining particle motion, is also extremely
221 sensitive to temperature in the vicinity of T_g ²⁹⁻³⁵. Different from hard surfaces, friction between
222 polymer surfaces originates from dissipative interactions of interdigitating chains^{30,31,33,35} .
223 Around T_g , adhesive interactions increase on account of an increase in true contact area, which
224 may lead to stronger cohesive ‘sticky’ forces and enhanced rolling friction^{21,31,32}. On account of
225 the viscoelastic nature of the interface between two particles sheared into contact, the friction
226 coefficient (μ) can either increase monotonically with T at moderate to high surface deformation
227 rates, or show a peak if the deformation rate is slow enough to cross over into the time scale of
228 surface relaxation³²⁻³⁵. In relation to shear thickening, simulations have shown that both higher
229 friction coefficients μ or the introduction of rolling friction could lead to more pronounced shear
230 thickening and larger β ¹².

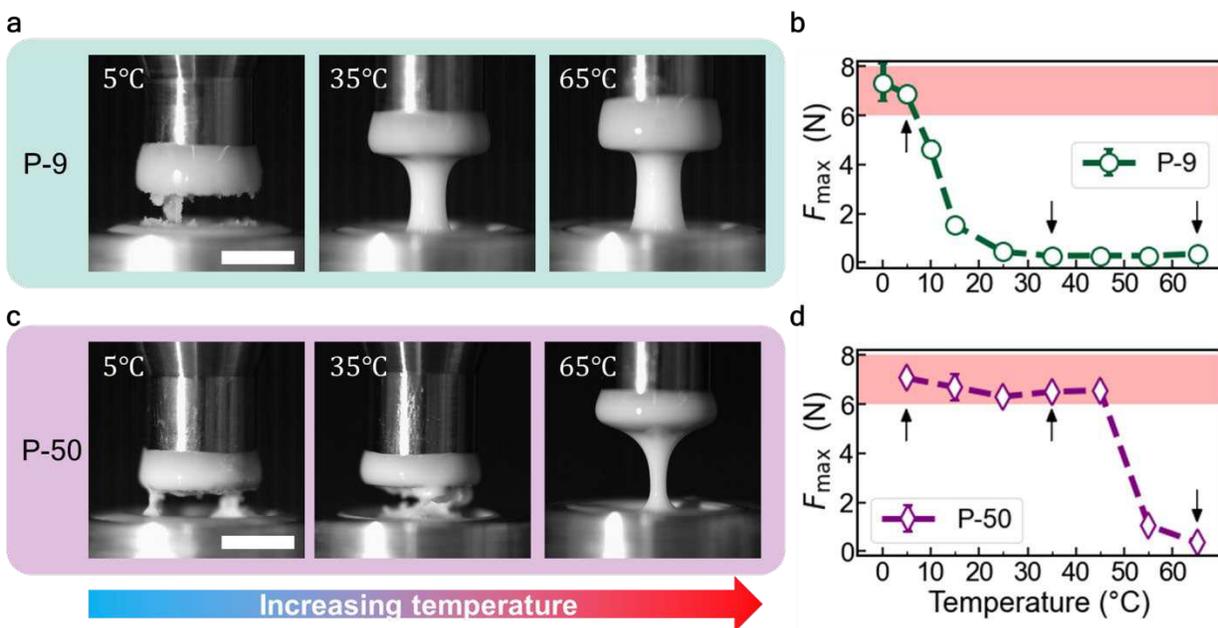
231 We suggest that the non-monotonic trend in the strength of shear thickening with temperature
232 (Fig. 3b-h) results either from a non-monotonic μ or from a competition between increasing μ
233 and decreasing mechanical stiffness. In both scenarios, shear thickening is most pronounced
234 when relative particle movement is most constrained. A proposed temperature dependency
235 mechanism is shown in Fig. 4.

236 It is worthwhile to consider the findings reported here in the context of devitrification, to results
237 from a different strategy by Hsu et al.²¹, in which polymers that can undergo a lower critical
238 solution temperature (LCST) transition²¹ were grafted onto hard silica particles. These authors
239 also report that adhesion and friction forces can be tuned as a function of temperature, thereby
240 influencing shear thickening. In our particles, the variation of apparent stiffness with temperature
241 is opposite to the effects of an LCST transition, and the non-monotonic trend in β suggests
242 previously unconsidered effects of surface deformability in addition to the effects related to μ .
243 Unlike the LCST transition, where the carrier fluid is limited to water and ionic liquids⁵⁶, a
244 strategy relying on T_g is potentially applicable to any carrier fluid.



246 **Fig. 4| Illustration of the proposed temperature dependency mechanism.** **a**, Below T_g , the particles
 247 are glassy and non-deformably. **b**, The particles exhibit maximum constraints near T_g due to greater
 248 frictional interactions between the polymer particles. **c**, At temperatures high above T_g surface
 249 deformability dominates and the particles are less constrained. The deformations are small, as estimated
 250 from contact mechanics calculations (Supplementary materials and Fig. S11), and they are exaggerated in
 251 this illustration for visual clarity.
 252

253 Finally, it is important to recall that suspensions that undergo strong or even discontinuous shear
 254 thickening in a steady-state rheological measurement may not exhibit shear jamming^{9,15}. To
 255 directly assess if our design strategy based on T_g can be used for switching shear jamming on or
 256 off at different temperatures, pull tests^{15,57} were carried out using the **P-9** and **P-50** suspensions.
 257 In these experiments, a cylindrical rod, initially immersed in the suspension, is pulled out
 258 vertically at a fixed rate, in our case 8mm/s. At 5°C, the **P-9** suspension shows a rough cleavage
 259 plane, indicating brittle fracture associated with the solid-like behavior of shear-jammed fluids.
 260 In contrast, at 35°C and 65°C, the **P-9** suspension exhibits a neck and pinch-off detachment
 261 which is characteristic of a liquid-like response (Fig. 5a). The transition between these two types
 262 of behavior is also reflected in the maximum normal force F_{max} during the deformation, which
 263 shows a sharp decrease near 10°C for the **P-9** system (Fig. 5b, see Supplementary Fig. S15 for
 264 the raw force curves). In contrast, **P-50** system shows brittle fracture and large F_{max} all the way
 265 up to 45°C, with liquid-like response occurring only above 45°C (Fig. 5c and Fig. 5d). This clear
 266 dependency on T_g demonstrates how the shear jamming response can be tailored by changing the
 267 T_g of the particles.



269 **Fig. 5| Tensile testing for shear jamming at varying temperatures.** **a** and **c**, Images of the suspensions
 270 under extensional deformation taken at $T = 5^{\circ}\text{C}$, 35°C and 65°C for **P-9** and **P-50** suspensions ($\phi =$
 271 56.0%). The pulling rate is 8 mm/s . The scale bar indicates 5 mm . **b** and **d**, The maximum normal force
 272 (F_{\max}) as a function of temperature. Shaded areas in red indicate large peak normal forces associated with
 273 shear jamming. The arrows indicate temperatures corresponding to the snapshots in **a** and **c**. Error bars
 274 represent the standard deviation of three replicate measurements. See Supplementary Fig. S15 for
 275 representative raw force traces.

276
 277

278 **Concluding remarks**

279 In this study, we have demonstrated that a pronounced temperature dependence of the strength of
 280 shear thickening in suspensions of polymer microparticles can be achieved by leveraging their
 281 glass transition temperature. Most strikingly, the suspensions exhibit maximum shear thickening
 282 near T_g , which is attributed to enhanced frictional interactions between the polymer particles
 283 sheared into contact. At temperatures above T_g , the particle surfaces become more deformable
 284 and do not constrain relative particle movement as strongly. This directly impacts force chain
 285 formation and, macroscopically, the resistance to flow as measured by the suspension viscosity
 286 (Fig. 4).

287 In recent years, there has been a growing interest in designing shear thickening fluids (STFs) for
 288 targeted material applications. Here we have shown how the thermal glass transition in polymers
 289 can be used in these efforts. Since T_g affords wide tunability by altering the chemical structure of

290 the polymer, we believe that this work provides a versatile platform for engineering STFs with
291 tailored mechanical performance.

292 From a theoretical perspective, this work raises many exciting questions that warrant deeper
293 investigation. For example, the contact mechanics at a polymer-polymer interface are
294 fundamentally different from those at conventional rigid particle surfaces. It remains to be seen
295 how the interfacial polymer dynamics (i.e., various relaxation times at various length scales)
296 affect the formation and destruction of inter-particle force chains. Conversely, given that DST
297 and SJ are exquisitely sensitive to the strength of particle-particle contact interactions, dense
298 suspension rheology provides a powerful lens with which to observe macroscale consequences
299 that are a direct result of interfacial polymer dynamics at molecular length and time scales.

300

301 **Materials and Methods**

302 **Materials.** Pentaerythritol tetrakis(3-mercaptopropionate) (PETMP) (>95.0%, Sigma-Aldrich),
303 trimethylolpropane triacrylate (TMPTA) (>90%, Sigma-Aldrich), 1,3,5-triacryloylhexahydro-
304 1,3,5-triazine (TAHTZ, Sigma-Aldrich), divinyl sulfone (>96.0%, TCI America), hexylamine
305 (HEA) (>99.0%, Sigma-Aldrich) and triethylamine (TEA) (>99.5%, Sigma-Aldrich),
306 polyvinylpyrrolidone with average molecular weight 40,000 (PVP) (Sigma Aldrich) were used as
307 received for reactions. Polyethylene glycol with average molecular weight 200 (PEG200) (Sigma
308 Aldrich) and dimethyl sulfoxide (DMSO) (>99.9%, Sigma-Aldrich) were used as received for
309 dispersing the particles. Solvents including methanol, acetonitrile were purchased from Sigma-
310 Aldrich and used as received. PPP-LFMR silicon probes were purchased from Asylum Oxford
311 Instruments.

312 **Synthesis of P-9 particles.** P-9 particles were synthesized via dispersion polymerization following
313 literature procedures. Monomers 5.93 g (20 mmol) of TMPTA and 7.33g (15 mmol) of PETMP
314 were dissolved in 270mL methanol. 3.0g of PVP was dissolved in 30mL methanol and transferred
315 to the reaction ask. The mixture of monomers and surfactant was stirred at 400rpm using a
316 mechanical stir. The reaction was started by adding in the base catalyst hexylamine (0.21g, 1.6wt%
317 relative to monomers) which was diluted by 10 times beforehand in methanol. The reaction was
318 carried out for 4 hours at ambient conditions. The base was neutralized by 1M HCl aqueous

319 solution prior to centrifugation. The dispersion was centrifuged at 1750 m/s² for 6 minutes and the
320 supernatant was thrown away. To remove the surfactants and catalyst, the particles were washed
321 in methanol at a concentration of around 0.04 g/mL under sonication and vortexing, followed by
322 centrifugation. This washing process was repeated for 3 times. The particles are dried at 0.2 torr
323 for 48 hours and kept in a desiccator before use. The second batch which was used for OM
324 measurement had a smaller particle size distribution averaged around 3.1 μ m. For synthesizing the
325 **P-9** particles of 2.5 μ m used for the temperature ramp experiments, triethylamine (4.0wt% relative
326 to monomers) was used instead.

327 **Synthesis of P-29 particles.** **P-29** particles were synthesized via dispersion polymerization with
328 the same procedure as the **P-9** particles with catalyst hexylamine (0.17g, 1.6wt% relative to
329 monomers). Monomers were changed to 3.54g (30 mmol) of DVS and 7.33g (15 mmol) of PETMP.

330 **Synthesis of P-50 particles.** **P-50** particles were synthesized via dispersion polymerization with
331 procedure similar to the **P-9** particles. The molar ratio of TMPTA to TAHTZ was kept 1:2.
332 Specifically, 1.98g (6.67 mmol) of TMPTA, 3.32g (13.33 mmol) of TAHTZ and 7.33g (15 mmol)
333 PETMP was used. Due to the low solubility of TAHTZ monomer at room temperature, the solvent
334 was preheated to 40°C and the monomer was sonicated with the solvent for 1 minute. 0.50g of
335 triethylamine was used as catalyst (4.0wt% relative to the monomers). The rest of the procedures
336 were identical to the synthesis of the **P-9** particles.

337 **Scanning electron microscopy.** The particles were solvent casted with methanol on silicon wafers
338 and dried in air. Before the SEM analysis, the particles were sputter coated with a 8 nm film of
339 Pt/Pd metal to enhance electron conductivity. The images were recorded on a Merlin SEM (Carl
340 Zeiss) at a voltage 1.5 kV using Inlens detectors and each image was averaged between 8-15
341 images. Particle sizes were analyzed with ImageJ.

342 **Optical microscopy.** OM images were taken with an optical microscope (Leica DM2700P) using
343 a 50x objective under transmission mode. Particle suspensions were confined in a channel of
344 around 50 μ m to avoid compression from the cover slip.

345 **Suspension preparation.** Dried particles were dispersed in carrier fluid at certain weight
346 percentages. The weight concentration is converted to volume concentration by the densities of
347 the polymer and the fluid. The mixture was stirred extensively and sonicated for 1 hour. For **P-9**

348 and P-50 particles, PEG200 was used as the carrier fluid. For **P-29** particles, a mixture containing
349 80vol% PEG200, 20vol% DMSO and 0.5 wt% NaCl was used to disperse the particles and screen
350 electrostatic interactions.

351 **Polymer film synthesis.** Monomers were dissolved in acetonitrile at 30 wt% concentration.
352 Triethylamine was added as a catalyst at a concentration of 0.6 wt% relative to the monomers.
353 After mixing, the solution was immediately injected between two glass slides separated by 1mm
354 spacer. The reaction was carried out overnight in solvent atmosphere. To remove the catalyst, the
355 film was washed with methanol and acetone alternately for 4 times. To evaporate the solvent, the
356 film was put in a vacuum oven at 2 torr and heated at 80 °C for 12 hours and then at 120°C for 4
357 hours. The catalyst concentration for the **P-29** film was reduced by half to counteract the higher
358 reactivity of the DVS monomer. The film sample for AFM measurement was cured with one side
359 facing a silicon wafer to ensure that it is smooth.

360 **Density determination.** A piece of polymer film was first immersed in water at 25 °C. 40 wt%
361 NaBr solution was added until the film was exactly levitated. The density of the NaBr solution
362 was then determined by a densimeter (DMA 4500 M, Anton Paar) and designated as the density
363 of the polymer.

364 **FT-IR spectra.** Shimadzu IRTracer-100 FT-IR with ATR diamond was used to characterize **P-9**,
365 **P-29** and **P-50** particles. Reduction of the thiol peak near 2550 cm^{-1} and the alkene peak near 800
366 cm^{-1} were used to monitor the reaction.

367 **DSC measurements.** DSC was performed with Discovery 2500 Differential Scanning
368 Calorimeter. 5-10 mg of sample were prepared in aluminum hermetic pans from TA. Typical tests
369 consist of a heat-cool-heat cycle (-40°C to 120°C) at a rate of 5 °C/min.

370 **DMA measurements.** Tests were conducted on a RSA-G2 dynamic mechanical analyzer (TA
371 Instruments) equipped with Forced Convection oven (20 °C —~500 °C) attached to an Air Chiller
372 System (-120°C ~20 °C). Samples with thickness of around 0.7 mm were prepared following the
373 method described above and measured under tensile mode. The temperature was ramped at
374 1.5 °C/min and the oscillatory frequency used was 1 Hz. For measuring the plasticized films, the
375 films were soaked in their respective carrier fluid at 20 °C above T_g for 10 days and the
376 measurement was done while immersed in the carrier fluid. For determination of the thermal

377 expansion coefficients, a constant force 0.1 N was maintained using the isoforce mode and the
378 length (L) change with temperature (T) was recorded. The linear thermal expansion coefficients
379 were extracted by linear fitting to $\ln L$ v.s. T . $\alpha = 1/L \times d(L)/d(T) = d(\ln L)/d(T)$ in the glassy
380 and rubbery regime.

381 **Shear rheometry measurements.** Rheological characterization was performed using an ARES-
382 G2 shear rheometer (TA Instruments) equipped with Forced Convection oven (20 °C ~500 °C)
383 attached to an Air Chiller System (-120°C ~20 °C). All the rheometry data were acquired with
384 25 mm parallel plates. Change of the gap size due to temperature was calibrated beforehand. The
385 suspension was loaded to the rheometer and extra fluid was trimmed at a gap size of 255 μ m. The
386 measurement gap size was maintained 240 μ m throughout the measurement. Temperature was
387 equilibrated for 10 minutes before each measurement followed by a preshearing step at a stress
388 around 2 times of the onset shear stress for 2 minutes. At each stress value, the fluid was
389 equilibrated for a minimum of 30 seconds and averaged over 15 seconds. The first point after
390 preshear was at least equilibrated for 105 seconds and averaged over 15 seconds. Stress controlled
391 measurements were done by looping a series of creep tests on the ARES-G2 rheometer.
392 Temperature ramp experiments were carried out at a ramp rate of 1.5°C/min for both heating and
393 cooling.

394 **Pull tests.** MCR302 rheometer (Anton Paar) was used to measure the pull force following
395 literature procedures¹⁵. A cylindrical metal cup with 2mm depth and 10mm in diameter was fixed
396 to the bottom plate to contain the suspension. An 8 mm (diameter) rod that was partially embedded
397 to a depth of 1mm in the sample surface and withdrawn at a speed of 8mm/s. Simultaneously, the
398 normal force response on the rod was recorded. Videos were taken with a high-speed camera.

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410 **Author contributions**

411 Chuqiao Chen, Dr. Abhinendra Singh and Dr. Neil Dolinski designed the experiments. Chuqiao
412 Chen and Michael van de Naald collected the data. Chuqiao Chen, Dr. Abhinendra Singh and Dr.
413 Grayson Jackson conceived and performed the data analysis. Dr. Heinrich M. Jaeger, Dr. Stuart
414 J. Rowan and Dr. Juan J. de Pablo supervised the whole project and provided academic advice.
415 All the authors contributed to the drafting process.

416 **Competing interests**

417 The authors have no competing/conflicting interests to declare.

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