



## 18 **Abstract**

19 Natural coagulants from plants resources have gained a lot of attention as it is  
20 renewable, biodegradable, non-hazardous, lower cost, and less sludge generated  
21 compared to chemical coagulants. However there are still some drawbacks, namely  
22 long settling time and possible increase of dissolved organic carbon (DOC) in the  
23 treated water. In this paper we tried to address these drawbacks by utilizing citrate  
24 modified Fe<sub>3</sub>O<sub>4</sub> to adsorb protein from *Leucaena leucocephala* as the active  
25 coagulating agent. The effect of trisodium citrate concentration and protein adsorption  
26 pH to the adsorbed protein was investigated. It was found that the trisodium citrate  
27 concentration of 0.5 M and pH 4.0 gave the highest protein adsorption. The obtained  
28 magnetic coagulant was furthermore characterized using SEM, XRD, FTIR, and  
29 TEM, to observe the characteristics before and after protein adsorption. Furthermore  
30 the effect of pH (2-10) and coagulant dosage (60-600 mg. L<sup>-1</sup>) to the removal of  
31 synthetic Congo red wastewater and sludge volume formation was investigated. It was  
32 found that pH 3.0 was the best pH for coagulation due to charge neutralization  
33 mechanism of leucaena protein. Furthermore the highest removal was obtained at  
34 dosage 420mg. L<sup>-1</sup> with 80% removal. This result was comparable with crude extract  
35 of leucaena with half settling time (20 min) and lower increase of permanganate  
36 value.

37 **Keywords:** Congo red, Fe<sub>3</sub>O<sub>4</sub>, iron oxide nanoparticles, *Leucaena leucocephala*,  
38 magnetic coagulant, natural coagulant

## 39 **1. Introduction**

40 In recent years, utilization of various natural resources as natural coagulant has  
41 gained a lot of interest due to its various advantages, such as: lower cost compared to

42 chemical coagulants, it comes from renewable sources, less sludge volume generated,  
43 and biodegradable- non-hazardous sludge [1, 2]. However there are some drawbacks  
44 in natural coagulant application, which we addressed in this research. Firstly, the  
45 settling time needed for separation of flocs is most likely between 60 to 120 min by  
46 gravity. It is important to decrease the settling time, as long residence time could lead  
47 to bigger designed settling tank is needed, which could lead to higher capital cost.  
48 Secondly, direct utilization of plant parts or its crude extract could increase the  
49 dissolved organic carbon (DOC) in the treated water, due to some soluble non-  
50 coagulant compounds from the plant [3]. It is known that high DOC could stimulate  
51 high microbial activities, making disinfection process more difficult.

52 There were some researchers that combined iron oxide nanoparticles and natural  
53 coagulant to improve the coagulation performance, especially in terms of settling  
54 time. There are two approaches that have been used, firstly the protein as active  
55 coagulating agent was used to functionalize the surface of iron oxide nanoparticles,  
56 secondly, the iron oxide nanoparticles was dispersed in crude extract of natural  
57 coagulant. [4] synthesized magnetic coagulant using composite of  $\text{Fe}_3\text{O}_4$  and  $\gamma\text{-Fe}_2\text{O}_3$   
58 water-oil emulsion and functionalized with purified protein from *Moringa oleifera*. It  
59 was obtained that 90% turbidity removal was obtained at 12 min settling under  
60 external magnet force, compared to gravitation only (240 min).

61 Different types of iron oxide nanoparticles,  $\alpha\text{-Fe}_2\text{O}_3$ ,  $\gamma\text{-Fe}_2\text{O}_3$ , and  $\text{Fe}_3\text{O}_4$ , have  
62 been studied by Santos group to remove turbidity and color from synthetic wastewater  
63 [5-9]. In those researches, iron oxide nanoparticles were dispersed in crude extract of  
64 *Moringa oleifera*. It was found that high of removal was obtained for turbidity and  
65 color within short settling time (less than 30 min) under magnetic settling. It was also  
66 found that the coagulation mechanism was mostly charge neutralization, where

67 protein acted as the active coagulating agent, and interaction between protein and iron  
68 oxide nanoparticles made the fast settling process possible. Similar result was also  
69 obtained by [10] where magnetically assisted coagulation of Congo red gave half  
70 settling time when compared to leucaena extract only with similar removal value.  
71 Vieira group isolated globulin and albumin fraction from *Moringa oleifera* and  
72 functionalized it with iron oxide nanoparticles [11, 12]. The obtained magnetic  
73 coagulant was used to remove color from synthetic dye waste namely Amaranth,  
74 Brilliant Blue, Sunset Yellow, and Reactive Black 5. Combination of albumin and  
75 iron oxide nanoparticles gave %removal around 52-94%, depending to the dyes, with  
76 5 min magnetic sedimentation.

77 Concerning the high DOC content of natural coagulant treated water; some efforts  
78 have been done by previous researchers. [1] suggested that extraction and isolation of  
79 active coagulating agent could tackle this problem. Extraction of active coagulating  
80 agent, especially protein, using saline has been extensively studied. It has been proved  
81 that salting-in interaction between NaCl and protein could increase the protein  
82 solubility, resulting in lower dosage needed in the coagulation. This extraction step  
83 could be followed by purification steps to isolate protein that act as active coagulating  
84 agent. Several purification methods have been investigated, such as ion exchange [13-  
85 15], dialysis [16], spray drying [17], ultrafiltration [18, 19], and lyophilization [20].  
86 However the previously mentioned methods required many complicated steps,  
87 making it impractical in large scale.

88 Iron oxide nanoparticles are known to be able to selectively bind protein thus  
89 could be used in protein purification [21]. However, for its application in aqueous  
90 medium, the hydrophobicity of iron oxide nanoparticles becomes its drawback [22].  
91 On the other hand, the presence of hydroxyl group on the surface of iron oxide

92 nanoparticles makes the surface of particles easily modified using various functional  
93 groups, one of which carboxylic acid [23]. Citric acid, a trivalent organic acid, has  
94 been widely used as capping agent to prevent agglomeration of iron nanoparticles.  
95 Furthermore, citric acid modified of iron oxide nanoparticles has shown affinity to  
96 immobilize protein, enzymes, drugs, etc. [24-29].

97 In this study, we investigate functionalized Fe<sub>3</sub>O<sub>4</sub> nanoparticles with protein from  
98 leucaena (*Leucaena leucocephala*) crude extract as magnetic natural coagulant to treat  
99 synthetic Congo red wastewater. To the best of authors' knowledge, this study is the  
100 first study that reported utilization of adsorbed protein on citrate modified Fe<sub>3</sub>O<sub>4</sub> as  
101 magnetic coagulant. Based on our previous study, leucaena protein could act as  
102 natural coagulant to remove turbidity [30] and color [31]. The Fe<sub>3</sub>O<sub>4</sub> was modified  
103 using citrate ion that act as a bridge for protein adsorption. The effect of pH  
104 modification and citrate ion concentration to the protein adsorbed was investigated.  
105 The best condition that gave the highest adsorbed protein was characterized and used  
106 as magnetic coagulant for Congo red removal from synthetic wastewater. The effect  
107 of coagulation pH, magnetic coagulant dosage, and removal kinetics under magnetic  
108 field were investigated.

## 109 **2. Methodology**

### 110 *2.1. Synthesis of magnetic coagulant*

111 The synthesis of magnetic coagulant was following method used by [27] with  
112 modification. A mixture of 80 mg Fe<sub>3</sub>O<sub>4</sub> (pure grade, Sigma Aldrich) and 160 mL  
113 trisodium citrate (p.a, Sigma Aldrich) was sonicated for 30 min, followed by mixing  
114 for 2 h, 80°C. The mixture was let cool to room temperature, then separated using  
115 magnet, and washed using distilled water to remove unadsorbed citrate anion. The

116 citrate modified  $\text{Fe}_3\text{O}_4$ , denoted as  $\text{Fe}_3\text{O}_4\text{-CA}$ , was then oven dried in vacuum  
117 condition at  $60^\circ\text{C}$ , and then stored in a closed lid in a desiccator.

118 Leucaena protein was used as the protein source to functionalize the  $\text{Fe}_3\text{O}_4\text{-CA}$ .  
119 Dried leucaena seeds were obtained from Probolinggo, East Java. The seeds kernel  
120 was separated from its coat by grinding and sieving to obtain seeds kernel powder  
121 with average size of 0.177 mm. Extraction of protein from seeds kernel powder was  
122 done by using 1 M NaCl solution with seeds to solvent mass ratio of 1:20 using  
123 dispersed batch method for 60 min. The cake was separated by mean of filtration, and  
124 the extract was used for  $\text{Fe}_3\text{O}_4\text{-CA}$  functionalization. To prevent any degradation  
125 during storage, the extract was freshly made prior to every experiment.

126 Functionalization of  $\text{Fe}_3\text{O}_4\text{-CA}$  was done by mixing 5 mL of leucaena crude  
127 extract, which pH was adjusted using 0.1 M citrate buffer solution, prior to mixing  
128 with 80 mg  $\text{Fe}_3\text{O}_4\text{-CA}$ . The mixture was sonicated for 1 min, followed by mixing at  
129 room temperature for 4 h. The protein functionalized iron nanoparticles, denoted as  
130  $\text{Fe}_3\text{O}_4\text{-CA-protein}$ , was separated using external magnet, washed with distilled water,  
131 and vacuum dried at  $60^\circ\text{C}$ . The obtained  $\text{Fe}_3\text{O}_4\text{-CA-protein}$  was stored in a closed lid  
132 in a desiccator and used as magnetic coagulant in this study.

133 The concentration of trisodium citrate and pH of protein adsorption was varied as  
134 presented in Table 1. The protein concentration in the solution before and after  
135 adsorption was determined using Bradford method [32], where the protein  
136 concentration was stated equivalent to bovine serum albumin (BSA) standard. The  
137 response observed was the protein adsorption capacity ( $q$ ; mg eq BSA.  $\text{mg Fe}_3\text{O}_4^{-1}$ ),  
138 which was calculated using Eq. 1, where  $C_t$  and  $C_e$  (mg eq BSA.  $\text{L}^{-1}$ ) were initial and

139 final protein concentration,  $m$  (mg) is the mass of  $\text{Fe}_3\text{O}_4$ , and  $V$  (L) is the volume of  
140 the solution.

141 [Table 1]

$$142 \quad q = \frac{(Ct-Ce) \times V}{m} \quad (1)$$

## 143 2.2. Characterization

144 The magnetic coagulant that gave the highest protein adsorption was  
145 characterized to observe the difference before and after protein functionalization. The  
146 functional groups of pristine  $\text{Fe}_3\text{O}_4$ , citrate modified  $\text{Fe}_3\text{O}_4$ , and protein functionalized  
147  $\text{Fe}_3\text{O}_4$  were characterized using KBr pellet method Fourier Transform Infrared  
148 Spectroscopy (FTIR; Prestige 21 Shimadzu Instruments). The morphology and atomic  
149 composition was observed using Scanning Electron Microscope (SEM; HITACHI  
150 SU3500). The particle size was observed using Transmission Electron Microscope  
151 (TEM; HITACHI HT7700), while the crystallinity was analyzed using X-Ray  
152 Diffraction (XRD; BRUKER D8 Advance). Based on the XRD spectra, the crystallite  
153 size ( $d$  in nm) was estimated using Scherrer equation (Eq. 2), where  $\theta$  is the Bragg  
154 angle;  $K$  is Scherrer constant (0.9);  $\lambda$  (nm) is the wavelength of Cu K- $\alpha$  radiation  
155 (0.15405 nm); and  $\beta$  is the full width at half maximum peak (FWHM).

$$156 \quad d = \frac{K \cdot \lambda}{\beta \cdot \cos \theta} \quad (2)$$

## 157 2.3. Jar test experiment

158 The obtained magnetic coagulant was tested to remove synthetic dye wastewater.  
159 Congo red solution with concentration of 10 ppm was used as the model dye in this  
160 study. Coagulation study was done by mixing magnetic coagulant and Congo red

161 solution with rapid mixing at 100 rpm for 2 min, followed by slow mixing at 20 rpm  
162 for 20 min using a jar test apparatus. The mixture was then let to settle in an Imhoff  
163 cone under array of neodymium magnets. During this step, sample of treated water  
164 was taken every 5 min until 1 h. The concentration of Congo red at initial condition  
165 and during sampling was measured using a spectrophotometer at its maximum  
166 wavelength (505 nm). The removal of Congo red was calculated using Eq. 3, where  
167  $A_i$  and  $A_t$  are initial and final absorbance respectively. The sludge volume ( $\text{mL} \cdot \text{L}^{-1}$ )  
168 was measured using Imhoff cone after 1 h settling, and calculated using Eq. 4. The  
169 wastewater pH and magnetic coagulant dosage were varied as presented in Table 2.

$$170 \quad \% \text{ removal} = \frac{A_i - A_t}{A_i} \times 100\% \quad (3)$$

$$171 \quad \text{sludge volume} = \frac{\text{sludge volume (mL)}}{\text{wastewater volume (L)}} \quad (4)$$

172 [Table 2]

173 The permanganate value (PV) was measured at the best pH and coagulant dosage  
174 using following method [33]. 5 mL of 4 N  $\text{H}_2\text{SO}_4$  and 10 mL of 0.1 N  $\text{KMnO}_4$  were  
175 added into 100 mL of sample solution. The mixture was heated for 10 minutes, after  
176 which 10 mL of 0.01 N  $\text{H}_2\text{C}_2\text{O}_4$  solutions was added. The solution is back titrated  
177 using  $\text{KMnO}_4$  solution until the end point was reached. The volume titration of the  
178 potassium permanganate solution used was recorded, and the PV ( $\text{mg KMnO}_4 \cdot \text{L}^{-1}$ )  
179 was calculated.

#### 180 2.4. Settling kinetic models

181 The evaluation of removal during settling was approached using several  
182 adsorption kinetic models. The value of adsorption capacity,  $q$  ( $\text{mg dye} \cdot \text{mg magnetic}$

183 coagulant<sup>-1</sup>), was calculated using equation 1. In the equation,  $C_t$  denotes  
184 concentration (mg dye. L<sup>-1</sup>) at time  $t$  min,  $C_e$  (mg dye. L<sup>-1</sup>) is concentration at  
185 equilibrium,  $m$  is the mass of magnetic coagulant (mg), and  $V$  is the volume of  
186 solution treated.

187 The kinetic models used in this study are pseudo-first order, pseudo-second order,  
188 Elovich, and intra-particle diffusion models, where the linearized form for each model  
189 is presented in Eqs. 5 to 8 [34], respectively. The  $q_t$  and  $q_e$  values in those equations  
190 represent adsorption capacity (mg dye. mg magnetic coagulant<sup>-1</sup>) as function of time  
191 (min) and at equilibrium. Constant  $k_1$  (1. min<sup>-1</sup>) represents pseudo first-order rate  
192 constant;  $k_2$  (mg dye. mg magnetic coagulant<sup>-1</sup>. min<sup>-1</sup>) is the pseudo second-order rate  
193 constant; and  $k_d$  (mg dye. mg magnetic coagulant<sup>-1</sup>. min<sup>-1/2</sup>) is the rate constant for  
194 intra-particle diffusion model. The value  $\alpha$  denotes initial adsorption rate (mg dye. mg  
195 magnetic coagulant<sup>-1</sup>. min<sup>-1</sup>) and  $\beta$  (mg magnetic coagulant. mg dye<sup>-1</sup>) is the activation  
196 energy related value of chemisorption for Elovich model.

$$197 \quad \ln(q_e - q_t) = \ln(q_e) - k_1 t \quad (5)$$

$$198 \quad \frac{t}{q_t} = \frac{t}{q_e} + \frac{1}{k_2 q_e^2} \quad (6)$$

$$199 \quad q_t = \frac{1}{\beta} \ln(\alpha\beta) + \frac{1}{\beta} \ln(t) \quad (7)$$

$$200 \quad q_t = k_d t^{1/2} \quad (8)$$

### 201 **3. Results and discussion**

#### 202 *3.1. Effect of pH and trisodium citrate concentration on the protein adsorption*

203 As mentioned before, the citrate ion was used as a bridge between Fe<sub>3</sub>O<sub>4</sub> and  
204 leucaena protein, making the adsorption process could happen effectively. The effect

205 of adsorption pH and trisodium citrate concentration is presented in Fig 1. It could be  
206 observed in Fig 1.a., that pH played an important role in protein adsorption. With the  
207 increase of adsorption pH from 3.0 to 4.0, the leucaena protein adsorption capacity  
208 was also increased and reached the highest adsorption capacity at pH 4.0. Further  
209 increase of adsorption pH to 6.0 led to the decrease of protein adsorption. It is known  
210 that electrostatic force plays important role in protein adsorption. At low pH both  
211  $\text{Fe}_3\text{O}_4$  and leucaena protein had positive charges, thus repulsive forces between them  
212 making low adsorption happened. Similar phenomenon was possibly happened at pH  
213 above 4.0. The highest protein adsorption capacity was obtained at pH 4.0, which was  
214 near isoelectric point of leucaena protein. It is known that at pH near isoelectric point,  
215 the protein structure is at more compact conformation state, lowering repulsion forces  
216 between particles thus making higher protein adsorption possible [35]. Similar  
217 phenomenon has also been reported before [35, 36]. The effect of trisodium citrate  
218 concentration to the protein adsorption was further investigated. It was found that  
219 addition of trisodium citrate could increase the protein adsorption capacity. Based on  
220 Fig 1.b, it could be observed addition of trisodium citrate to 0.5 M increase the protein  
221 adsorption. We speculate it was possible due to with increase of citrate ion in the  
222 modification process, more citrate ion was adsorbed on  $\text{Fe}_3\text{O}_4$  surface, making more  
223 protein adsorption possible. Further addition of citrate ion did not increase the  
224 adsorption capacity, due to all  $\text{Fe}_3\text{O}_4$  surface was already occupied. Similar result was  
225 also obtained by previous researchers [27]. Based on these results, the trisodium  
226 citrate of 0.5 M and protein adsorption at pH 4.0 were further characterized and used  
227 as magnetic coagulant.

228 [Fig. 1]

229

### 230 3.2. Characterization of Fe-CA-Protein

231 The characteristics of Fe<sub>3</sub>O<sub>4</sub> before and after protein modification are presented in  
232 Fig 2. Based on the SEM observation, the nanoparticles were in form of aggregation  
233 of Fe<sub>3</sub>O<sub>4</sub>. The functionalization did not give any significant difference to the particle  
234 morphology. Similar spectra were also observed for Fe<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O<sub>4</sub>-CA-protein  
235 samples, where both samples exhibited (111), (202), (311), (222), (400), (422), (511),  
236 and (440) peaks of magnetite [37]. Further calculation using Scherer equation showed  
237 that functionalized Fe<sub>3</sub>O<sub>4</sub> had bigger average diameter of 58.08 nm, compared to  
238 pristine Fe<sub>3</sub>O<sub>4</sub> (47.31 nm). Based on the Fe<sub>3</sub>O<sub>4</sub> IR spectra, it could be observed that  
239 the sample exhibited a Fe-O vibration at 580 cm<sup>-1</sup>, and peaks at 1613, 3436 cm<sup>-1</sup> that  
240 came from O-H vibration of water molecule on the crystal structure [38, 39]. After  
241 modification using CA, the Fe<sub>3</sub>O<sub>4</sub>-CA sample exhibited stronger peak at 1620 and  
242 3436 cm<sup>-1</sup> indicating symmetric stretching of C=O and O-H vibration from CA  
243 molecules that adsorbed on the surface of Fe<sub>3</sub>O<sub>4</sub>. After adsorption of protein, there are  
244 several peaks that could be observed: 1397 cm<sup>-1</sup> bending vibration of C-H bonds,  
245 ~1600 cm<sup>-1</sup> peak of N-H bending, while peaks around 3200-3400cm<sup>-1</sup> came from  
246 overlap of O-H and N-H stretching [27, 40]. The observed peaks indicated that  
247 protein from *Leucaena* crude extract has been adsorbed on the surface of modified  
248 Fe<sub>3</sub>O<sub>4</sub>. The presence of coating of protein on Fe<sub>3</sub>O<sub>4</sub> was visible in TEM image (Fig  
249 2.f, white arrow), compared to pristine Fe<sub>3</sub>O<sub>4</sub>.

250 [Fig. 2]

251

### 252 3.3. Effect of pH in coagulation

253 The effect of pH in the coagulation process is presented in Fig 3. It could be  
254 observed that there was increase of removal from pH 2 to 3, and the highest removal  
255 of Congo red was obtained at pH 3. Very low removal was obtained while increasing  
256 the pH from 4 to 10, indicating no coagulation process happened. The leucaena  
257 protein on magnetic coagulant possessed pI around 4, thus at pH below 4, the  
258 magnetic coagulant would be positively charged. This charge was the opposite of  
259 Congo red molecules, which is known to be negatively charged at  $\text{pH} \leq 3$ , making the  
260 coagulation process was possible through charge neutralization mechanism. At pH 2,  
261 low coagulation performance was possible due to denaturation of protein molecules  
262 on the magnetic coagulant. Denaturation of protein is commonly observed at  
263 extremely low pH [41], making it inactive for coagulation process. On the other hand,  
264 at pH above leucaena protein pI value, both the coagulant and Congo red molecules  
265 were positively charge, thus no coagulation occur at these condition. Along with the  
266 increase of destabilized Congo red molecules, the more sludge volume was generated,  
267 as observed in pH 3. As very low removal was observed at pH 4-10, minimum  
268 destabilization was occurred, resulting in no observed sludge. Similar result was  
269 obtained in our previous studies using Leucaena crude extract as natural coagulant,  
270 where pH 3 was the best pH for coagulation [10, 31].

271 [Fig. 3]

#### 272 *3.4. Effect of magnetic coagulant dosage*

273 The study of magnetic coagulant dosage was done at pH 3, which was found as  
274 the best pH for coagulation. The profile of % removal and sludge volume at various  
275 dosages is presented in Fig 4. At low coagulant dosage, there was insufficient  
276 coagulant to neutralize the Congo red molecules, resulting on low removal. With

277 increase of magnetic coagulant dosage, the removal was also increased until dosage of  
278 210 mg. L<sup>-1</sup>. Further increase of magnetic coagulant dosage to 300 mg. L<sup>-1</sup> did not  
279 give any significant increase to the removal of Congo red. This was possible due to  
280 over addition of coagulant could limit the adsorption efficiency, as the magnetic  
281 coagulant particle could aggregate to each other [42] lowering the coagulation  
282 efficiency. Furthermore colloid re-stabilization is known to be commonly happened  
283 under over addition of coagulant [43]. This phenomenon could decrease the removal  
284 efficiency. Similar trend was also observed for the sludge volume.

285 [Fig. 4]

286 The Congo red removal as function of time is presented in Fig 5. It could be  
287 observed that significant removal was obtained at the first 20 min and became  
288 relatively constant until 60 min. This observation showed the significance of Fe<sub>3</sub>O<sub>4</sub> in  
289 the magnetic coagulant that increased the removal kinetics, compared to crude extract  
290 that need 40 min before reached constant. It could be also observed in Fig 5.b, the  
291 Fe<sub>3</sub>O<sub>4</sub> did not contribute to the Congo red removal, indicating the leucaena protein  
292 was the active coagulating agent. The Congo red removal kinetics was further  
293 investigated using various kinetic models, namely: pseudo 1<sup>st</sup> order, pseudo 2<sup>nd</sup> order,  
294 Elovich, and interparticle diffusion models. It is known that coagulation mechanism  
295 in this study was charge neutralization which is usually preceded by adsorption of dye  
296 molecules on active coagulating agent. The adsorption step usually becomes the rate  
297 determining step in coagulation study, making adsorption models suitable for removal  
298 evaluation [44]. According to [45] this phenomenon is possible due to the polymeric  
299 nature of natural coagulants. The fitting result of various kinetic models is presented  
300 in Table 3, and sample of model plots is presented in Fig 6. Based on the R<sup>2</sup> value, it  
301 could be seen that pseudo 2<sup>nd</sup> order kinetics was highly suitable for kinetics modeling

302 with  $R^2$  value of 0.99, while the Elovich and intra-particle diffusion models were also  
303 gave good model-data correlation with  $R^2$  value around 0.70 to 0.90. Suitability of the  
304 pseudo 2<sup>nd</sup> order and Elovich kinetics to the removal of Congo red implied that the  
305 adsorption occurred during coagulation was chemisorption. It was possible due to the  
306 different charges between proteins on the magnetic coagulant and the Congo red  
307 molecules, making dipole-dipole interaction possible [46]. A 2 phase plot was  
308 observed in the interparticle diffusion model (Fig 6.d), indicating there are 2  
309 determining step, namely surface adsorption followed by intra-particle diffusion.  
310 Similar conclusion of removal kinetic was also obtained in previous researches [9, 10,  
311 47, 48].

312 [Fig. 5]

313 [Table 3]

314 [Fig. 6]

315 Based on the characterization results and suitability of the kinetic models, an  
316 illustration of coagulation mechanism is presented in Fig 7. One  $-\text{COOH}$  of citrate  
317 ions was adsorbed to the surface of  $\text{Fe}_3\text{O}_4$ , while the others were available for protein  
318 binding. The overall magnetic coagulant was positively charged, following the charge  
319 of leucaena protein adsorbed on  $\text{Fe}_3\text{O}_4\text{-CA}$ , thus neutralizing the negatively charged  
320 Congo red molecules. The measurement of permanganate value (PV) was done at the  
321 best magnetic coagulant condition (pH 3, dosage of  $420 \text{ mg. L}^{-1}$ ). Initial Congo red  
322 wastewater had PV of  $8.554 \text{ mg KMnO}_4. \text{L}^{-1}$ , and water treated using crude extract  
323 showed  $14.991 \text{ mg KMnO}_4. \text{L}^{-1}$  (increase of 49%). This increase was possible due to  
324 the presence of various soluble organic compounds in the crude extract. The magnetic

325 coagulant showed lower increase of PV (18%), compared to the crude extract, due to  
326 desorbed protein in the treated wastewater.

327 [Fig. 7]

#### 328 **4. Conclusion**

329 This study focused on synthesis of magnetic coagulant by means of leucaena protein  
330 adsorption on the surface of citrate modified Fe<sub>3</sub>O<sub>4</sub>. Various trisodium citrate  
331 concentration and protein adsorption pH was investigated. Trisodium citrate was  
332 found to act as bridge between Fe<sub>3</sub>O<sub>4</sub> and protein molecules, where at concentration  
333 of 0.5 M and pH 4.0, the highest protein adsorption was achieved. Further trisodium  
334 citrate concentration did not give any increase in protein adsorption. The  
335 functionalization of Fe<sub>3</sub>O<sub>4</sub> did not change the morphology and crystallinity, however,  
336 bigger average crystal size was observed after protein functionalization. The  
337 adsorption of citrate and protein on the surface of Fe<sub>3</sub>O<sub>4</sub> was confirmed by using  
338 FTIR analysis. The obtained magnetic coagulant was tested for its coagulation  
339 performance. At various coagulation pH, the highest removal was obtained at pH 3,  
340 indicating charge neutralization mechanism due to the positively charged protein at  
341 pH around 3. At various magnetic coagulant dosage, the increase of magnetic  
342 coagulant dosage increased the removal of Congo red, until the highest removal at  
343 420 mg. L<sup>-1</sup>. Further increase did not give any effect to the removal. From  
344 investigation using several kinetic models, it was found that the removal kinetic was  
345 well fitted with pseudo 2<sup>nd</sup> order kinetic model, reflected in high R<sup>2</sup> value (>0.99).  
346 The best coagulation was obtained at pH 3 and dosage of 420 mg. L<sup>-1</sup> with 80%  
347 removal. This result was comparable with crude extract of leucaena with half settling  
348 time (20 min) and lower increase of permanganate value

349 **Declarations**

350 **Availability of data and materials**

351 All data generated or analyzed during this study are available from the corresponding  
352 author upon reasonable request.

353 **Competing interests**

354 The authors declare they have no competing interests.

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362 **Contributions**

363 ER and HK carried out laboratory experimental studies and drafted the manuscript.  
364 HK, SP, and AKS designed the study and secured the funding. SP and AKS critically  
365 reviewed and edited the final manuscript. All the authors read and approved the final  
366 manuscript.

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525



527 **Figure and Table Legend**

528 **List of figures:**

529 **Fig. 1** The profile of protein adsorption capacity at various pH (trisodium citrate  
530 concentration 0.5 M) and various trisodium citrate concentration (protein adsorption  
531 at pH 4.0)

532 **Fig. 2** Morphology of Fe<sub>3</sub>O<sub>4</sub> (a) and Fe<sub>3</sub>O<sub>4</sub>-CA-protein (b) at magnification of  
533 30,000×, XRD spectra (c), FTIR spectra, and TEM images of Fe<sub>3</sub>O<sub>4</sub> (e) and Fe<sub>3</sub>O<sub>4</sub>-  
534 CA-protein (f)

535 **Fig. 3** The effect of pH to the coagulation performance (coagulant dosage 60 mg. L<sup>-1</sup>)

536 **Fig. 4** The effect of magnetic coagulant dosage to the coagulation performance

537 **Fig. 5** Kinetics parameter of settling at various magnetic coagulant dosages (a) and  
538 their comparison to crude extract and Fe<sub>3</sub>O<sub>4</sub> (b)

539 **Fig. 6** Plots of pseudo 1<sup>st</sup> order (a), pseudo 2<sup>nd</sup> order (b), Elovich (c), and inter-particle  
540 diffusion (d) kinetic model (pH 3, magnetic coagulant dosage 420 mg. L<sup>-1</sup>)

541 **Fig. 7** Illustration of Fe<sub>3</sub>O<sub>4</sub> – CA – protein interaction and charge neutralization  
542 coagulation of Congo red

543

544 **List of tables:**

545 **Table 1** Variations in synthesis of Fe<sub>3</sub>O<sub>4</sub>-CA-protein

546 **Table 2** Variations in jar test study

547 **Table 3** Kinetics parameter of Congo red removal

548

549

550 **Table 1** Variations in synthesis of Fe<sub>3</sub>O<sub>4</sub>-CA-protein

Parameter	pH	Trisodium citrate concentration (M)
Effect of pH to protein adsorption	3.0; 3.5; 4.0; 4.5; 5.0; 5.5; 6.0	0.5
Effect of trisodium citrate concentration to protein adsorption	Best pH	0.0; 0.25; 0.5; 0.75; 1.0

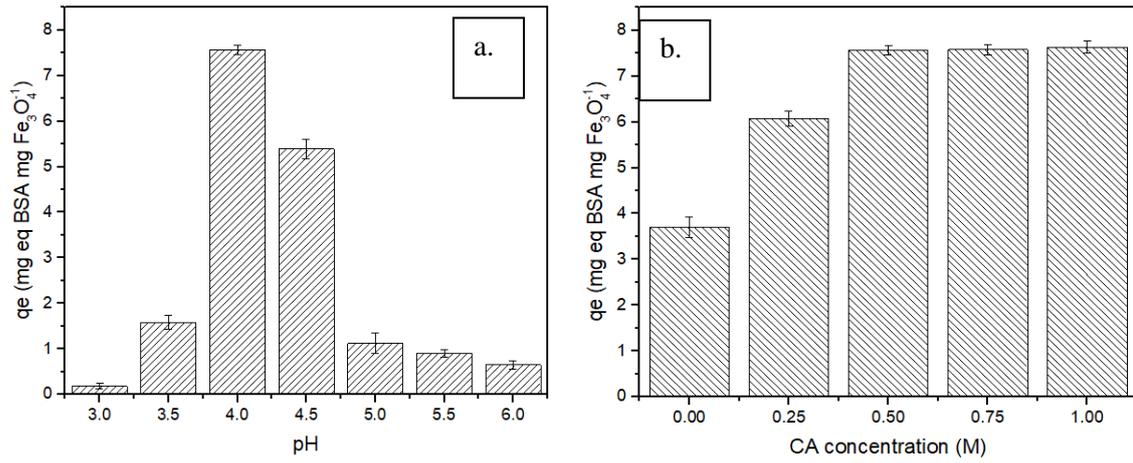
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552 **Table 2** Variations in jar test study

Parameter	pH	Magnetic coagulant dosage (mg. L <sup>-1</sup> )
Effect of pH	2, 3, 4, 5, 6, 7, 8, 9, 10	60
Effect of magnetic coagulant dosage	Best pH	60, 120, 180, 240, 300, 360, 420, 480, 540, 600

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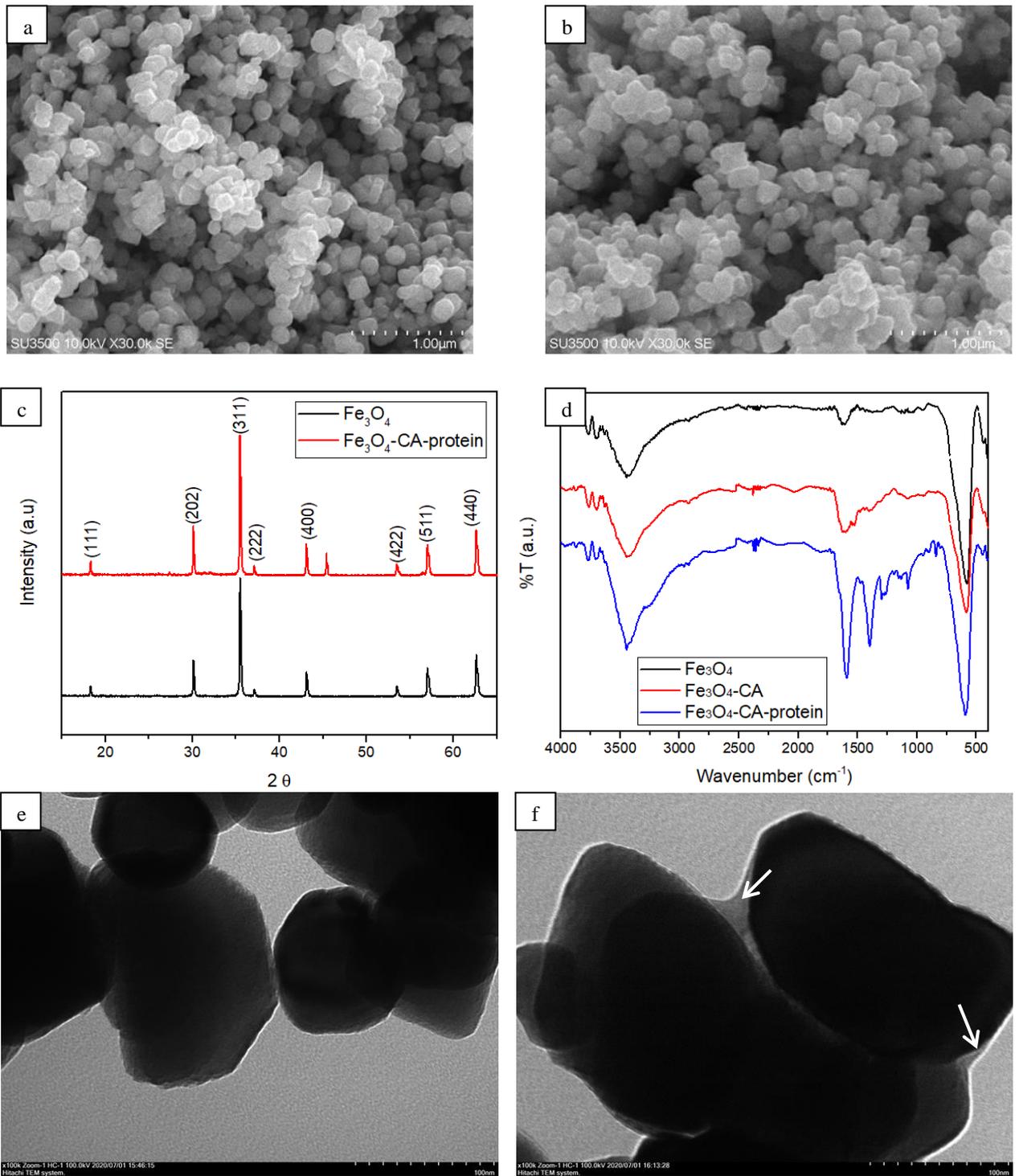
Coagulant	Dosage (mg. L <sup>-1</sup> )	Pseudo 1 <sup>st</sup> order		Pseudo 2 <sup>nd</sup> order		Elovich			Intra-particle diffusion	
		k <sub>1</sub>	R <sup>2</sup>	k <sub>2</sub>	R <sup>2</sup>	α	β	R <sup>2</sup>	kd	R <sup>2</sup>
<b>Fe<sub>3</sub>O<sub>4</sub>- CA- protein</b>	60	0.0438	0.491	0.0268	0.994	245.7	0.1922	0.8260	7.019	0.9061
	120	0.0463	0.4004	0.0352	0.9984	1541.7	0.3134	0.7375	7.160	0.9369
	180	0.041	0.4664	0.0387	0.9983	944.2	0.3451	0.7646	5.471	0.904
	240	0.0437	0.415	0.0504	0.9974	2501	0.4373	0.8708	5.378	0.9306
	300	0.0513	0.5889	0.0549	0.9988	4237	0.5282	0.7435	4.825	0.9156
	360	0.0313	0.0126	0.0338	0.9984	123.7	0.3497	0.9046	4.542	0.9412
	420	0.0495	0.4313	0.039	0.9979	149.1	0.4018	0.7797	4.358	0.9652
	480	0.0328	0.2475	0.0441	0.998	69.93	0.4013	0.8236	3.873	0.9694
	540	0.0291	0.2036	0.0433	0.9977	47.44	0.4381	0.8785	3.341	0.9692
	600	0.0358	0.3235	0.0571	0.9983	81.69	0.5299	0.8200	3.136	0.9658
<b>Leucaena crude extract</b>		0.0554	0.4313	0.0389	0.9978	6.245	7.132	0.1754	0.9674	0.9818
<b>Fe<sub>3</sub>O<sub>4</sub></b>		0.0206	0.6233	0.0498	0.5314	0.2289	0.2288	0.9325	0.785	0.7808



556

557 **Fig. 1** The profile of protein adsorption capacity at various pH (trisodium citrate  
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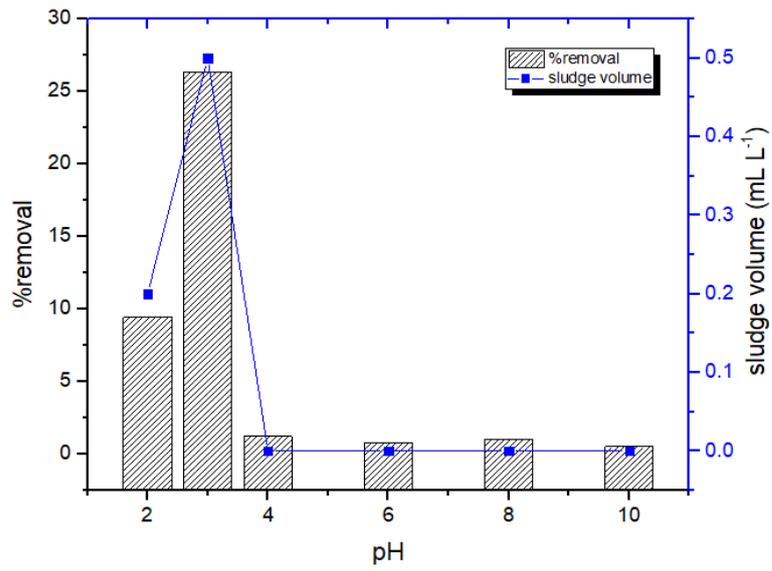
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562 **Fig. 2** Morphology of  $\text{Fe}_3\text{O}_4$  (a) and  $\text{Fe}_3\text{O}_4$ -CA-protein (b) at magnification of  
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 564 CA-protein (f)

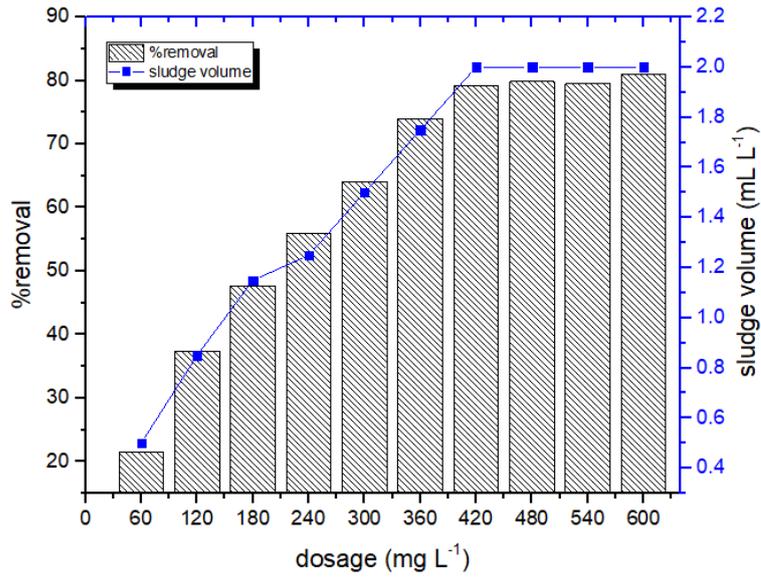
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566

567 **Fig. 3** The effect of pH to the coagulation performance (coagulant dosage 60 mg. L<sup>-1</sup>)

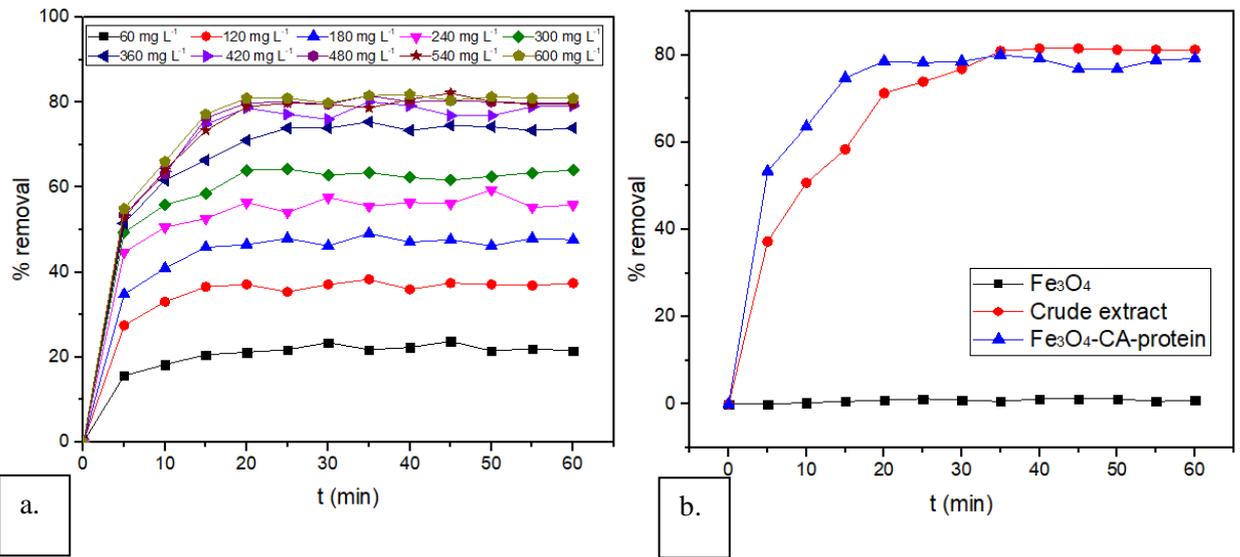
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570 **Fig. 4** The effect of magnetic coagulant dosage to the coagulation performance

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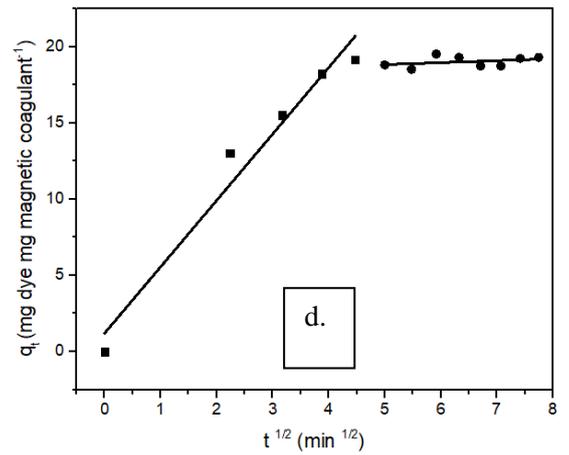
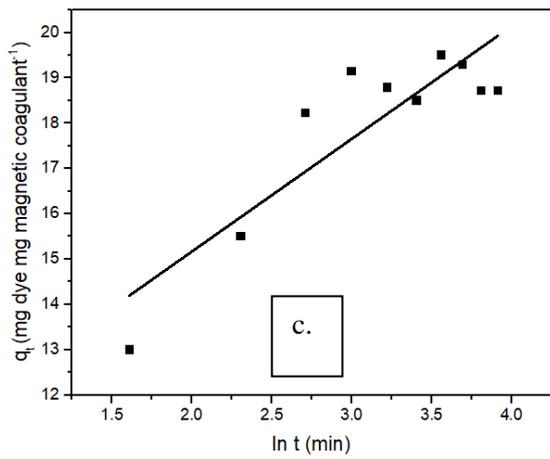
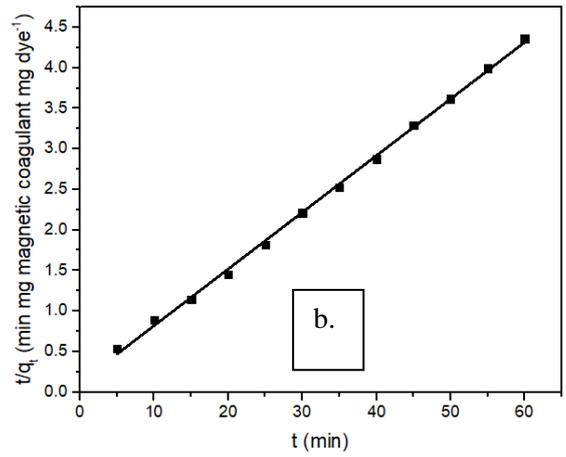
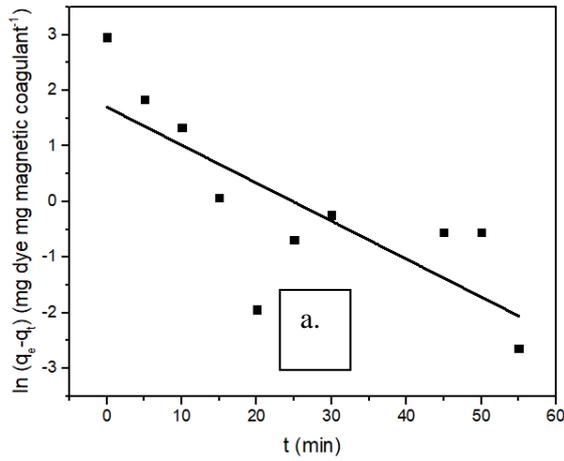


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