

# Microbial hydrogen consumption leads to a significant pH increase under high-saline-conditions– implications for hydrogen storage in salt caverns

Nicole Dopffel (✉ [nicd@norceresearch.no](mailto:nicd@norceresearch.no))

NORCE Norwegian Research Center AS

Kyle Mayers

NORCE Norwegian Research Center AS

Abduljelil Kedir

NORCE Norwegian Research Center AS

Edin Alagic

NORCE Norwegian Research Center AS

Biwen Annie An-Stepec

NORCE Norwegian Research Center AS

Ketil Djurhuus

NORCE Norwegian Research Center AS

Daniel Boldt

Equinor ASA

Janiche Beeder

Equinor ASA

Silvan Hoth

Equinor ASA

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## Article

**Keywords:** Hydrogen underground storage, salt caverns, sulphate reducing microbes, methanogenesis

**Posted Date:** May 3rd, 2023

**DOI:** <https://doi.org/10.21203/rs.3.rs-2854152/v1>

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**Additional Declarations:** No competing interests reported.

**Version of Record:** A version of this preprint was published at Scientific Reports on June 29th, 2023. See the published version at <https://doi.org/10.1038/s41598-023-37630-y>.

# Abstract

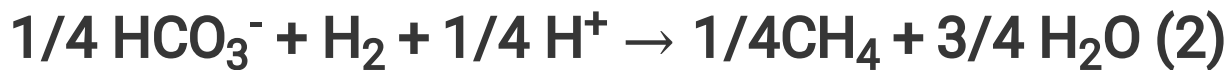
Salt caverns have been successfully used for natural gas storage globally since the 1940s and are now under consideration for hydrogen (H<sub>2</sub>) storage, which is needed in large quantities for the Green Shift. Salt caverns are not sterile, and H<sub>2</sub> is a ubiquitous electron donor for microorganisms. This could entail that the injected H<sub>2</sub> will be microbially consumed, leading to a volumetric loss and potential production of toxic H<sub>2</sub>S. However, the extent and rates of this microbial H<sub>2</sub> consumption under high-saline cavern conditions are not yet understood. To investigate microbial consumption rates, we cultured the halophilic sulphate-reducing bacteria *Desulfohalobium retbaense* and the halophilic methanogen *Methanocaldococcus halotolerans* under different H<sub>2</sub> partial pressures. Both strains consumed H<sub>2</sub>, but consumption rates slowed down significantly over time. The activity loss correlated with a significant pH increase (up to pH 9) in the media due to intense proton- and bicarbonate consumption. In the case of sulphate-reduction, this pH increase led to dissolution of all produced H<sub>2</sub>S in the liquid phase. We compared these observations to an original brine retrieved from a salt cavern located in Northern Germany, which was incubated with 100% H<sub>2</sub> over several months. We again observed a H<sub>2</sub> loss (up to 12%) with a concurrent increase in pH up to 8.5 especially when additional nutrients were added to the brine. Our results clearly show that sulphate-reducing microbes present in salt caverns will consume H<sub>2</sub>, which will be accompanied by a significant pH increase, resulting in reduced activity over time. This potentially self-limiting process of pH increase during sulphate-reduction will be advantageous for H<sub>2</sub> storage in low-buffering environments like salt caverns.

## Introduction

Many renewable energy systems utilize “Power-to-Gas” technologies, which use renewable electricity to produce hydrogen (H<sub>2</sub>), a universal energy carrier. H<sub>2</sub> can be utilized, transported or stored for later use for several industrial sectors like chemical industry, heavy transport and steel production. Storage of H<sub>2</sub> is needed to buffer daily to seasonal variations in energy supply and demand <sup>1-3</sup>. Underground storage in salt caverns is suggested to be the ideal option for large-volume storage of H<sub>2</sub> when the gas can be injected into a cavern and can be withdrawn flexibly for energy generation <sup>4-6</sup>. This process is very similar to the current storage of natural gas or oil. Salt caverns are solution mined large underground cavities inside a salt layer or salt dome by gradually dissolving the salt with freshwater or seawater. The resultant voids are several tens of meters in diameter and several hundreds of meters in length, with volumes ranging from several hundreds of cubic meters and maximum pressures of 200 × 10<sup>5</sup> Pa (200 bar). They are proposed to be ideal for short- to mid-term storage, with opportunities for rapid injection and withdrawal of gases for energy balancing. Major benefits of salt cavern storage are the available high volumes and relatively low operational costs <sup>5</sup>. As the demand for more storage sites rises, and upfront capital investments for salt caverns are high (~ 30 M€/onshore cavern <sup>7</sup>) there is an increasing need for improved understanding of possible microbiologically triggered subsurface reactions of H<sub>2</sub> within the salt cavern. These potentially can reduce the caloric value as well as leading to

health/safety/environmental relevant generation of H<sub>2</sub>S, which constrain the operational window and requires purification measures. Currently there are four salt caverns used for H<sub>2</sub> storage worldwide<sup>5</sup>, without reported failures but operational data is not available.

Salt caverns are, like most subsurface environments, not sterile but harbour diverse microbial organisms<sup>8-11</sup>. Specially adapted extremophiles (halotolerant or halophilic) can live in or even require high-salt conditions, as can be found in salt caverns, for their survival<sup>12,13</sup>. Although high osmotic stress is suggested to cause energetic constraints<sup>14</sup> by forcing the microorganisms to spend high amounts of energy for osmoregulation, i.e., production of compatible solutes; a higher salinity in cavern brines or cavern brine sumps does not necessarily lower the risks of microbial presence and/or activity. In case of H<sub>2</sub> storage, the microorganisms will be in direct contact with the stored H<sub>2</sub> for an extended period (up to several months for mid-/long- term storage). H<sub>2</sub>, being an excellent and ubiquitous electron donor, is an important driver for microbial activity in living environments<sup>15,16</sup>, which is in stark contrast to natural gas (CH<sub>4</sub>). Microbial activity in H<sub>2</sub> filled salt caverns could induce a variety of processes and risks related to them: gas volumetric effects, gas composition changes and purity loss by e.g. sulphate-reducing microbes (SRM) forming the toxic gas H<sub>2</sub>S (see reaction 1), methanogenic archaea forming CH<sub>4</sub> (see reaction 2), overall causing a reduced energetic value<sup>17,18</sup>.



In field trials for H<sub>2</sub> storage in porous reservoirs and aquifers, microbial H<sub>2</sub> consumption and conversion into CH<sub>4</sub> has been described several times<sup>19,20</sup>. It is unclear whether or how these microbial H<sub>2</sub> oxidation processes will occur in salt caverns and if so, to what extent. Some modelling approaches have indicated potential H<sub>2</sub>S formation<sup>21,22</sup>. However, these models are based on kinetic rates of general sulphate-reducers, and it can be assumed that a) growth and consumption is different with H<sub>2</sub> as an electron donor, and b) that extremely halophilic strains show different rates due to their energy expenditures on osmoregulation. For better prediction of the microbial risks, it is therefore necessary to study specific halophilic microbial rates to estimate the extent of microbial H<sub>2</sub> oxidation under high-salt conditions.

Therefore, the aim of this study was to investigate known halophilic H<sub>2</sub>-consuming microbial strains to obtain not only H<sub>2</sub> consumption rates but also to find some key parameters that influence and/or can be used as indicators for microbial H<sub>2</sub> consumption. Furthermore, we compared our findings with microbial enrichments from a brine sampled in a salt cavern located in Northern Germany. These enrichments were incubated with H<sub>2</sub> for over 150 days at the cavern specific temperature range. Our study clearly shows that microbial H<sub>2</sub> consumption is a relevant topic for salt cavern storage delivers important kinetic data on H<sub>2</sub> consumption of both cultured and environmental samples.

## Material and methods

**Source of organisms.** The two halophilic cultures *Desulfohalobium retbaense* DSM5692<sup>23</sup> and *Methanocalculus halotolerans* DSM14092<sup>24</sup> were purchased from the DSMZ (German Collection of Microorganisms and Cell Cultures GmbH). The original cavern brine was sampled at a cavern field located in Northern Germany. Samples were taken at the wellhead. Before taking samples the first brine was discarded (around of 10 minutes flushing) to avoid sampling the brine standing in the well. Afterwards the samples were filled into sterile and anoxic glass bottles under continuous nitrogen flush to preserve anoxic conditions and then immediately shipped to the lab.

**Standard culture conditions.** Both reference strains were routinely cultured in their specific media given by the DSMZ. For *D. retbaense* DSM5692: 1 g/L NH<sub>4</sub>Cl, 0.3 g/L K<sub>2</sub>HPO<sub>4</sub>, 0.3 g/L KH<sub>2</sub>PO<sub>4</sub>, 20 g/L MgCl<sub>2</sub> x 6 H<sub>2</sub>O, 100 g/L NaCl, 2.7 g/L CaCl<sub>2</sub>, 4 g/L KCl, 3 g/L Na<sub>2</sub>SO<sub>4</sub>, 1 mL/L trace element solution SL-10, 0.3 g/L Na<sub>2</sub>S x 9 H<sub>2</sub>O – pH 7.2. For *M. halotolerans* DSM14092: 1 g/L NH<sub>4</sub>Cl, 0.3 g/L K<sub>2</sub>HPO<sub>4</sub>, 0.3 g/L KH<sub>2</sub>PO<sub>4</sub>, 3.2 g/L MgCl<sub>2</sub> x 6 H<sub>2</sub>O, 50 g/L NaCl, 0.6 g/L CaCl<sub>2</sub>, 0.17 g/L KCl, 3 g/L Na<sub>2</sub>SO<sub>4</sub>, 10 mL/L modified Wolins mineral solution, 0.3 g/L Na<sub>2</sub>S x 9 H<sub>2</sub>O, 2 g/L NaHCO<sub>3</sub> – pH 7.2. Carbon sources and yeast extract were added separately to the bottles depending on the experiment. Both microorganisms were incubated at their respective optimal temperature of 37°C. Standard growth for *D. retbaense* was on 24 mM lactate with 0.1% yeast extract and 0.1% peptone. *M. halotolerans* was routinely cultivated with 20 mM acetate, 20 mM formate, 0.05% yeast extract and 80% H<sub>2</sub>, 20% CO<sub>2</sub>. Growth was confirmed by gas production (H<sub>2</sub>S or CH<sub>4</sub>).

**H<sub>2</sub> consumption experiments.** Bottles (total volume 58.35 mL) were always filled with 25 mL medium. For growth on H<sub>2</sub>, *D. retbaense* cultures were amended with 24 mM acetate and 0.35 mL modified Wolins vitamin solution, inoculum 10% (2.5 mL) of a culture grown on lactate for 7 days. The incubations of *M. halotolerans* were amended with 20 mM acetate, 35 mM formate, 0.05% yeast extract, inoculum 10% (2.5 mL) of a culture grown on 80%/20% H<sub>2</sub>/CO<sub>2</sub> for 4 days. Different amounts of H<sub>2</sub> were added to headspace to obtain 10% (~ 4 mL), 40% (~ 11 mL) and 100% (~ 25 mL)(rest gas: N<sub>2</sub>) of the total headspace volume. Fluid and gas volume was always kept constant. Because *M. halotolerans* requires CO<sub>2</sub> for methanogenesis, 5% of the gas phase was CO<sub>2</sub>, which was re-supplied after gas analysis at each sampling point. Incubation temperature was 37°C for both strains. Each experiment was conducted twice independently. The original cavern brine was anoxically filled in sterile bottles and the headspace was flushed with 100% H<sub>2</sub>. In some bottles, 20 mM acetate and 0.04% yeast extract were added as growth boosters. Incubation temperatures were 30°, 60° and 80°C. All bottles were stored upside down during incubation to minimize loss of H<sub>2</sub> due to diffusion through the rubber stopper. Still, we observed diffusion through the stoppers especially over longer incubation periods.

**Sampling and calculations.** Pressure measurements, gas analysis and liquid sampling were performed in regular intervals during the incubation: For *D. retbaense* every week, for *M. halotolerans* every day/every second day and for the original brine enrichment every 50 days. Pressure measurements of the

experiments were conducted before and after each sampling session. When the pressure fell below 25 mbar (detection limit of the microGC), the bottles were re-pressurized with N<sub>2</sub> (for *D. retbaense*) or N<sub>2</sub>/CO<sub>2</sub> (for *M. halotolerans*). At some sampling points 1 mL liquid were withdrawn for pH, HPLC and cell number determination. To calculate the amount of H<sub>2</sub> in the bottles, the ideal gas law (3) was used to correlate temperature (T in Kelvin), pressure (p) in the bottles with atmospheric pressure – water vapor pressure at the given temperature (in Pascal) and the gas constant 8.3144 (J/mol K). The measured composition of the gas phase (%) and the known volume of the bottle (58.3 mL – liquid medium + additions) was used to calculate gas volume of H<sub>2</sub> the bottles containing the medium V (in m<sup>3</sup>).

$$p \times V = n \times R \times T \quad (3)$$

The resulting mol of H<sub>2</sub> was calculated into mL by assuming STP (Standard temperature and pressure) (1 mol = 22.4 L). For each sample we calculated the volume of H<sub>2</sub> before and after the sampling procedure by measuring pressure at the beginning and at the end of the sampling. The loss of H<sub>2</sub> in between is related to withdrawal of gaseous and liquid samples. This loss through sampling was calculated and subtracted from the calculated first pressure value to obtain the volume of consumed H<sub>2</sub>.

**Analytical methods.** Gas composition was measured with a micro gas chromatography (microGC) 490 (Agilent) by directly measuring the gas in the headspace of the serum bottles. Pressure in the bottles was measured using a pressure sensor from Sensortech 0–3 barg Press D/C 2916 with an individual set-up for direct measurement of the headspace of serum bottles. Liquid samples were analyzed by using liquid chromatography of Agilent 1260II UHPLC equipped with a Flexible pump, autosampler, 1260 RI, and 1260 DA HS detectors. All analytes were identified and quantified based on their respective reference standard calibration curves. For determining cell numbers, we isolated DNA from 1 mL of sample which was withdrawn using syringes and centrifuged for 20 min at 13,000 rpm. The pellet was frozen for several hours at -80°C and after that at -20°C. This procedure was necessary because the pellets did not freeze at -20°C due to the high salt content. Prior to DNA isolation, the pellet was ultrasonicated for 5 minutes, frozen for several hours at -80°C, and again ultrasonicated 5 minutes. DNA was isolated using the Blood&Tissue Kit (Qiagen) following manufacturer's instructions. Cell numbers were measured via digital droplet PCR (ddPCR; BioRad) using Dsr1 primer for sulphate-reducing bacteria<sup>25</sup> or standard 16S rRNA Archaea<sup>26</sup>. The ddPCR reactions were run with a total volume of 20 µL on a DX200 instrument (BioRad) using 1x EvaGreen supermix (BioRad) and 250 nM (final concentration) of primers. Complete PCR reactions were emulsified with QX200 Droplet Generation Oil for EvaGreen using the QX200 Droplet Generator and then transferred to a 96-well plate. PCR reactions were performed in a C1000 Touch Thermocycler with deep-well module (BioRad) using the following program: 95 °C for 15 minutes, 40 cycles of 95 °C for 30 seconds, 57.1 °C (sulphate-reducing bacteria) or 63.1 °C (archaea) for 1 minute, 4 °C for 5 minutes, 90 °C for 10 minutes and finally an infinite hold at 4 °C. Plates were equilibrated to room temperature for at least 10 minutes before being analysed on a QX200 Droplet Reader (BioRad). Thresholds for positive and negative droplets were manually set using positive (bacteria or archaea cultures) and negative (ultra-pure water) controls.

# Results

**Hydrogen consumption during halophilic sulphate reduction.** The halophilic sulphate-reducing bacteria *Desulfohalobium retbaense* consumed H<sub>2</sub> in the headspace over several weeks. The cells consumed 10% H<sub>2</sub> (around 4 mL H<sub>2</sub>) after 20 days while the incubations with 40% (initial 11 mL H<sub>2</sub>) and 100% (initial 25 mL H<sub>2</sub>) H<sub>2</sub>-headspace were only partially consumed (Fig. 1A). We observed maximum rates of 0.31, 0.44 and 0.62 mL/day for 10, 40 and 100% respectively. In the set-ups with 10% H<sub>2</sub>, we added 10% H<sub>2</sub> at day 35 after the first consumption but subsequently consumption rate was significantly slower with a maximum rate of 0.09 mL/day. In total *D. retbaense* consumed 3.8 + 1.8 (initial 10% + renewed addition of 10%), 7.5 (40% set-up) and 14.3 (100% set-up) mL of H<sub>2</sub>, which correspond to the relative amounts of 99% + 52%, 65% and 57% (Fig. 1B). The experiment was repeated twice with a standard deviation variation of the maximum rates between 7–23% (see all data in suppl. Table 1). In sterile controls 0, 0.9 and 1.5 mL of H<sub>2</sub> was lost for the 10%, 40% and 100%, respectively, through diffusion out of the rubber stopper or by other reactions, which shows that only minimal loss occurs abiotically. During the incubation, no measurable (10%) or only minor amounts of acetate were consumed (0.7 mM with 40% and 1.1 mM with 100% H<sub>2</sub>) (Table 1), which shows that acetate was not limiting. From an initial 2.80E + 10 cells/mL, cell numbers did only slightly increase with all H<sub>2</sub> concentrations to around 4E + 10 cells/mL indicating that the strain was not able to build up substantially more cell mass.

Only minor amounts of H<sub>2</sub>S were detected in the headspace with a maximum value of around 4000 ppm at day 32 in one duplicate of the 40% bottles. However, at the next sampling stage the H<sub>2</sub>S concentration was again back to the background level (suppl. Figure S1). This indicates a changing H<sub>2</sub>S/HS<sup>-</sup> dissolution in the liquid, which was confirmed by pH measurements, showing a significant increase in pH over time. Starting from pH 7.5 at day 0 and resulting in a final pH of 8.9 for 10% H<sub>2</sub> and pH 9.1–9.2 for the 40% and 100% H<sub>2</sub> bottles (Fig. 1A & Table 1, all pH values over time can be found in supplemental table 2). Sulphate was not quantified but was in excess (21 mM) in the media allowing for theoretical consumption of 47 mL H<sub>2</sub>. We therefore assume that sulphate was never limiting.

**Hydrogen consumption during methanogenesis.** The halophilic methanogen *Methanocalculus halotolerans* consumed H<sub>2</sub> much faster compared to *D. retbaense* but still slow compared to other reported methanogenic growth<sup>27,28</sup>. In all set-ups all H<sub>2</sub> was consumed (Fig. 2A) with maximum rates of 1.1, 4.1 and 4.7 mL/day for the 10%, 40% and 90% set-ups. Re-addition of 10% H<sub>2</sub> in the 10% bottles led to an increased growth with a consumption rate of 1.7 mL/day (Fig. 2B). The experiment was conducted twice with a standard deviation between maximum rates between 15–37%. CH<sub>4</sub> was produced accordingly in all set-ups with consumption of CO<sub>2</sub> (suppl. Figure S2). CO<sub>2</sub> was always re-added when values dropped below 1.5%, to not limit growth. Formate was completely consumed after 1 day in all set-ups also the non-hydrogen controls. Acetate was consumed only in low concentrations for the 10% (0.2 mM acetate consumed) and 40% bottles (0.5 mM acetate consumed). 2.2 mM acetate were consumed in the 90% H<sub>2</sub> bottles (Table 1). Cells numbers increased from 7.2E + 09 cell/mL to 4E + 10, 4.5E + 10 and

5.1E + 10 cells/mL for the 10%, 40% and 90% set-ups. Similar to *D. retbaense*, pH increased in all the *M. calculus* cultures. Starting from a pH of 7.2, it increased to pH 8.6, 8.5 and 8.8 (Table 1, Fig. 2A, Supplemental table 2).

**Hydrogen consumption of a real salt cavern brine community.** The sampled cavern is located in Northern Germany in the Permian Zechstein Group salt layer. It has been filled with brine since the initial leaching several decades ago. The brine has a salinity of 27%, pH 7.4 and a high sulphate content of  $4190 \pm 57$  mg/L. The pure cavern brine was incubated in serum bottles with a headspace of 100% H<sub>2</sub>. We incubated for 176 days at 30°C which is relevant for this specific cavern. We added acetate and yeast extract to one set of bottles to trigger microbial activity, the other set was pure brine without any additional supplements. Sterile water with 100% H<sub>2</sub> lost 1.6 mL of H<sub>2</sub> during the incubation of 211 days. The brine sample incubated only with 100% H<sub>2</sub>, consumed 1.7 mL H<sub>2</sub> on average (Fig. 3A). One bottle showed significantly lower total H<sub>2</sub> loss compared to the duplicate, although initial consumption rate was similar. In contrast with addition of acetate and yeast, 5.3 mL H<sub>2</sub> (corresponding to ~ 11%) (Fig. 3B) was consumed in both bottles with the maximum rate of 0.069 mL/day and a total of 0.9 mM acetate was consumed after 136 days. Interestingly, at day 100 no acetate was consumed although sulphate-reduction was already visible. This indicates that the first carbon from either the brine or the yeast extract was used before acetate was consumed. H<sub>2</sub>S was first detected after 94 days with a maximum of 1505 ppm at day 136 in the H<sub>2</sub> + acetate + yeast bottles and declined afterwards due to the increase in pH. In the pure H<sub>2</sub> bottles, H<sub>2</sub>S was not detected in the headspace, but black precipitates were visible on the glass wall, which indicates possible FeS formation caused by H<sub>2</sub>S reacting with ferrous iron ions. pH first decreased to around 7 and afterwards increased to 8.5 in the H<sub>2</sub> + acetate + yeast bottles and to pH 7.8 in the pure H<sub>2</sub> bottles. Interestingly at the last sampling point (after 176 days), trace amounts of CH<sub>4</sub> (< 0.1%) were detected in one incubation of the acetate + yeast + H<sub>2</sub> experiment. CO<sub>2</sub> concentrations were always below 0.1%. We therefore assume that the CH<sub>4</sub> production is attributed to acetogenic or methylotrophic methanogens. Further investigations are needed to confirm this observation.

Cultures containing 10% CO<sub>2</sub> + 90% H<sub>2</sub> were established to investigate activities of hydrogenotrophic methanogens and acetogens, but no CH<sub>4</sub> or acetate production was observed at any time. It must be mentioned that the addition of CO<sub>2</sub> led to a pH decrease to pH 6.5 because of the lack of buffering compounds in the brine, which might have affected the microbial community.

**Table 1: Measured and calculated results for hydrogen consumption and growth of *D. retbaense* (incubation at 37°C for 71 days, starting pH 7.5, initial cell number 2.80E+10 cells/mL), *M. halotolerans* (incubation 37°C for 10 days, starting pH 7.4, initial cell number 7.2E+09 cells/mL) and an original salt brine sample (incubated at 30°C, starting pH 7.4). All experiments were performed in 58 mL glass bottles containing 25 mL medium/brine. n.d. = not determined**



	Volume H <sub>2</sub> in headspace day 0 [mL]	Hydrogen consumed/lost [mL]	Acetate consumed [mM]	Cell number at end of incubation [cells/mL]	pH at end of incubation
<i>Desulfohalobium retbaense</i>	3.9 ± 0.1	3.9 ± 0.0	0 ± 0.6	4.10E + 10	8.9 ± 0
	3.5 ± 0.1	1.8 ± 0.0			
<i>Desulfohalobium retbaense</i>	11.5 ± 0.7	7.5 ± 0.9	0.7 ± 0.1	4.13E + 10	9.2 ± 0.1
<i>Desulfohalobium retbaense</i>	24.9 ± 0.1	14.3 ± 2.4	1.1 ± 3.7	4.12E + 10	9.1 ± 0
Sterile medium	3.4 ± 0.2	0	-	-	7.3 ± 0.1
Sterile medium	11.3 ± 0.2	1 ± 0.2	-	-	7 ± 0
Sterile medium	24.5 ± 0.4	1.5 ± 0.2	-	-	6.9 ± 0.1
<i>Methanocalculus halotolerans</i>	3.4 ± 0.2	3.4 ± 0.6	0.2 ± 0	4.04E + 10	8.6 ± 0.1
	4.1 ± 0.5	4.1 ± 0.5			
<i>Methanocalculus halotolerans</i>	11.9 ± 0.9	11.9 ± 0.9	0.5 ± 0.1	4.45E + 10	8.5 ± 0.1
<i>Methanocalculus halotolerans</i>	23.6 ± 1.4	22.8 ± 2.2	2.2 ± 0.6	5.08E + 10	8.8 ± 0.1
Sterile medium	3.6 ± 0.3	0.4 ± 0.1	-	-	7.4
Sterile medium	10.5 ± 0.3	0.1 ± 0.1	-	-	7.8
Sterile medium	22.5 ± 0.2	2.3 ± 0.3	-	-	7.7
Salt cavern brine – 30C	54.1 ± 1.3	2.2 ± 0.9	-	n.d.	8.5 ± 0.1
Salt cavern brine – 30C + acetate/yeast extract	57.3 ± 0.4	5.8 ± 0.1	0.9 ± 0.3	n.d.	7.8 ± 0.1
Sterile water	56.2	1.6	-	-	-

## Discussion

**Hydrogen consumption of halophilic microbes.** With the increased interest in storing H<sub>2</sub> in the subsurface and especially in salt caverns, it becomes important to understand the risks of microbial H<sub>2</sub> consumption during storage within high-salt environments. Many Bacteria and Archaea can live and even thrive under

high salt concentrations. Although high salinity environments are hostile for many groups of microorganisms<sup>13,29</sup>, diverse microbial communities can still be found in high-saline environments like salt lakes and also salt caverns<sup>30</sup>. However, a distinction between halophilic and halotolerant must be made. The former ranging from slightly to moderate to extreme) require a certain amount of salt to grow and show their optimum growth behavior typically at salinities above 100 g/L (Oren, 2011) and can tolerate up to extreme ranges (> 200 g/L). The latter, do not need high salt concentrations but can tolerate it to a certain degree. Salinity is a common stress factor and microorganisms have different strategies to adapt to the osmotic pressure imposed by the ionic strength of the surrounding environment<sup>31</sup>. Both strategies, the “salt-in”- or the “osmotic solutes” strategy, require a certain amount of energy (ATP) to uphold cell activity. Either ATP is used directly in the production of compatible solutes (Oren, 2006), or ATP is required to uphold the correct sodium and potassium gradient between the inside and the outside of the cell. This is also the reason why many halophilic microbes living at the “energetic edge”, using much energy for upholding their cell stability, tend to grow slower compared to non-halophilic counterparts. Therefore, it is very important to specifically assess H<sub>2</sub> oxidation by halophilic H<sub>2</sub>-oxidizers because the relative kinetic rates in such environments are largely unknown.

To estimate the H<sub>2</sub> consumption rates and associated effects in high-salt subsurface environments, we investigated and cultured two halophilic microorganism which belong to the two most relevant metabolic groups regarding H<sub>2</sub> consumption: i) Sulphate reduction is a very widespread metabolism with many different microbial groups potentially using H<sub>2</sub> as electron donor in the presence of sulphate as electron acceptor<sup>32</sup>, resulting in the production of the toxic and corrosive gas H<sub>2</sub>S; ii) Methanogenesis from H<sub>2</sub> and CO<sub>2</sub> is another highly relevant H<sub>2</sub> consumption process, which recently received major attention for potentially producing “green” methane (biomethanation) in the subsurface after injecting renewable H<sub>2</sub> with captured CO<sub>2</sub><sup>33</sup>. The two investigated strains in our study are halophilic with *Desulfohalobium retbaense* at a salt optimum at 12% growing up to 24%<sup>23</sup> and *Methanocalculus halotolerans* with the optimum of 5% growing up to 12.5% salinity<sup>24</sup>. Both strains were originally described to be able to use H<sub>2</sub> for growth, both requiring acetate as an additional carbon source. To estimate the potential H<sub>2</sub> consumption kinetics in the high-saline subsurface we carefully cultured the strains with different volumes of H<sub>2</sub> in the headspace. We clearly observed H<sub>2</sub> consumption over time, with an increased H<sub>2</sub> loss relative to the initial concentration when growing with 10% H<sub>2</sub> instead of 40% or 100%. H<sub>2</sub> is normally a very scarce electron donor in the environment, typically in the nmol range. So high amounts of H<sub>2</sub> seem to have a negative effect on cellular H<sub>2</sub> uptake or involved hydrogenase enzymes. It is known from H<sub>2</sub>-producing cultures that increased H<sub>2</sub> partial pressure has a product-inhibition effect on the enzymes<sup>34</sup>. A similar effect could be at play also during H<sub>2</sub> oxidation, but details need to be further investigated. *D. retbaense* was not able to oxidize all the provided H<sub>2</sub> in the 40% and 100% H<sub>2</sub> set-ups although acetate and sulphate was provided in excess. This lack of continued activity or consumption can be explained by an intense pH increase during H<sub>2</sub>-oxidation. It can be seen in the reaction rate of H<sub>2</sub>-dependent sulphate reduction (1) that this reaction is a proton consuming process leading to an increase

in surrounding pH<sup>35,36</sup>. This also explains the near complete absence of gaseous H<sub>2</sub>S throughout our study. At higher pH H<sub>2</sub>S will be in its highly soluble form HS<sup>-</sup> (HS<sup>-</sup> + H<sup>+</sup> ⇌ H<sub>2</sub>S). HS<sup>-</sup> is a weak acid which should partly counteract the pH increase but clearly the intense H<sub>2</sub> oxidation is the main driver and overrides the HS<sup>-</sup> effect. In biogas plants and biocorrosion studies it is commonly reported that intense sulphate-reduction can lead to a pH increase<sup>37,38</sup>. As biogas and corrosion involves also intermediate H<sub>2</sub>, this is also a direct effect of H<sub>2</sub> oxidation. Although it has been long known that H<sub>2</sub> is an electron donor for SRMs, it was never clearly described that the significant pH effect limits the microbial activity when growing on pure H<sub>2</sub>. As the pH approached pH 9, which is beyond the acceptable limit for *D. retbaense*, its activity ceased. Another inhibiting effect could be significant amounts of dissolved HS<sup>-</sup> (theoretically based on the amount of H<sub>2</sub> consumed: 1.4, 1.9 and 3.6 mL for the 2x10%, 40% and 100% H<sub>2</sub> respectively), which might have an additional inhibitory effect. When growing on lactate as an electron donor, pH did not rise significantly with an end value of pH 7.8 after 7 days with H<sub>2</sub>S concentrations far beyond 15% of the headspace. So, the observed pH effect is purely associated to H<sub>2</sub> oxidation.

We were however not able to correlate the overall volume of H<sub>2</sub> consumed with the pH. In the 40% set-up the strains consumed 6.6 mL (consumption minus the diffusion loss observed in the sterile controls) and in the 100% set-up it consumed almost double with 12.4 mL and both reached a pH 9.1–9.2. One possible explanation could be that under 100% H<sub>2</sub> atmosphere more H<sub>2</sub> is dissolved in the media. H<sub>2</sub> has a low solubility in water (0.0014 g gas per kg water at 37°C) and even lower in saline brine. So, growth will be limited by H<sub>2</sub> dissolution, which will be increased with higher H<sub>2</sub> concentration or pressure. Given the optimal growing conditions in the beginning (optimal pH and nutrients) and a high initial cell number, 100% H<sub>2</sub> gives the cells more electron donor to be active in the initial growth phase compared to 40%. Another possibility are concurrent chemical reactions of the H<sub>2</sub> gas with the slightly alkaline media, leading to additional abiotic H<sub>2</sub> loss. Further careful investigations combined with chemical and biological kinetic modelling will help to answer understand the H<sub>2</sub>- and proton consumption.

The H<sub>2</sub> electron chain towards sulphate is well understood and relatively conserved in members of the Deltaproteobacteria<sup>39</sup>, therefore it can be assumed that the observed effects of pH increase when grown on H<sub>2</sub> is a general phenomenon and not strain specific.

Similarly, methanogenesis is a proton consuming process (reaction rate 2). Also, during methanogenesis the Archaea are consuming bicarbonate/CO<sub>2</sub> from the media, which reduces buffer potential and increases pH as described previously<sup>40</sup>. We observed in our set-ups with *M. halotolerans* a pH increase, although not as intense as with *D. retbaense*. All H<sub>2</sub> was consumed in all cases although activity rates decreased during the end of incubation for the 100% H<sub>2</sub> bottles probably because pH increased and was close to the upper pH limit of this strain. Again, the strain had much higher relative consumption rates with 10% H<sub>2</sub> compared to 40 and 100%. Renewed addition of 10% gave an even increased rate which is related to an increased cell number.

**Potential risks for souring of salt caverns.** Halophilic Archaea and Bacteria have been isolated from pure halite crystals in salt mines<sup>41</sup> and it is therefore expected that that also salt caverns will be habitat to a diverse set of microbes. Recent studies of salt cavern microbiology showed microbes in all studied caverns<sup>11</sup>. Also, our studied salt cavern brine was microbiologically active and after several months of incubation with and without nutrient addition we observed H<sub>2</sub> consumption. With addition of the growth booster yeast extract (supplying microbes with a variety of vitamins and trace elements) and the carbon source acetate, a significant H<sub>2</sub> consumption was measurable together with acetate consumption, H<sub>2</sub>S production and also a significant pH increase. At the end of the incubation the pH increased 1 log factor from an initial 7.5 to 8.5. This shows that H<sub>2</sub> oxidation by halophilic SRMs does indeed lead to a significant pH increase similarly to what we observed with our type strain *D. retbaense*. In the pure brine bottles without addition of carbon source or yeast extract, H<sub>2</sub> consumption was less pronounced. This shows that the natural community is limited by a certain growth factor, trace element, vitamin or similar. No H<sub>2</sub>S formation was measurable but again a pH increase indicating sulphate-reduction. We hope to be able to identify and enrich the sulphate-reducing community in future studies to better understand the growth behavior.

If we assume that the studied sulphate-reducers will also be active in the salt cavern when in contact with H<sub>2</sub>, there is indeed a real risk for H<sub>2</sub> loss and souring. The sampled cavern brine has a very high sulphate content of over 4000 mg/L (~ 44 mM), which gives sulphate-reducing organisms sufficient electron acceptors. A back of the envelope calculation of a typical salt cavern with a volume of 600.000 cubic meters (most volume will be occupied with gas but roughly 3000 m<sup>3</sup> will be brine in the sump together with insoluble minerals) contains 12.6 metric tons of sulphate in the cavern to be potentially converted by sulphate-reducing organisms. However, in case of 100% sulphate conversion without any additional input, the cavern could contain around 3E + 06 L liters of H<sub>2</sub>S or only 0.6% of the total cavern volume. Based on the equilibrium (1), four times the amount of H<sub>2</sub> would be needed as electron source (1.2E + 07 L), a loss of around 2% of the total volume. As we observed in our enrichments, another limiting factor will be the amount of available carbon source and/or growth factors, which could lead to a H<sub>2</sub> loss of maximum 5–13% under laboratory conditions. The consumption rates will be dependent on the surface area of the brine-gas interphase and therefore the cavern shape. A higher surface area will allow for a higher H<sub>2</sub> availability for the microbes. Dissolved organic carbon has been detected in the cavern brine of around 85 mg/L and was most likely introduced by the leaching process using diesel oil as a leaching blanket or by different operational procedures. Still, additional growth enhancers were necessary for significant sulphate reduction to occur, which significantly slowed down when pH approached 9. This means that during the first H<sub>2</sub> storage cycles, some volumes of H<sub>2</sub> will be converted by microbes until the pH value will be outside of the optimum for these microbes to thrive. As a cautionary note, that the derived laboratory enrichments can only give hints about the metabolic potential in extreme environments since most microbes do not grow under lab conditions. A much more complex and chemolithoautotrophic community with higher cell numbers might be present and active in the cavern leading to a) faster H<sub>2</sub> consumption and b) longer and more intense H<sub>2</sub> consumption. For example, it

could be that alkali-tolerant strains will take over H<sub>2</sub> oxidation as soon as neutrophilic strains reached their limit or a certain adaptation to higher pH will occur. Indeed, given the production of methane after 170 days when pH was seemingly too high for the sulphate-reducing community, methanogenesis is inferred.

Our data shows that artificially leached salt cavern can contain H<sub>2</sub>-consuming microbes, especially sulphate-reducers which seem to be nutrient limited and additionally will significantly increase pH. Field tests are now required to understand if the observed effects regarding H<sub>2</sub> consumption and pH will also occur in the cavern itself

## Conclusions

- Halophilic hydrogen-consuming sulphate-reducers and methanogens are able to consume significant volumes of H<sub>2</sub> over time.
- H<sub>2</sub> oxidation leads to a significant pH increase in both cases. In case of SRMs pH exceeds growth limits and H<sub>2</sub> is not completely consumed.
- Original salt cavern brine contains active SRMs which are able to consume parts of the available H<sub>2</sub> especially when carbon and nutrients were added.
- The pH increase caused by H<sub>2</sub> oxidizing-SRMs might limit microbial H<sub>2</sub> consumption over long-term and might therefore be a self-limiting process.

## Declarations

### Acknowledgements

We want to thank Equinor for funding this project and providing salt cavern brine for the experimental studies. We also want to thank Carsten Reekers, Nils Kruse and Michael Mollenhauer for their help in the project and the good discussions.

### Data availability

All main data generated or analysed during this study are included in this published article (and its Supplementary Information files).

### Competing interests

The author(s) declare no competing interests.

### Author contributions

ND: conceptualization, methodology, experiments, writing. KM: cell number analysis. AK: water and HPLC analysis. DB: sampling. EA: writing and editing. BAS: writing and editing. KD: lab support. JB:

conceptualization. SH: conceptualization, writing, acquiring internal grant.

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## Figures



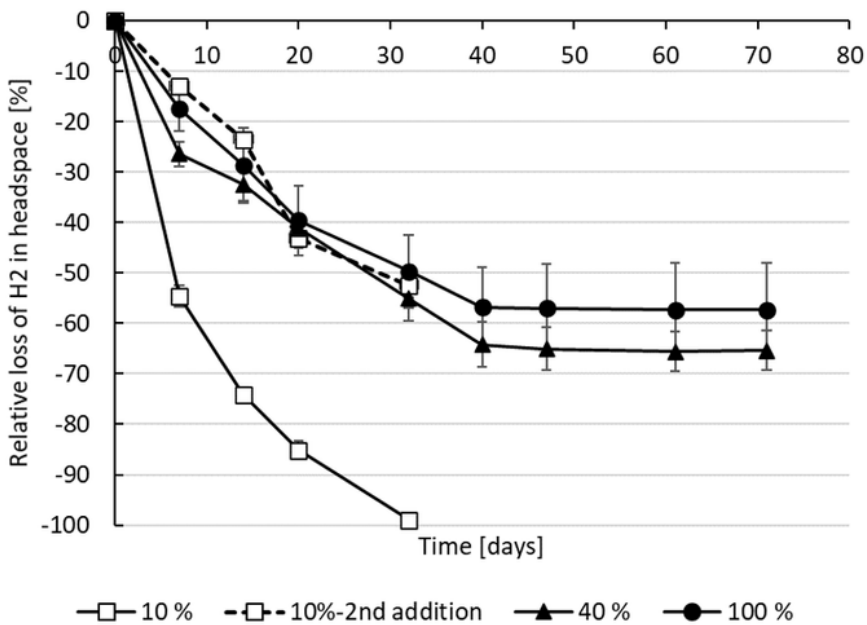
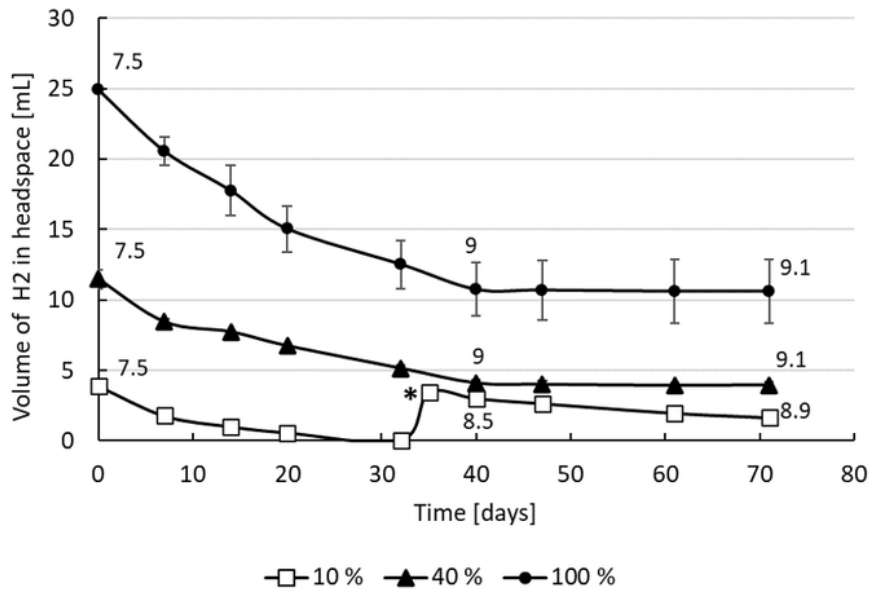


Figure 1

1A: Consumed hydrogen of *Desulfohalobium retbaense* in ml over time measured in the headspace of bottles incubated at near atmospheric pressure and 37 °C. Bottles were amended with 100% H<sub>2</sub> (●, solid line), 40% H<sub>2</sub> (▲, solid line) and 10% H<sub>2</sub> (□, solid line). The star \* at 35 days indicates re-feeding the bottles with 10% H<sub>2</sub>. pH measured at the day are given above the line. 1B: Values plotted in loss in % over

time. Error bars indicate deviation from the mean of duplicates. At day 35, 10% of H<sub>2</sub> was again added to the 10% bottles (dashed line - 2nd addition).

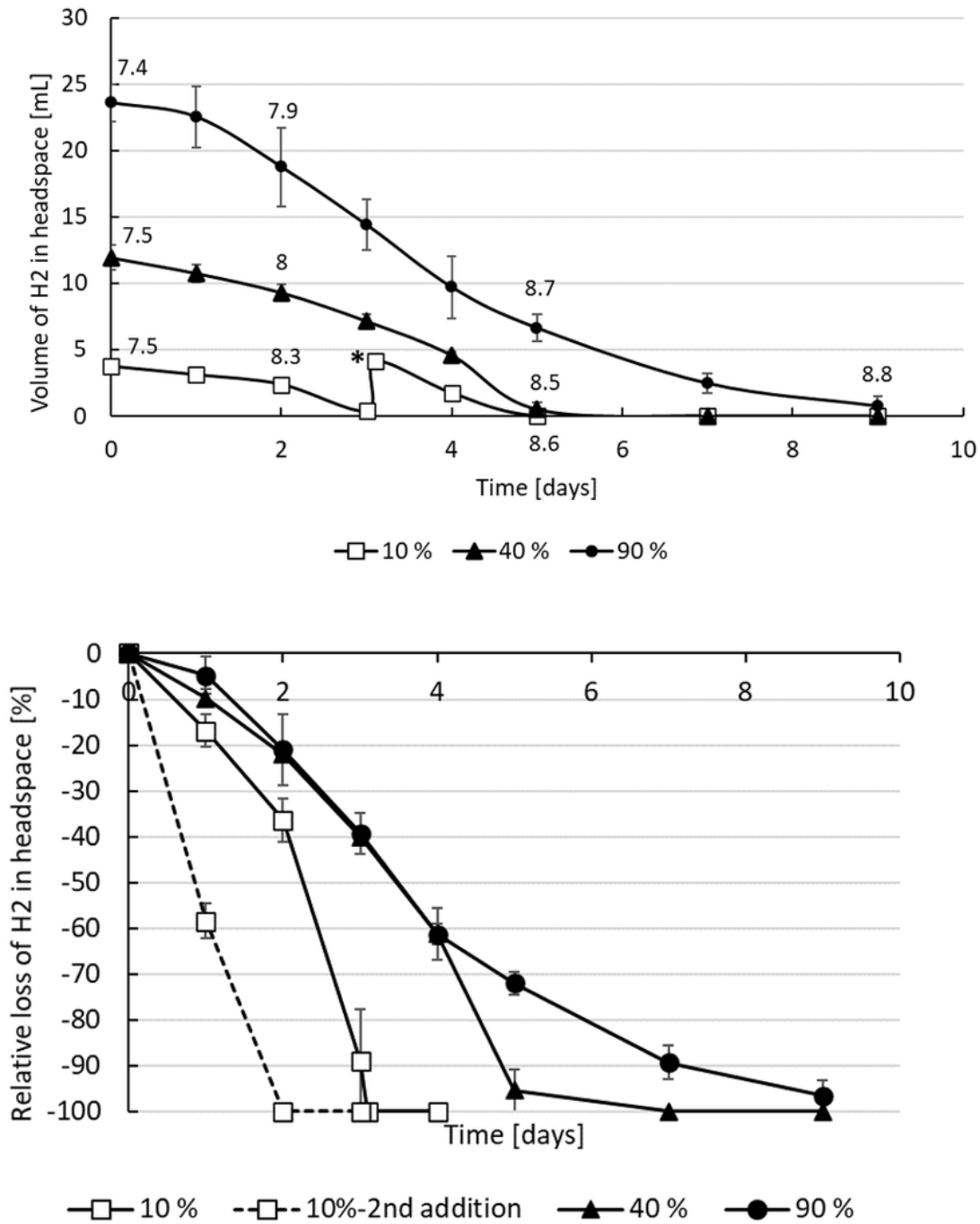
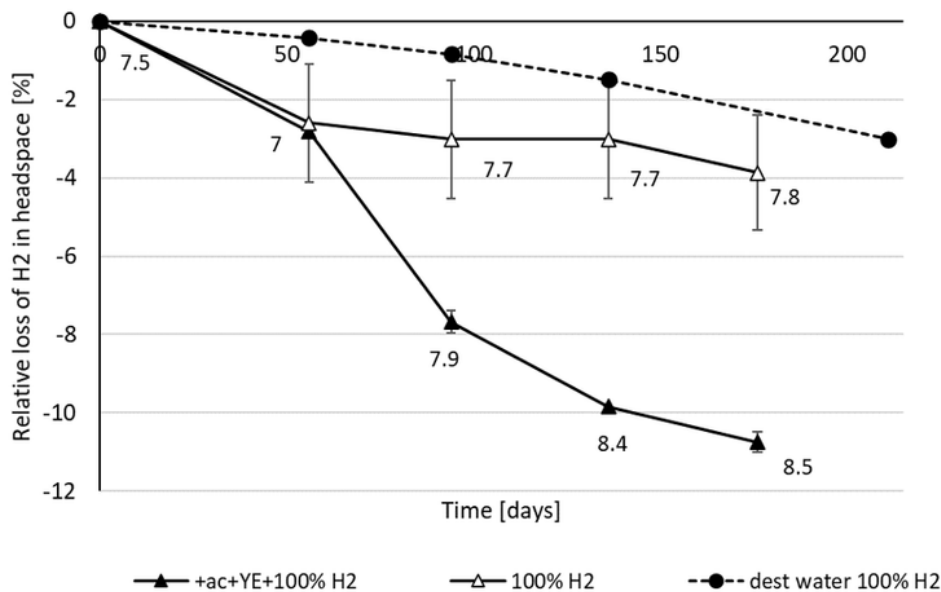
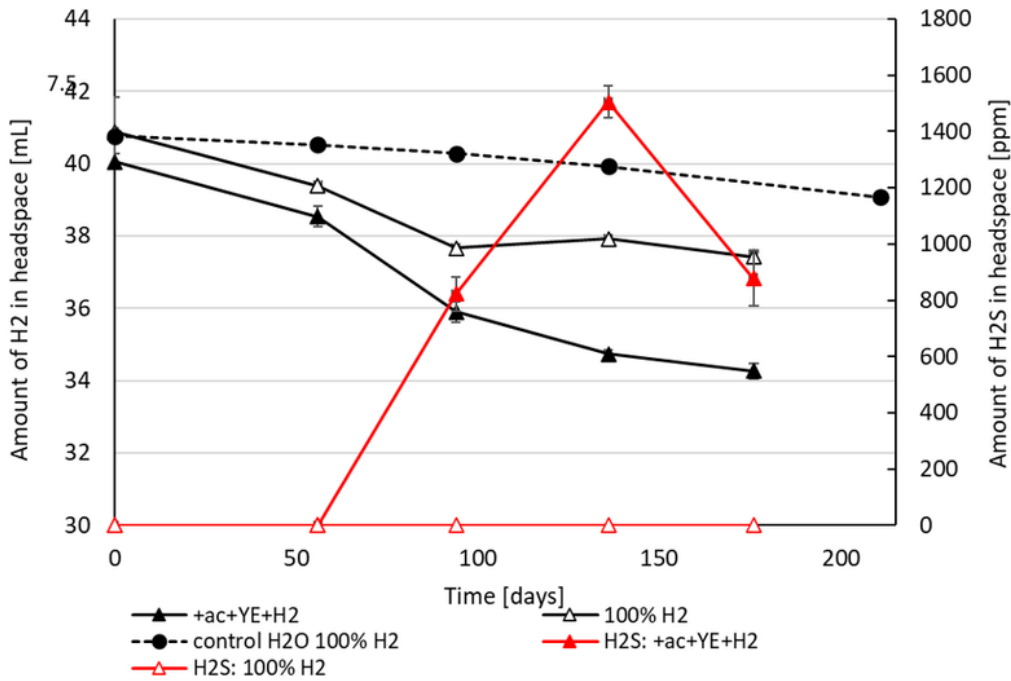


Figure 2

2A: Consumed hydrogen of *Methanocalculus halotolerans* in mL over time measurable in the headspace of bottles incubated at near atmospheric pressure and 37°C. Bottles were amended with 90% H<sub>2</sub> (●, solid

line), 40% H<sub>2</sub> (⊗, solid line) and 10% H<sub>2</sub> (□, solid line). The star \* at 35 days indicates re-feeding the bottles with 10% H<sub>2</sub>. pH measured at the day are given above the lines (10% day 5 is under line). 2B: Values plotted in loss in % over time. At day 3, 10% H<sub>2</sub> was re-added in the 10% set-ups (dashed line-2<sup>nd</sup> addition). Error bars indicate deviation from the mean of duplicates.



## Figure 3

3A: Consumed hydrogen of an original salt cavern brine in mL over time measurable in the headspace of bottles incubated at near atmospheric pressure and 30°C. Bottles were amended with 100% hydrogen ( $\Delta$ , solid line) or with addition of 20 mM acetate and 0.04% yeast extract ( $\blacktriangle$ , solid line).  $H_2S$  measured in ppm in the headspace is given on the secondary axis for the acetate+yeast extract bottles (red line). Diffusion loss in an only sterile lab water bottle is shown with  $\bullet$ , solid line. 3B: Values plotted in % loss. pH values are given at the single sampling points in the graph. Error bars indicate deviation from the mean of duplicates.

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