

Study of The Effect of pH on The Performance of Microbial Fuel Cell for Generation of Bioelectricity

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Research

Keywords: Microbial fuel cell, Bioelectricity, Current density, Power density, Wastewater

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Study of the effect of pH on the performance of microbial fuel cell for generation of bioelectricity

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Abstract

Background: Day by day microbial fuel cell (MFC) technology is becoming a thought-provoking topic to the researcher because for its simultaneous utilization e.g. electricity production and wastewater treatment. Since wastewater is an important source of electrolyte for MFC, the key tenacity of this study was to investigate the outcome of pH happening various (Municipal, Bhairab river and Hospital) wastewaters used as electrolyte in dual chamber MFC.

Findings: The lab-scale experiment was conducted in batch mode, where zinc plate ($0.0027m^2$) as anode and copper plate ($0.0027m^2$) as cathode. In this study a single electrolyte (any one of earlier mentioned three electrolytes) was used in five dual-chambers MFC where the pH of the electrolyte was 6, 7, 8, 9 and 10. The MFC was worked on a temperature ranged from $27^{\circ}C$ to $34^{\circ}C$. Maximum outputs were found in terms of current density ($1288.9mA m^{-2}$), voltage (1132 mV) and power density ($1459.02 mW m^{-2}$) were

26 obtained at pH 8 by using Bhairab river water as an electrolyte in MFC chamber. A
27 substantial amount of COD removal (94%) was also achieved in the same MFC chamber at
28 the same pH (i.e. pH 8). However, the optimum operating pH for MFC containing municipal
29 wastewater and hospital wastewater was found to be 8 and 9, respectively.

30 **Conclusion:** The results suggest that various wastewaters may act as feasible feedstocks for
31 bioelectricity generation in MFC. The results also show that COD can be removed from
32 wastewater that suggest a treatment possibility of wastewater .

33

34 **Keywords:** Microbial fuel cell, Bioelectricity, Current density, Power density, Wastewater.

35

36 **Introduction**

37 In contemporary years, utilization of energy in the whole world has been increased
38 enormously (Rahimnejad et al. 2015). Energy comes from various sources such as renewable
39 as well as non-renewable. All non-renewable (fossil) based energy has a negative impact on
40 environment by producing greenhouse gases (Feng et al. 2018). However, for the sake of
41 adversative effect (global heating and contamination) on the environment, the accumulation
42 of fossil energies as a vigor source desires to be abridged (Slate et al. 2019). Considering cost
43 effectiveness and environmental problems, an environmental friendly renewable energy
44 source is very urgent. Microbial fuel cell is imminent system, which provides a potential
45 renewable energy source that might help achieving energy security. MFC can produce energy
46 (electricity) by decomposing the carbon-based substance existing in the electrolyte whereas
47 various wastewaters as well as industrial effluents can be used. Since effluents and
48 wastewaters are causing environmental pollution very much, their treatment is required
49 indeed to improve the environmental condition from pollution. Apart from the classical
50 wastewater treatment, MFC is reported to be used for wastewater management (Gotovtsev et

51 al. 2016). In developed countries 1-3% electricity for domestic consumption comes from
52 sewage wastewater treatment plants (Maktabifard et al. 2018). At a same time MFC generate
53 electricity and treat wastewater too (Mustakeem 2015; Dong et al. 2015). Variety of
54 knowledge from engineering, biology and chemistry is required for the assembly and finest
55 procedure of microbial fuel cells (Mansoorian et al. 2014; Rajeswari et al. 2016). The most
56 three key materials of MFC are electrode, membrane, and electrolyte which, determine the
57 performance of the MFCs. In MFC bio-electrochemical both half-cell reactions occurs on the
58 outward of the anode and cathode. However, better yield optimization and improvement of
59 electrode of MFC are still thought-provoking research topic worldwide (Li et al. 2017). Ion
60 exchange membrane (IEMs) particular cation exchange membrane (CEM) is very effective
61 on large-scale with greater depth of electrolyte (Ge and He 2016; Liang et al. 2018). Though,
62 the MFC can extravagances numerous cations, such for example Na^+ , Ca^{2+} , K^+ , and NH_4^+
63 present in the electrolyte (wastewater), which contest by protons that attribute to the minus
64 charged functional groups in the CEM (Rozendal et al. 2006), which can reduce in electrical
65 energy creation subsequently long-standing process (Ge and He 2016; Liang et al. 2018).
66 Bacteria can help to increase the output of MFC and reject mediator from anode chamber
67 (Reshetilov et al. 2017). Literature shows that, electrolytes like chemical based industrial
68 wastewater (Venkata Mohan et al. 2008), dairy wastewater (Porwal et al. 2015), soak liquor
69 (Sawasdee and Pisutpaisal 2016), dye factory wastewater (Kalathil et al. 2012; Patade et al.
70 2016), starch treating wastewater (Quan et al. 2014), leachate (Damiano et al. 2014), sugar
71 mill sewage (Kumar et al. 2016), Domestic wastewater (Asai et al. 2017), Poultry dropping
72 wastewater (Oyiwona et al. 2018), rice bran (Takahashi et al. 2016) beside through new
73 spreads in the usage of various substrates (Pandey et al. 2016) can be treated by MFC.
74 Beside wastewater MFC can usage clean mixtures such as acetate or butyrate (Hidalgo et al.
75 2016), alcohol, fatty acid, monosaccharide sugar (Asensio et al. 2016), sucrose and glucose as

76 electrolyte. To improve the output of MFC, recently researchers did several studies to the
77 practice of MFC through membrane (Ghasemi et al. 2015), short of membrane (Logan et al.
78 2007), using moderator, short of moderator (Sevda and Sreekrishnan 2012) also using bio-
79 cathodes (Gonzalez del Campo et al. 2014). Various operating parameters such as pH (Jadhav
80 and Ghangrekar 2009), anode and cathode ingredients (Scott et al. 2008), the space among
81 the electrodes (Hong et al. 2009a), external resistance (Hong et al. 2009a), temperature (Hong
82 et al. 2009a), conductivity (Hong et al. 2009b), also carbon-based substance of the deposit
83 (Wang et al. 2012) distresses the generated outputs of the microbial fuel cell.

84

85 The foremost interest of our experiment is to examine the effect of initial pH of various
86 wastewaters obtained from Jashore on the output of MFC and to find the most favorable
87 value of pH at which the system works best. To achieve that several experiments on
88 municipal wastewater, bhairab river water and hospital wastewater were conducted by using
89 zinc plate as anode, copper plate as cathode, and salt bridge as proton exchange membrane.

90

91 **Materials and Methods**

92 In this section, design and construction procedures of MFC are discussed with detailed
93 description of construction materials. The reactor configuration and operation of the whole
94 processes (micro-organism inoculation, electrolyte collection, salt bridge and electrode
95 preparation, data collection and performance analysis) are also discussed.

96

97 **Materials collection and cell construction**

98 Various materials were used for this research work. Each material has its specific function.
99 However, the coordinated function of these materials is to construct microbial fuel cell and to

100 operate it optimally. The name and its operation of the used ingredients are given in the [Table](#)
101 [1](#).

102

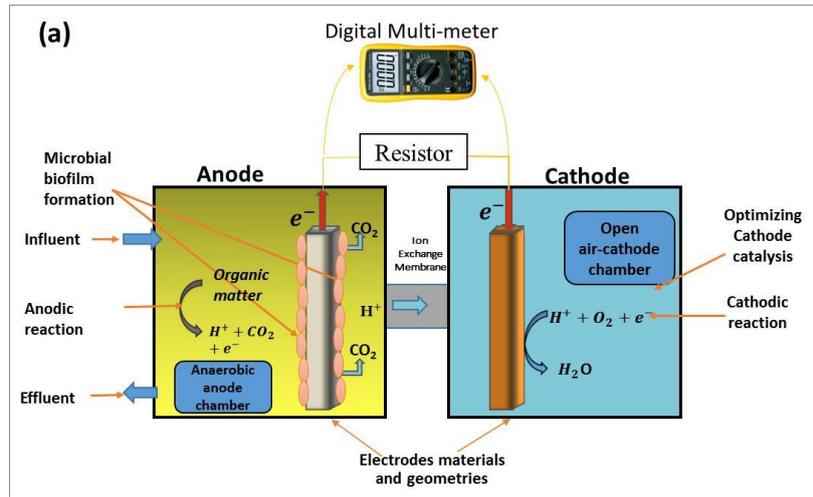
103 **Table 1** Name and function of ingredients used in microbial fuel cell.

Name	Function
Zinc plate and Copper plate	Anode and Cathode
Glass	Body of MFC
PVC pipe, Potassium sulphate salt, Agar-agar and Surgical cloth	Constituents for salt bridge
Waste water	Electrolyte
Digital Multimeter	Collecting data

104

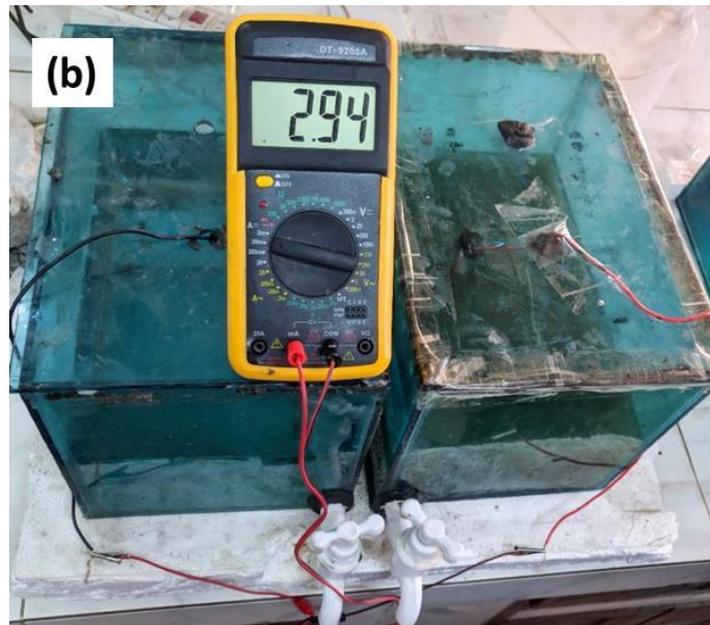
105 Zinc and Copper plates (for anode and cathode) were purchased from local scientific shop at
106 Jashore, Bangladesh. All other items were purchased from local shops. To construct the main
107 body (the chamber) of the MFC, locally available window glass was used. The volume of
108 each chamber was 0.005 m³ (length 0.25 m, width 0.10 m and height 0.20 m) where there
109 were three intros; single designed for adding, second for deletion of electrolyte as well as rest
110 one for the connection with former compartment. The two chambers were connected using an
111 agar salt bridge with a length and diameter of 4.0 cm and 0.5 cm, separately. For the
112 preparation of salt bridge 0.1M salt solution of 5 gm agar was prepared in which several
113 pieces of surgical cloths were kept for 2-3 h. A small PVC tube approximately 4.0 cm long
114 was packed by the surgical cloths immersed the agar-salt resolutions. All joints of MFC were
115 enclosed using M-seal (K1 Mart, India) to avert the outflow. The prepared microbial fuel cell
116 (MFC) is shown in [Fig. 1](#).

117



118

119



120

121

122 **Fig. 1(a)** Schematic diagram and **(b)** constructed MFC for the experiment.

123

124 **Microbe inoculation and electrolyte collection**

125 Locally available microorganisms (*Escherichia coli*, *Anabaena*, *Rhodospirillum* and some
 126 cyanobacteria) were used in all experiment. At first organic rich bottom feeders were
 127 collected from the local pond, which was then cultured for proper growth of micro-organisms.

128 It was done by mixing 1.5 ($W/W\%$) cow dung and 0.2($W/W\%$) sugar with bottom feeders.

129 The mixture was kept in an anaerobic condition for 48 h. After inoculation these microbes
 130 were used in anode chamber for the experiment. The untreated raw wastewaters (collected
 131 from Municipal drain, Bhairab River and Jashore General Hospital) were used in anode
 132 chamber. For first experiment we collected wastewater from municipal drain where the water
 133 flow rate was $225 \text{ ml}\cdot\text{s}^{-1}$. In second experiment we collected wastewater from Bhairab River
 134 at 150 cm depth from the surface. In third experiment we collected wastewater from Jashore
 135 General Hospital pipeline where the water flow rate was $195 \text{ ml}\cdot\text{s}^{-1}$. The average chemical
 136 compositions of these wastewaters throughout the experiment are abridged in [Table 2](#). The
 137 average COD concentration of the raw municipal wastewater was $784 \text{ mg}\cdot\text{L}^{-1}$, Bhairab river
 138 water was $832 \text{ mg}\cdot\text{L}^{-1}$ and hospital wastewater was $842 \text{ mg}\cdot\text{L}^{-1}$.



(a) Municipal drainage



(b) Bhairab river

Fig. 2 Sources of wastewater used as electrolyte.

139

140

141 **Table 2:** The average chemical composition of various wastewaters in Jashore, Bangladesh.

Parameter	Municipal wastewater ($\text{mg}\cdot\text{L}^{-1}$)	Bhairab river water ($\text{mg}\cdot\text{L}^{-1}$)	Hospital wastewater ($\text{mg}\cdot\text{L}^{-1}$)
HCO_3^-	347.4	354.8	294.6
Cl^-	395.8	565.6	835.3
Ca^{2+}	32.4	38.6	56.6

Mg^{2+}	26.7	32.3	18.7
Na^+	17.3	21.9	19.9
NO_3^-	4.42	3.24	13.18
SO_4^{2-}	82.3	87.5	127.5
PO_4^{2-}	6.25	5.8	3.9

142

143 **Collection of data and its analysis**

144 To monitor the effect of electrode materials, data was collected manually by using a digital
 145 multi-meter (DT-9205A, China) at a fixed interval of 20 min. The average values of voltage
 146 and current were calculated as follows:

$$Average\ voltage = \frac{Total\ voltage}{Number\ of\ count} \quad (1)$$

$$Average\ current = \frac{Total\ current}{Number\ of\ count} \quad (2)$$

147 Founded on the documented electrical energy (voltage, current and power) current density
 148 (I_{anode} , $A \cdot m^{-2}$) as well as power density (P_{anode} , $W \cdot m^{-2}$) were determined as follows:

$$Current\ density, I_{anode} = \frac{I}{A} \quad (3)$$

$$Power\ density, P_{anode} = \frac{P}{A} \quad (4)$$

149 where, I is current (A), P is the power (W), and A is the external area (m^2) of the anode.

150

151 **Calculation of COD removal**

152 Chemical Oxygen Demand (COD) specifies the quantity of oxygen (O_2) that can be
 153 consumed by reactions in a measured solution. The carbon-based substance existing in the
 154 water sample is dissolved by potassium dichromate ($K_2Cr_2O_7$) in the attendance of sulfuric
 155 acid (H_2SO_4), silver sulfate (Ag_2SO_4) and mercury sulfate ($HgSO_4$) to harvest carbon dioxide
 156 (CO_2) and water (H_2O). COD can be calculated by using [Equation 5](#).

$$\text{COD} = \frac{8 \times 1000 \times \text{DF} \times \text{M} \times (\text{V}_B - \text{V}_S)}{\text{Volume of sample (in ml)}} \quad (5)$$

157 where, DF stands for the Dilution Factor, M stands for the Molarity of standardized Ferrous
 158 Ammonium Sulfate $(\text{NH}_4)_2\text{Fe}(\text{SO}_4)_2 \cdot 6\text{H}_2\text{O}$ solution, V_B stands for the Volume used up in
 159 titration through blank preparation, V_S stands for the Volume used up in titration through
 160 sample preparation.

161

162 To calculate the removal percentage of COD we used the [Equation 6](#).

$$\begin{aligned} \text{COD removal efficiency (\%)} & \quad (6) \\ & = \frac{\text{COD}_{in} - \text{COD}_{out}}{\text{COD}_{in}} \times 100 \end{aligned}$$

163 Where, subscript *in* and *out* indicates influent and effluent fluid, respectively.

164

165 **Results and discussion**

166 Parameters such as pH (Jadhav and Ghangrekar [2009](#)), electrode constituents (Scott et al.
 167 [2008](#)), the space among the electrodes (Hong et al. [2009a](#)), external resistance (Hong et al.
 168 [2009a](#)), temperature (Hong et al. [2009a](#)), conductivity (Hong et al. [2009b](#)), also biological
 169 matter of the residue (Wang et al. [2012](#)) are reported to affect the power production of the
 170 microbial fuel cell. The performance of MFCs increased for long term operation when
 171 electro-genic biofilm formed on the electrode surface. The pH of electrolytes acting a
 172 vigorous character in bioreactor performance (Gil et al. [2003](#)). Likewise, electrolyte pH
 173 acting a vigorous key role in MFC's power output. Acidic pH lower than 6 drastically
 174 reduces the power generated from MFC (Gil et al. [2003](#)). It means, low-slung pH situations
 175 exposed a contrary consequence on the electro-chemically lively bacteriological inhabitants,
 176 which in chance clues to an extreme fall in power generation. So, pH strongly influences the
 177 output of MFC for both in batch feed and continuous feed way of action. A perfect pH variety

178 for favored fuel cell arrangement was quantified to be in the mid of 7–8 (Liu and
179 Ramnarayanan 2004). This section mainly discussed the effect of pH on various locally
180 available wastewaters for the output of microbial fuel cells.

181

182 **Effect of pH while using municipal wastewater as electrolyte**

183 In microbial fuel cell operation, pH is considered to be an important parameter that may
184 affect the generation of electricity. A series of experiments were conducted by varying the pH
185 (from pH 6 to pH 10) of the electrolyte (municipal wastewater in this case) while the other
186 parameters such as operating temperature, volume of the electrolyte, materials of electrodes,
187 surface area of electrodes etc. were kept constant. The results are depicted in Fig. 3 (a, b and
188 c). As shown in Fig. 3(a), it was obvious that pH 8 gave highest output (in the form of
189 voltage) all through the experimental period (1 – 15 days) compared to other experimented
190 pH. The voltage gradually increased up to day 4 and then it started to decline. The highest
191 value of voltage (1125 mV) was obtained at day 4 for the process operated at pH 8. On the
192 other hand, current density increases up to day 3 for all tested pH as shown in Fig. 3 b. Then
193 it starts decreasing gradually. However, the maximum value of current density was found to
194 be 1155.6 mA m^{-2} for pH 8 at day 3. Like voltage and current density the supreme power
195 density was obtained at pH 8 which is 1245.7 mW m^{-2} , where the other top values are
196 1008.7 mW m^{-2} , 1066.8 mW m^{-2} , 990.9 mW m^{-2} and 837.8 mW m^{-2} for pH 6, 7, 9 and 10,
197 respectively as shown in Fig. 3 (c). It is obvious from Fig. 3(a, b and c) that voltage, current
198 density and power density increases for first several days and then starts to decrease gradually.
199 The increase in extent of current density, voltage and power density in initial days happens
200 because (Abhilasha 2013) shows that microbial inoculation enabled higher current yield. In
201 this experiment it takes three to four days for complete inoculation of bacteria. Again the
202 decrease in extent may happen owing to the fact that with time a biofilm may form on the

203 exterior of the anode. However after 15 days of operation, cumulative yields for voltage,
 204 current density and power density were tabulated in Table 3 from where it is obvious that pH
 205 8 showed highest values.

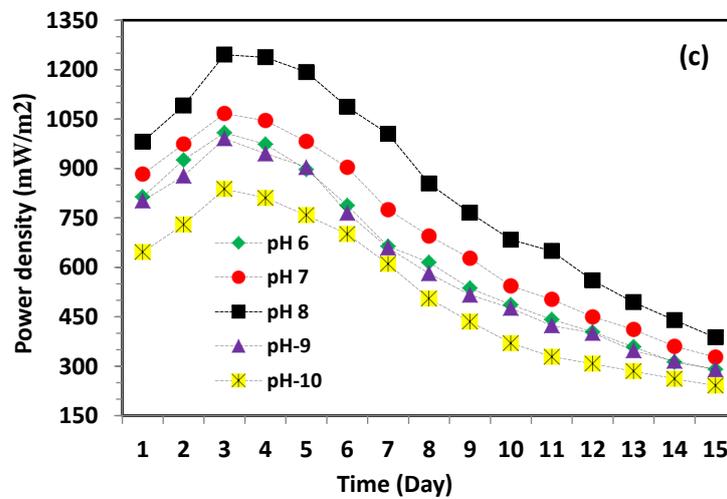
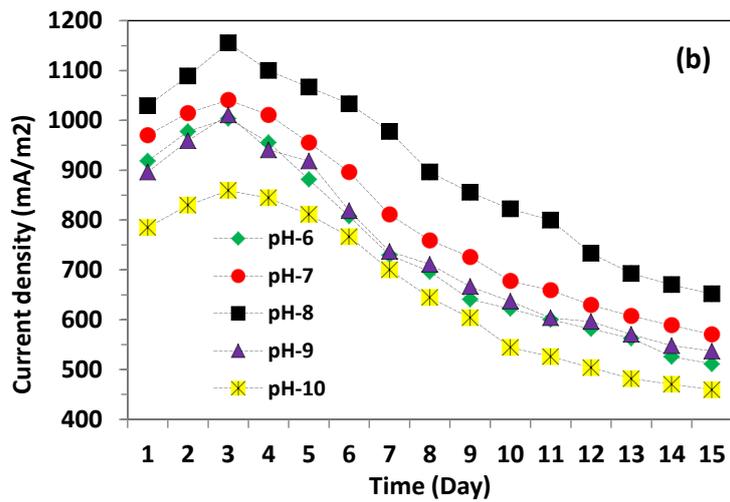
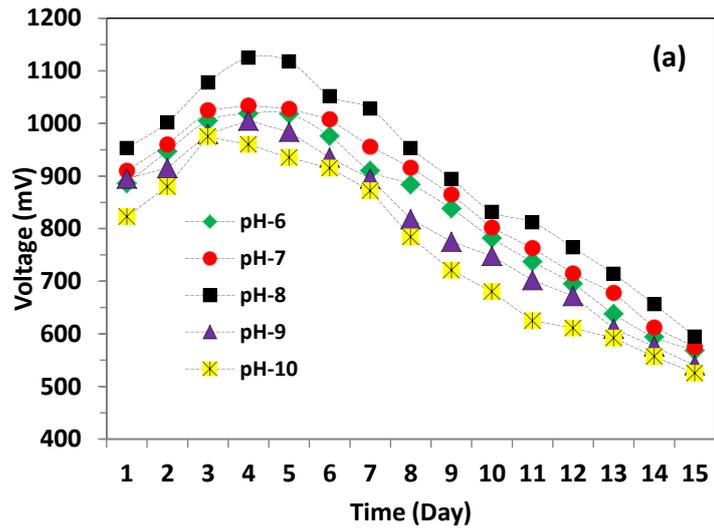
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207 **Table 3: Cumulative yield obtained from municipal wastewater for various pH in 15**
 208 **days using microbial fuel cell (MFC).**

Operating pH	Measurement	Cumulative value
6	Voltage (mV)	12497
	Current density (mAm^{-2})	11014.8
	Power density (mWm^{-2})	9518.8
7	Voltage(mV)	12847
	Current density (mAm^{-2})	11918.5
	Power density (mWm^{-2})	10551.1
8	Voltage (mV)	13577
	Current density (mAm^{-2})	13574.1
	Power density (mWm^{-2})	12676.2
9	Voltage (mV)	12050
	Current density (mAm^{-2})	11151.8
	Power density (mWm^{-2})	9298.1
10	Voltage (mV)	11455
	Current density (mAm^{-2})	9829.6
	Power density (mWm^{-2})	7830.4

209

210



211 **Figure 3:** Effect of various pH on the (a) generated voltage, (b) current density and (c) power

212 density from double chamber MFC for municipal wastewater.

213

214 For comparison with other reported values, a comparative statement has been tabulated in
 215 [Table 4](#). It is apparent that the present study gives better result in terms of extent of voltage,
 216 current density and power density compared to many other reported values.

217

218 **Table 4: Comparative statement with related published research findings.**

pH	Electrode	Electrolyt e	Voltage	Current/ Current density	Power/ Power density	Reference
8	Zinc and copper	Municipal wastewater	1125 mV	1155.6 $mA m^{-2}$	1245.7 $mW m^{-2}$	Present study
	copper boride alloy	Municipal wastewater		3500 $mA m^{-2}$	3055 $mW m^{-2}$	Paweł and Barbara 2019
6.9	carbon paper and magnesium oxide	Sugar industry wastewater	1420 m V	23.66 mA	5.1 $mW m^{-2}$	Omprakash 2019
7	graphite felt		445 mV			Zhang et al. 2011
6–7	graphite felt			400 μA		Biffinger et al. 2008

graphite felt		223.8	He et al.
		$mA\,m^{-2}$	2008
graphite rod	urban	18 $mW\,m^{-2}$	Sebastia et
	wastewater		al. 2010

219

220 This findings is very much resemble with (Jadhav and Ghangrekar 2009), who express that
 221 highest current is obtained between pH of 6.5 and 8, but this values were lesser at pH
 222 of 9 plus pH under 7. The main reason behind this, at higher pH than optimum value
 223 affects the growth of bacteria, which decrease he generated voltage (Sebastia et al. 2010).

224

225 COD removal is an important parameter for microbial fuel cell. (Zinadini et al. 2017)
 226 indicates that high COD deletion and columbic efficiency (CE) improve significantly the
 227 productivity of MFCs. The initial COD of municipal waste water in Jashore municipality was
 228 538 ppm. In this experiment the COD removal were over 86%, 89%, 91%, 88% and 86% for
 229 the electrolyte having initial pH 6, 7, 8, 9 and 10, respectively.

230

231 **Effect of pH while using Bhairab river water as electrolyte**

232 A series of experiments were conducted by varying the pH (from pH 6 to pH 10) of the
 233 electrolyte (Bhairab river water in this case) while the other parameters such as operating
 234 temperature, volume of the electrolyte, materials of electrodes, surface area of electrodes etc.
 235 were kept constant. Water collected at 150 cm depth from the surface of the river water. The
 236 results are depicted in Fig. 4(a), 4(b) and 4(c). As shown in Fig. 4(a), it was obvious that pH 8
 237 gave highest output (in the form of voltage) all through the experimental period (1 – 15 days)

238 compared to other experimented pH. The voltage gradually increased up to day 4 and then it
 239 started to decline. The highest value of voltage (1132 mV) was obtained at day 4 for the
 240 process operated at pH 8. It is also seen in (Fig. 4a) that, in operation period pH 8 gives the
 241 best result in all time. The yield from pH 7 is better than the other three. Obtained voltage
 242 from pH 6 and pH 9 are approximately the same, but for higher pH (10) the yield is lower
 243 than the others. Like voltage, current density (Fig. 4b) spike in first four days goes a
 244 maximum value of $1144.4mA\text{m}^{-2}$, $1174.1mA\text{m}^{-2}$, $1288.9mA\text{m}^{-2}$, $1181.5mA\text{m}^{-2}$, and
 245 $1122.2mA\text{m}^{-2}$ for pH 6, 7, 8, 9 and 10, respectively, and then current density decreased in a
 246 similar way to voltage. In this experiment the maximum current density obtained for pH 8.
 247 Similar to voltage and current density the supreme power density obtained for pH 8 which is
 248 1459.02 mWm^{-2} , where the other top values are 1199.4 mWm^{-2} , 1272.7 mWm^{-2} ,
 249 1250 mWm^{-2} and 1120 mWm^{-2} for pH 6, 7, 9 and 10, correspondingly which is shown in
 250 Fig. 4c. It shows that for maximum output pH 8 is better than the other, so, it can be said that,
 251 when Bhairab river water is used as electrolyte pH 7 to pH 8 produce the better yield.
 252 Variation of pH from this value the outlet will be declined. The total obtained values are
 253 shown in Table 5.

254

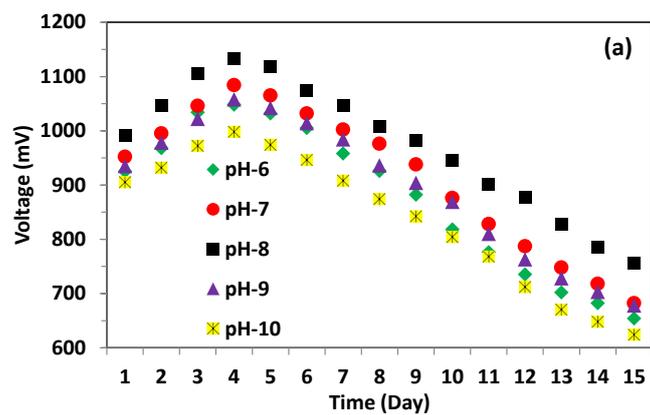
255 **Table 5: Cumulative yield obtained from Bhairab river water for various pH in 15 days**
 256 **using microbial fuel cell (MFC).**

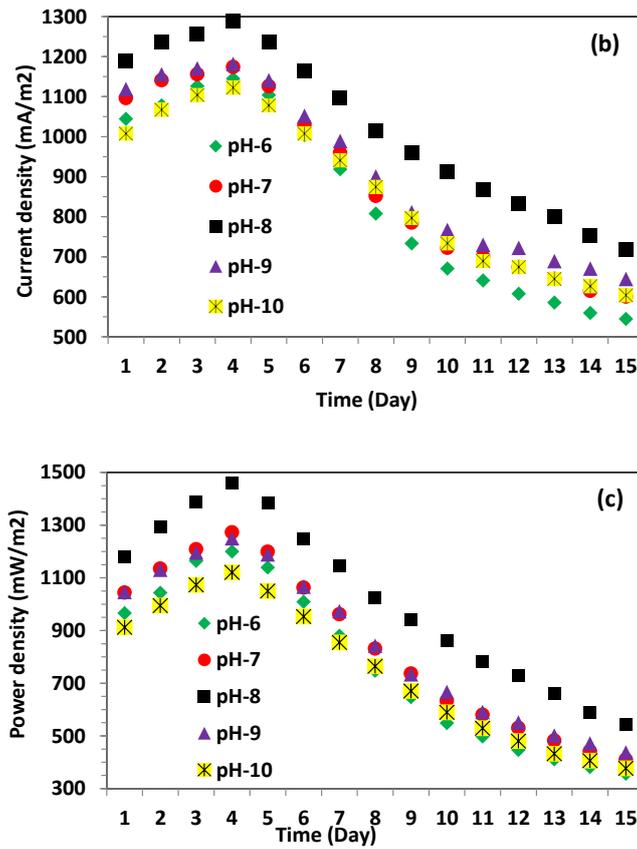
Operating pH	Measurement	Cumulative value
6	Voltage (mV)	13145
	Current density ($mA\text{m}^{-2}$)	12566.7
	Power density ($mW\text{m}^{-2}$)	11435.4

7	Voltage (mV)	13729
	Current density (mAm^{-2})	13274.1
	Power density (mWm^{-2})	12526.3
8	Voltage (mV)	14597
	Current density (mAm^{-2})	15322.2
	Power density (mWm^{-2})	15233.5
9	Voltage (mV)	13424
	Current density (mAm^{-2})	13740.7
	Power density (mWm^{-2})	12644.02
10	Voltage (mV)	12577
	Current density (mAm^{-2})	12966.7
	Power density (mWm^{-2})	11202.7

257

258





259 **Figure- 4:** Effect of various pH on the (a) generated voltage, (b) current density, (c) power
 260 density from double chamber MFC for bhairab river wastewater.

261

262 For comparison with other reported values, a comparative statement has been tabulated in
 263 Table 6. It is apparent that the present study gives better result in terms of extent of voltage,
 264 current density and power density compared to many other reported values.

265

266 **Table 6: Comparative statement with related published research findings.**

pH	Electrode	Electrolyte	Voltage	Current density	Power density	Reference
8.0	Zinc and copper	Bhairab river water	1132 mV	1288.9 mA m ⁻²	1459.02 mW m ⁻²	This study

6	graphite rods and PbO ₂ graphite	River water	937mV	382 (μA/cm ²)	86 (μW/cm ²)	Dhiraj et al. 2020
6.5 to 7.5	Carbon cloth	Domestic wastewater			120 mWm ⁻²	Li and Chen 2018
6.7	Hybrid with stainless steel and plain graphite	Musi river water	mV	62.23 mAcm ⁻²	15.56 mWm ⁻²	Venkata et al. 2009

267

268 In fifteen days operation the COD removal were over 88%, 90%, 94%, 91% and 89% for the
269 electrolyte having initial pH 6, 7, 8, 9 and 10 respectively. COD removal rates of (Zhang et
270 al. 2011) were 85%, 86%, 83%, and 88% at initial pH (4, 5, 6, and 7) respectively. We got all
271 the maximum findings at pH 8. (Zhang et al. 2011) also said that, on anode surface biofilms
272 formed by both long and short rod-shaped biomass bacteria. But acidic medium the thickness
273 of biofilm is less than the neutral medium. So, biofilms can break at pH ≤5, which can drop
274 down into the inner portion of the electrode, resulting in decies the generated electricity.
275 (Behera et al. 2010) identified that; slightly alkaline anodic pH (7.5) is favorable for better
276 electricity generation and COD removal. (Gil et al. 2003) said that at higher pH more than 10
277 power generations decreased for low proton transfer.

278

279 **Effect of pH while using Jashore General Hospital wastewater as electrolyte**

280 To examine the consequence of pH on the output of microbial fuel cell, several experiments
281 were done by using Jashore General Hospital wastewater as electrolyte. The experiment

282 performed at room temperature and Zinc plate used as an anode and Copper plate used as a
 283 cathode. In this experiment, the only variable was the initial pH (6 to 10) of electrolyte.
 284 Whereas, the other operating conditions (temperature, volume, electrolyte, and electrode) are
 285 the same. Here the Jashore General Hospital wastewater was collected from the outlet of
 286 hospital pipeline. The results are depicted in Fig. 5a, 5b and 5c. As shown in Fig. 5a, it was
 287 obvious that pH 9 gave highest output (in the form of voltage) all through the experimental
 288 period (1-15 days) compared to other experimented pH. The voltage gradually increased up
 289 to day 4 and then it started to decline. The highest value of voltage (1016 mV) was obtained
 290 at day 4 for the process operated at pH 9. Again, in current density it increases up to day 4 for
 291 all tested pH as shown in Fig. 5b. Then it starts decreasing gradually. However, the maximum
 292 value of current density was found to be $1007.41 \text{ mA}m^{-2}$ for pH 9 at day 4. Like voltage and
 293 current density the extreme power density was obtained at pH 9 which is $1023.53 \text{ mW}m^{-2}$,
 294 where the other top values are $767.31 \text{ mW}m^{-2}$, $830.27 \text{ mW}m^{-2}$, $980.71 \text{ mW}m^{-2}$ and
 295 $886.5 \text{ mW}m^{-2}$ for pH 6, 7, 8 and 10, respectively as shown in Fig. 5c. All the figures show
 296 that, for Jashore General Hospital wastewater as electrolyte pH 9 is better than the other.
 297 Where, (Parkash 2018) got pick output at pH 8.5. Variation of pH from this value the outlet
 298 will be declined. The total obtained values are shown in Table 7.

299

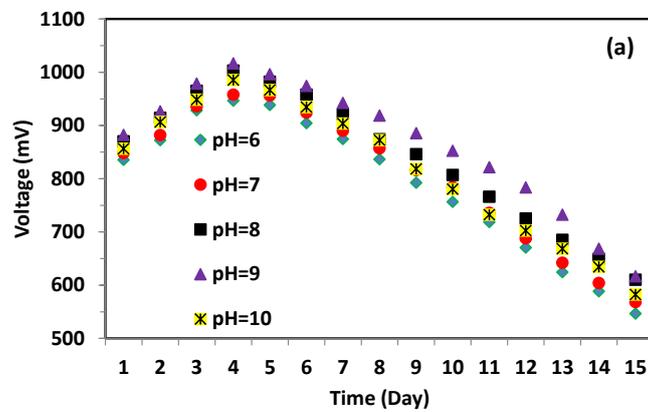
300 **Table 7 Cumulative yield obtained from Jashore General Hospital wastewater for**
 301 **various pH in 15 days using microbial fuel cell (MFC).**

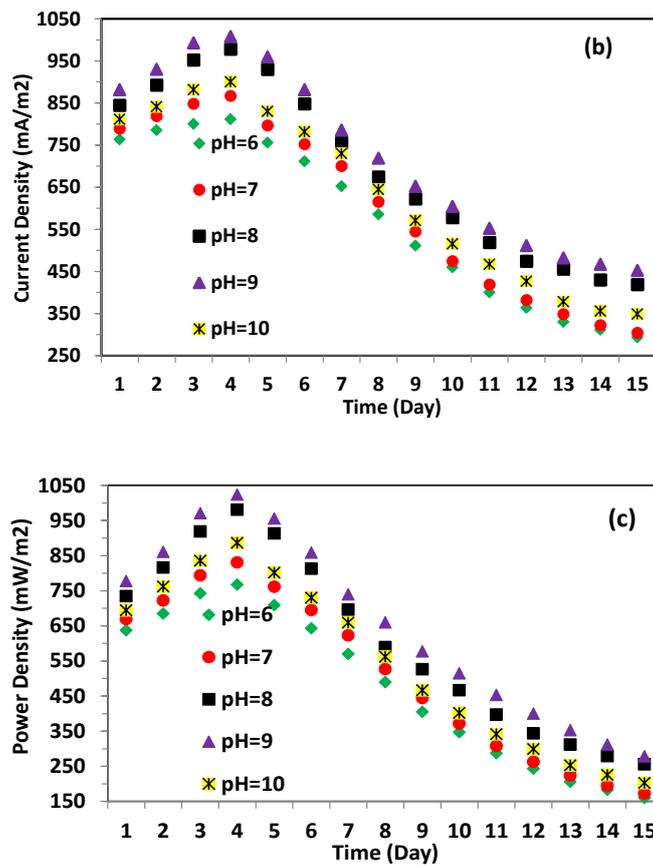
Operating pH	Measurement	Cumulative value
6	Voltage (mV)	11827
	Current density ($\text{mA}m^{-2}$)	8529.63
	Power density ($\text{mW}m^{-2}$)	7072.72

7	Voltage (mV)	12089
	Current density (mAm^{-2})	8977.78
	Power density (mWm^{-2})	7597.98
8	Voltage (mV)	12575
	Current density (mAm^{-2})	10370.37
	Power density (mWm^{-2})	9039.91
9	Voltage (mV)	12989
	Current density (mAm^{-2})	10874.07
	Power density (mWm^{-2})	9732.85
10	Voltage (mV)	12286
	Current density (mAm^{-2})	9477.78
	Power density (mWm^{-2})	8119.42

302

303





304 **Fig. 5** Effect of various pH on the (a) generated voltage, (b) current density, (c) power
 305 density from double chamber MFC for Jashore General Hospital wastewater.

306
 307 For comparison with other reported values, a comparative statement has been tabulated in
 308 Table 8. It is apparent that the present study gives better result in terms of extent of voltage,
 309 current density and power density compared to many other reported values.

310

311 **Table 8** Comparative statement with related published research findings.

pH	Electrode	Electrolyte	Voltage	Current density	Power density	Reference
8.0	Zinc and copper	Jashore	1016	1007.41	1023.53	This
		General	mV	$mA\,m^{-2}$	$mW\,m^{-2}$	experiment

		Hospital				
		wastewater				
7.5	Graphite granules and graphite rod	Hospital wastewater			140 ± 10 mWm^{-2}	Aelterman et al. 2006
9.0	Graphite felt and carbon cloth		439.7 ± 0.1 mV	231.3 ± 1.1 $mA m^{-2}$	107.1 ± 1.0 mWm^{-2}	He et al. 2008
9.5	Graphite rod and air-cathode	Urban wastewater			18.0 mWm^{-2}	Sebastia et al. 2010

312

313 COD removal is very significant to treat wastewater. Higher COD removal means the process
 314 is more applicable for wastewater treatment. In fifteen days operation the COD removal were
 315 over 78%, 83%, 86%, 88% and 84% for the electrolyte having initial pH 6, 7, 8, 9 and 10
 316 respectively.

317

318 **Conclusion**

319 Initial pH greatly affects the output of microbial fuel cell along with COD removal from
 320 wastewater. In every experiment initially the productivity (voltage, current density and power
 321 density) increased then after a certain period these values gradually decreased with time. The
 322 main reason behind this anodic microbe took time for their proper growth, after complete
 323 inoculation the growth of microbes is decreased. The optimum pH for municipal waste water
 324 of Jashore and bhairab river water is 8.0, where the maximum voltage, current density and
 325 power density were 1125 mV, $1155.6 mA m^{-2}$, $1245.7 mWm^{-2}$ and 1132 mV,

326 $1288.9\text{mA}\text{m}^{-2}$, $1459.02\text{mW}\text{m}^{-2}$ respectively. But for hospital wastewater the top results
327 obtained at pH 9 these were 1016 mV, $1007.41\text{mA}\text{m}^{-2}$ and $1023.53\text{mW}\text{m}^{-2}$. The
328 maximum COD removal was 91%, 94% and 88% from municipal, bhairab river and hospital
329 wastewater respectively. At lower pH anodic biofilm will break which result the lower
330 output.

331

332 **Declarations**

333

334 **Ethics approval and consent to participate**

335 Not applicable.

336

337 **Consent for publication**

338 Not applicable.

339

340 **Availability of data and materials**

341 All data generated through experiments and analyzed during this study are included in this
342 article.

343

344 **Competing interests**

345 The authors declare that they have no competing interests.

346

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348 Not applicable.

349

350 **Authors' contributions**

351 MAH conceptualized the methodology, wrote original draft, MOR gave general advice, MI
352 designed and conducted the experiments, RK designed and conducted the experiments, and
353 BKB laid the guideline, edited and reviewed the manuscript. All authors read and approved
354 the final manuscript.

355

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358

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361 Jashore-7408, Bangladesh.

362

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534

Figures

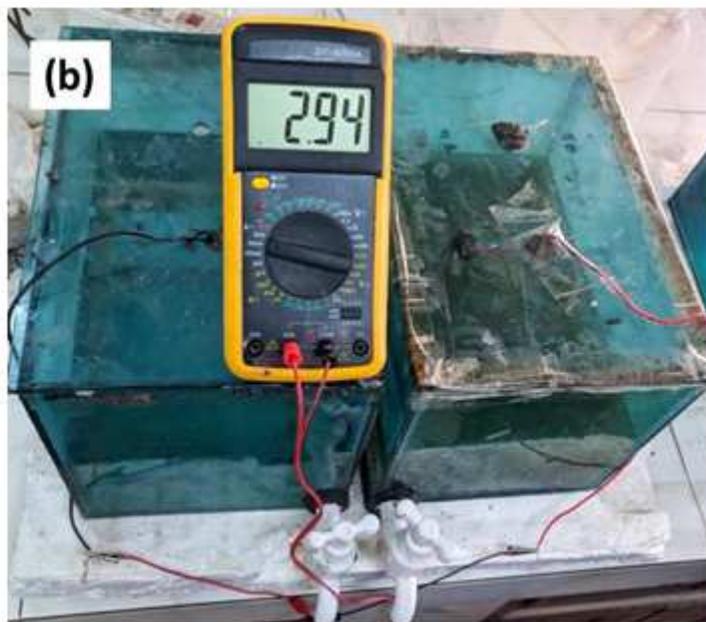
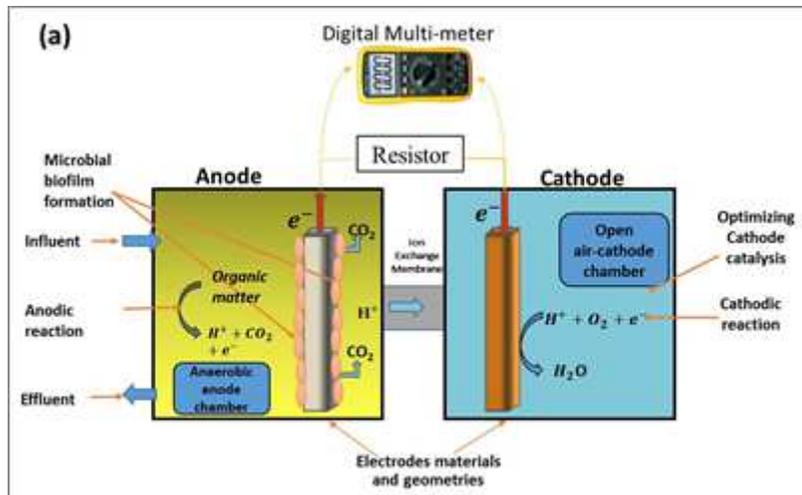


Figure 1

(a) Schematic diagram and (b) constructed MFC for the experiment.



(a) Municipal drainage



(b) Bhairab river

Figure 2

Sources of wastewater used as electrolyte.

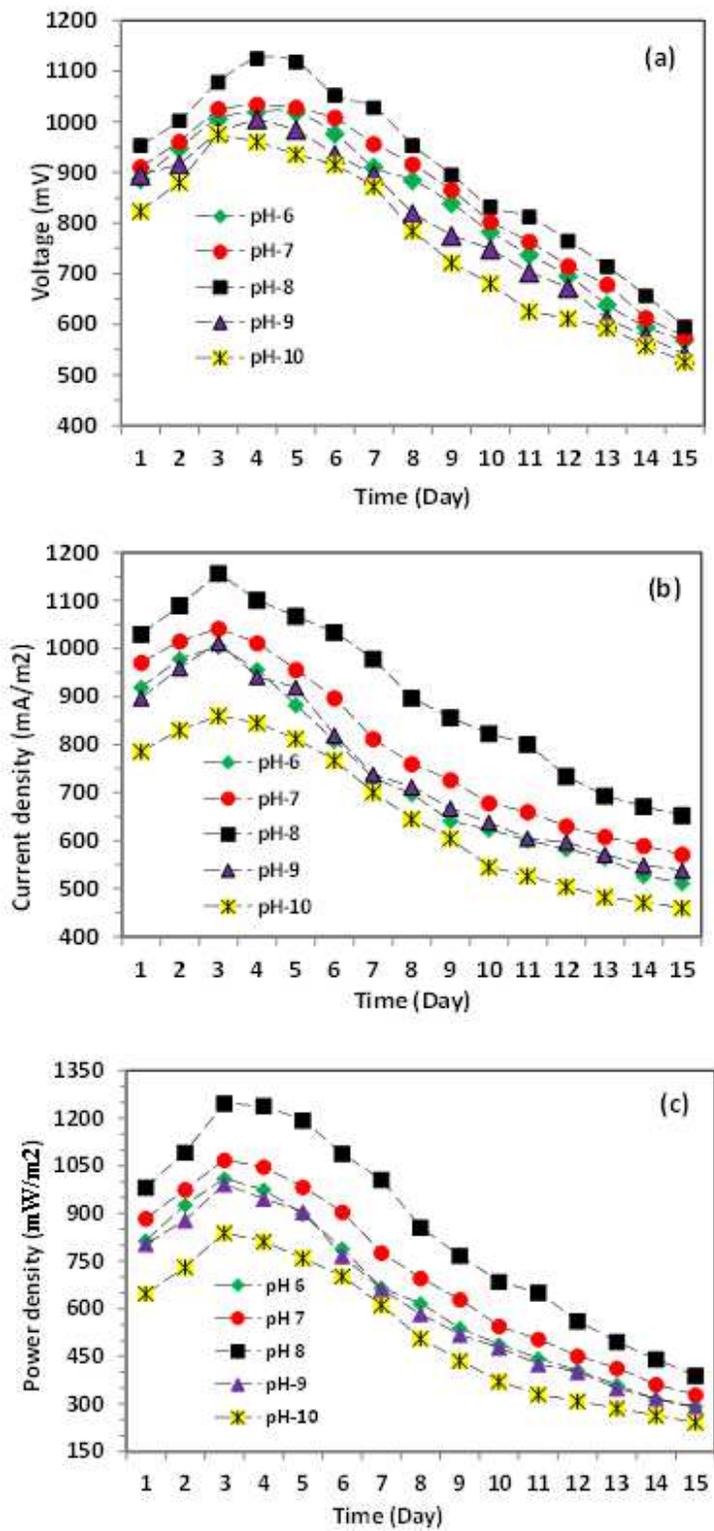


Figure 3

Effect of various pH on the (a) generated voltage, (b) current density and (c) power density from double chamber MFC for municipal wastewater.

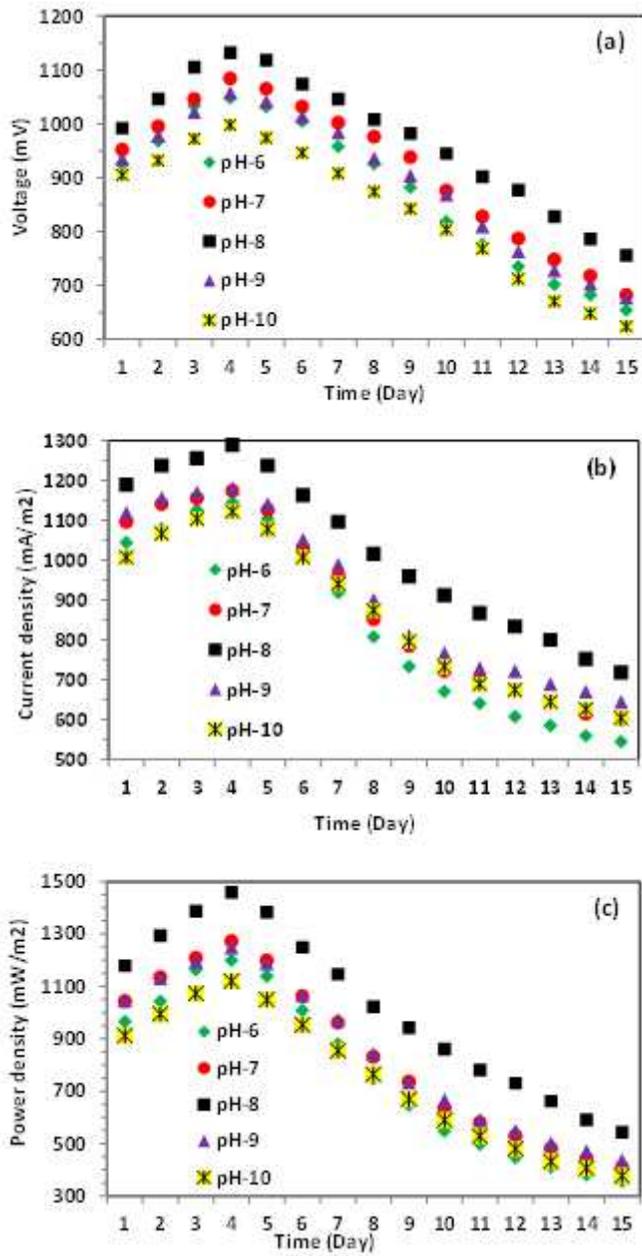


Figure 4

Effect of various pH on the (a) generated voltage, (b) current density, (c) power density from double chamber MFC for bhairab river wastewater.

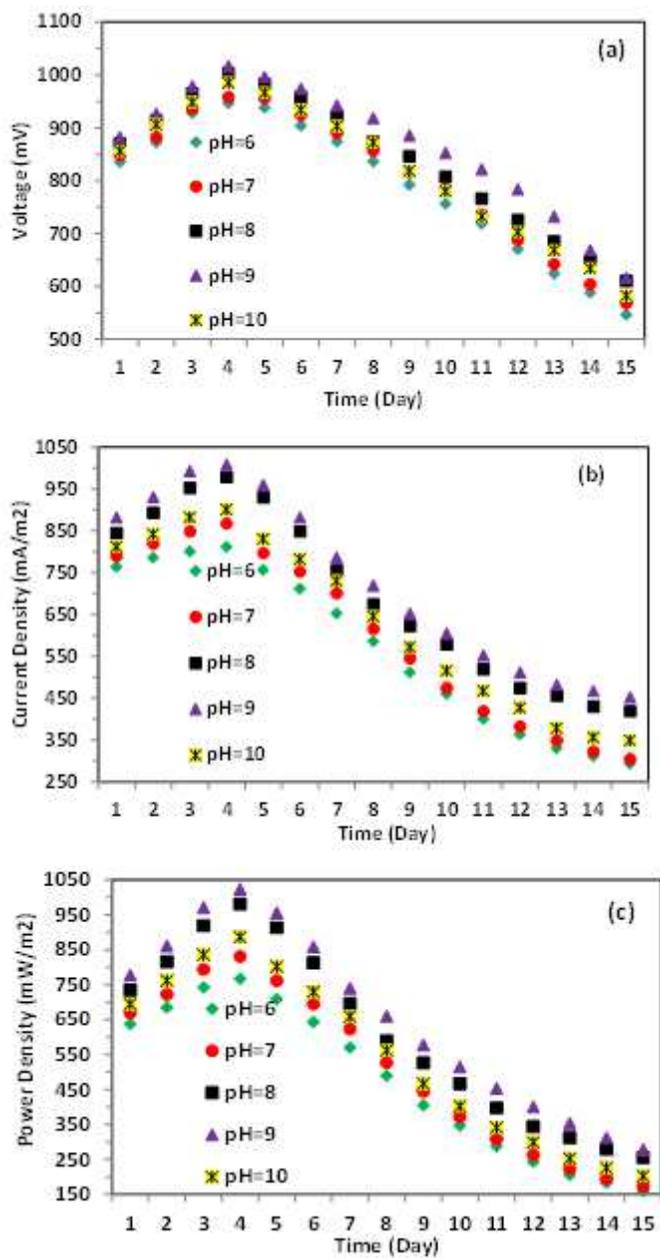


Figure 5

Effect of various pH on the (a) generated voltage, (b) current density, (c) power density from double chamber MFC for Jashore General Hospital wastewater.

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