

# Purification Effect Evaluation of the Designed New Volcanic Soil Adsorption Material Containing Bioreactor for Eutrophic Water Treatment

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## Research Article

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2 **containing bioreactor for eutrophic water treatment**

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16

17 **Abstract**

18 To investigate the purification effect of the new adsorption material containing  
19 bioreactor and the critical role of non-culture (VBNC) bacteria in eutrophication  
20 ecosystem, major water quality parameters and microbial community were determined  
21 and analyzed in prepared eutrophic water for 2 years monitoring. The results showed  
22 that removal rates of total phosphorus (TP), total nitrogen (TN), chlorophyll-a (Chl-a)  
23 and chemical oxygen demand (COD) ranged of 90.7% - 95.9%, 84.5% - 92.4%, 87.9% -  
24 95.8% and 68.3% - 82.7%, respectively, indicating the designed bioreactor possessed  
25 high efficiency in eutrophic water treatment. Although the bioreactor had been operated  
26 for 2 years, water from treatment group was more clearer and odorless than control  
27 group, exhibiting the long service life of the bioreactor. Stopping operation in August  
28 caused the removal rates of major water quality parameters significantly decrease ( $p <$   
29 0.05), revealing stopping operation and high temperature in Summer exerted dual effect  
30 on the bioreactor, whereas the impact could be minimized when the bioreactor was  
31 running. According to most probable number (MPN) method, the total bacteria under  
32 +Rpf treatment were higher than under -Rpf treatment, implying Rpf could resuscitate  
33 VBNC bacteria in eutrophication ecosystem. Nine VBNC bacteria were isolated based  
34 on the BLAST results of 16S rRNA gene, and these bacteria might contribute to  
35 eutrophic water treatment based on their functions, such as phosphorus-collecting and  
36 denitrification. Those results provided new insights for engineering technology  
37 innovation and had benefit in eutrophic water treatment.

38 **Keywords** Eutrophication · volcanic soil · bioreactor · viable but non-culture (VBNC)

39 bacteria · resuscitation-promoting factor (Rpf)

40

## 41 **Introduction**

42 In recent decades, aquatic ecosystem has suffered much more serious problems of  
43 water eutrophication due to anthropogenic pollution and climate change (Le et al. 2010;  
44 Smith 2003; Kosten et al. 2012; Andersen et al. 2020a; Freeman et al. 2020).  
45 Eutrophication is often accompanied with rapid occurrences of harmful algal blooms  
46 (HABs), especially of chlorella, cyanobacteria (Wang et al. 2019a), and diatoms (Paerl  
47 et al. 2016, 2019; Huisman et al. 2018; Woolway et al. 2019; Kim et al. 2020), which  
48 threaten other aquatic life and change the color and/or odor of the water body  
49 (Vollenweider and Kerekes 1982). Therefore, eutrophic water will finally lose its  
50 original functionality, such as aquatic food production and safe-drinking water supply  
51 (Huisman et al. 2018). Meanwhile, eutrophication is worldwide environmental  
52 problems and have been found in many countries, such as Israel (Geisler et al. 2020),  
53 Mexico (Caballero and Vazquez 2020) and USA (Tomasko et al. 2020). It is  
54 summarized that over 75% of the closed water bodies (e.g., lakes, ponds and reservoirs)  
55 in Africa, Asia and Latin America have deteriorated largely and encountered some  
56 extents of eutrophication since the 1990s (UN-Water 2018).

57 Evaluating the trophic state of eutrophic water have become a research hotspot in  
58 the water ecology community based on several water quality parameters, including total  
59 phosphorus (TP), total nitrogen (TN), chlorophyll-a (Chl-a) and chemical oxygen  
60 demand (COD) (Chao Rodriguez et al. 2014; Smith and Schindler 2009; Carlson 1977).  
61 Previous studies demonstrated that the excessive accumulation of N and P in aquatic

62 ecosystem is closely related to eutrophication, which, on the one hand, causes greater  
63 primary production (Ahlgren et al. 2005; Feuchtmayr et al. 2009) and, on the other hand,  
64 hinders the restoration process of the eutrophic ecosystem (Banerjee 2016), thus results  
65 in hyper-eutrophication and subsequent water quality deterioration (Ahlgren et al. 2005).  
66 At the same time, Chl-a and COD are the key indicators of eutrophic water, which  
67 reflect the eutrophication level and the biomass of HABs, and further uncover the  
68 intrinsic essence of eutrophication. Therefore, systematically monitoring the trophic  
69 state of aquatic ecosystem can effectively evaluate the degree of eutrophication and  
70 assess the feasibility of new technical for eutrophic aquatic ecosystem restoration.

71 Former experiences in eutrophic aquatic ecosystem restorations specifically  
72 emphasizing reductions of external nutrient inputs might fail to alleviate the  
73 eutrophication (Paerl et al. 2016; Wang et al. 2019a; Lurling and Mucci 2020). As  
74 plenty of studies announce that effective removal of excessive N and P are of concern  
75 for the aquatic ecosystem balance (Gruber and Galloway 2008; Domangue and  
76 Mortazavi 2018; Stoliker et al. 2016), the potential impacts from internal nutrient  
77 eliminating should be taken into considerations for eutrophic water treatment (Paerl et al.  
78 2019; Wang et al. 2019a; Qin et al. 2020). Physical (Schauer et al. 2003), chemical  
79 (Walpersdorf et al. 2004; Wauer et al. 2005) and biological (Xu et al. 2011; Liu et al.  
80 2012; Lu et al. 2014; Petersen et al. 2014; Wu et al. 2015) methods were adopted in  
81 extensive researches during the past decades. However, as the reason of financial and  
82 labor-intensive challenge, limited to biotic and abiotic restriction and high risk of

83 secondary pollution, these methods were difficult to meet the high frequency for  
84 eutrophic water treatment, especially for projects with wide distributions (Liang et al.  
85 2014). Hence, new ecological techniques are considered to be the most promising  
86 technology depending on its unique features.

87 Nowadays, numerous studies have reported that new volcanic soil adsorption  
88 materials and microbial communities also played important roles in water purification  
89 (Ding et al. 2009, 2011; Zhou and Wang 2010). Simultaneously, viable but  
90 non-culturable (VBNC) bacteria are frequently found in dyeing workshop (Jin et al.  
91 2017), pharmaceutical waste water (Li et al. 2014) and polychlorinated biphenyls (PCBs)  
92 (Su et al. 2014) polluted soils in recent years. The VBNC bacteria can survive under  
93 extreme environments by passing into the viable but non-culturable state, and can  
94 become culturable under the condition of adding resuscitation promoting factor (Rpf)  
95 cultivation (Ding et al. 2011; Mukamolova et al. 2002; Serpaggi et al. 2012). Previous  
96 studies have certified a number of VBNC bacteria could be recovered by Rpf, including  
97 high G+C gram-positive bacteria, low G+C gram-positive bacteria and several  
98 gram-negative bacteria (Ding et al. 2011; Yu et al. 2015). However, whether VBNC  
99 bacteria surviving in eutrophic water and weather VBNC bacteria possessing certain  
100 environmental purification function had not been reported to the best of our knowledge.

101 In this study, a new volcanic soil adsorption material containing multi-stage  
102 tandem type bioreactor has been designed. The purification effect of eutrophic water (TP,  
103 TN, Chl-a and COD) and the functional microbial communities, especially VBNC

104 bacteria, have been assessed and analyzed based on seasonal changing. This work has  
105 benefit in further understanding the microbial clustering in sewage treatment system and  
106 provide new insights for enhancing the efficiency of eutrophic water treatment by  
107 improving the engineering technology.

## 108 **Materials and methods**

### 109 **Preparation of eutrophic water**

110 The water sample in the bioreactor was composed of synthetic nutrient matrix  
111 mixed with raw water from a eutrophic lake (Xinyue lake, Jinhua, China), and the ratio  
112 of synthetic nutrient matrix and raw water was 97:3 (V/V). The initial compositions of  
113 synthetic nutrient matrix were as follows: beef extract (1.000 g), yeast extract (1.000 g),  
114  $K_2HPO_4$  (0.272 g),  $KH_2PO_4$  (0.456 g), water (1.0 L). The quality parameters of water  
115 sample were TP 22.4 mg/L, TN 16.5 mg/L, Chl-a 218.5  $\mu$ g/L and COD 202.4 mg/L. The  
116 water sample (100 L) recycling treatment in the bioreactor was denoted as treatment  
117 group, and the other water sample (100 L) placement under natural condition was  
118 denoted as control group.

### 119 **The novel adsorption material**

120 The novel adsorption material in the bioreactor was a mixture of several efficient  
121 adsorption materials, which made from volcanic soil. It had granular appearance and its  
122 diameter ranged from 2 to 4 mm (Fig. 1) (Ding et al. 2009). The surface area of 1 L  
123 novel adsorption material can be up to 21,476  $m^2$  and is suit for microbial habitat as its

124 micron-scale holes. Therefore, when sewage flowed through the bioreactor, the new  
125 adsorption materials could effectively absorb chemicals and enrich microbial doubly.

### 126 **Construction and operation of the bioreactor**

127 The self-designed bioreactor was composed of 9 tower tanks (volume of tower  
128 tank was 550 mL), and every 3 of them were in series (Fig. 2). The water sample flowed  
129 into the bottom of the first tower tank and transferred into the bottom of the subsequent  
130 tower tank from the top of the former tower tank after flowing through the filter plate  
131 and the new adsorption material (200 g). Then the bioreactor treated water returned into  
132 reservoir through reflux pipe and merged for next purification.

133 Based on eutrophication preferred to occur in spring, summer, autumn and less  
134 outbreak in winter, 3 running and 2 stopping stages were designed during the  
135 experiment. Two years stable operation scheme of the bioreactor was enacted as follows:  
136 1 year running before summer - stopping in summer - running in autumn - stopping in  
137 winter - running after winter. The details for actual operation and the environmental  
138 temperature were listed in Table 1.

### 139 **Water quality parameters detection**

140 The major water quality parameters of water samples were detected about every 3  
141 months both in treatment and control group. The TP, TN, Chl-a and COD were  
142 measured according to ammonium molybdate spectrophotometric method, alkaline  
143 potassium persulfate digestion UV spectrophotometric method, spectrophotometric

144 method and HACH method, respectively. The removal rates were calculated through the  
145 following equation:  $R = (1 - C/C_0) \times 100\%$ , where R was the removal rate (%) of major  
146 water quality parameter, C and  $C_0$  were the concentrations of major water quality  
147 parameter in treatment and control group, respectively. Three replicates were set for  
148 control and treatment group of water samples. T-test was performed using SPSS 19.0  
149 software. The results were expressed as the mean  $\pm$  SD (standard deviation).

#### 150 **TP detection**

151 The water sample was adjusted to neutral and then 25 mL water sample was  
152 transferred into a 50 mL plug scale tube. About 4 mL  $K_2S_2O_8$  solution was added into  
153 the plug scale tube for digestion in a autoclave. Two hours later, when temperature  
154 dropped to 80°C, the plug scale was took out and diluted to the tick mark with ultrapure  
155 water. Ascorbic acid (1 mL) was added to the diluted digestion solution and then mixed  
156 completely. Thirty seconds later, 2 mL molybdate solution were added into the plug  
157 scale and placed for 15 min at room temperature. The absorbance was determined at the  
158 wavelength of 700 nm. The content of TP was determined according to the following  
159 formula:

$$160 \quad TP \text{ (mg/L)} = m/V;$$

161 where “m” was the P content in water sample ( $\mu\text{g}$ ), “V” was the volume of water  
162 sample (mL).

#### 163 **TN detection**

164 The pH of water sample was adjusted to 5 - 9 and 10 mL water sample was  
165 transferred into a 25 mL colorimetric tube. About 5 mL alkaline potassium persulfate  
166 solution was added into the colorimetric tube for digestion in a autoclave. Thirty  
167 minutes later, when pressure dropped to 80°C, the colorimetric tube was took out and  
168 cooled down. Hydrochloric acid (1 mL) was added into the digestion solution and then  
169 diluted to the tick mark with ultrapure water. About 5 mL diluted solution were added to  
170 cuvette. The absorbance was determined at the wavelength of 200 and 275 nm, and the  
171 absorbance  $A = A_{220} - A_{275}$ . The content of TN was determined according to the  
172 following formula:

$$173 \quad \text{TN (mg/L)} = m/V;$$

174 where “m” was the N content in water sample ( $\mu\text{g}$ ), “V” was the volume of water  
175 sample (mL).

#### 176 **Chl-a detection**

177 Water sample (1000 mL) and 1%  $\text{MgCO}_3$  (5 mL) were mixed completely. About  
178 200 mL mixtrue was filtered with 0.45  $\mu\text{m}$  glass fiber filter film. When filtering finished,  
179 the filter film was clamped out with clean tweezers. After folded in half twice, the filter  
180 film was put into a centrifuge tube with 10 mL 95% ethanol and incubated at 4°C for 20  
181 h. Following the centrifuge tube were 3000 rpm centrifuged for 15 min and then  
182 determined the absorbance at the wavelength of 649, 665 and 750 nm. The content of  
183 Chl-a was determined according to the following formula:

$$184 \quad \text{Chl-a} = (13.7 * (A_{665} - A_{750}) - 5.76 * (A_{649} - A_{750})) * (E/F) * L;$$

185 where “E” was the extraction volume (mL), “F” was the filtration volume (L), “L”  
186 was the width of cuvette (mm).

### 187 **COD detection**

188 Water sample (2.5 mL), K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub> solution (1.5 mL) and Ag<sub>2</sub>SO<sub>4</sub> solution (3.5 mL)  
189 were mixed completely in HACH. Then the mixture was digested under 150°C for 2 h  
190 and cooled down for 30 min. The absorbance was determined by DR1010.

### 191 **Most probable number (MPN) method for bacteria identification in the bioreactor**

192 Bacteria were isolated from the bioreactor using the most probable number (MPN)  
193 method (McCrary et al. 1915). The VBNC bacteria were isolated by adding Rpf protein  
194 coming from *Micrococcus luteus* culture supernatant (Ding et al. 2012; Su et al. 2014).  
195 The liquid medium consisted of peptone 5.0 g, yeast extract 0.5 g, glucose 5.0 g, sodium  
196 chloride 2.5 g, distilled water 1.0 L, pH 7.0-7.2, including the active Rpf (+Rpf) and  
197 inactive Rpf (-Rpf), respectively, where the volume ratio was 4:1. Three replicates were  
198 set for adding +Rpf and -Rpf treatments, respectively. The bacteria solution was  
199 prepared by mixing weighted 1 g novel volcanic soil adsorption material and 9 mL 0.9%  
200 normal saline. Bacteria solution (0.25 mL) and liquid medium (2.25 mL) was mixed.  
201 Then, the mixture was gradually diluted from 10<sup>-1</sup> to 10<sup>-7</sup> with the prepared liquid  
202 medium. The bacteria solution with different dilutions were incubated at 30°C and the  
203 turbidity of bacteria solution was measured by microplate reader at the wavelength of  
204 660 nm (OD<sub>660</sub>). When the flora was in stationary phase, turbidity or non-turbidity of

205 the cultivate tube was recorded as positive or negative, respectively. The total number of  
206 bacteria in +Rpf and -Rpf treatments were determined by the MPN table (Fig. S1).

### 207 **Rpf effect and VBNC bacteria status evaluation**

208  $V_R$  was the ratio of total amount of bacteria in +Rpf treatment and in -Rpf  
209 treatment, and was used to evaluate the activity abundance of Rpf.  $V_R$  greater than 5  
210 indicated that there had dominant bacteria in VBNC state, which was sensitive to Rpf.

211 Denaturing Gradient Gel Electrophoresis (DGGE) of the diluted bacteria solution  
212 from  $10^{-1}$  to  $10^{-6}$  in +Rpf and -Rpf treatments were also carried out to identify the  
213 presence of VBNC bacteria. Genomic DNA was extracted using the MiniBEST  
214 Bacterial Genomic DNA Extraction Kit Ver.2.0 (Takara, Dalian, China), and 16S rDNA  
215 V3 region was amplified by the following primers: F, 5'-CGCCCGCCG  
216 CGCGCGGCGGGCGGGGCGGGGGCACGGGGGGCCTACGGGAGGCAGCAG-3'  
217 and R, 5'-ATTACCGCGGCTGCTGG-3'. The PCR amplified procedure was shown in  
218 Table S1.

219 The PCR product was detected by 1% agarose gel electrophoresis (AGE) and  
220 purified. The qualified PCR products was separated by denaturing gradient gel  
221 electrophoresis (DGGE) with 8% polyacrylamide and 40%-60% denaturing solution.

### 222 **Constructing the phylogenetic trees of the isolated bacteria**

223 16S rRNA gene of the bacteria, which isolated from the bioreactor, was amplified  
224 by the primers: F, 5'-AGAGTTTGATCCTGGCTCAG-3', and R, 5'-GGCTACCTTGTT

225 ACGA-3'. The sequences of 16S rRNA gene were blasted in NCBI ([http://www.](http://www.ncbi.nlm.nih.gov/)  
226 [ncbi.nlm.nih.gov/](http://www.ncbi.nlm.nih.gov/)) and EzTaxon server (<http://www.eztaxon.org/>) to identify the genera  
227 of bacteria. The phylogenetic tree of all isolated bacteria was constructed by MEGA 5.0.  
228 The neighbor-joining method was selected in the instruction of phylogenetic tree  
229 (Saitou and Nei 1987). The evolutionary distance matrix was calculated using Kimura's  
230 two-parameter method (Kimura 1980). And the bootstrap values were set for 1000  
231 replications (Felsenstein 1985).

## 232 **Results**

### 233 **Removal effect of TP in the bioreactor**

234 The TP concentrations in water sample (both in control and treatment groups) and  
235 the removal rate of the bioreactor were shown in Fig. 3. The TP concentrations ranged  
236 of 0.91 - 2.06 mg/L and 20.09 - 23.38 mg/L in treatment group and control group,  
237 respectively. All of the TP concentrations in treatment group were significantly lower  
238 than in control group ( $p < 0.05$ ), no matter the bioreactor was running or stopping. The  
239 TP removal rates of the bioreactor ranged from 90.7% to 95.9%, indicating the  
240 bioreactor could efficiently reduce the TP concentration of eutrophic water. The TP  
241 removal rate in February of TY was 92.8% and was significantly lower than in  
242 November of SY (94.2%) and May of TY (94.4%) ( $p < 0.05$ ), showing bioreactor  
243 stopping operation affected TP elimination. Meanwhile, the TP removal rate in August  
244 of SY was 90.7% and was significantly lower than other detection months ( $p < 0.05$ ),

245 exhibiting the bioreactor stopping and the high temperature were the two key factors for  
246 influencing TP removing. What's more, the TP removal rate in March of SY (95.9%)  
247 were significantly higher than the other detection months ( $p < 0.05$ ), implying the  
248 bioreactor had the best purification effect in Spring.

#### 249 **Removal effect of TN in the bioreactor**

250 The TN concentrations in water sample (both in control and treatment groups) and  
251 the removal rate of the bioreactor were shown in Fig. 4. The TN concentrations ranged  
252 of 1.32 - 2.44 mg/L and 13.86 - 17.50 mg/L in treatment group and control group,  
253 respectively. All of the TN concentrations in treatment group were significantly lower  
254 than in control group ( $p < 0.05$ ), no matter the bioreactor was running or stopping. The  
255 TN removal rates of the bioreactor ranged from 84.5% to 92.4%, indicating the  
256 bioreactor could effectively reduce the TN concentration of eutrophic water. The TN  
257 removal rate in February of TY was 85.8% and was significantly lower than in  
258 November of SY (89.6%) and May of TY (91.8%) ( $p < 0.05$ ), showing the bioreactor  
259 stopping operation affected TN elimination. Meanwhile, the TN removal rate in August  
260 of SY was 84.5% and was significantly lower than other detection months ( $p < 0.05$ ),  
261 exhibiting the bioreactor stopping and the high temperature also influenced TN  
262 removing. Simultaneously, the TN removal rate in March of SY (92.4%) were  
263 significantly higher than the other detection months, except in September of FY (91.9%)  
264 and May of TY (91.8%), suggesting the bioreactor had the better purification effect in  
265 Spring and Autumn.

266 **Removal effect of Chl-a in the bioreactor**

267 The Chl-a concentrations in water sample (both in control and treatment groups)  
268 and the removal rate of the bioreactor were shown in Fig. 5a. The Chl-a concentrations  
269 ranged of 8.41 - 28.46 µg/L and 200.11 - 234.38 µg/L in treatment group and control  
270 group, respectively. All of the Chl-a concentrations in treatment group were  
271 significantly lower than in control group ( $p < 0.05$ ), no matter the bioreactor was  
272 running or stopping. The Chl-a removal rates of the bioreactor ranged from 87.9% to  
273 95.8%, indicating the bioreactor could efficient reduce the Chl-a concentration of  
274 eutrophic water. The Chl-a removal rate in February of TY was 93.7% and was  
275 significantly lower than in November of SY (95.2%) and May of TY (95.8%) ( $p < 0.05$ ),  
276 showing bioreactor stopping operation affected Chl-a elimination. Meanwhile, the Chl-a  
277 removal rate in August of SY was 87.9% and was significantly lower than other  
278 detection months ( $p < 0.05$ ), exhibiting the bioreactor stopping and the high temperature  
279 exerted doubly effect on Chl-a removing. Meanwhile, the Chl-a removal rate in March  
280 of SY (95.6%) were significantly higher than the other detection months, except in  
281 November of SY (95.2%) and May of TY (95.8%), suggesting the bioreactor had the  
282 better purification effect in Spring and Autumn. The real comparison of water sample  
283 between control and treatment group was showed in Fig. 5b.

284 **Removal effect of COD in the bioreactor**

285 The COD concentrations in water sample (both in control and treatment groups)  
286 and the removal rate of the bioreactor were shown in Fig. 6. The COD concentrations

287 ranged of 32.13 - 45.11 mg/L and 185.26 - 208.42 mg/L in treatment group and control  
288 group, respectively. All of the COD concentrations in treatment group were significantly  
289 lower than in control group ( $p < 0.05$ ), no matter the bioreactor was running or stopping.  
290 The COD removal rates of the bioreactor ranged from 68.3% to 82.7%, indicating the  
291 bioreactor could efficiently reduce the COD concentration of eutrophic water. The COD  
292 removal rate in February of TY was 78.6% and was significantly lower than in  
293 November of SY (82.7%) and May of TY (81.3%) ( $p < 0.05$ ), showing bioreactor  
294 stopping operation affected COD elimination. Meanwhile, the COD removal rate in  
295 August of SY was 68.3% and was significantly lower than other detection months ( $p <$   
296  $0.05$ ), exhibiting the bioreactor stopping and the high temperature severely affected  
297 COD cleaning. Meanwhile, the COD removal rate in March of SY (82.5%) was  
298 significantly higher than the other detection months, except in November of SY (82.7%),  
299 suggesting the bioreactor had the better purification effect in Spring and Autumn.

### 300 **The OD<sub>660</sub> value of bacteria solution in +Rpf and -Rpf treatment**

301 In present study, bacteria were cultivated by using MPN method. The OD<sub>660</sub> values  
302 in the stationary phase of bacteria solution were listed in Table 2. No significant  
303 difference of OD<sub>660</sub> values were observed between +Rpf and -Rpf treatment under the  
304 dilution of  $10^{-1}$  and  $10^{-3}$ , respectively. However, the OD<sub>660</sub> values under the dilution  
305 from  $10^{-4}$  to  $10^{-6}$  were continuously higher in +Rpf treatment than in -Rpf treatment,  
306 revealing the number, species or number and species of bacteria was increased under the  
307 adjunction of Rpf. The total number of bacteria attached on the novel volcanic soil

308 adsorption material were  $2.4 \times 10^9$  and  $1.1 \times 10^8$  cells/g in +Rpf and -Rpf treatments,  
309 respectively. The  $V_R$  value was 21.8, indicating there had dominant bacteria in VBNC  
310 state, which were sensitive to Rpf.

### 311 **The DGGE analysis of bacteria solution in +Rpf and -Rpf treatment**

312 The PCR results of 16S rDNA V3 region in MPN culture system (same as the  
313 above experiment) were showed in Fig. 7. The target bands were clear and bright,  
314 indicating the PCR product could be used for DGGE analysis after purification.

315 For DGGE analysis, the highlight bands in the lanes of +Rpf treatment were more  
316 than -Rpf treatment, especially under the dilution from  $10^{-2}$  to  $10^{-6}$  (Fig. 8), which were  
317 in accordance with the  $OD_{660}$  values, indicating Rpf had a certain effect on promoting  
318 bacteria resuscitation in the eutrophic water treatment system. What's more, the bands  
319 under the dilution of  $10^{-3}$ ,  $10^{-5}$  and  $10^{-6}$  +Rpf treatment appeared on the top of the lanes,  
320 whereas the bands under the dilution of  $10^{-2}$  +Rpf treatment appeared at the bottom of  
321 the lane, suggesting the microbial would compete with each other and would not both  
322 take function under the same dilution.

### 323 **Blast results of 16s rDNA PCR products**

324 In this study, 24 strains of bacteria were isolated from the bioreactor (Table 3). The  
325 isolated bacteria were belonged to 11 genera, including *Bacillus*, *Brevibacillus*,  
326 *Burkholderia*, *Enterobacter*, *Lysinibacillus*, *Microbacterium*, *Micrococcus*,  
327 *Ochrobactrum*, *Paenibacillus* and *Pseudomonas*. Most of the isolated bacteria were

328 belonged to Low GC gram-positive (50%), followed by gram-negative bacteria (42%)  
329 and poor in high GC gram-positive bacteria (8%). Therefore, Rpf not only promoted the  
330 resuscitation of gram-positive bacteria, but also activated gram-negative bacteria in the  
331 bioreactor. At the same time, 9 strains of VBNC bacteria were native from 4 genera,  
332 including *Bacillus* (3), *Burkholderia* (2), *Enterobacter* (2) and *Pseudomonas* (2). The  
333 phylogenetic tree was constructed and showed in Fig. 9.

## 334 **Discussion**

### 335 **Efficient purification capacity of the volcanic soil containing bioreactor**

336 Based on former researches, TP, TN, Chl-a and COD were the major water quality  
337 parameters for evaluating the trophic state of eutrophic water (Chao Rodriguez et al.  
338 2014; Smith and Schindler 2009, Carlson 1977). Excessive accumulation of N and P in  
339 aquatic ecosystem not only caused greater primary production (Ahlgren et al. 2005,  
340 Feuchtmayr et al. 2009), but also slowed down the restoration process of water  
341 ecosystem (Banerjee 2016), thus resulted in eutrophication (Ahlgren et al. 2005) and  
342 accompanied with occurrences of HABs. Simultaneously, Chl-a and COD were the key  
343 indicators for reflecting the degree of eutrophication. Therefore, systematically  
344 monitoring the trophic state of eutrophic water could effectively assess the purification  
345 effect of the designed multi-stage tandem type bioreactor. In this study, 2 years  
346 systematically monitoring job were carried out by real-time detection the 4 major water  
347 quality parameters. The results showed that the self-designed bioreactor could efficient

348 removal TP, TN, Chl-a and COD, no matter the bioreactor was running or stopping. The  
349 average removal rates of TP, TN, Chl-a and COD reached to 93.6%, 89.6%, 93.4% and  
350 78.5%, respectively. In addition, regardless the high efficient removal rate of the major  
351 water quality parameters, the bioreactor had a long service life. Until now, although the  
352 bioreactor has been operated for more than 2 years, the water from treatment group was  
353 clear and odorless, whereas the water from control group was cloudy and odorous.  
354 What's more, as the reason of vulnerable influenced by temperature and light intensity,  
355 the removal rate of other reported bioremediation methods could easily been affected,  
356 such as the aquatic plant and macrophytic algae restoration system (Zuo et al. 2014; Xu  
357 et al. 2011) and the *Ipomoea aquatica* with low-energy ion implantation method (Li et  
358 al. 2009). However, the removal rate of the designed bioreactor were little influenced  
359 when the bioreactor was running, especially for TP, TN and Chl-a, which the removal  
360 rates were approximately or greater than 90%. Furthermore, when compared with other  
361 eutrophic water treatment system, the bioreactor also revealed the better purification  
362 effect than them, such as the constructed wetlands system (Zhao et al. 2012), the  
363 integrated floating island system (Lu et al. 2014), the coordinated restoration of animals  
364 and plants system (Hua et al. 2008), and the combination treatment of bacteria and  
365 plants system (Hua et al. 2010). Therefore, the designed bioreactor could meet the  
366 demand for large-scale eutrophication ecosystem restoration.

### 367 **Season-changing and stopping operation affect the removal rate of the bioreactor**

368 Numerous researches had indicated the climate alteration as well as season

369 changing were the key factors for water eutrophication (Le et al. 2010; Smith 2003). At  
370 the same time, water temperature and nutrient availability were believed to be two of  
371 the most important factors in facilitating occurrences of HABs (Beaulieu et al. 2013;  
372 Rigosi et al. 2014; Tong et al. 2019a). Therefore, understanding the potential impacts of  
373 eutrophication and water temperatures and their interactions with seasonal changing was  
374 crucial to assess the designed bioreactor. In present study, a continuously running  
375 process of the bioreactor was designed in the first year, whereas two stopping status  
376 (Summer and Winter) were designed in the next year, so that we could comprehensively  
377 evaluate the effect of season changing on the purification of the bioreactor. According to  
378 the results, the removal rates of the 4 major water quality parameters in February of TY  
379 were significantly lower than in November of SY and in May of TY ( $p < 0.05$ ),  
380 indicating stopping operation could significantly influence the purification effect of the  
381 bioreactor, despite eutrophication was less likely to occur in Winter. What's more, the  
382 removal rates of the 4 major water quality parameters in August of SY were  
383 significantly lower than the other detection months ( $p < 0.05$ ), exhibiting stopping  
384 operation and the high temperature in Summer could doubly affect the removal rates of  
385 the bioreactor. Warming in surface waters was the most direct response of water body in  
386 summer (Rigosi et al. 2014; Piccolroaz et al. 2020), where was usually the place for  
387 phytoplankton living. As the overall function of aquatic ecosystems alteration in  
388 Summer, such as biochemical transformations of nutrients (Wu et al. 2017; Ding et al.  
389 2018; Jenny et al. 2020), there might create an environment which is particularly

390 beneficial for phytoplankton surviving (e.g. cyanobacteria) and result in HABs (Paerl et  
391 al. 2016; Freeman et al. 2020). From the results, although stopping operation and high  
392 temperature could affect the removal rates of the bioreactor, there had little influence on  
393 the purification effect when the bioreactor was running, showing the good effect of the  
394 bioreactor. Meanwhile, the removal rates of the 4 major water quality parameters in  
395 March and December of SY were always higher than the other detection months,  
396 suggesting the bioreactor had the better purification effect in Spring and Autumn.

### 397 **Potential ability of VBNC bacteria in eutrophication ecosystem restoration**

398 It has been reported that the eutrophication level was well associated with the  
399 activities of bacteria in aquatic ecosystem, such as nitrogen-fixing bacteria, nitrifying  
400 bacteria and denitrifying bacteria (Fosso-Kankeu and Mulaba-Bafubiandi 2014).  
401 Meanwhile, the nitrogen absorbed and utilized by microbial and algae would dissolve  
402 back into the water body again with death and decomposition, resulted in nitrogen  
403 concentration increasing. In the Lake Taihu, China,  $\text{NO}_3^-$ -N concentration in Spring  
404 over 10 times higher than in summer (Xu et al. 2010, 2015; Wang et al. 2019b), and had  
405 confirmed that nitrification rates were highest in March and lowest in July based on  
406 stable-isotope techniques (Hampel et al. 2018), which implied microbial could positive  
407 take part in eutrophic water treatment. In this study, the total bacteria count in +Rpf  
408 treatment group was obviously higher than in -Rpf treatment group, which were in  
409 consistent with the  $\text{OD}_{660}$  values and the DGGE results of MPN culture system,  
410 indicating adding active Rpf could efficiently facilitate microbial resuscitation. What's

411 more, the VR value was 21.82, implying there had dominant VBNC bacteria in  
412 eutrophic water treatment system, which was sensitive to Rpf. Meanwhile, 24 bacteria  
413 were isolated from the novel volcanic soil adsorption material, and were native from 11  
414 genera. Nine isolated strains belonged to VBNC bacteria based on the BLAST results of  
415 16S rDNA gene, and were annotated into 4 genera, including genera *Bacillus*,  
416 *Burkholderia*, *Enterobacter* and *Pseudomonas*. Numerous researches had certified that  
417 bacteria from genera *Bacillus* owned the ability of algae-lysing and heterotrophic  
418 nitrification (Kim et al. 2005). Whereas bacteria from *Pseudomonas* possessed the  
419 ability of phosphorus-collecting and participated in sewage treatment as their function  
420 of nitrification and denitrification (Li et al. 2015; Srinandan et al. 2011). In addition,  
421 *Bacillus* and *Pseudomonas* are two crucial genera in heavy metals (HMs) treatment as  
422 their high adsorption and transformation ability for heavy metal ions, such as  $\text{Co}^{2+}$ ,  $\text{Ni}^{2+}$   
423 and  $\text{Pb}^{2+}$  (Giridhar Babu et al. 2013; Haroun et al. 2017). Meantime, *Burkholderia* and  
424 *Enterobacter* bacteria were reported to purify sewage and to promote organic matter  
425 degradation (Mcneely et al. 2009; Tiar et al. 2018), respectively. Therefore, the verified  
426 VBNC bacteria of the 4 genera potential had the functions of degrading organic matter,  
427 denitrification, phosphorus-collecting and algae-lysing, which had benefit in eutrophic  
428 water treatment. Although the definite function of the isolated bacteria remained  
429 limitation to the best of our knowledge, the role VBNC bacteria provide new insights  
430 for eutrophication ecosystems restoration.

## 431 **Conclusion**

432 In present study, the purification effect of the designed bioreactor was investigated  
433 by detection the major water quality parameters for 2 years. We found that, first of all,  
434 the bioreactor revealed high removal rates of TP, TN, Chl-a and COD, indicating the  
435 efficient purification ability of the volcanic soil containing bioreactor. Secondly,  
436 although stopping operation and high temperature in Summer affected purification  
437 effect, the impact could be minimized when the bioreactor was running. Thirdly, the  
438 bioreactor had a long service life, which meet the demand for long period treatment.  
439 Fourthly, Rpf could resuscitate the VBNC bacteria in eutrophication ecosystem, and  
440 these bacteria could potential participate in eutrophic water treatment. These results had  
441 benefit in new engineering technology innovation for aquatic ecosystems restoration,  
442 and provided new insights for water environment treatment by VBNC bacteria.

443 **Ethical Approval**

444 Not applicable.

445 **Consent to Participate**

446 Not applicable.

447 **Consent to Publish**

448 Not applicable.

449 **Authors Contributions**

450 **Huiling Fu:** Conceptualization, Methodology, Writing - original draft.

451 **Linxian Ding:** Conceptualization, Supervision, Writing-Review & Editing.

452 **Jingyu Zhai:** Methodology, Investigation, Formal analysis, Visualization.

453 **Xuesong Wang:** Conceptualization, Supervision, Writing-Review & Editing.

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#### 457 **Competing Interests**

458 The authors declare that they have no competing interests.

#### 459 **Availability of data and materials**

460 The datasets used or analyzed during this study are available from the  
461 corresponding author on reasonable request.

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465

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689

## Figures

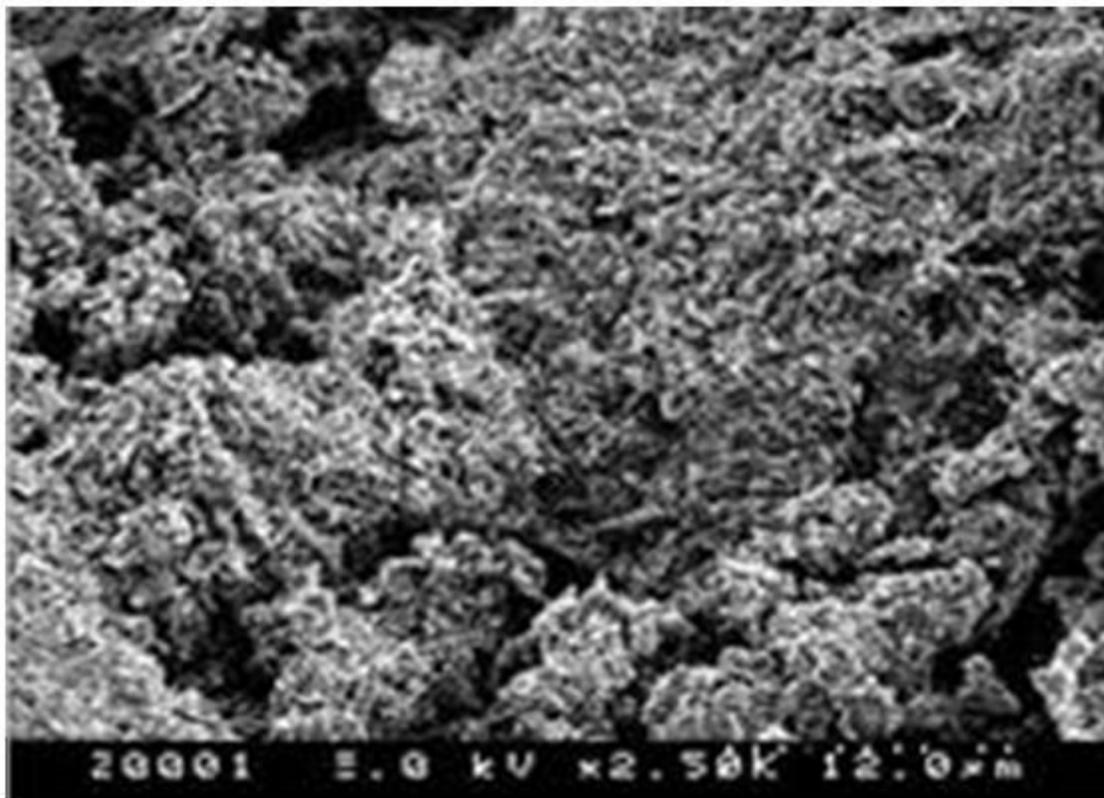
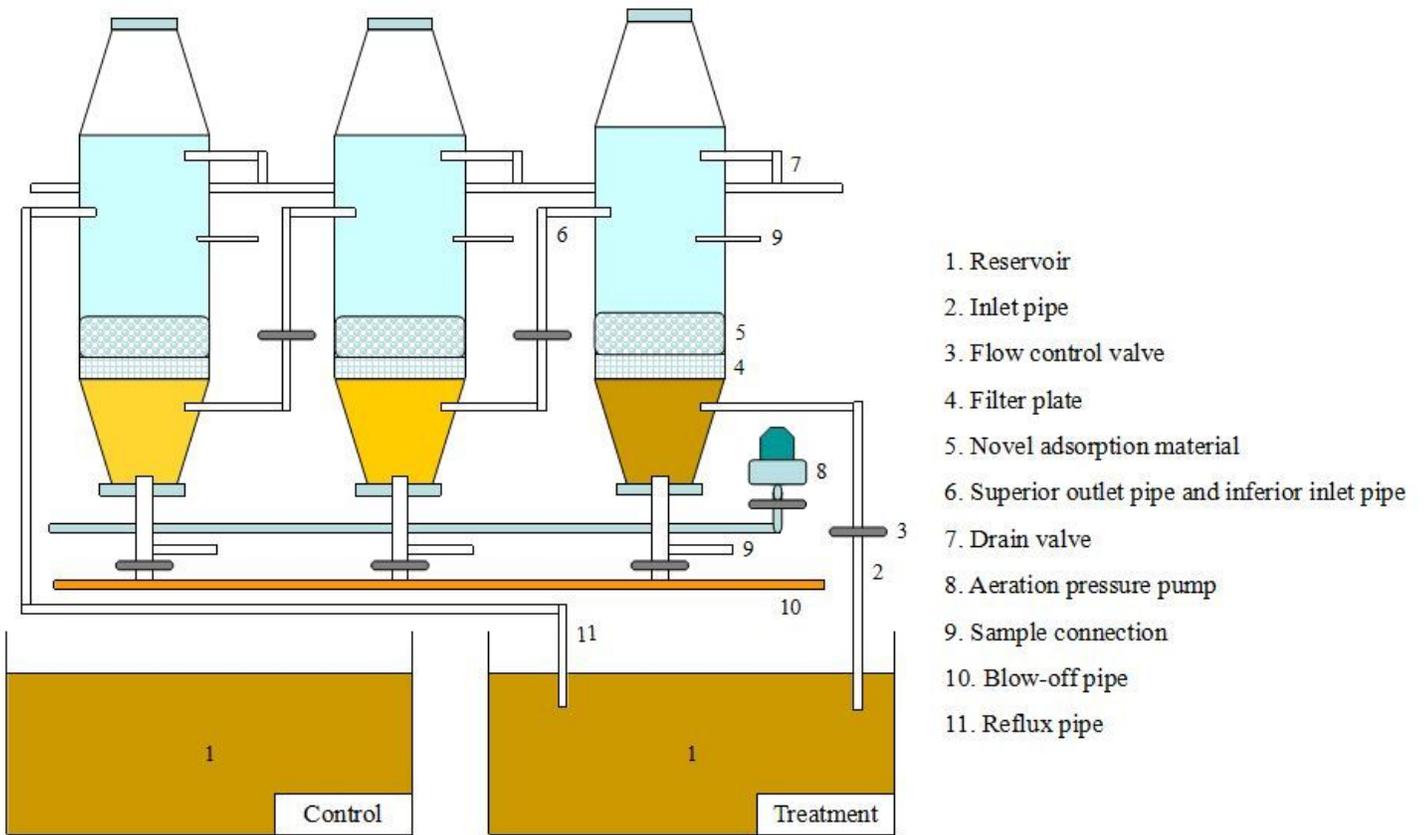


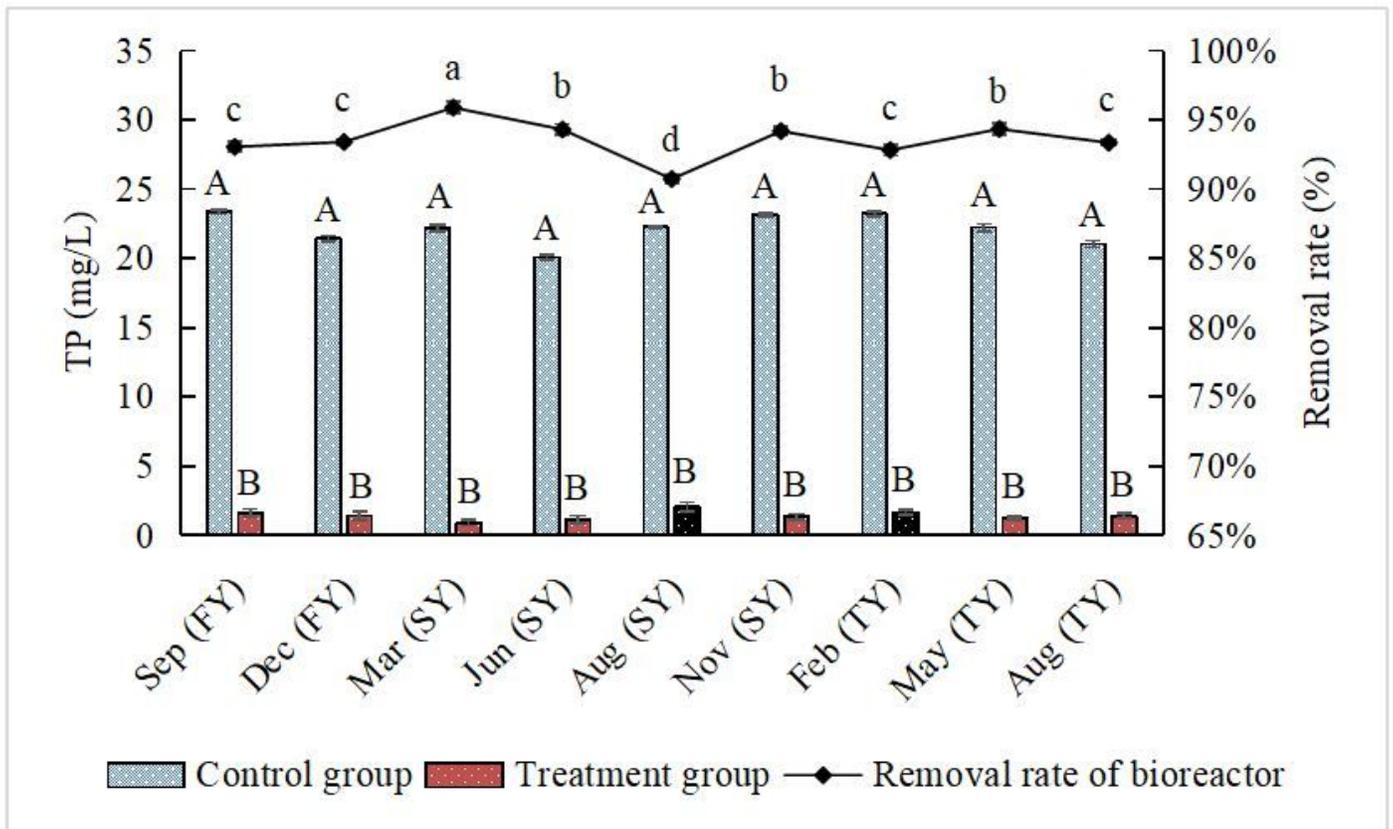
Figure 1

Scanning electron microscope (SEM) image of new adsorption material



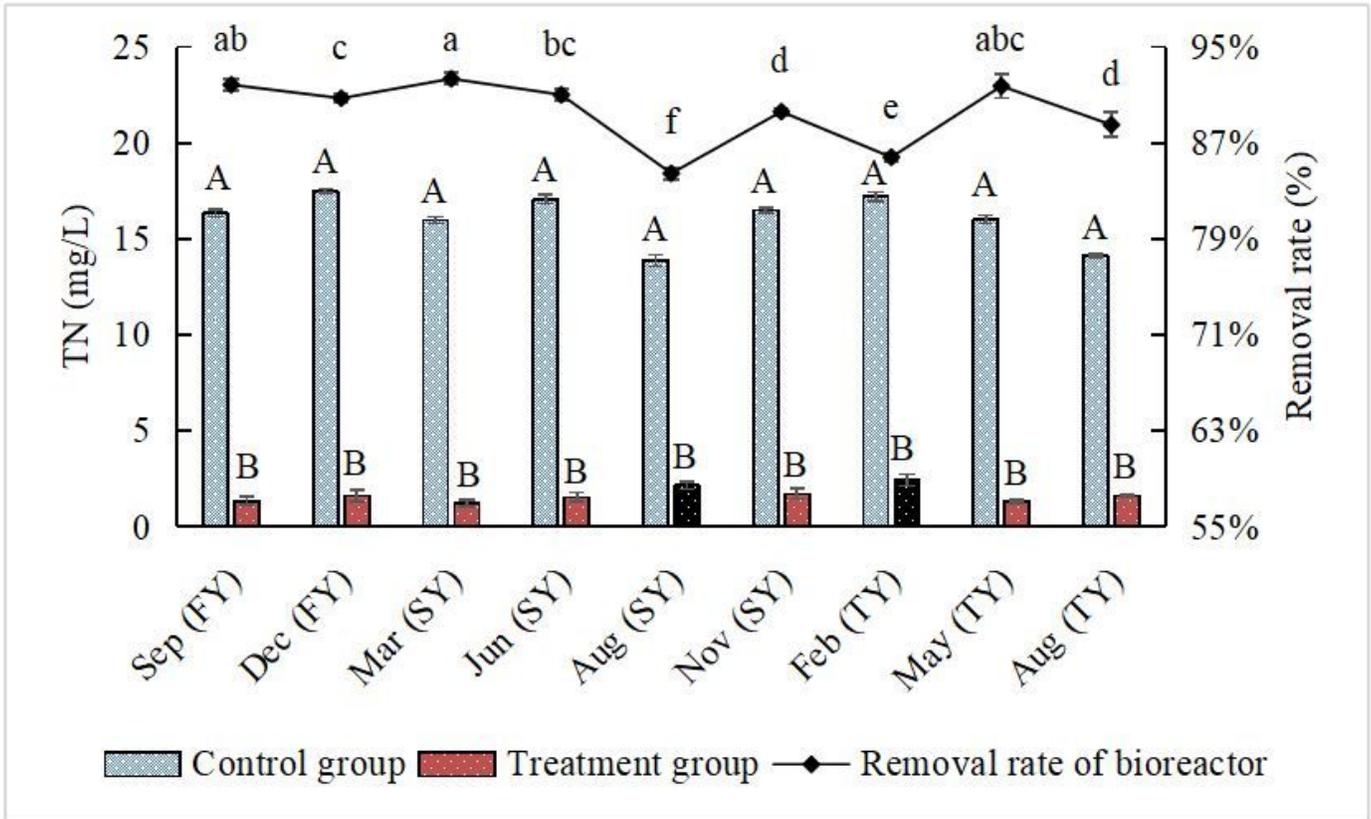
**Figure 2**

Design diagram of the bioreactor



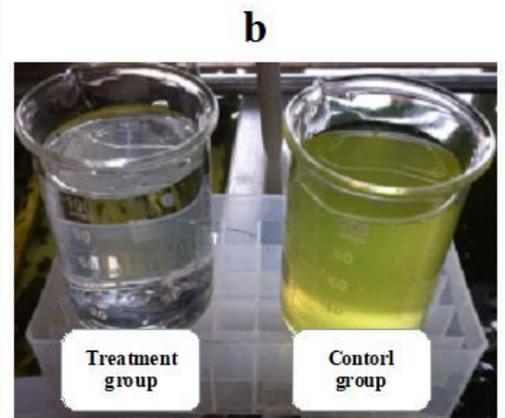
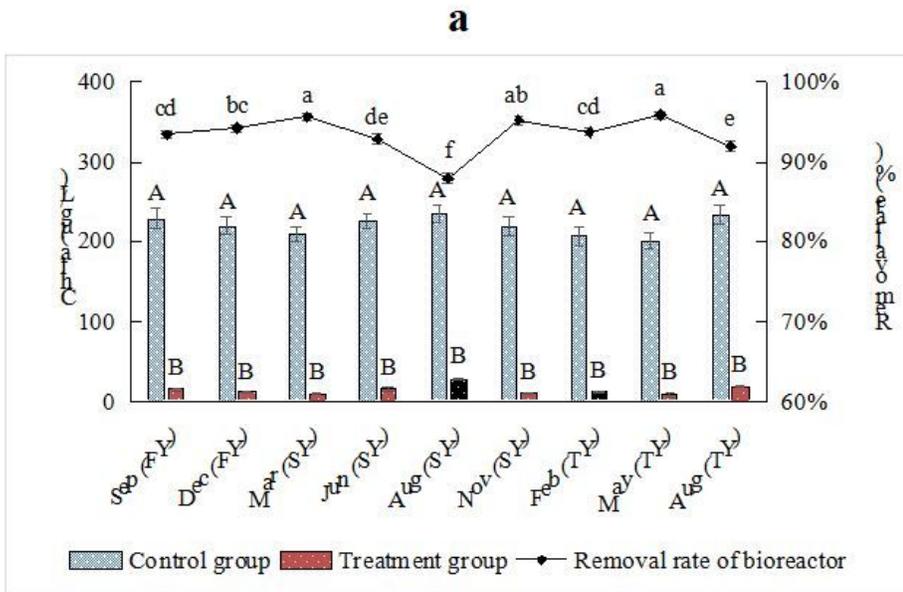
**Figure 3**

The TP concentrations in control and treatment group as well as the TP removal rate of the bioreactor. Different small letters indicate significant differences at  $p < 0.05$  level of LSD test of the removal rates under different detection months. Different capital letters indicate significant differences at  $p < 0.05$  level between control and treatment groups at the same detection month. The black bar in treatment group represented the TP concentrations of water sample when the bioreactor was stopping.



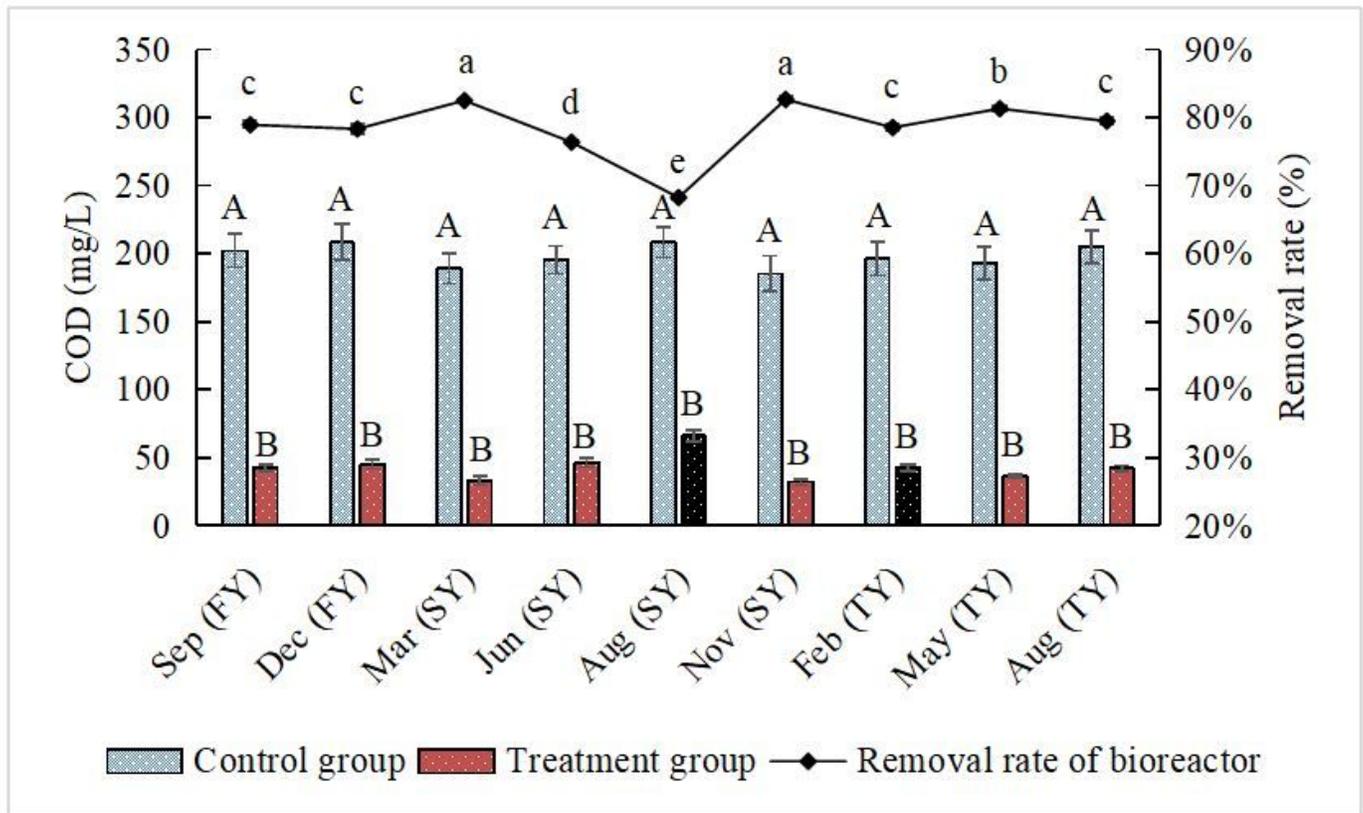
**Figure 4**

The TN concentrations in control and treatment group as well as the TN removal rate of the bioreactor. Different small letters indicate significant differences at  $p < 0.05$  level of LSD test of the removal rates under different detection months. Different capital letters indicate significant differences at  $p < 0.05$  level between control and treatment groups at the same detection month. The black bar in treatment group represented the TN concentrations of water sample when the bioreactor was stopping.



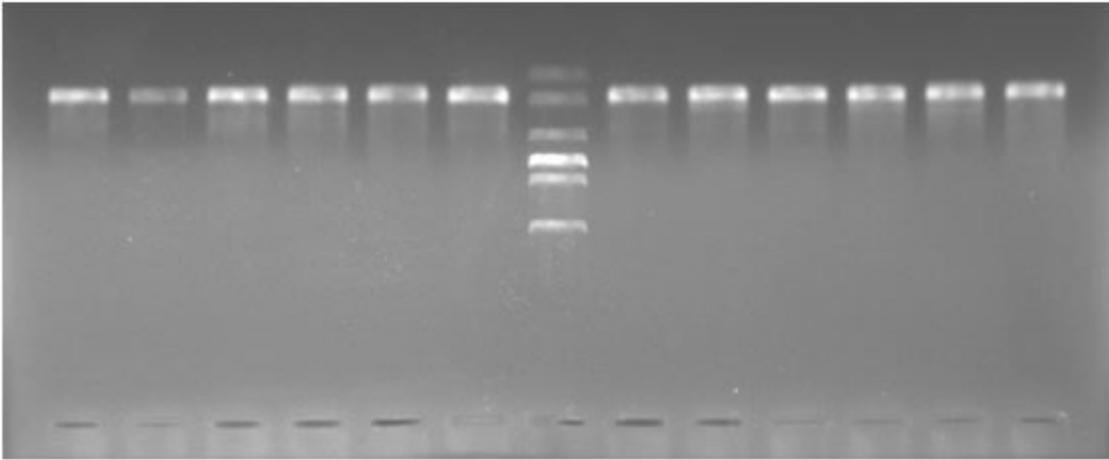
**Figure 5**

a) The Chl-a concentrations in control and treatment group as well as the Chl-a removal rate of the bioreactor; b) The real comparison between control and treatment group. Different small letters indicate significant differences at  $p < 0.05$  level of LSD test of the removal rate under different detection months. Different capital letters indicate significant differences at  $p < 0.05$  level between control and treatment groups at the same detection month. The black bar in treatment group represented the TN concentrations of water sample when the bioreactor was stopping.



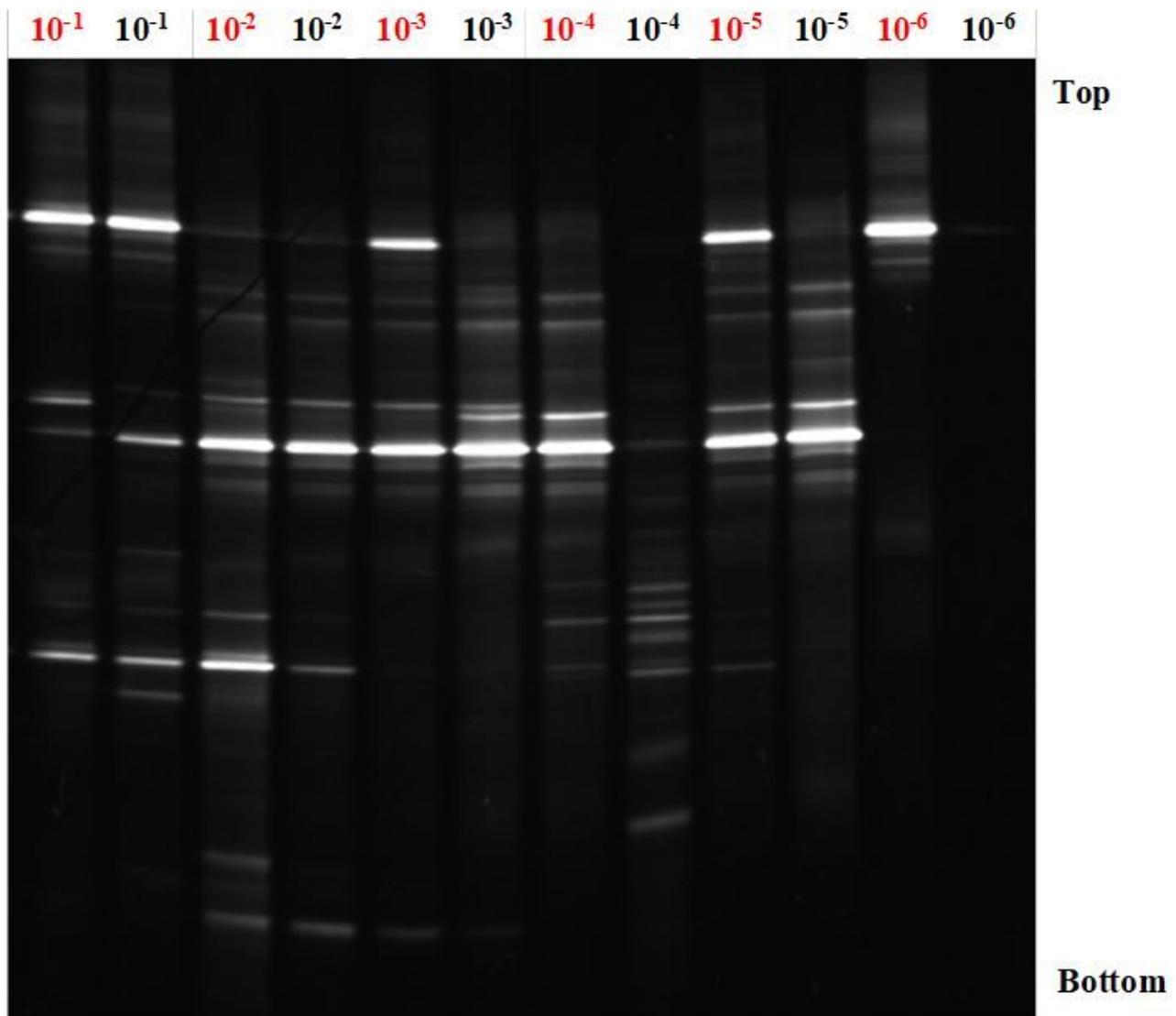
**Figure 6**

The COD concentrations in control and treatment group as well as the COD removal rate of the bioreactor. Different small letters indicate significant differences at  $p < 0.05$  level of LSD test of the removal rate under different detection months. Different capital letters indicate significant differences at  $p < 0.05$  level between control and treatment groups at the same detection month. The black bar in treatment group represented the TN concentrations of water sample when the bioreactor was stopping.



**Figure 7**

AGE analysis of the PCR products in MPN culture system of an experiment. The middle band was DNA Marker 2000; the left and right bands were the PCR products of dilution bacteria liquid from  $10^{-1}$  to  $10^{-6}$  with +Rpf and -Rpf treatments, respectively.



**Figure 8**

DGGE profiles of 16S rDNA V3 region PCR products (dilution bacteria liquid from  $10^{-1}$  to  $10^{-6}$ ). The red  $10^{-1}$  to  $10^{-6}$  represented the dilution bacteria liquid from  $10^{-1}$  to  $10^{-6}$  with adding +Rpf treatment; the black  $10^{-1}$  to  $10^{-6}$  represented the dilution bacteria liquid from  $10^{-1}$  to  $10^{-6}$  with adding -Rpf treatment; the blue marked 1 to 10 represented the clear bands for DGGE analysis.

