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Catalytic degradation of "trinitrogen" by Fe-Ce-SiO2 aerogel@TiO2

Jie Li	
East China University of Science and Technology	
Yuxiang Yang (📨 yxyang@ecust.edu.cn)	
East China University of Science and Technology	https://orcid.org/0000-0003-1836-1341
zhiyong Han	
Chengdu University of Technology	
yan Huang	
East China University of Science and Technology	
hongming Yuan	
Jilin University	
chaoying Ni	
University of Delaware	

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3 4	Jie Li ^a , Yuxiang Yang ^{a,c*} , Zhiyong Han ^b , Yan Huang ^a , Hongming Yuan ^d , Chaoying Ni ^c
5	^a School of Chemistry and Molecular Engineering, East China University of
6	Science & Technology, Shanghai 200237, China
7	^b State Key Laboratory of Geohazard Prevention and Geoenvironment Protection
8	(Chengdu University of Technology), Chengdu 610059, P.R.China
9	^c Department of Materials Science and Engineering, University of Delaware,
10	Newark, Delaware 19716, United States
11	^d State Key Laboratory of Inorganic Synthesis and Preparative Chemistry, Jilin
12	University, Changchun 130012, China
13	*Corresponding author: yxyang@ecust.edu.cn, cni@udel.edu

14 Abstract

15 The "Three nitrogens" [Ammonia nitrogen (NH₄ ⁺ -N), Nitrate nitrogen (NO₃ ⁻ -N) and Nitrite nitrogen (NO₂⁻-N)] from industrial or domestic wastewater can lead to 16 eutrophication of water bodies, ammonia The conversion of nitrogen into nitrate 17 nitrogen will cause high nitrogen and oxygen demand (NOD), which will also lead to 18 methemoglobinemia, and the high content of nitrite in the water body will increase the 19 20 risk of cancer. In this paper, SiO₂ aerogel is used as a carrier to synthesize Fe-Ce bimetal-doped composite materials (Fe-Ce/SiO2 and Fe-Ce-SiO2/TiO2) for the 21 adsorption and degradation of "three nitrogens". The effect of metal Fenton reagent (Fe-22 Ce/SiO₂) Fenton catalysis and photo-Fenton cooperative catalysis (Fe-Ce-SiO₂/TiO₂) 23 on the degradation efficiency of "three nitrogens". 24

SiO₂/TiO₂ was prepared by dipping method, and Fe and Ce bimetals were loaded on the surface of SiO₂/TiO₂ material, and the effect of photo-Fenton oxidation on the degradation rate of "three nitrogen" under different materials was explored. The results showed that: when the dosage of catalyst was 0.01 g, pH value was 11.0, and the concentration of H₂O₂ was 80 mmol/L, the photocatalytic efficiency was the best, and

- the degradation efficiency of "three nitrogen" remained above 70%.
- 31 **Keywords:** "Three Nitrogen" degradation; Fenton oxidation; Photocatalysis.

32 **1 Introduction**

Environmental remediation technologies are one of the most studied topics in 33 environmental science because many industrial activities generate pollutants. The 34 "three nitrogens" [ammonia nitrogen (NH₄⁺-N), nitrate nitrogen (NO₃⁻-N) and nitrite 35 nitrogen (NO₂⁻-N)] from industrial or domestic wastewater can lead to eutrophication 36 37 of water bodies. The conversion of nitrogen to nitrate increases the nitrogen and oxygen demand (NOD), which can contribute to methemoglobinemia. High levels of nitrite in 38 water increase the risk of cancer. Advanced oxidative processes involving 39 photocatalytic mechanisms (photooxidation, photoreduction, and photodegradation) 40 41 have received substantial attention in the past 50 years since the introduction of photocatalytic technology by Fujishima and Honda in 1970. Photocatalytic oxidation is 42 an environmentally safe and promising method for degrading polluted wastewater 43 (Chen et al. 2004;Lin et al. 2013). Compared with other techniques such as adsorption, 44 chemical oxidation and ozonation, photocatalytic oxidation is a regenerative process 45 with a lower cost. A photocatalyst with high activity is an important parameter in 46 photocatalytic oxidation. TiO₂ is a well-known photocatalyst (J.Síma et al. 2013; K. 47 Hashimoto et al.2013). However, the photocatalytic effect of pure TiO₂ is unsatisfactory, 48 suggesting the need for modification of TiO_2 to improve its industrial application. In 49 addition to doping and structural modification of TiO₂ nanoparticles to alter the 50 photocatalytic properties, TiO2 supported on powdered activated carbon (PAC-TiO2), 51 granular activated carbon (GAC-TiO2), and zeolite (Z-TiO2), i.e., supported TiO₂, also 52 exhibits photocatalytic properties that differ from those of TiO₂ alone (Síma et al. 2013; 53 Hashimoto et al. 2005; Harraz et al. 2013). SiO₂ aerogel is a very light solid with high 54 porosity and remarkable thermal insulation (Rankin et al. 2014). It appears like a 55 "foamy" translucent substance, hence the name "frozen smoke". Silica-titanium dioxide 56 (SiO₂/TiO₂) composites are well-known materials (Camblor et al. 1995; Rao et al. 2003; 57 Gao et al. 2012). Several studies have revealed the relationship between the 58 59 photocatalytic activity of materials and the structure of surface TiO₂, method of 60 preparation, and loading. In order to improve the stability and other properties of SiO₂/TiO₂, a synthetic method of SiO₂/TiO₂ has recently been developed, which 61 involves the formation of hierarchical structures or aerogels. One-dimensional SiO₂-62 TiO_2 nanofibers exhibit large surface area and high thermal stability of anatase TiO_2 , 63

and SiO₂ effectively prevents phase transformation of TiO₂ from anatase to rutile 64 65 structure at high temperatures (Cui et al. 2019; Wang et al. 2019). They exhibit strong ability to separate the photogenerated electron-hole pairs (Wang et al. 2019), resulting 66 in improved photocatalytic performance. Therefore, SiO₂/TiO₂ aerogels exhibit 67 excellent photocatalytic properties. Their mesoporous structure can overcome the 68 69 inherent defects, especially in terms of electron transport. Results of a previous study confirmed the strong light-harvesting properties of SiO₂/TiO₂ with mesoporous 70 71 structure (Kwon et al. 2015).

However, the Fe-CeO_x bimetallic compound supported by the surface of 72 SiO₂/TiO₂ combines photocatalysis with Fenton degradation, resulting in enhanced 73 74 degradation efficiency of target pollutants. According to Fenton's principle, hydroxyl 75 radicals are generated by the decomposition of hydrogen peroxide (H₂O₂) in the presence of Fe^{2+} . Exposure to UV-Vis radiation improves the efficiency of this method, 76 especially resulting in the regeneration of iron ions and OH• radicals, with increased 77 specific surface area of TiO₂ boosting the activity of Fe-CeO_x bimetallic catalyst (Wang 78 et al. 2011). A surface density of 2.5~14.5 CeO_x/nm² resulted in excellent catalytic 79 80 activity.

In this study, TiO_2 nanoparticles were introduced into the catalyst system, and Fe-Ce bimetals were layered on the surface of SiO_2/TiO_2 to support bimetallic Fe-CeO_x to perform the photo-Fenton-catalyzed "trinitrogen" degradation. The effect of "trinitrogen" under different catalytic systems was explored. The degradation efficiency was determined and the possible mechanism was investigated.

86 2. Materials and methods

87 2.1 Materials

All chemicals were analytical, unpurified and used as received. Ethanol, tetrabutyl titanate, acetic acid, ferrous chloride tetrahydrate, cerium chloride heptahydrate, and hydrogen peroxide (AR) were purchased from Sinopharm Chemical Group,Shanghai,Chana.

92 2.2 Experimental procedures

93 2.2.1 Preparation of three catalysts including SiO₂@TiO₂-Fe-Ce

94 2.2.1.1 Preparation of SiO₂@TiO₂ composite aerogels

Preparation of SiO₂ aerogel sample was referenced to the invention patent we applied for, patent number: 202011361256.7. Then, a 3.3 mL aliquot of tetrabutyl titanate was added to 25 mL of absolute ethanol under magnetic stirring for 5 min. SiO₂
aerogel (0.8 g) was ultrasonically mixed with 75 mL of deionized water and stirred
magnetically to form a suspension. The ethanol solution of tetrabutyl titanate was added
dropwise into the suspension at a constant speed using a constant flow pump. The pH
value of the system was controlled to approximately 2.3 by adding 0.5 mol/L acetic
acid solution. The solution was suction-filtered after 1 h of reaction, and dried in an
oven at 90°C for 6 h to obtain SiO₂@TiO₂ composite aerogels.

104 2.2.1.2 Preparation of three catalysts: $SiO_2@TiO_2$ -Fe-Ce, $SiO_2@TiO_2$ -Fe and 105 $SiO_2@TiO_2$ -Ce

SiO₂/TiO₂ composite aerogel prepared above was accurately weighed to 1.0 g 106 and mixed with 50 mL of deionized water to form a suspension. Next, 2.24 g of 107 CeCl₃ ·7H₂O and 2.39 g of FeCl₂ ·4H₂O were dissolved in 30 mL of deionized water 108 and mixed uniformly at room temperature. The mixture was added to the suspension 109 with a peristaltic pump at room temperature under a N₂ atmosphere, followed by the 110 dropwise addition of 0.5 mol/L sodium hydroxide solution. Following suction filtration 111 and washing three times with deionized water, the filtered product was placed in a 112 113 vacuum-dried oven at 60°C for 6 h. The dried and filtered product was calcined at 500°C for 2 h to obtain SiO₂@TiO₂-Fe-Ce catalyst. 114

Further, only 2.39 g of FeCl₂·4H₂O was added during the preparation to obtain FeSiO₂@TiO₂ catalyst. However, the addition of 2.24 gCeCl₃·7H₂O yielded SiO₂@TiO₂Ce catalyst.

118 2.2.2 Catalyst performance

A quartz reaction tube containing 30 mL each of ammonia nitrogen, nitrate 119 nitrogen and nitrite nitrogen with a concentration of 0.1 mg/mL was treated with 0.01 120 g of catalyst, followed by static adsorption of the degradation solution for 20 min under 121 dark to reach equilibrium. A small amount of the reaction solution was removed for 122 123 centrifugation, and the absorbance of the supernatant (A_0) was determined. The UV light source in the UV reaction box was switched on for photocatalytic degradation. 124 The solution was removed and centrifuged at high speed. The absorbance of the 125 supernatant was denoted as At. The reaction time was 120 min. The degradation rate 126 was calculated using the following formula: 127

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$$H = (C_0 - C_t)/C_0 \times 100\% \quad (2-1)$$

129 C_0 represents the concentration under adsorption equilibrium, whereas C_t is the

130 concentration when the reaction time is t.

2.2.3 Effects of different conditions on the efficiency of three catalysts in Fentondegradation of "Trinitrogen"

A 250 mL conical flask containing 50 mL of 0.1 mg/mL ammonia nitrogen, nitrate nitrogen and nitrite nitrogen solutions was used. Two of the three conditions including pH, H₂O₂ dosage and catalyst system were fixed first, while changing the other condition. The conical flask was treated with different catalysts and shaken in a constant temperature oscillator. A sample was obtained every 20 min and its absorbance was measured. The degradation rate was then calculated.

2.2.4 Effects of different conditions on the photo-Fenton degradation efficiency of threenitrogen catalysts

141 A quartz UV reaction test tube containing 50 mL of 0.1 mg/mL ammonia nitrogen, nitrate nitrogen and nitrite nitrogen solutions was used to determine the effect of 142 different conditions on the photo-Fenton degradation efficiency of the nitrogen catalysts. 143 Two of the three conditions of pH, H₂O₂ dosage and catalyst system were held constant, 144 and the third condition was changed. A 0.01 g of catalyst was added to the reaction test 145 146 tube, and the reaction was carried out under a 300 W ultraviolet mercury lamp. A sample was obtained every 20 min to measure the absorbance and calculate the degradation 147 148 rate.

- 149 **3 Results and discussion**
- **3.1 Characterization of catalyst**

As shown in Figure 1(a), the diffraction peaks at 2θ of 25.68° , 37.6° , 48.2° , 55.4° , 57.2°, 64.6° , 69.4° and 75.1° correspond to eight crystal planes of anatase TiO₂ (101), (004), (200), (101), (211), (204), (220) and (215) (JCPDS, 21-1272), demonstrating that the TiO₂ in the catalyst material is anatase. No obvious diffraction peaks of Fe, Ce and SiO₂ are visible in the Figure, which may be due to the reduced levels of Fe and Ce in the catalyst, which led to weak diffraction peaks and absence of characteristic peaks of other phases, suggesting no new phase formation.

Figure 1(b) shows the N₂ adsorption and desorption curves of the catalyst and its pore size distribution. As shown in the Figure, the catalyst exhibits type IV adsorption and desorption curves, based on the IUPAC classification and a H3 hysteresis loop, indicating that the presence of mesoporous material with pore diameters ranging between 10 nm and 15 nm. According to the BET analysis, the SiO₂@TiO₂-Fe-Ce catalyst has a surface area of 455.8 m²/g, a pore volume of 0,6025 cm³/g, a most probable pore size of 16.23 nm, and an average pore size of 14.98 nm.



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Fig.1 XRD, BET, FT-IR and Raman spectra of Fe-Ce-SiO₂/TiO₂ catalyst

Figure 1(c) shows the FT-IR spectrum of the SiO₂@TiO₂-Fe-Ce catalyst. As 169 shown in the Figure, the broad bands of 3430 cm⁻¹ and 1630 cm⁻¹ in the spectrum 170 correspond to the stretching of hydroxyl groups and surface adsorbed water, 171 respectively. The samples exhibit characteristic peaks at 500 cm⁻¹, 1080 cm⁻¹ and 950 172 cm⁻¹, which are attributed to the stretching vibrations of Ti-O and Si-O-Si of the silica 173 framework, and Ti-O-Si, respectively. The hydroxyl and hydrogen bonds on the surface 174 of the aerogel enhance its adsorption capacity for "trinitrogen" and therefore promote 175 subsequent photocatalytic degradation. These results suggest that the incorporation of 176 TiO₂ into SiO₂ results in the formation of a binary TiO₂-SiO₂ system, and the vibrational 177 peaks indicate the interaction between Ti and Si at the molecular level. 178

In order to validate the presence of TiO₂ in the SiO₂@TiO₂-Fe-Ce catalyst, the sample was characterized by Raman spectroscopy. The results presented in Figure 1(d) indicate that 198(Eg), 398(Eg), 515(Eg) and 640(Eg), correspond to anatase TiO₂, which are consistent with the results of XRD analysis.



183 3.2 XPS Analysis

Fig. 2 XPS of SiO₂@TiO₂-Fe-Cecatalyst

220 Figure 2 illustrates the XPS characterization of the SiO₂@TiO₂-Fe-Ce catalyst. The elemental composition and chemical valence states of elements, such as O, Si, Ti, 221 Ce, and Fe on the surface of the catalyst samples were studied. Figure 2(a) represents 222 the full spectrum of the catalyst sample, indicating the presence of six main elements, 223 224 including C, Si, O, Fe, Ce and Ti. The C element may be due to incomplete calcination or contaminant residues on the sample surface. Figures 2(b) to 2(f) represent the high-225 resolution spectra of O1s, Ti2p, Si2p, Ce3d and Fe2p, respectively. As shown in Figure 226 2(b), the O element exhibits four chemical forms in the catalyst, with electron binding 227 energies of 529.2 eV, 530.9 eV, 532.1 eV and 532.5 eV attributed to Ti-O-Ce and Ti-O-228 Si, Ti-OH and Si-O-Si chemical bonds, respectively. Figure 2(c) is the XPS high-229 resolution spectrum of Ti2p showing two chemical states of Ti in the catalyst system. 230 The peak of the electron binding energy is attributed to Ti⁴⁺ in the catalyst, which 231 corresponds to the binding energy of Ti in Ti-O-Ti and Ti-O-Si. Figure 2(d) represents 232 the XPS image of Si2p, with the two peaks appearing at 102.6 eV and 103.2 eV, 233 respectively, after the peak separation, which are attributed to Si2p in Si-O-Si and Ti-234 O-Si. As shown in Figure 2(e), the results of peak separation of Ce3d reveal the 235 characteristic peaks of electron binding energy at 882.28 eV, 884.95 eV and 898.04 eV 236 belonging to the spin-orbits of the electronic states of Ce3d5/2, while the peaks at 237 900.71 eV, 903.24 eV and the characteristic peak at 916.32 eV are assigned to the spin-238 orbit of the electronic state of Ce3d3/2. The characteristic peaks of binding energy at 239 884.95 and 903.24 eV correspond to Ce³⁺ (3d104f1 electronic state), and the rest of the 240 characteristic peaks are assigned to Ce⁴⁺ (3d104f0 electronic state) (Shao et al. 2013). 241 indicating that both Ce^{3+} and Ce^{4+} exist on the catalyst surface. The presence of oxygen 242 vacancies and unsaturated bonds in Ce³⁺ increases the chemical adsorption of oxygen 243 on the surface of the Fe-Ce-SiO₂/TiO₂ catalyst. Ce⁴⁺ captures the photogenerated 244 electrons to generate Ce^{3+} . The photogenerated electrons are transferred to the O_2 245 molecules adsorbed on the surface of the catalyst. Finally, superoxide radicals $(O_2 \cdot)$ are 246 247 generated, which increase the photocatalytic efficiency of the catalyst. Figure 2(f) is the XPS spectrum of Fe2p indicating that the characteristic peak at 711.6 eV belongs to 248 Fe2+ while the characteristic peaks at 716.2 eV and 719.3 eV belong to Fe^{3+} (Lenza et 249 al. 2002; Vilarrasa et al.2015), indicating the presence of Fe on the catalyst surface in 250 two forms, Fe^{2+} and Fe^{3+} . 251



Fig. 3 TEM and SEM images of SiO₂@TiO₂-Fe-Ce catalyst

Figures 3 a, b, and c represent the TEM images of the SiO₂@TiO₂-Fe-Ce catalyst under different magnifications. The catalyst samples obtained after Fe and Ce doping exhibit strong dispersion and uniform particle size. As shown in Figure 3(c), the average diameter is about 15 nm.

Figures 3 d, e, and f are the SEM images of the SiO₂@TiO₂-Fe-Ce catalyst under different magnifications, revealing a spherical catalyst structure and uniform distribution, with typical SiO₂ gas condensation. The microstructure is similar to that of glue, with uniform pore distribution and particle aggregation after the introduction of TiO₂. As shown in the Figure, the anatase-type TiO₂ particles are mainly located on the surface of spherical particles, and doping with iron and cerium yields strong photocatalytic activity.

3.4 Effect of pH on the degradation of "trinitrogen" by SiO₂@TiO₂-Fe-Ce catalyst with or without photocatalysis

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 $Fe^{3+}+H_2O_2 \rightarrow Fe-OOH_2+H^+(3-3)$ 326

$$Ce^{3+}+HO \rightarrow Ce^{4+}+OH^{-}(3-8)$$

 $Fe-OOH^{2+} \rightarrow Fe^{2+} + HO_2 \cdot (3-4)$ 327

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 $Ce^{3+}+HO_2/O_2^{-} \rightarrow Ce^{4+}+H_2O(3-9)$ $Fe^{3+}+HO_2 \rightarrow Fe^{2+}+O_2+H^+(3-5)$ $Ce^{4+}+H_2O_2 \rightarrow HO_2 \cdot /O_2 \cdot +H^+ (3-10)$ $Ce^{4+}+HO_2\cdot/O_2^{-}\to Ce^{3+}+H^++O_2(3-11)$

 Ce^{4+} cannot be produced when the pH of the system is less than 4.0, and its 330 removal cannot be enhanced. Increase in pH to 5.0 generates intermediates of 331 $Ce(OH)_3OOH$ in the system, which promote the conversion of Ce^{3+} to Ce^{4+} as well as 332 the generation of HO₂·/O₂-·, facilitating the conversion of Fe³⁺ to Fe²⁺, thereby 333 generating additional HO \cdot and improving the reaction performance. Figure 4.8(b) 334 shows the same trend as Figure 4.7(a), with a degradation efficiency of 63.4% without 335 336 significant difference at pH 7.0 and 9.0. Figure 4(c) shows the degradation of nitrite nitrogen, with the highest degradation efficiency of 64.2% at pH 5.0. 337

Figures 4 (d) (e) and (f) show the degradation efficiency of SiO₂@TiO₂-Fe-Ce 338 catalyst for "trinitrogen" under different pH values, indicating that the increase of 339 system pH enhances degradation rate of "three nitrogens". The degradation efficiency 340 was the best at pH 11. The removal rate of ammonia nitrogen reached 75.9%, while the 341 342 removal efficiency of nitrate nitrogen reached 71.3%, and the removal efficiency of nitrite nitrogen reached 71.3%. The rate of 70.1% may be explained by the effect of 343 initial pH of the system on the presence of "trinitrogen" in the solution. A gradual 344 345 increase in the pH increases the number of OH⁻ ions in the system generated by photo-346 Fenton catalysis. The increase of OH^{\cdot} in the presence of ammonia nitrogen generates further free NH3 in the solution. The rare earth element Ce generates electrons and 347 holes due to its unique outer electronic structure. In addition, Ce also carries a specific 348 oxygen storage capacity. It can increase the charge generated on the surface of the 349 SiO₂@TiO₂-Fe-Ce catalyst, which is conducive to the transfer of holes from the interior 350 of the particles to the surface for "trinitrogen" adsorption. A large amount of OH- on 351 the entire interface is also conducive to $OH \cdot generation$. Further, as the reduced steric 352 hindrance of the free "trinitrogen" facilitates the catalytic reaction while Fe is a better 353 hole-trapping agent with a strong synergistic effect when combined with Ce, which 354 greatly increases the overall catalytic activity. The removal efficiency of the "three 355 nitrogens" is also increased. The relevant reactions are represented by equations (3-12) 356 to (3-19): 357

 $SiO_2(a)TiO_2$ -Fe-Ce+ hv \rightarrow $SiO_2(a)TiO_2$ -Fe-Ce+ (e⁻+ h⁺) (3-12)358

 $Ce^{4+} + e^{-} \rightarrow Ce^{3+}$

(3-13)

359

 $Fe^{3+} + e^{-} \rightarrow Fe^{2+}$ (3-14)360

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$$Ce^{3+} + O_2 \rightarrow Ce^{4+} + O_2^{-}$$
 (3-15)
362 $Fe^{2+} + O_2 \rightarrow Fe^{3+} + O_2^{-}$ (3-16)

$$H_2O + h^+ \rightarrow H^+ + \cdot OH \qquad (3-17)$$

$$364 \qquad \cdot O_2^- + 2H^+ \rightarrow 2 \cdot OH \qquad (3-18)$$

365
$$Dye^+ + \cdot HO \rightarrow degradation products$$
 (3-19)

366 3.5 Effect of H₂O₂ dosing concentration on photocatalytic degradation rate of

367 "trinitrogen"





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Fig. 5 The degradation rate of the "three nitrogen" by catalysts under different H₂O₂ dosing concentrations. (a) ammonia nitrogen, (b) nitrate nitrogen, (c) nitrite nitrogen

It can be seen from Figure 5 that under similar experimental conditions, the 380 increases H₂O₂ dosage increases the rate of photocatalytic degradation of "trinitrogen" 381 initially, followed by a decline. When the dosage of H₂O₂ was 80 mmol/L the 382 degradation efficiency of the catalysts for "three nitrogens" reached the highest level, 383 with a 79.8% degradation rate for ammonia nitrogen, whereas the degradation rate of 384 nitrate nitrogen was 74.6%, and the degradation rate of nitrite nitrogen was 73.7%. 385 H₂O₂ itself captures the photogenerated electrons. The addition of Fe prolongs the 386 recombination of holes and electrons. The doping of rare earth Ce results in additional 387

photogeneration of electrons by the holes. In the case of UV light irradiation, H_2O_2 itself decomposes to generate adequate OH·, suggesting that Fe-Ce-SiO₂/TiO₂ catalyst and H_2O_2 exhibit a strong synergistic effect under UV light. Excessive concentrations of H_2O_2 have a negative effect on the overall catalysis probably because the high levels of H_2O_2 and self-clearance contribute to the reduction of OH· and attenuation of the "trinitrogen" degradation.

394 3.6 Degradation rate of "trinitrogen" under different catalytic systems

395 3.6.1 Effects of different catalytic systems on the degradation rate of ammonia nitrogen



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Figure 6 Photocatalytic degradation of ammonia nitrogen. Pseudo-first-order kinetic equation of photocatalytic degradation of ammonia nitrogen

Figure 6a shows the degradation rate of ammonia nitrogen by sample SiO_2/TiO_2 410 under dark conditions and the degradation rate curves of SiO₂/TiO₂, Fe-SiO₂/TiO₂, Ce-411 SiO₂/TiO₂ and Fe-Ce-SiO₂/TiO₂ under UV light. As shown in the Figure, the efficiency 412 of catalytic degradation of ammonia nitrogen under UV light is greatly improved 413 414 compared with dark conditions. Compared with Fe-SiO₂/TiO₂ and Ce-SiO₂/TiO₂, the ammonia nitrogen degradation rate of TiO₂ samples and Fe-Cerium co-doped samples 415 is always higher than that of single dopants. The degradation rate of ammonia nitrogen 416 reached 88.7% within 120 min, which was 10%-20 higher than under other conditions, 417 indicating that the photocatalytic performance of the catalyst was significantly 418 419 improved after doping with iron and cerium. The improved performance of the catalyst after iron-cerium bimetallic doping may be due to the formation of Ti-O-Si bonds after 420 TiO₂ was added to the system, indicating the formation of additional defects and 421 electron capture, which further inhibited the agglomeration of nanoparticles in the 422 system. Ce^{4+} in the form of Ce^{3+}/Ce^{4+} ion pair captures photogenerated electrons as a 423

424 Lewis acid, which facilitated the separation of electron-hole pairs.

Δ	25	5

Sample/Condition	First order kinetic	R ²	K(min ⁻¹)
	equation		
SiO ₂ /TiO ₂ dull	y =0.00205x-0.023	0.96977	0.00205
SiO ₂ /TiO ₂ UV light	y =0.0033x+0.012	0.98667	0.0033
Fe-SiO ₂ /TiO ₂ UV light	y=0.00795x-0.067	0.97419	0.00795
Ce-SiO ₂ /TiO ₂ UV light	y =0.0077x+0.162	0.95987	0.0077
Fe-Ce-SiO ₂ /TiO ₂ UV light	v = 0.01165x + 0.047	0 98439	0.01165

Table 1 Kinetic equation of ammonia nitrogen solution degradation with different catalysts

426 Figure 6b represents the kinetic reaction equation of different catalysts using UV light as the light source. The change in ammonia nitrogen concentration curve under 427 different reaction times fitted the kinetic curve, based on the kinetic equation under 428 different series. The catalytic degradation of ammonia nitrogen conforms to first-order 429 430 kinetic equation. The fitting parameters of the first-order kinetic equation are shown in 431 Table 1. The relatively high linear correlation suggests increased catalytic degradation 432 of ammonia nitrogen in dilute solution. The photocatalytic degradation reaction basically follows the first-order kinetic equation. 433





SiO ₂ /TiO ₂ UV light	y =0.0017x+0.0695	0.9805	0.0017
Fe-SiO ₂ /TiO ₂ UV light	y =0.0177x+0.1085	0.97395	0.0177
Ce-SiO ₂ /TiO ₂ UV light	y =0.0243x+0.1895	0.9735	0.0243
Fe-Ce-SiO ₂ /TiO ₂ UV light	y =0.0316x+0.2442	0.9736	0.0316

Figure 7b represents the kinetic reaction equation of different catalysts using UV light. The change in the nitrate nitrogen concentration under different reaction times is subjected to kinetic curve fitting. The fitting kinetic equation under different series suggests that the catalytic degradation of nitrate nitrogen conforms to first-order reaction kinetics, and the fitting parameters of the first-order kinetic equation are shown in Table 2. The high linear correlation suggests that the photocatalytic degradation of nitrate nitrogen in dilute solution follows the first-order kinetics.

457 3.6.3 Effects of different catalytic systems on nitrite nitrogen degradation rate



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Figure 8(a) Photocatalytic degradation of nitrite nitrogen; (b) pseudo-first-order kinetic equation representing photocatalytic degradation of nitrite nitrogen

Figure 8(a) shows the degradation rate of nitrite nitrogen under different catalytic systems. As shown in the Figure, the catalytic degradation rate of nitrite nitrogen under UV light is significantly higher than that under dark conditions, indicating that the photo-Fenton-catalyzed degradation effectively improves the degradation efficiency of nitrite nitrogen. The degradation efficiency of bimetallic doping was higher than that of single metal, reaching 80.2% within 120 min, indicating a synergistic effect of ironcerium bimetallic combination.

480 Table 3 Kinetic equations of degradation of nitrite nitrogen solution by different catalysts

Sample/Condition	First order kinetic	R ²	K(min ⁻¹)
	equation		
SiO ₂ /TiO ₂ dull	y =0.00103x-0.00476	0.94704	0.00103
SiO ₂ /TiO ₂ UV light	y =0.01674x-0.03048	0.99627	0.01674
Fe-SiO ₂ /TiO ₂ UV light	y =0.02254x-0.01381	0.9978	0.02254
Ce-SiO ₂ /TiO ₂ UV light	y =0.02257x-0.01289	0.97349	0.02257
Fe-Ce-SiO ₂ /TiO ₂ UV light	y=0.03117x+0.2381	0.96199	0.03117

As shown in Figure 8(b) and Table 3, the photo-Fenton-catalyzed degradation of 482 nitrite nitrogen by Fe-Ce-SiO₂/TiO₂ catalyst conforms to the first-order reaction 483 kinetics, and its linear relationship is represented by the equation, y = 0.03117x +484 $0.2381, R^2 = 0.96199.$ 485

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3.7 Catalytic degradation products and possible mechanisms 487

488 Figure 9(a) shows the levels of various components of the degradation products following 6 sessions of photocatalysis of ammonia nitrogen simulating wastewater 489



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nitrate nitrogen (b) and nitrite nitrogen (c) degradation products

As shown in Figure 9(a), the final levels of nitrate nitrogen and nitrite nitrogen in 495 1 mg/mL of ammonia nitrogen degradation products were 0.114 mg/mL and 0.012 496 mg/mL, respectively, while the degradation rate of ammonia nitrogen under this 497 condition was 88.7%, suggesting that nearly 62.08% of ammonia nitrogen was finally 498 converted to N₂ in the whole reaction. Kishor (Kishor et al. 2015) proposed that strong 499 oxidizing free radicals and superoxide ions are generated during ammonia nitrogen 500 degradation by this series of catalysts, which induces a series of redox reactions 501 summarized by the reaction equations (3-20) to (3-24): 502

 $NH_4^++2OH^- \rightarrow NO_2^-+3H_2$

 $NO_3^++2H^++2e^-\rightarrow NO_2^-+H_2O$

 $NO_3^-+10H^++8e^-\rightarrow NH_4^++3H_2O$

 $2NO_3^++12H^++10e^- \rightarrow 2N_2+3H_2O$

 $2NO_2 + O_2 \rightarrow 2NO_3$

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510 The above equations indicate that specific intermediates are generated during 511 ammonia nitrogen degradation, and approximately 62.08% of ammonia nitrogen may 512 eventually be converted to N₂.

(3-20)

(3-21)

(3-22)

(3-23)

(3-24)

As shown in Figure 9(b), the degradation rate of nitrate nitrogen gradually increased at the beginning of the reaction, reaching 71.1% at 120 min. The degradation of nitrate nitrogen gradually increased the levels of nitrite nitrogen and ammonia nitrogen in the system. The nitrite nitrogen content reached the maximum within 40 min, followed by a decline eventually, while the ammonia nitrogen content increased and plateaued, indicating that nitrite nitrogen was an intermediate, and its degradation mechanism is shown in Figure 10 (a).

As shown in Figure 9(c), the final degradation product of nitrite nitrogen was 520 ammonia nitrogen, with a degradation efficiency reaching 71.4% within 120 min, and 521 the final ammonia nitrogen concentration was 12.3 mg/L, indicating the presence of 522 gaseous products during the degradation. The formation of NO_2^- may involve N₂, NO, 523 N₂O and other nitrogen oxides, and the overall gaseous product conversion efficiency 524 was calculated to be 38.12%, indicating that the photocatalytic degradation of NO₂⁻ 525 entailed oxidation and reduction (Ebrahimi et al. 2017). The primary oxide species 526 carry photogenerated holes (h⁺), superoxide (O₂-) and hydroxyl radicals (.OH) during 527 heterogeneous photocatalytic degradation(Tomova et al. 2015). Figure 10(b) shows the 528 possible degradation mechanism. 529





Fig.10 (a) Possible mechanism of photocatalytic degradation of nitrate nitrogen; (b) Possible mechanism of photocatalytic degradation of nitrite nitrogen

Figure 10(a) shows the possible mechanism of photocatalytic degradation of nitrate nitrogen, suggesting that N₂ and ammonia nitrogen are the final degradation products. The first step of nitrate photolysis involves the transition of $\pi \rightarrow \pi *$ in the excited state. The unstable nitrate species is produced as shown in equation (3-26). The NO₂· preferentially dimerizes and releases N₂O₄, followed by rapid hydrolysis and subsequent generation of NO₂⁻, which is reduced to NH⁴⁺ and N₂(Sowmya et al. 2014; Dong et al. 2019). The related reaction equations are as follows:

 $H_{2}O+h_{vb}^{+} \rightarrow H^{+}+OH^{-} (3-25)$ $O^{-}+H_{2}O \rightleftharpoons OH^{-}+OH^{-} (3-27)$ $2NO_{2}^{-} \leftrightharpoons N_{2}O_{4} (3-29)$ $NO_{3}^{-}+e^{-} \rightarrow NO_{3}^{2-} (3-31)$ $NO_{2}^{-}+e^{-} \rightarrow NO_{2}^{-} (3-33)$ $2NO_{2}^{-}+8H^{+}+6e^{-} \rightarrow N_{2}+4H_{2}O (3-35)$

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540

542 4 Conclusion

In this study, Fe-Ce-SiO₂/TiO₂ catalyst was fabricated by introducing TiO₂ into the catalytic system and using tetrabutyl titanate as the precursor via impregnation. The catalyst was characterized by XRD, FT-IR, BET, TEM, SEM, XPS and other methods. The results show that TiO₂ in the catalyst exists in the form of anatase on the surface, and the prepared catalyst carries a high specific surface area (455.8 m²/g) and pore volume (0.6025 cm³/g). The catalyst exhibits high dispersibility, and the iron and cerium elements in the system exist in the form of Fe²⁺/Fe³⁺ and Ce³⁺/Ce⁴⁺. In addition, the photo-Fenton degradation performance of "trinitrogen" in the catalyst was studied. The results showed optimal photocatalytic effect of Fenton's reagent at a catalyst dosage of 0.01 g, pH 11.0, and H₂O₂ concentration of 80 mmol/L. The degradation efficiency of "trinitrogen" remained above 70%. The photo-Fenton degradation of "trinitrogen" under different catalytic systems conformed to first-order reaction kinetics. The corresponding degradation products of "trinitrogen" were analyzed.

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Authors Contributions

- 558 Jie Li: Methodology, Investigation.
- 559 Yuxiang Yang: Conceptualization, Supervision, Writing-Original Draft, Project
- administration, Funding acquisition, Writing and Editing.
- 561 Yan Huang: Formal analysis, Visualization.
- 562 Hongming Yuan: Validation, Resources.
- 563 **Zhiyong Han:** Data Curation.
- 564 **Chaoying Ni:** Reviewing.
- 565

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- 573 **Ethics approval and consent to participate:** Not applicable.
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- 576

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