

Development of a Superstructure Optimization Framework for the Design of Municipal Solid Waste Facilities

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Research

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1 Development of a Superstructure Optimization Framework for
2 the Design of Municipal Solid Waste Facilities

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7

8 **Abstract**

9 The main objective of this study is to develop a decision-making tool for the design of
10 the optimal municipal solid waste (MSW) facilities based on superstructure
11 optimization. Currently, the disposal of MSW is a major problem due to the lack of
12 awareness of the negative impacts resulting from dumping MSW into the environment.
13 This poses a challenge for the authorities. MSW valorization such as anaerobic
14 digestion (AD), pyrolysis, gasification etc has been increasingly focused on as an
15 approach when handling MSW to enhance both economic and environmental
16 sustainability. However, with an increasing array of processing technologies, the design
17 of MSW facilities involving the integration of these technologies is becoming tedious
18 and unmanageable. To deal with this problem, superstructure optimization is proposed.
19 It is an effective tool for the design of several chemical processes because it is able to
20 consider all potential process alternatives including the optimal solution using
21 mathematical models based on mass and energy balances. Uncertainty is incorporated
22 into the optimization framework to enhance the robustness of the solution. The
23 proposed methodology was applied in the design process of the MSW facility in Ubon
24 Rathathani province, Thailand, with the objective function of maximizing the profit.

25 The optimization problem was developed as Mixed Integer Linear Programming
26 (MILP) and it was solved using an optimization platform, GAMS, with CPLEX as the
27 solver related to obtaining the optimal solution. The results show there to be as positive
28 profit that is economically viable compared to the use of landfill technology.

29 **Keywords:** superstructure optimization, MSW management, waste valorization,
30 process design

31 **1. Introduction**

32 Municipal solid waste (MSW) is an undesirable material that is thrown away by
33 households, e.g. packaging, plastic, and food waste etc [1]. It is typically collected and
34 disposed of by the municipal authorities. MSW has increasingly become an issue of
35 global concern as the amount of MSW increases. It is reported that the amount of MSW
36 generated worldwide is around 1.3 billion tons and the generation of MSW is expected
37 to reach 2.2 billion tons by 2025 [2] as a result of a growing population, urbanization,
38 and changes in life style [3]. Specifically, the MSW generated in Thailand totaled
39 approximate 27.37 million tons or 1.13 kg/capita/day in 2017 [4]. It has been found that
40 39% of the total MSW is disposed of appropriately, 34% is reused/recycled, and the
41 remainder is still disposed of incorrectly [5]. Regarding waste reuse/recycling, waste

42 can be recycled into valuable products, e.g. glass, paper, and plastic. An increase in
43 MSW can cause serious problems for the environment and human health such as ground
44 water contamination and air pollution. MSW management is a challenging task due to
45 the limited resources and increasing population. Inefficient waste management may
46 cause significant environmental problems, e.g. the generation of greenhouse gases
47 (GHGs) and an increase in the number of bacteria causing disease in humans. The
48 common approach to disposing of MSW in developing countries includes open
49 dumping, sanitary landfills, and incineration. These are commonly used technologies
50 despite the high potential to pollute the environment because of the relatively low
51 investment cost [2]. The main problem of the conventional disposal approach is the
52 shortage of landfill and dumping sites inland [6]. This requires a sustainable and
53 efficient approach to be present in the waste management system. However, this is a
54 challenging task due to the limited resources and increasing population.

55 Recently, several studies in the field of waste management have focused on
56 resource recovery and minimizing waste disposal. Various technologies and initiatives
57 have been developed as alternatives for waste disposal by considering MSW a valuable
58 resource [7-8]. These technologies can generate electricity, useful heat, syngas,

59 biodiesel, compost, fertilizer, and other by-products [9] so the concept of integrated
60 waste management can be an effective and sustainable waste management method [10].
61 The design of integrated waste processing technologies has been performed using many
62 concepts and tools including zero waste [11], urban metabolism [12], substance flow
63 analysis [13] and life cycle assessments [14-15]. However, these techniques do not
64 guarantee an optimal solution. With an increasing array of treatment technologies for
65 waste management, the selection of the most appropriate treatment technology is
66 becoming a challenging task since it involves several parties and different factors within
67 complex decision-making. Each processing pathway has its own pros and cons
68 including investment, operating, and resource recovery. This calls for a systematic
69 technique or holistic approach to select the optimal solution and the most suitable
70 technology. Superstructure optimization is one of the most powerful approaches used
71 to handle such problems. It has proven to be an effective approach for the design of
72 chemical engineering processes [16]. It was introduced in Umeda et al. [17] and
73 involved three main steps: i) postulating a superstructure which proposes a set of all
74 feasible process structures, ii) translating the superstructure into a mathematical model,
75 and iii) computing the optimal process structure based on the proposed mathematical

76 model using the chosen numerical algorithms [16]. The superstructure initially assumes
77 all possible alternatives related to the potential conversion technologies, including any
78 optimal solutions that are hidden. A common way to formulate a superstructure
79 involves a mathematical model of mass and energy balances. This framework has been
80 applied previously with several applications, e.g. a water network [18] and wastewater
81 treatment [19]. There have been a few studies investigating the application of
82 superstructure optimization in MSW management [20-24]. Although previous studies
83 have presented the potential of superstructure optimization in order to handle the
84 simultaneous selection of waste processing technologies and operating conditions,
85 solid/liquid residue and uncertainty analysis are typically overlooked. This
86 consequently does not account for the concept of integrating waste processing
87 technologies. In this study, the main objective of this study is to develop a decision-
88 making tool based on the concept of superstructure optimization for the design of MSW
89 management to convert waste into multiple products through the integration of various
90 processing technologies. The paper is organized as follows: Section 2 reviews the
91 previous studies on the design of waste management. The proposed methodology
92 regarding superstructures has been described in Section 3. Section 4 presents the case

93 study using the proposed approach and the results have been presented in Section 5.
94 Finally, the key contributions will be concluded in Section 6.

95 **2. Design of MSW facilities**

96 MSW management involves a set of activities used to manage MSW from its origin
97 through final disposal [25]. This includes transportation, collection, treatment
98 approaches, and final disposal in order to deal with all of the materials in the waste
99 stream to protect human health, promote environmental quality, support economic
100 productivity, and enhance sustainability. This is a challenging task as it requires the
101 fulfilment of technical, economic, environmental, and social constraints. Various
102 computer-aided methods have been developed to help decision makers to reach a
103 conclusion [26]. Several studies have investigated solid waste management focusing on
104 economic, energy and environmental analysis for specific treatment and processing
105 technologies in specific areas. Khan et al. [27] developed a techno-economic model for
106 the economic assessment of MSW utilization pathways. The developed model was able
107 to determine suitable locations for the waste conversion facilities based on a geographic
108 information system (GIS). It compared nine different waste management scenarios
109 which included landfill, composting, and gasification. The proposed method was

110 applied to a case study in Alberta, Canada. Some of the studies also used the life cycle
111 assessment as a tool to examine the environmental impact of the selected process
112 alternatives [15], [28]. However, these techniques do not guarantee that the selected
113 processing technology is optimal in terms of the economic, energy, and environmental
114 aspects. To address the problem, a wide variety of techniques and optimization models
115 have been developed in the field of process system engineering for the design of waste
116 management systems. Recently, process design and optimization for MSW
117 management has received attention. Ng et al. [22] developed an optimization model
118 to use in the supply chain design of MSW management. The proposed method allowed
119 for the optimal selection of the thermochemical and biochemical treatment
120 technologies. However, the developed optimization framework did not consider the
121 potential of recyclable materials which can be further processed to compensate for any
122 expenses. Santibañez-Aguilar et al. [29] developed a mathematical programming model
123 used to determine the reuse of MSW to maximize the economic objective while
124 considering the environmental and safety aspects simultaneously. Satchatippavarn et
125 al. [24] employed a superstructure optimization approach together with the biorefinery
126 concept for the design of an integrated MSW management system. A case study in

127 Bangkok presented the potentials and benefits related to achieving self-sufficiency.

128 Niziolek et al. [30] proposed a superstructure-based approach to produce liquid

129 transportation fuels, olefins, and aromatics from MSW. The non-convex MINLP

130 optimization model was formulated and solved by using deterministic global

131 optimization solvers to optimality. Rizwan et al. [23] developed an optimization

132 framework to optimize the processing route to convert MSW into energy and valuable

133 products. The optimization model was formulated as MINLP which was later linearized

134 into MILP. The proposed method was applied to a case study in Abu Dhabi. The

135 optimal results consisted of an integrated MSW conversion pathway. Morero et al. [31]

136 presented an optimization model for the selection of an MSW treatment focusing on

137 AD. It was able to quantify the advantages of AD over landfilling and composting.

138 Although there have been a number of studies focusing on the design of MSW

139 management based on superstructure optimization, the potential of resource recovery

140 from waste management is not focused on. The residue stream including biosolids as

141 well as leachates and the uncertainty analysis are not accounted for. This can change

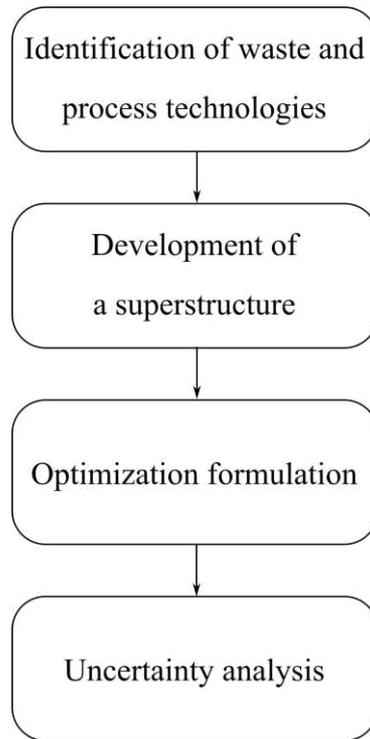
142 the optimal processing technology. In this study, the research gap is addressed by

143 developing a systematic framework based on superstructure optimization for the design

144 of a sustainable waste processing pathway. This can produce valuable products such as
145 electricity, bioethanol, and recycled materials under the presence of uncertainty.

146 **3. Framework for the design of waste management using superstructure** 147 **optimization**

148 The design of a sustainable waste management facility involves multiple waste
149 streams from particular locations to determine the best integrated waste processing
150 technology to convert the waste into valuable resources under a particular set of
151 constraints. This calls for a rigorous and efficient approach in order to account for all
152 possible process alternatives. The objective of this study is to develop a model-based
153 methodology using superstructure optimization to determine the optimal MSW
154 processing facility that can achieve economic sustainability. It is expected that all
155 wastes can be utilized and converted into energy and valuable products under economic
156 consideration. In this study, the framework of the superstructure optimization in the
157 design of the waste processing pathway is presented in **Fig 1**. It consists of 4 steps and
158 each step in the framework can be explained as follows:



159

160 **Fig 1.** The superstructure optimization methodology for the design of an optimal MSW

161 processing facility

162 *3.1 Identification of waste and process technologies*

163 In the first step, the identification of the MSW and the possible waste processing

164 technologies to include in the superstructure is carried out. This involves defining the

165 quantity and composition of the waste in a given location. Then the possible waste

166 processing technologies are investigated for each waste stream. The preliminary

167 selection of the waste processing technologies is screened based on information

168 regarding techno-economics (cost of each technology and recovery efficiency) and

169 process efficiency. This can be reviewed using technical reports, the published
170 literature, and mathematical models.

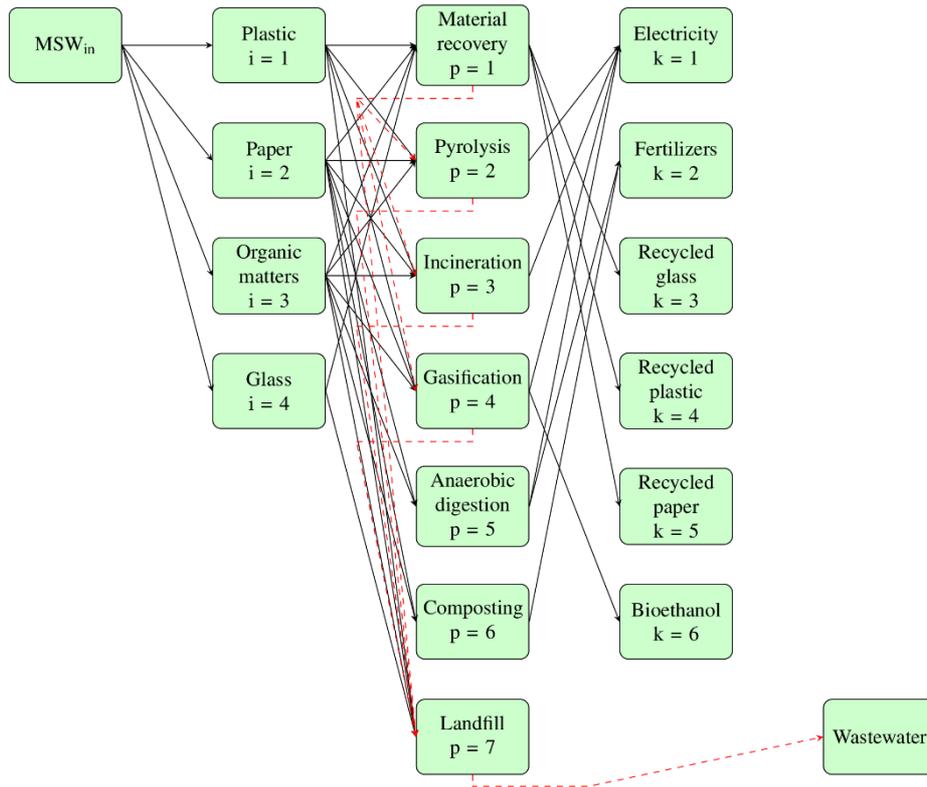
171 *3.2 Development of a superstructure*

172 After defining the amount of waste, the waste composition and the possible waste
173 processing technologies in use, it is possible to combine the information from the first
174 step into the superstructure as illustrated in **Fig 2**. The superstructure consists of
175 different compositions of waste, possible waste process technologies, potential
176 products, and likely residues. It is divided into three stages: waste segregation (index
177 i), waste processing (index p) and products (index k). The incoming MSW is
178 segregated into different fractions of waste. Then the waste is sent to the waste
179 processing technology to produce one or more products i.e. organic waste is sent to AD
180 which can potentially produce electricity and fertilizer. The residue from the waste
181 processing technology is also taken into account. For example, the residue from the
182 material recovery facility (MRF) can be sent to incineration or landfill.

183

184

185



186

187 **Fig 2.** Illustrative representation of the superstructure of the waste conversion
 188 technologies (black line – the flow of waste and the products from waste recovery; red
 189 dashed line – residue from the waste processing technologies).

190 *3.3 Optimization formulation*

191 The superstructure optimization is formulated based on the material balance to
 192 optimize the MSW processing pathway in terms of economic sustainability. The
 193 optimization formulation involves two types of variables:

- 194 • Binary variable: y – This type of variable is used to represent the selection of
195 the waste processing technologies and the associated interconnections. It is
196 equal to 1 if the corresponding technology is chosen; Otherwise, it is equal to 0.
- 197 • Continuous variable: x – This variable represents the flow and concentration of
198 the waste.

199 This study aims to evaluate and choose the best waste processing technology for
200 the MSW treatment process in the early stages of design. Binary variables are important
201 in this context because they can be used to select the most appropriate process
202 technologies from among a set of process alternatives used to identify the optimal waste
203 processing pathway. The optimization problem can be formulated as follows:

$$\begin{aligned} & \max_{x,y} \text{KPI}(x,y) \\ & \text{s.t. } h(x) = 0 \\ & \qquad \qquad \qquad g(x,y) \leq 0 \\ & \qquad \qquad \qquad x \in X, y \in \{0,1\} \end{aligned} \tag{1}$$

204 where $\text{KPI}(x,y)$ is the set of objective functions in which the economic or
205 environmental indicator or both can be used. It is a function of both types of variable.

206 $h(x)$ is the equality constraints representing the material balances. $g(x,y)$ is the
207 inequality constraints referring to the design specification and environmental
208 regulations, e.g. the maximum limit of the discharge. Details of the superstructure
209 optimization is presented as follows.

210 3.3.1 Objective function

211 The maximization of the annual profit is selected as the objective function of the
212 optimization model describing the MSW management given by:

$$z = \sum_{k \in K} SALE_k - \sum_{p \in P} CAP_p + \sum_{p \in P} OPE_p \quad (2)$$

213 where z is the annual profit (objective function); CAP_p and OPE_p are the
214 annual capital cost and operating cost of the waste processing technology p . $SALE_k$
215 is the annual revenue from selling the products, listed as k . The annual capital cost or
216 the initial investment cost includes land acquisition, any equipment, raw material, and
217 indirect costs such as the planning cost, contractual support, and financial services. The
218 annual operating cost includes maintenance and labor. In this study, it is assumed that
219 the annual capital and operating costs are dependent linearly on the flow entering the
220 processing technology. This can be calculated as follows:

$$CAP_p = \sum_{i \in I} F_{i,p}^{in} CCF_p \quad (3)$$

$$OPE_p = \sum_{i \in I} F_{i,p}^{in} CPF_p \quad (4)$$

221 where CCF_p and CPF_p are the annual capital and operating cost factors of the
 222 waste processing technology p . $F_{i,p}^{in}$ is the amount of waste i sent to the waste
 223 processing technology p . The product sale ($SALE_k$) is determined as follows:

$$SALE_k = \sum_{p \in P} F_{p,k} P_k \quad (5)$$

224 where $F_{p,k}$ is the amount of the product k obtained from the waste processing
 225 technology p and P_k is the selling price of the products k .

226 3.3.2 Material balance

227 The superstructure optimization framework in this work is based on the material
 228 balance constraints. For each stage in the superstructure, the material balance needs to
 229 be satisfied. As the MSW contains several compositions, it initially needs to be
 230 segregated to make it easier for processing and utilization. In the first stage, the
 231 incoming MSW to this stage is segregated into different groups. For simplicity, the four
 232 most common fractions of MSW are used for this calculation including organic waste,
 233 glass, paper, and plastic. The overall mass balance in this stage is given by:

$$MSW^{in} = \sum_{i \in I} W_i \quad (6)$$

234 where MSW^{in} is the flow of incoming MSW and W_i is the amount of waste i .

235 Different types of waste are sent to waste processing technologies as denoted by indices

236 p .

$$W_i = \sum_{p \in P} F_{i,p} \quad (7)$$

237 where $F_{i,p}$ is the amount of waste i sent to the processing technology p . Given

238 the flow of the waste stream, the selection of each interconnection linked to different

239 technologies for the MSW treatment facility is given by:

$$F^{lo} \cdot y \leq F \leq F^{up} \cdot y \quad (8)$$

240 where F^{lo} and F^{up} is the lower and upper bounds of the flow of the waste

241 streams. y is the binary variable used to select the existence of the waste stream or

242 waste processing technology. It is equal to 1 if the stream or technology is selected,

243 otherwise it becomes 0. In the second stage or the waste processing technology state,

244 the flow of the waste streams entering the conversion technology is described by:

$$F_p^{in} = \sum_{i \in I} F_{i,p} + \sum_{p' \in P} F_{p',p} \quad (9)$$

245 where F_p^{in} the flow of waste i entering the waste processing technology p . $F_{p',p}$

246 is the flow of the waste from conversion technology p' to the waste processing

247 technology p (residual flow). Note that some waste processing technologies do not
 248 have residual streams, so the $F_{p',p}$ is 0. The amount of waste residue leaving the
 249 processing technology is calculated based on the efficiency of the waste processing
 250 technology as follows:

$$\sum_{p' \in P} F_{p',p} = F_p^{in}(1 - E_p) \quad (10)$$

251 where E_p is the efficiency of the processing technology p . The amount of product
 252 obtained from the waste processing technology is given by:

$$\sum_{p \in P} F_{p,k} = \sum_{p \in P} F_p^{in} YIELD_{p,k} \quad (11)$$

253 where $YIELD_{p,k}$ is the yield of the product k obtained from the waste processing
 254 technology p .

255 3.3.3 Solution strategies

256 The proposed superstructure optimization model in this study corresponds to mixed
 257 integer linear programming (MILP). This problem was modeled using the optimization
 258 platform, GAMS. In this study, the CPLEX optimization solver is used for solving all
 259 of the problems to optimality.

260

261

262 *3.4 Uncertainty analysis*

263 Uncertainty analysis is performed to enhance the robustness of the solution. It is
264 important to show that the waste processing facility is feasible to operate over the set
265 of uncertain parameters. For example, the yield of products from each processing
266 technology may change over time as well as be different from place to place. This may
267 change the network of the waste processing technology so uncertainty has to therefore
268 be considered during the design. In order to incorporate the uncertainties into the
269 optimization problem, a common approach for handling uncertainties is two-stage
270 stochastic programming. It is based on a probabilistic model considering uncertainty
271 explicitly and there is the existence of recourse representing the corrective actions that
272 are available after a set of uncertainties has been realized. Regarding the two-stage
273 stochastic programming, a set of uncertainties is modeled using discrete or continuous
274 probability distribution and incorporated into the optimization formulation. This leads
275 to a robust-sufficient solution or an expectedly optimal solution. Two-stage stochastic
276 programming is commonly used in process design [32]. It involves a separation of the
277 decision variables into two sets namely the first-stage decision and second-stage
278 decision. In the first stage, the structural decisions are determined before the uncertainty

279 is realized. The second stage involves operational decisions when the uncertain values
280 are realized.

281 To account for a particular set of uncertainty in the optimization problem, it
282 involves three steps: uncertainty characterization, uncertainty mapping and decision-
283 making under uncertainty. In the first step, a set of uncertain parameters is identified
284 and sampled using the Latin Hypercube Sampling technique. This is a statistical method
285 used for scenario generation based on a predefined distribution function of uncertain
286 parameters [33-34]. In the second step, the optimization problem is solved separately
287 for each scenario to investigate the impact of the uncertainty on the objective function.
288 Finally, the optimization problem is reformulated using two-stage stochastic
289 programming (Eq. 12 and 13) and solved for different combinations of uncertain
290 parameters obtained from the sampling. The robustness of the optimal result can be
291 achieved using the following:

292

293

294

$$\begin{aligned}
& \min_{x,y} E_{\theta}[KPI(x, y, \theta)] \\
& \text{s.t. } h(x, \theta) = 0 \\
& g(x, y, \theta) \leq 0 \\
& x \in X, y \in \{0, 1\}, \theta \in \{\theta^{LO}, \theta^{UP}\}
\end{aligned} \tag{12}$$

295 where $E_{\theta}[KPI(x, y, \theta)]$ is the expected value of the objective function in the
296 presence of uncertainty and θ is the vector of uncertain parameters. The calculation of
297 the expected value in the presence of uncertainty requires a large computational burden.
298 The optimization problem in Eq. 12 can be reformulated into the deterministic
299 equivalent as given by:

$$\begin{aligned}
& \min_{x,y} \sum_{s=1}^S P_s \cdot KPI(x, y, s) \\
& \text{s.t. } h(x, s) = 0 \\
& g(x, y, s) \leq 0 \\
& x \in X, y \in \{0, 1\}, s \in S
\end{aligned} \tag{13}$$

300 where s is the number of scenarios from the sampling and P_s is the probability of
301 the realization of uncertainty. Note that the number of equations increases with the
302 number of scenarios.

303 4. Case study

304 The proposed approach has been applied to the design of a MSW treatment facility
305 in Ubon Ratchathani province in Thailand as a case study to identify economically
306 sustainable MSW processing technologies. Ubon Ratchathani province is a large city
307 in the northeastern of Thailand with a population of 1.875 million. It generated 1,800
308 tons of MSW per day in 2018 [4]. In terms of waste characteristics, the MSW is
309 categorized as organic waste (61%), plastic (17%), glass (6%), papers (8%), metal
310 (2%), wood (1%), rubber/leather (1%), cloth (1%), and other waste (3%) [35]. For the
311 sake of simplicity, the four largest compositions of MSW are considered in this study.
312 The current practice for waste management in Ubon Ratchathani province is where
313 most of the waste is sent to open dump sites which can potentially cause pollution
314 problems. This is becoming a disastrous issue because of the rapidly growing
315 population. This calls for better waste management for the improvement of the current
316 practice. The developed approach is able to provide suggestions to determine promising
317 technologies for waste management.

318 As mentioned previously, superstructure optimization is used for the design of an
319 MSW processing pathway. The superstructure is illustrated in **Fig 2** and the

320 corresponding optimization formulation is presented in Section 3. The superstructure
321 consists of three stages including segregation, the conversion of MSW, and the resulting
322 products. In the first stage (segregation), it is assumed that the MSW is screened at the
323 MSW source points which allow it to be sorted into different constituents based on their
324 properties. It is expected that the recyclable separation is performed at the source point
325 by the residents and then collected by the local authorities. Different components are
326 sent to different treatment and conversion technologies to be transformed into various
327 products. The list of waste processing technologies including waste to energy
328 technologies, composting, material recycle facilities as well as landfill. The
329 corresponding yields are presented in **Table 1**. Note that additional processing
330 technologies can be included in the superstructure to enhance the sustainability. Most
331 of the input parameters such as the conversion of waste into products has been taken
332 from the published literature. In the final state, the products obtained from each waste
333 processing technology are presented including electricity, bioethanol, and any
334 recyclable materials. It is noted that the recovered heat is only used for process
335 operation as it is practically not for sale in Thailand. In terms of the cost analysis, the

336 annual capital, operating cost and the selling price of the products have been given in
337 detail in **Tables 2** and **3**, respectively.

338 It is important to note that the transportation and waste collection costs are not
339 included in the economic analysis because this study aims to determine the optimal
340 processing pathway for converting MSW into valuable products. The costs presented
341 in **Table 2** are estimated since the actual cost may depend on various factors, e.g. raw
342 materials, government incentives, and skilled labor.
343

344 **Table 1.** List of the waste processing technology used in the superstructure and the product yields

345

Technology	Yield						Reference
	Electricity (kwh/tMSW)	Fertilizer (t/tMSW)	Paper (t/tMSW)	Plastic (t/tMSW)	Glass (t/tMSW)	Bioethanol (t/tMSW)	
Pyrolysis	490	-	-	-	-	-	[22]
Gasification I*	1,000	-	-	-	-	-	[22]
Gasification II**	-	-	-	-	-	0.255	[23]
Incineration	340	-	-	-	-	-	[22]
AD	187.5	0.27	-	-	-	-	[22]
MRF	-	-	0.9	0.75	0.89	-	[13]
Composting	-	0.3	-	-	-	-	[13]

346 *Gasification I – gasification with electricity generation, ** Gasification II – gasification with bioethanol generation.

347 **Table 2.** Details of the annual capital and operating cost factors for each waste
 348 processing technology per ton of MSW

Technology	<i>CCF</i> (\$/tMSW/yr)	<i>CPF</i> (\$/tMSW/yr)	Reference
Pyrolysis	400	50	[36]
Gasification I	250	45	[36]
Gasification II	447	113	[27]
Incineration	400	40	[36]
AD	50	5	[36]
Landfill	25	2.5	[36]
MRF	20	3.7	[14]
Composting	17	17	[37]

349 **Table 3.** Selling price of the recovered products

Product	Price	Reference
Electricity	\$0.20 USD/kWh with incentive	[38]
Fertilizer	\$70 USD/ton	[37]
Recycled paper	\$66.67 USD/ton	[39]
Recycled plastic	\$90 USD/ton	[40]
Recycled glass	\$53 USD/ton	[39]
Bioethanol	\$971 USD/ton	[41]

350 5. Results and discussion

351 5.1 Optimal waste processing network

352 Scenario-based analysis is performed to address the MSW processing problem with
353 respect to the maximization of the annual profit. It is divided into 2 scenarios: Scenario
354 I and Scenario II: Scenario I considers all waste processing technologies used to
355 develop the integrated waste treatment facility and Scenario II considers only the
356 landfill technology. The summary of the optimization results has been given in **Table**
357 **4**. The corresponding optimal waste processing pathway is illustrated in **Fig 3** for
358 Scenarios I. The optimal waste processing pathway for the Scenario I consists of AD
359 for the treatment of the organic fractions of MSW, recyclable materials, e.g. plastic,
360 paper, and glass are sent to the MRF. Residues from the MRF are sent to the landfill
361 for final disposal where the leachate generated is sent to the wastewater treatment
362 facility as presented in **Table 4**. The annual profit associated with the MSW processing
363 pathway in Scenario I is equal to \$6.90 million USD. It is positive which means that it
364 is profitable and shows economical feasible for the MSW management system.
365 Although the capital cost and operating cost are high, they are compensated for by the
366 large amount of revenue from the recovery of electricity in the AD of the organic waste,

367 fertilizers and the recycling of paper, plastics and glass. Further analysis reveals that
368 the annual profit is dominated by the revenue of products from material recovery. There
369 are five products obtained from the integrated waste processing facility: electricity,
370 fertilizers, recycled plastic, recycled paper, and recycled glass accounting for 42.62%,
371 21.48, 9.30%, 5.68%, and 20.92%, respectively. The capital cost involves three waste
372 processing technologies: AD (80.68%), MRF (16.62%), and landfill (2.70%). The
373 operating cost of the Scenario I consists of AD (57.32%), MRF (40.75%), landfill
374 (1.92%), and additional cost from the leachate treatment (0.01%). Other potential
375 technologies such as gasification or pyrolysis have not been selected because these
376 technologies have larger capital cost and operating cost which cannot possibly be
377 compensated for by the revenue.

378 It is worth investigating the comparison between the optimal result and the landfill
379 in the Scenario II which is the current practice in many places. The results show that
380 when all waste is sent to the landfill, the annual profit is equal to \$-16.36 million USD.
381 This is negative, meaning that it is not economically viable compared to Scenario I. The
382 annual profit in Scenario II is dominated by the capital cost of the landfill accounting
383 for \$15.11 million USD per year and \$1.51 million USD per year for the operating cost.

384 It was found that revenue is equal to \$0 USD per year or there is no product recovery
385 from the landfill site. Although the capital cost and operating cost of Scenario I are
386 higher than in Scenario II, the revenue from the product recovery in Scenario I is much
387 larger than Scenario II. This can compensate for the higher capital cost and operating
388 cost. It was found that Scenario I provides a promising alternative for MSW
389 management in a manner that is both profitable and economically sustainable. The use
390 of AD and the recycling of MSW in the MRF has been investigated by several
391 researchers but the study of an integrated system is limited. The results from Scenario
392 I can be a guideline for the decision-makers or local authorities to use to focus on the
393 potential waste processing alternatives for sustainable waste management in Ubon
394 Ratchathani province.

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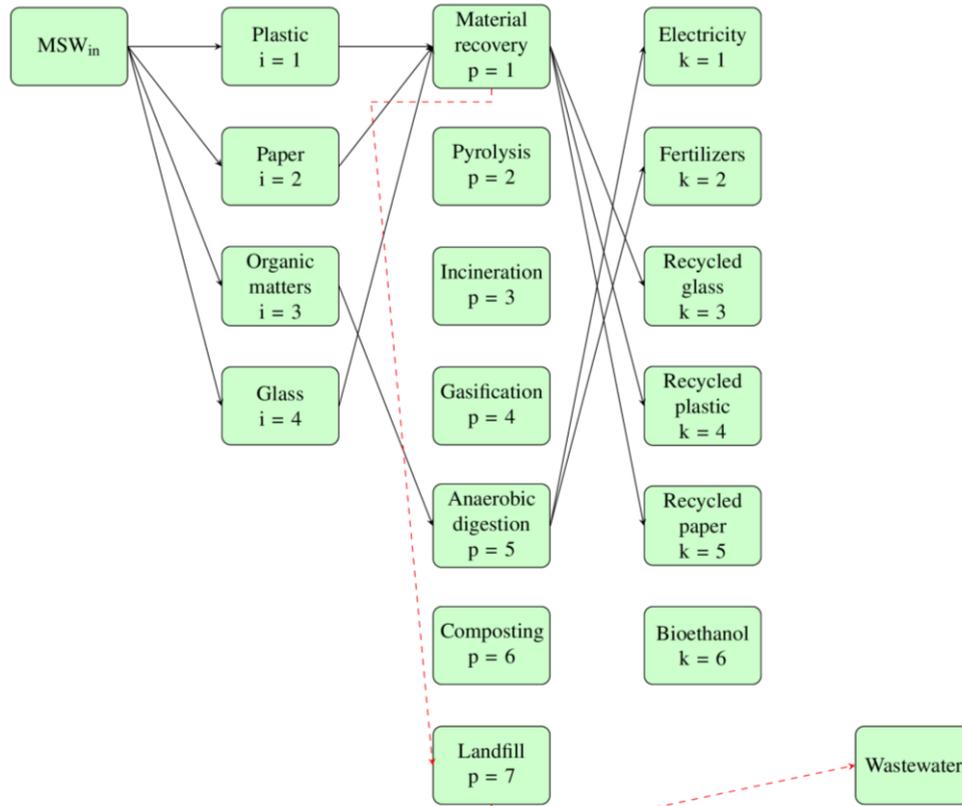
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400 **Table 4.** Summary of the optimal waste processing facilities in Scenarios I, II and the
 401 optimal waste processing facility under uncertainty.

Details	Unit	Scenario I	Scenario II	Optimal under uncertainty
Annual profit	M\$/YR	6.90	-16.63	6.64
CAP	M\$/YR	24.72	15.11	24.72
MRF	%	16.62	0.00	16.62
AD	%	80.68	0.00	80.68
Landfill	%	2.70	100.00	2.70
OPE	M\$/YR	3.48	1.51	3.48
MRF	%	40.75	0.00	40.75
AD	%	57.32	0.00	57.32
Landfill	%	1.92	99.29	1.92
Wastewater treatment	%	0.01	0.71	0.01
SALE	M\$/YR	35.10	0.00	34.87
Electricity	%	42.62	0.00	42.88
Fertilizer	%	21.48	0.00	21.59
Recycled paper	%	9.30	0.00	9.03
Recycled glass	%	5.68	0.00	20.97
Recycled plastic	%	20.92	0.00	5.53



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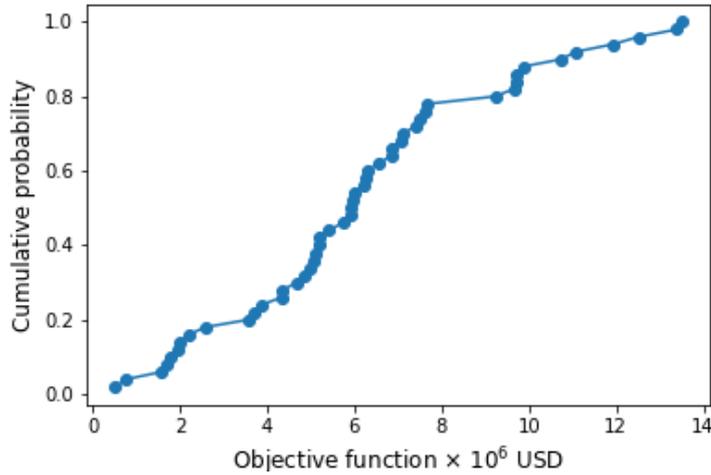
403 **Fig 3.** The optimal waste processing configuration for Scenario I

404 *5.2 Uncertainty analysis*

405 In this study, the yields of the products are considered to be included in the set of
 406 uncertainty. These parameters represent the performance of each waste processing
 407 technology which may be different from plant to plant. A fluctuation in the yield of the
 408 products may requires the recourse action of changing the waste streams to other waste
 409 processing technologies. The uncertain parameters were sampled based on the Latin
 410 hypercube sampling technique to define 50 future scenarios with a uniform probability
 411 distribution in order to reflect the characterization of uncertainty. It is assumed that

412 there is no correlation between the uncertain parameters. After the 50 future scenarios
413 were generated, a separate optimization problem was solved. The results show that two
414 different waste processing pathways are selected as a function of the uncertainty
415 realization. The majority of the solutions with respect to the uncertainty realization
416 (94%) select similar waste processing network as in Scenario I in Section 5.1. For the
417 second waste processing network (6%), it consists of composting organic waste instead
418 of AD. Paper, plastic and glass are sent to the MRF for plastic and glass recovery while
419 the remaining materials from the MRF are sent to the landfill. The cumulative
420 probability distribution of the objective function is illustrated in **Fig 4** where the
421 objective function (the annual profit) is displayed on the x-axis and the cumulative
422 distribution on the y-axis represents the probability that the objective function will be
423 lower than the stated value. It was found that a variability of the objective function can
424 be observed ranging from \$0.51 to \$13.48 million USD per year. To compare this with
425 the optimal solution in Scenario I as presented in **Table 4**, it can be found that 66% of
426 the scenarios yields a lower objective function and 6% yields a different waste
427 processing configuration. This indicates that the uncertainty in terms of the product
428 yields has a large impact on the performance of the pathway and the associated

429 decision-making, so it is important to consider carefully in the decision-making
430 process.



431

432 **Fig 4.** Cumulative probability distribution of the objective function

433 Finally, the optimization problem under uncertainty is formulated and solved as
434 presented in Eq. 13. The MILP problem consists of 16,501 constraints and 4,600 binary
435 variables. The summary of the optimal solution under uncertainty realization has been
436 presented in **Table 4**. The results show that the annual profit obtained is \$6.64 million
437 USD. The optimal waste processing network under uncertainty has a similar network
438 to the optimal waste processing network without considering uncertainty (Scenario I in
439 Section 5.1) with a lower objective function of 3.91%. This indicates the robustness of
440 the optimal solution. This proposed methodology is expected to be a decision-making
441 tool for the local authorities, and/or engineers. It can be used for comparing waste

442 processing technologies and for the selection of the best waste processing technologies
443 among the alternatives with respect to the desired criteria in order to provide the optimal
444 solution while complying with the standard regulations. Note that the current study
445 has presented the underlying theory and practical implementation of the proposed
446 methodology based on an illustrative example. Future studies will consider i) updating
447 and expanding the database on the processing technologies in a superstructure and ii)
448 evaluating the environmental impact.

449 **6. Conclusions**

450 This paper presents the potential for superstructure optimization in the design of an
451 integrated waste treatment facility. The proposed method is applied for the case study
452 in Ubon Ratchathani province, Thailand to illustrate its applicability. The results have
453 shown that the proposed waste processing pathway is economically viable in reference
454 to a positive annual profit. This is important because the integrated waste treatment
455 facility has presented the concept of a circular economy which is the driving force
456 towards sustainability. After that, the uncertainty is incorporated into the optimization
457 framework. Variations in the waste processing network and the objective function
458 values in the different scenarios are obtained. The developed approach is expected to

459 support and evaluate the waste processing technologies used in the design and
460 retrofitting of the waste processing facility. Future work will focus on the updating and
461 extension of the superstructure, the evaluation of the environmental impacts of the
462 different waste processing networks as well as the flexibility of the waste processing
463 network as a whole.

464 **Declarations**

465 **Availability of data and materials**

466 All data generated or analyzed during this study are available from the corresponding
467 author on reasonable request.

468 **Competing interests**

469 The authors declare they have no competing interests.

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473 **Authors' contributions**

474 CP conducted research, developed the mathematical optimization framework, prepared,
475 read and approved the manuscript.

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479 **References**

- 480 1. Verma RL, Borongan G, Memon M. Municipal Solid Waste Management in Ho
481 Chi Minh City, Viet Nam, Current Practices and Future Recommendation.
482 Procedia Environ Sci. 2016;35:127–39.
- 483 2. Hoornweg D, Perinaz BT. What a waste: a global review of solid waste
484 management. Urban Dev Ser Knowl Pap. 2012;15:87–8.
- 485 3. Dhokhikah Y, Trihadiningrum Y. Solid waste management in Asian developing
486 countries: Challenges and opportunities. J Appl Environ Biol Sci. 2012;2:329–
487 35.
- 488 4. Pollution Control Department. Situation report on current disposal sites of
489 municipal solid waste in Thailand in 2018 [Internet]. 2019. Available from:
490 <http://infofile.pcd.go.th/Waste/Wst2018.pdf>
- 491 5. Pollution Control Department. Booklet on Thailand state of pollution 2018
492 [Internet]. 2019. 6–18 p. Available from: <http://www.pcd.go.th/file/Booklet on>

- 493 Thailand State of Pollution 2018.pdf
- 494 6. Dong C, Jin B, Li D. Predicting the heating value of MSW with a feed forward
495 neural network. *Waste Manag.* 2003;23:103-106.
- 496 7. Moya D, Aldás C, López G, Kaparaju P. Municipal solid waste as a valuable
497 renewable energy resource: a worldwide opportunity of energy recovery by
498 using Waste-To-Energy Technologies. *Energy Procedia.* 2017;134:286–95.
- 499 8. Pour N, Webley PA, Cook PJ. Potential for using municipal solid waste as a
500 resource for bioenergy with carbon capture and storage (BECCS). *Int J Greenh
501 Gas Control.* 2018;68:1–15.
- 502 9. Tsui T-H, Wong JWC. A critical review: emerging bioeconomy and waste-to-
503 energy technologies for sustainable municipal solid waste management. *Waste
504 Dispos Sustain Energy.* 2019;1(3):151–67.
- 505 10. Ikhlayel M, Nguyen LH. Integrated Approaches to Water Resource and Solid
506 Waste Management for Sustainable Development. *Sustain Dev.*
507 2017;25(6):467–81.
- 508 11. Zaman AU, Lehmann S. The zero waste index: a performance measurement tool
509 for waste management systems in a ‘zero waste city.’ *J Clean Prod.* 2013;50:123–

- 510 32.
- 511 12. Guibrunet L, Sanzana Calvet M, Castán Broto V. Flows, system boundaries and
512 the politics of urban metabolism: Waste management in Mexico City and
513 Santiago de Chile. *Geoforum*. 2017;85:353–67.
- 514 13. Markic DN, Carapina HS, Bjelic D, Bjelic LS, Ilic P, Pesic ZS, et al. Using
515 material flow analysis for waste management planning. *Polish J Environ Stud*.
516 2019;28(1):255–65.
- 517 14. Pressley PN, Levis JW, Damgaard A, Barlaz MA, De Carolis JF. Analysis of
518 material recovery facilities for use in life-cycle assessment. *Waste Manag*.
519 2015;35:307-317.
- 520 15. Khandelwal H, Thalla AK, Kumar S, Kumar R. Life cycle assessment of
521 municipal solid waste management options for India. *Bioresour Technol*.
522 2019;288:121515.
- 523 16. Mencarelli L, Chen Q, Pagot A, Grossmann IE. A review on superstructure
524 optimization approaches in process system engineering. *Comput Chem Eng*.
525 2020;136:106808.
- 526 17. Umeda T, Hirai A, Ichikawa A. Synthesis of optimal processing system by an

- 527 integrated approach. *Chem Eng Sci.* 1972;27(4):795–804.
- 528 18. Khor CS, Chachuat B, Shah N. Fixed-flowrate total water network synthesis
529 under uncertainty with risk management. *J Clean Prod.* 2014;77:79–93.
- 530 19. Puchongkawarin C, Gomez-Mont C, Stuckey DC, Chachuat B. Optimization-
531 based methodology for the development of wastewater facilities for energy and
532 nutrient recovery. *Chemosphere.* 2015;140:150–8.
- 533 20. Ali RA, Nik Ibrahim NNL, Lam HL. Conversion Technologies: Evaluation of
534 Economic Performance and Environmental Impact Analysis for Municipal Solid
535 Waste in Malaysia. *Processes.* 2019;7(10):1-14.
- 536 21. Cimpan C, Maul A, Jansen M, Pretz T, Wenzel H. Central sorting and recovery
537 of MSW recyclable materials: A review of technological state-of-the-art, cases,
538 practice and implications for materials recycling. *J Environ Manage.*
539 2015;156:181–199.
- 540 22. Ng WPQ, Lam HL, Varbanov PS, Klemeš JJ. Waste-to-Energy (WTE) network
541 synthesis for Municipal Solid Waste (MSW). *Energy Convers Manag.*
542 2014;85:866–874.

- 543 23. Rizwan M, Saif Y, Almansoori A, Elkamel A. Optimal processing route for the
544 utilization and conversion of municipal solid waste into energy and valuable
545 products. *J Clean Prod.* 2018;174:857–867.
- 546 24. Satchatippavarn S, Martinez-Hernandez E, Leung Pah Hang MY, Leach M, Yang
547 A. Urban biorefinery for waste processing. *Chem Eng Res Des.* 2016;107:81–
548 90.
- 549 25. Wilson DC, Rodic L, Scheinberg A, Velis CA, Alabaster G. Comparative
550 analysis of solid waste management in 20 cities. *Waste Manag Res.*
551 2012;30(3):237–54.
- 552 26. Abeliotis K, Karaiskou K, Togia A, Lasaridi K. Decision support systems in solid
553 waste management: A case study at the national and local level in Greece. *Glob
554 Nest J.* 2009;11:117–126.
- 555 27. Khan MM-U-H, Jain S, Vaezi M, Kumar A. Development of a decision model
556 for the techno-economic assessment of municipal solid waste utilization
557 pathways. *Waste Manag.* 2016;48:548–564.
- 558 28. Fernández-Nava Y, del Río J, Rodríguez-Iglesias J, Castrillón L, Marañón E.
559 Life cycle assessment of different municipal solid waste management options: a

- 560 case study of Asturias (Spain). *J Clean Prod.* 2014;81:178–189.
- 561 29. Santibañez-Aguilar JE, Martinez-Gomez J, Ponce-Ortega JM, Nápoles-Rivera F,
562 Serna-González M, González-Campos JB, et al. Optimal planning for the reuse
563 of municipal solid waste considering economic, environmental, and safety
564 objectives. *AIChE J.* 2015;61(6):1881–1899.
- 565 30. Niziolek AM, Onel O, Floudas CA. Municipal solid waste to liquid
566 transportation fuels, olefins, and aromatics: Process synthesis and deterministic
567 global optimization. *Comput Chem Eng.* 2017;102:169–187.
- 568 31. Morero B, Montagna AF, Campanella EA, Cafaro DC. Optimal process design
569 for integrated municipal waste management with energy recovery in Argentina.
570 *Renew Energy.* 2020;146:2626–2636.
- 571 32. Awasthi U, Marmier R, Grossmann IE. Multiperiod optimization model for
572 oilfield production planning: bicriterion optimization and two-stage stochastic
573 programming model. *Optim Eng.* 2019;20(4):1227–1248.
- 574 33. Bozkurt H, Quaglia A, Gernaey K V., Sin G. A mathematical programming
575 framework for early stage design of wastewater treatment plants. *Environ Model*
576 *Softw.* 2015;64:164–176.

- 577 34. Nikzad E, Bashiri M, Oliveira F. Two-stage stochastic programming approach
578 for the medical drug inventory routing problem under uncertainty. *Comput Ind*
579 *Eng.* 2019;128:358–370.
- 580 35. Boonpa S, Sharp A. Waste-to-energy policy in Thailand. *Energy Sources, Part B*
581 *Econ Planning, Policy.* 2017;12(5):434–442.
- 582 36. Kumar A, Samadder SR. A review on technological options of waste to energy
583 for effective management of municipal solid waste. *Waste Manag.* 2017;69:407–
584 422.
- 585 37. Pandyaswargo AH, Premakumara DGJ. Financial sustainability of modern
586 composting: the economically optimal scale for municipal waste composting
587 plant in developing Asia. *Int J Recycl Org Waste Agric.* 2014;3(3):1-14.
- 588 38. A. H. Pandyaswargo and D. G. J. Premakumara, “Financial sustainability of
589 modern composting: the economically optimal scale for municipal waste
590 composting plant in developing Asia,” *Int. J. Recycl. Org. Waste Agric.*, vol. 3,
591 no. 3, p. 4, 2014, doi: 10.1007/s40093-014-0066-y.
- 592 39. EPPO. Policy of electricity purchase: Feed in tariff [Internet]. 2015. Available
593 from http://www.eppo.go.th/images/Power/pdf/FT-history/FiT_2558.pdf

- 594 40. Wongpanit, “History purchase price of recycling materials”, 2020. Available
595 from http://www.wongpanit.com/list_history_price.
- 596 41. Tan ST, Lee CT, Hashim H, Ho WS, Lim JS. Optimal process network for
597 municipal solid waste management in Iskandar Malaysia. *J Clean Prod.*
598 2014;71(2014):48–58.
- 599 42. CEIC. Thailand reference price: Ethanol price [Internet]. 2018. Available from
600 [https://www.ceicdata.com/en/thailand/biofuel-reference-price/ref erence-price-](https://www.ceicdata.com/en/thailand/biofuel-reference-price/reference-price-ethanol-price)
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Figures

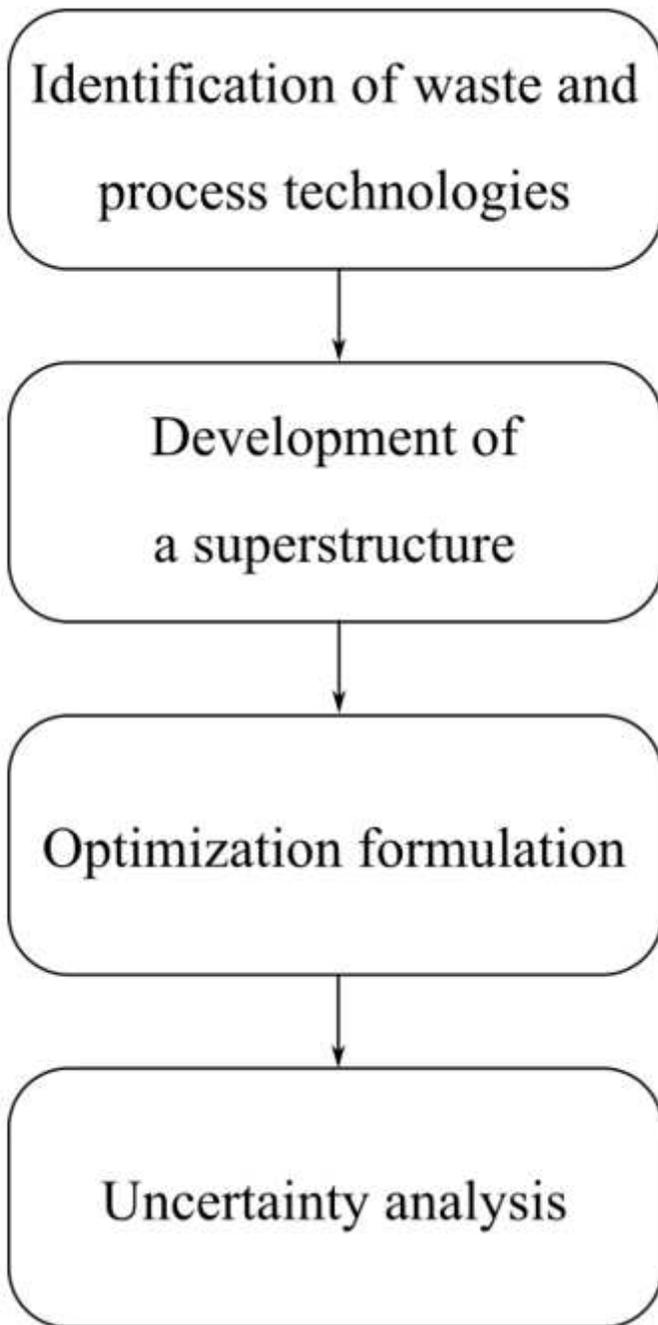


Figure 1

The superstructure optimization methodology for the design of an optimal MSW processing facility

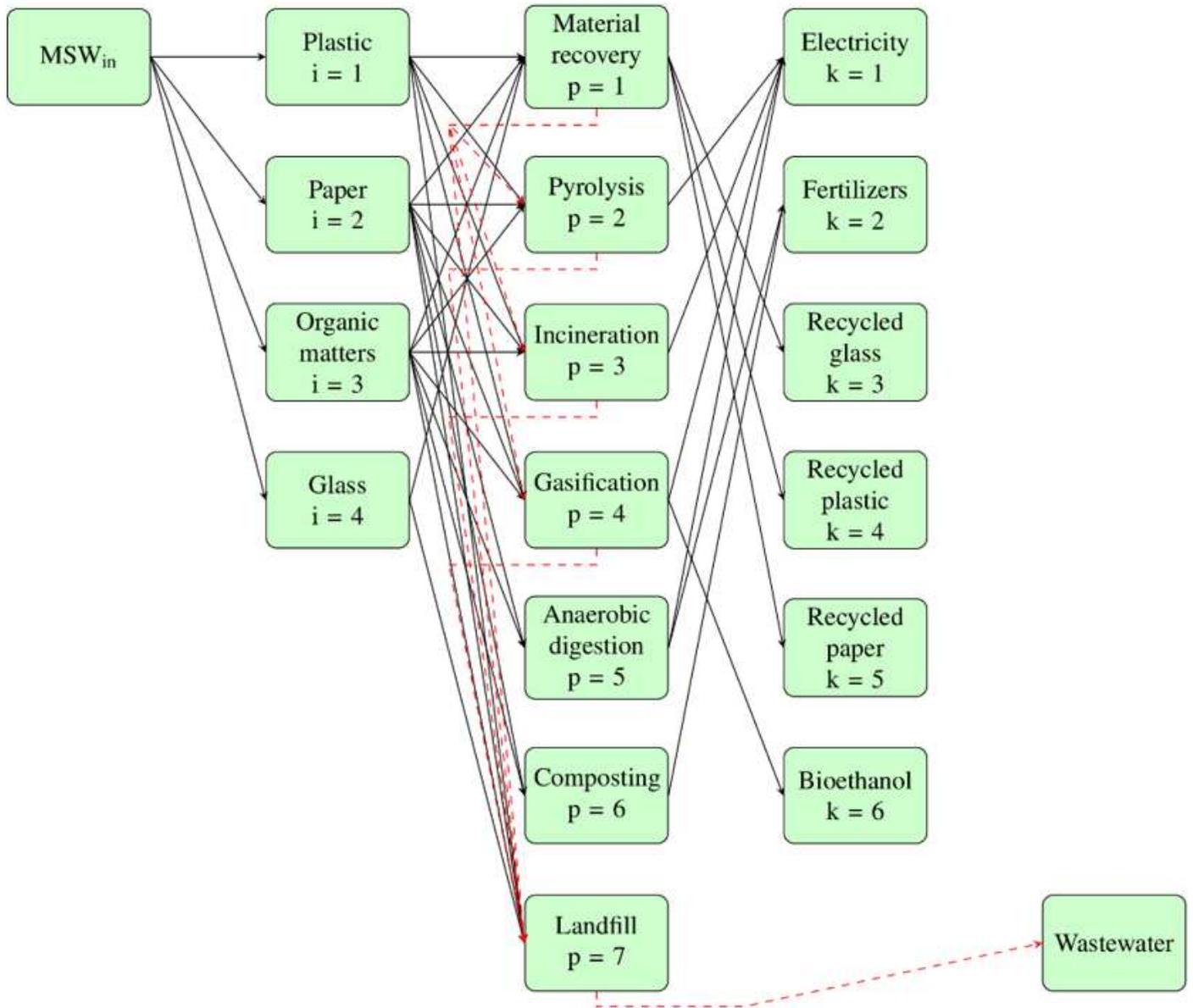


Figure 2

Illustrative representation of the superstructure of the waste conversion technologies (black line – the flow of waste and the products from waste recovery; red dashed line – residue from the waste processing technologies).

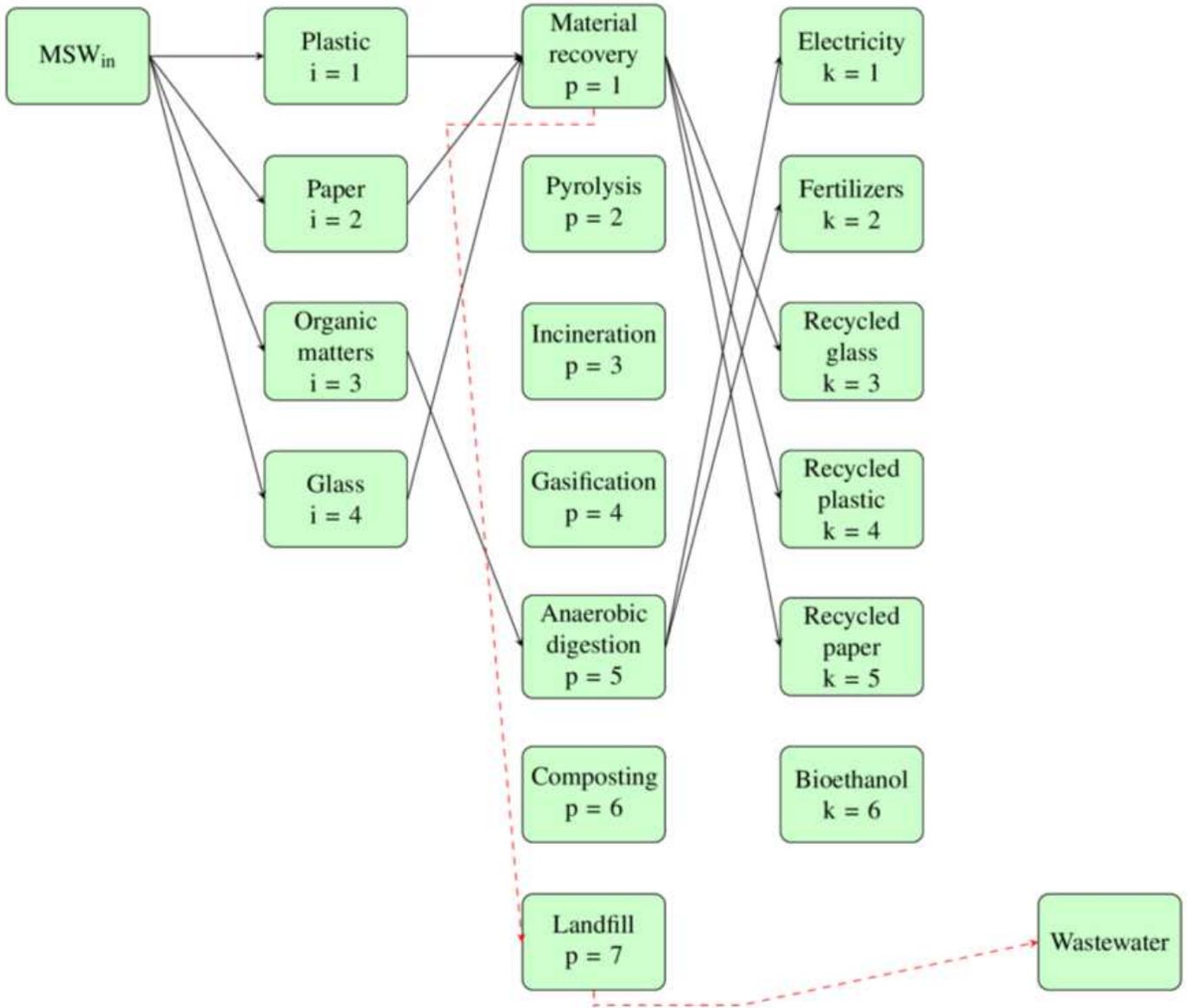


Figure 3

The optimal waste processing configuration for Scenario I

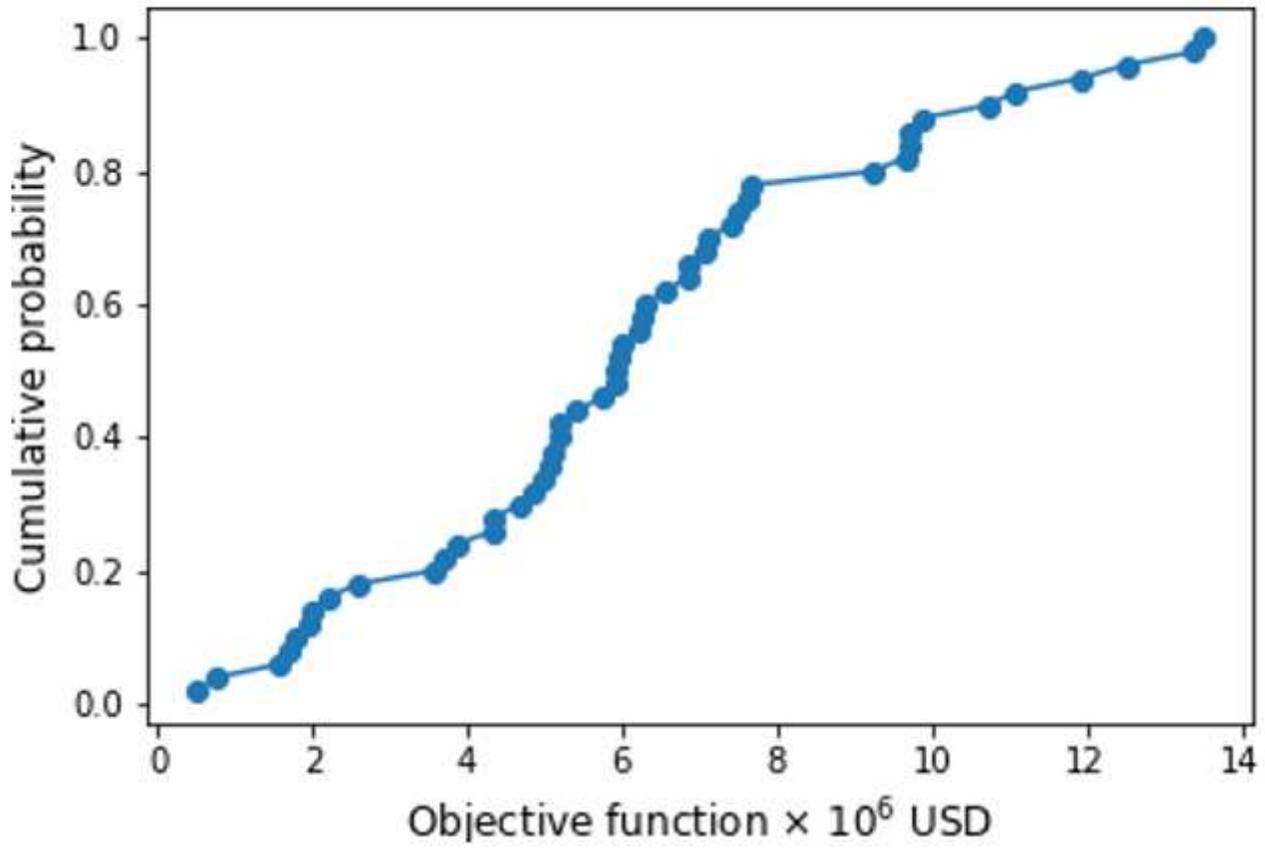


Figure 4

Cumulative probability distribution of the objective function