

# Synthesis of High Specific Surface Lithium ion Sieve Templated by Bacterial Cellulose for Selective Adsorption of Li<sup>+</sup>

Xudong Zheng (✉ [Zhengks@outlook.com](mailto:Zhengks@outlook.com))

Changzhou University <https://orcid.org/0000-0003-2688-4855>

Ang Li

Changzhou University

Dandan Wang

Changzhou University

Da Xia

Changzhou University

Yuzhe Zhang

Changzhou University

Zhongyu Li

Changzhou University

---

## Research Article

**Keywords:** Lithium ion sieve, Bacterial cellulose, Hydrothermal method, Titanium, Selective adsorption

**Posted Date:** June 21st, 2021

**DOI:** <https://doi.org/10.21203/rs.3.rs-580568/v1>

**License:** © ⓘ This work is licensed under a Creative Commons Attribution 4.0 International License.

[Read Full License](#)

---

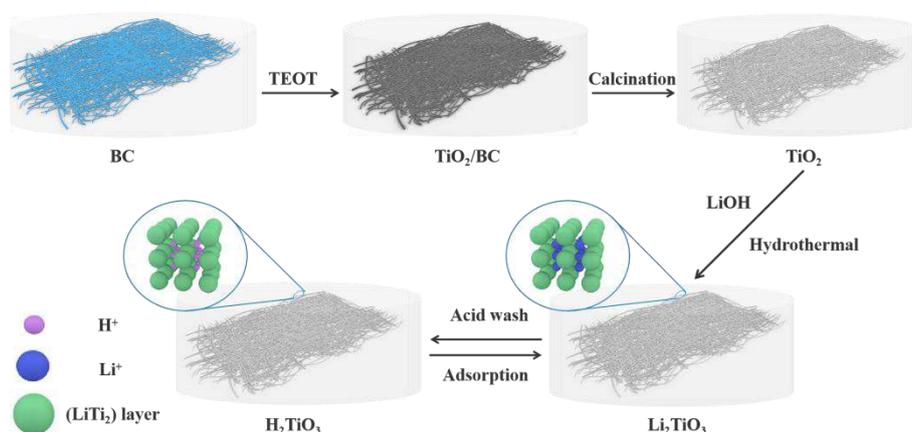
# ipSynthesis of high specific surface lithium ion sieve templated by

## bacterial cellulose for selective adsorption of Li<sup>+</sup>

Xudong Zheng\*, Ang Li, Dandan Wang, Da Xia, Yuzhe Zhang, Zhongyu Li\*

\*Correspondence to: X. Zheng (E-mail: zhengks@outlook.com); Z. Li (E-mail: zhongyuli@mail.tsinghua.edu.cn);

### Graphical Abstract



Lithium ion sieve templated by bacterial cellulose for selective adsorption of Li<sup>+</sup>

### Abstract

In recent years, the lithium market has ushered in a golden period of development. With the development of batteries, ceramics, glass, lubricants, refrigerants, the nuclear industry and the optoelectronics industry, the demand for lithium has grown rapidly, and continuous mining has led to scarcity of land resources. On the other hand, due to the rich lithium resources in sea water and salt lake brines. How to selectively adsorb and separate lithium ions from seawater and salt lake brine has attracted more and more scholars' attention and research. Lithium ion sieve stands out because of its excellent performance of specific adsorption and separation of lithium ions. This article reports the preparation of mesoporous TiO<sub>2</sub> and LiOH hydrothermal reaction using bacterial cellulose as a biological template. After calcination at 600°C, spinel lithium titanium oxide Li<sub>2</sub>TiO<sub>3</sub> is formed. H<sub>2</sub>TiO<sub>3</sub> was obtained by eluting the precursor with HCl eluent. FT-IR, SEM and XRD were used to characterize Li<sub>2</sub>TiO<sub>3</sub> and H<sub>2</sub>TiO<sub>3</sub>. The adsorption performance of H<sub>2</sub>TiO<sub>3</sub> was

24 studied through adsorption pH, adsorption kinetics, adsorption isotherms, competitive  
25 adsorption and so on. The results show that  $\text{H}_2\text{TiO}_3$  is a single layer chemical  
26 adsorption process, which has a good adsorption effect on lithium ions at pH 11.0,  
27 with the maximum adsorption capacity can reach  $35.45 \text{ mg}\cdot\text{g}^{-1}$ . The lithium ion sieve  
28 has selective adsorption to  $\text{Li}^+$ , and its distribution coefficient is  $2242.548 \text{ mL g}^{-1}$ . It  
29 may be predicted that the lithium-ion sieve prepared by biological template has a  
30 broad application prospect.

31 **Keywords:** Lithium ion sieve; Bacterial cellulose; Hydrothermal method; Titanium;  
32 Selective adsorption

### 33 **1. Introduction**

34 Lithium is the rarest element among alkali metals(Zeng et al. 2018). It is the  
35 lightest silver-white metal with strong chemical activity, can synthesize inorganic and  
36 organic compounds of lithium with various elements. Lithium and a variety of metals  
37 constitute light alloys, wear-resistant alloys, etc. Al-Li and Mg-Li alloys will become  
38 new structural materials for the next generation of aerospace industry. Lithium  
39 resources in China are mainly distributed in Qinghai-Tibet Plateau, Xinjiang, Inner  
40 Mongolia, Sichuan and Jiangxi, accounting for 25.6 % of the world's lithium reserves,  
41 ranking second in the world(DING et al. 2018). Among them, salt lake brine lithium  
42 resources are the main form of lithium resources in China, accounting for about 85 %  
43 of the total proved lithium reserves in China(Liu et al. 2021). Therefore, it is very  
44 important to study how to transform lithium extraction technology and extract lithium  
45 efficiently from Salt Lake brine(Argurio et al. 2019). At present, there are many  
46 known methods for adsorption and separation of lithium  $\text{Li}^+$  from salt lake brine. For  
47 example, precipitation method(Song et al. 2017), electrochemical method(Romero et  
48 al. 2018), solvent extraction method(Gza et al. 2020; Zhao et al. 2017), ion exchange  
49 method(Grágeda et al. 2018; Michel et al. 2018) and so on. Among them, ion-  
50 exchange method stands out from many lithium extraction methods because of its  
51 simple process, high recovery rate and economic and green advantages(Ma et al.  
52 2018). Compared with some natural inorganic minerals and carbon materials(Wen et  
53 al. 2017), there is a lack of adsorption selectivity(Lihua et al. 2018) for  $\text{Li}^+$ . Lithium

54 ion sieve has the characteristics of selective adsorption of  $\text{Li}^+$  because it is first  
55 inserted into the precursor by  $\text{Li}^+$  and then eluted by eluent(Peng et al. 2019). As the  
56 main representative of lithium ion sieves, spinel manganese oxide ion sieves have  
57 high specific adsorption for  $\text{Li}^+$  after acid elution of precursors. For example, Gao A,  
58 Sun Z and others synthesized representative adsorbent  $\text{Li}_{1.6}\text{Mn}_{1.6}\text{O}_4$  for lithium ion  
59 sieves(Gao et al. 2018). Its maximum adsorption capacity can reach  $44 \text{ mg}\cdot\text{g}^{-1}$ .  
60 Similarly, Yang, Shan Shan, Zhou, Ma Li, Ma Li et al. Through  $\text{LiOH}$ ,  
61  $\text{Mn}(\text{CH}_3\text{COO})_2$ ,  $\text{H}_2\text{O}_2$  and ethanol, using sol gel method, hydrothermal method and  
62 low-temperature solid-phase method combined with manganese oxide lithium ion  
63 sieve made a series of research(Yang et al. 2016). Keiko Sasaki and Qianqian Yu and  
64 their colleagues synthesized a lithium ion sieve with microtubule morphology using  
65 manganese-oxidizing fungus as biological template by calcination solid-phase  
66 bonding. The effect of adsorption capacity at different calcination temperatures was  
67 studied. The structural and morphological characterization and adsorption  
68 experiments show that the weight fraction of spinel lithium manganese oxide ion  
69 sieve also changes with different calcination temperatures, and it will affect its  
70 crystallinity, so the choice of calcination temperature directly affects the adsorption  
71 capacity of lithium ion sieve(Sasaki and Yu 2015). Song et al. Spinel structure  $\text{Li}_{1+x}$   
72  $\text{Mn}_{2-x}\text{O}_4$  materials for lithium ion-sieve precursor were synthesized by high  
73 temperature solid state method. The results showed that the  $\text{Li}_{1.3}\text{Mn}_{1.7}\text{O}_4$  material had  
74 the largest adsorption capacity and it reached up to  $24.06 \text{ mg}\cdot\text{g}^{-1}$  when the pH value  
75 was 12 and the adsorption time was 10 h(Img et al. 2021). However, the current Li-  
76 Mn-O ion sieve have the same shortcomings in the process of acid pickling: the  
77 appearance of  $\text{Mn}^{2+}$  in the process of elution causes partial dissolution of the ion  
78 sieves, which reduces the repeatability of the lithium ion sieves. On the other hand,  
79 the appearance of titanium-based lithium ion sieves compensated for the dissolution  
80 of Ti during acid pickling. For example, Shulei Wang, Ping Li and others synthesized  
81  $\beta\text{-Li}_2\text{TiO}_3$  by hydrothermal method of  $\text{TiO}_2$  and  $\text{LiOH}\cdot\text{H}_2\text{O}$ (Zhang et al. 2019).  
82 Compared with manganese ion sieves, the dissolution rate of Ti is also reduced while  
83  $\text{Li}^+$  is highly selectively adsorbed by manganese ion sieves. Cheng-Long Yua,

84 Kazumichi Yanagisawa et al, synthesized pure  $\text{Li}_2\text{TiO}_3$  nanoparticles by hydrothermal  
85 reaction of anatase  $\text{TiO}_2$  and  $\text{LiOH}\cdot\text{H}_2\text{O}$ , and studied the formation of  $\text{Li}_2\text{TiO}_3$ , the  
86 diffusion and insertion mechanism of lithium ions(Garay-Rodríguez et al. 2019).  
87 Ramesh et al. Anatase type  $\text{TiO}_2$  and  $\text{Li}_2\text{CO}_3$  were mixed, ground and heated in an  
88 alumina crucible at  $700\text{ }^\circ\text{C}$  in air to obtain the lithium ion sieve precursor ( $\text{Li}_2\text{CO}_3$ ).  
89 The measured adsorption capacity of the adsorbent is  $32.6\text{ mg}\cdot\text{g}^{-1}$ (Garcia et al. 2018b).  
90 Unfortunately, most of the known lithium ion sieves are powdered, which is not  
91 conducive to the mass production of ion sieves in practical applications. Therefore,  
92 the preparation of mesoporous nanomaterials to synthesize lithium ion sieve is of  
93 special significance(Elik et al. 2018). Cellulose is a polysaccharide with a wide  
94 coverage and the largest content in nature(Li et al. 2019). Rich content and low price  
95 make it naturally attract the attention of scientific researchers in recent years.  
96 However, natural cellulose has some impurities such as lignin and hemicellulose,  
97 especially the coarse fiber diameter of natural cellulose, which affects the  
98 performance of cellulose(Tomer and Malik 2019). With the in-depth of bacterial  
99 cellulose (BC) synthesized by microorganisms under different conditions, the  
100 chemical structure of BC is the same as that of plant cellulose(Aimar et al. 2019). The  
101 difference is that BC has the advantages of higher purity and finer fiber diameter than  
102 plant cellulose. Due to the formation of ultrafine network structure of bacterial  
103 cellulose and the "nano-effect", bacterial cellulose has the characteristics of high  
104 water absorption and water retention, high permeability to liquids and gases, high wet  
105 strength, and in-situ processing and moulding, especially in wet state. High purity and  
106 excellent performance can be widely used in many fields.

107 As far as we know, there is no report about the preparation of  $\text{Li}_2\text{TiO}_3$  by  
108 hydrothermal reaction using bacterial cellulose as template. Thus, in this research, We  
109 first proposed using BC as a template to form titanium dioxide mesoporous membrane  
110 on the substrate. Then, the precursor of  $\text{Li}_2\text{TiO}_3$  was preliminarily obtained by  
111 hydrothermal method with  $\text{LiOH}$ (Garcia et al. 2018a). The morphology of the  
112 precursor was stabilized by calcination at high temperature and the lithium ion sieve  
113 with mesoporous shape was obtained by acid elution. Finally, we also proved the

114 excellent adsorption effect of this lithium ion sieve using bacterial cellulose as  
115 template in the adsorption experiment, and expected its application prospects.

## 116 **2. Experimental**

### 117 **2.1 Synthesis of the $\text{Li}_2\text{TiO}_3$**

118 Bacterial cellulose (BC) hydrogel, titanium ethoxide (TEOT), lithium hydroxide  
119 (LiOH). Deionized water was used in all experiments. Hydrochloric acid (HCl) and  
120 other drugs used are analytically pure, without the need for further processing and  
121 purification. Bacterial cellulose (BC) hydrogel was placed in deionized water for 15  
122 min to achieve swelling effect. After freezing with liquid nitrogen and freeze-drying,  
123 the bacterial cellulose (BC) aerogel with a network structure was obtained. The  
124 bacterial cellulose (BC) aerogel was immersed in titanium ethoxide (TEOT) solution  
125 for 2 h. Then, after alternately rinsing with ethanol and ultrapure water for 4 to 5  
126 times, it was placed in ultrapure water and mechanically stirred for 2 hours, and the  
127 product was repeatedly washed with deionized water. Finally, the bacterial cellulose  
128 film material  $\text{TiO}_2/\text{BC}$  wrapped in  $\text{TiO}_2$  was obtained after drying in the oven (Zhu et  
129 al. 2020).  $\text{TiO}_2$  with a weight of 0.826 g was obtained by calcining at 600 °C for 6 h at  
130 4 °C/ min in a tubular furnace. The  $\text{TiO}_2$  was dissolved in 10.45 ml of  $\text{H}_2\text{O}$  with 0.5 g  
131 of LiOH. The Li: Ti molar ratio of 2:1, unstable spinel  $\text{Li}_2\text{TiO}_3$  is obtained after  
132 hydrothermal reaction at 180 °C for 18 h. The stable spinel  $\text{Li}_2\text{TiO}_3$  was obtained after  
133 being calcined at 4 °C/ min at 600 °C for 6 h in a tube furnace.

### 134 **2.2 Synthesis of the $\text{H}_2\text{TiO}_3$**

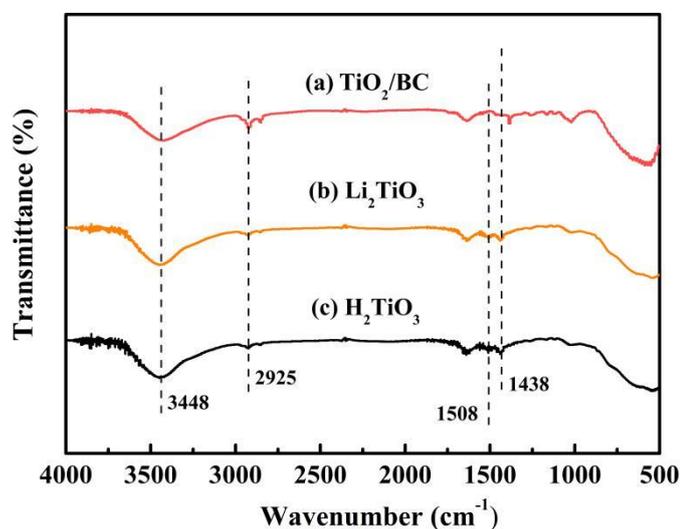
135  $\text{Li}_2\text{TiO}_3$  was eluted in the 0.1 mol/L of HCl at 65 °C for 12 h, and then the eluate  
136 was changed again to ensure the elution. Finally, the eluted product was washed and  
137 filtered with ultra-pure water and dried in an oven at 70 °C. The final product was  
138 spinel titanium oxide ion screen. The titanium based lithium ion sieves  $\text{H}_2\text{TiO}_3$  with  
139 high adsorption and specific adsorption for  $\text{Li}^+$  were obtained.

## 140 **3. Results and discussion**

### 141 **Characterizations of $\text{Li}_2\text{TiO}_3$ and $\text{H}_2\text{TiO}_3$**

142 In order to analyze functional groups of  $\text{TiO}_2$ ,  $\text{Li}_2\text{TiO}_3$  and  $\text{H}_2\text{TiO}_3$ , FT-IR  
143 analysis was performed and presented in Figure 1. Broad peaks at 3448 and 2925  $\text{cm}^{-1}$

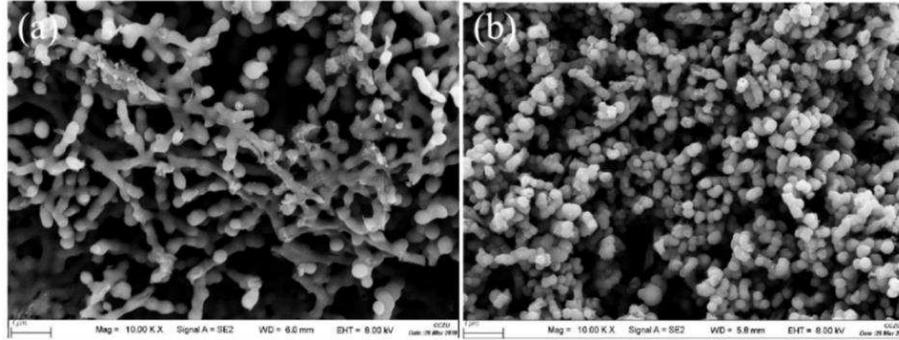
144 were observed for three materials' FT-IR spectra, which can be interpreted as O-H  
145 and C-H stretching vibrations, respectively. Among them, OH peak was observed.  
146 This peak was due to the isolated O-H bond not participating in the interaction with  
147 other hydroxyl groups. In addition, compared with the FT-IR spectra of  $\text{TiO}_2$ , the new  
148 peaks at 1438 and 1508  $\text{cm}^{-1}$  appeared after lithium insertion, which belonged to the  
149 characteristics vibration of Li-O-Ti band. It indicates that the precursor ( $\text{Li}_2\text{TiO}_3$ ) was  
150 formed. In the case of  $\text{Li}_2\text{TiO}_3$ , the disappearance of peaks at 1438 and 1508  $\text{cm}^{-1}$   
151 show successful elution of lithium ions, and the preparation of lithium ion sieve  
152 ( $\text{H}_2\text{TiO}_3$ ) was completed. As can be seen in the SEM diagram in Figure 2(a), the  
153 titania films formed with bacterial cellulose as template feature pronounced high pore  
154 volume network structure. After the hydrothermal calcination with LiOH, the films  
155 become denser with crystals grow and aggregate, resulting in the formation of spinel  
156  $\text{Li}_2\text{TiO}_3$  (Figure 2b). The nitrogen sorption data of  $\text{H}_2\text{TiO}_3$  showed a BET surface area  
157 of 27.4006  $\text{m}^2/\text{g}$ . Based on the adsorption desorption isotherm of nitrogen (Figure 3)  
158 shows that the pore structure in the material is consistent with the results of SEM. It  
159 can further be inferred that bacterial cellulose as template is effective.



160

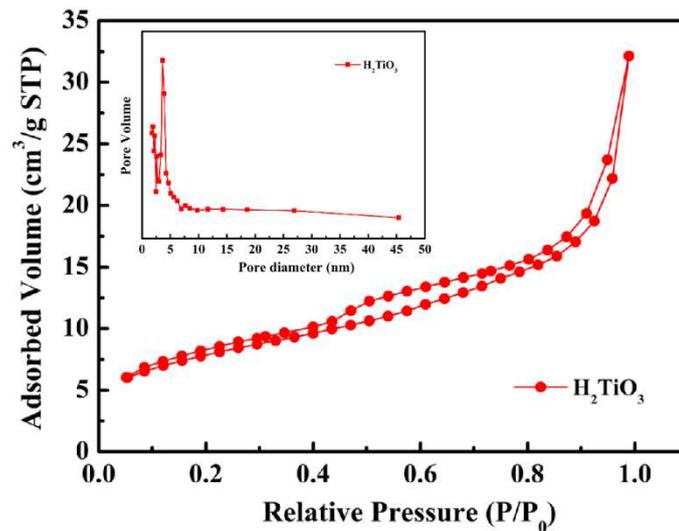
161

Fig. 1 (a) FT-IR spectra of  $\text{TiO}_2/\text{BC}$ ; (b)  $\text{Li}_2\text{TiO}_3$ ; (c)  $\text{H}_2\text{TiO}_3$



162  
163

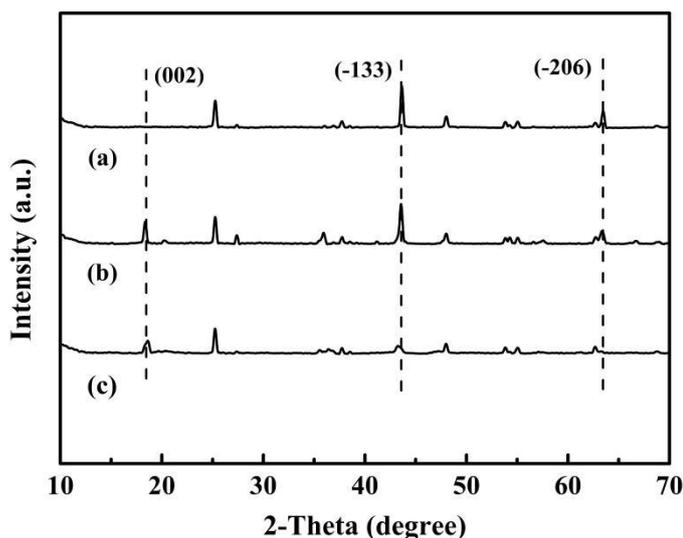
Fig. 2 (a) SEM image of TiO<sub>2</sub>/BC; (b) SEM images of Li<sub>2</sub>TiO<sub>3</sub>.



164  
165  
166

Fig. 3 Nitrogen adsorption-desorption isotherm of H<sub>2</sub>TiO<sub>3</sub>. Inset showing Inset showing pore size distributions.

167 As shown in Figure. 4, XRD pattern of the Li<sub>2</sub>TiO<sub>3</sub> before calcination, Li<sub>2</sub>TiO<sub>3</sub>  
168 after calcination and H<sub>2</sub>TiO<sub>3</sub> were collected at the 2θ angle from 10 to 70°. In the  
169 XRD pattern of the Li<sub>2</sub>TiO<sub>3</sub>, a new diffraction peak at (002) appeared after calcination,  
170 which belonged to the growth of (002) diffraction peak needs higher calcination  
171 temperature(Gebreslase and Technology 2018). The occurrence of diffraction peaks  
172 of (002), (-133), (-206) and (062) can be seen in the Figure 4(b), indicating that Li<sup>+</sup> is  
173 orderedly inserted into TiO<sub>2</sub>,which were matched well with the pure monoclinic  
174 crystal of Li<sub>2</sub>TiO<sub>3</sub>(Peng et al. 2019). After eluting, the position of the diffraction  
175 peaks can be observed to be about the same, and the diffraction peak of (-133) and (-  
176 206) almost disappears, which proves on exchange occurs in Li<sup>+</sup>/H<sup>+</sup> and the formation  
177 of H<sub>2</sub>TiO<sub>3</sub> structure.



178

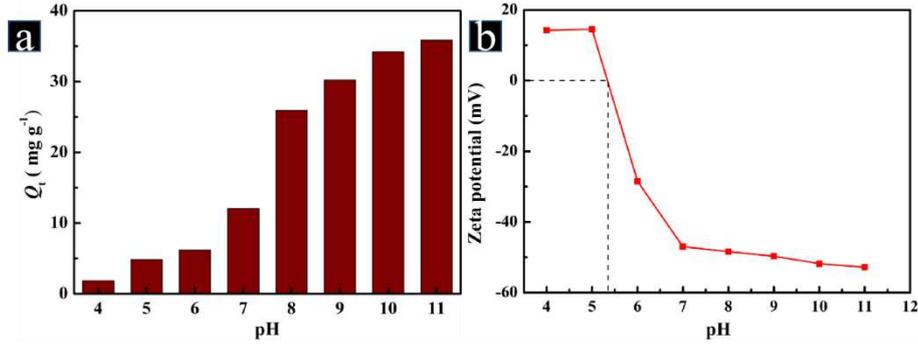
179 Fig. 4 (a) XRD patterns of  $\text{Li}_2\text{TiO}_3$  before calcination; (b)  $\text{Li}_2\text{TiO}_3$  after calcination; (c)  $\text{H}_2\text{TiO}_3$

180 **4. Adsorption performance of  $\text{H}_2\text{TiO}_3$**

181 **4.1 Effect of pH**

182 Here we briefly explore the relationships between  $\text{Li}^+$  and its adsorption  
 183 mechanism, in which the pH value dominates the study. The pH value is particularly  
 184 critical for the adsorption capacity of  $\text{H}_2\text{TiO}_3$ . As shown in Fig. 5a, with the pH value  
 185 increases, the adsorption amount of  $\text{Li}^+$  also increases gradually (Sw et al.). It can be  
 186 seen that the adsorption of  $\text{Li}^+$  is favorable under alkaline condition. In order to avoid  
 187 adding more NaOH to adjust the higher pH concentration, thus increasing the effect of  
 188 cations in the solutions and considering that the excessively high pH value is not  
 189 conducive to mass production in industrial applications. Therefore, the recovery of  
 190  $\text{Li}^+$  in this experiment was mainly carried out at pH 11. Fig. 5b shows the zeta  
 191 potential test of lithium ion sieve. with the pH increases, the value of the electrostatic  
 192 negative charge value on the material also gradually increases. It keeps coincident  
 193 with the pH tests results.

194



195  
196 Fig. 5 (a) Effect of pH on adsorption capacities (b) Zeta potential measurement of H<sub>2</sub>TiO<sub>3</sub>

## 197 4.2. Adsorption kinetics

198 Through the adsorption kinetics experiment, the connection between the  
199 adsorption amount ( $Q_t$ ) and the adsorption time ( $t$ ) was analyzed. We can see in Figure  
200 6, the adsorption curve of the ion sieve adsorbent increased rapidly from the beginning,  
201 reaching about 80% of the maximum adsorption capacity at 200 min, then the  
202 adsorption curve increases slightly and eventually gradually tends to adsorption  
203 equilibrium at about 6 h. The adsorption process of ionic sieve H<sub>2</sub>TiO<sub>3</sub> in LiCl  
204 solution was fitted by pseudo-first-order kinetic model (PFOKM), pseudo-second-  
205 order kinetic model (PSOKM) to explore the adsorption rate constant and mechanism.  
206 The fitting equation of the PFOKM and PSOKM as follows:

$$Q_t = Q_e - Q_e e^{-k_1 t} \quad (1)$$

$$Q_t = \frac{k_2 Q_e^2 t}{1 + k_2 Q_e t} \quad (2)$$

207 Where,  $Q_t$  (mg·g<sup>-1</sup>) corresponds to the amount of Li<sup>+</sup> adsorbed at time  $t$ (min) and  
208  $Q_e$  (mg·g<sup>-1</sup>) corresponds to the amount of adsorption at equilibrium.  $k_1$  (min<sup>-1</sup>) and  $k_2$   
209 (g·mg<sup>-1</sup>·min<sup>-1</sup>) are the rate constants of the PFOKM and PSOKM, respectively. In  
210 addition, the  $h$  (mg·g<sup>-1</sup>·min<sup>-1</sup>) and  $t_{1/2}$  (min) of the PSOKM are listed in the following  
211 formulas (3) and (4):

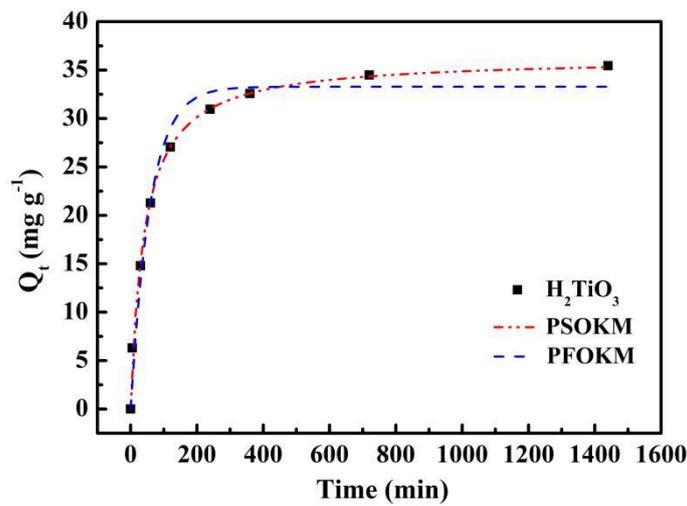
$$h = k_2 Q_e^2 \quad (3)$$

$$t_{1/2} = \frac{1}{k_2 Q_e} \quad (4)$$

212 The kinetic curve of adsorption was fitted by PFOKM and PSOKM. The fitting  
213 curve and corresponding parameters are presented in Figure 6 and Table 1,  
214 respectively. Obviously, the correlation coefficient of  $R^2$  fitted by PSOKM is larger

215 than the correlation coefficient of  $R^2$  fitted by PFOKM, which better matches the  
 216 experimental data.

217 At the same time, the equilibrium adsorption amount calculated based on the  
 218 PFOKM and the PSOKM. Compared with the actual values, the results of the pseudo-  
 219 secondary dynamics model are closer to reality. Therefore, we believe that PSOKM is  
 220 more in line with the adsorption of ion sieve  $H_2TiO_3$  in LiCl solution. This further  
 221 illustrates that the adsorption process of  $Li^+$  by  $H_2TiO_3$  is mainly completed under the  
 222 chemical action.



223

224 Fig.6 Kinetic data and modeling for the adsorption of  $Li^+$ : Fitting curves of PFOKM and PSOKM

225

Table 1. Kinetic parameters for the PFOKM and PSOKM

Sorbents	$Q_{e,exp} (mg \cdot g^{-1})$	PFOKM			PSOKM		
		$Q_{e,c} (mg \cdot g^{-1})$	$k_1 (min^{-1})$	$R^2$	$Q_{e,c} (mg \cdot g^{-1})$	$k_2 \times 10^{-2} (g \cdot mg^{-1} \cdot min^{-1})$	$R^2$
$H_2TiO_3$	35.45	33.28	0.0172	0.975	36.29	0.068	0.991

### 226 4.3. Adsorption isotherms

227 By statically testing equilibrium adsorption data and adsorption curves in LiCl  
 228 solutions ( $100-2000 mg \cdot L^{-1}$ ), so as to explore the equilibrium concentration and  
 229 adsorption amount of the adsorbent in different concentrations of lithium-containing  
 230 solutions. Among them, from the curve fitted by Langmuir and Freundlich equation  
 231 (Figure 7), the adsorption effect will become higher with the increase of  $Li^+$   
 232 concentration. The saturation adsorption capacity of  $H_2TiO_3$  is  $35.45 mg \cdot g^{-1}$ . The  
 233 related isothermal constants are listed Table 2. It is not difficult to see that the

234 correlation parameters of the Langmuir and Freundlich adsorption isotherm models  
 235 are  $R^2=0.996$  and  $R^2=0.978$ , respectively. In comparison, the Langmuir isotherm  
 236 adsorption model can better match the experimental data, which also corresponds to  
 237 the single layer adsorption. This indicates that fitting experimental data with  
 238 Langmuir equation is closer to actual data. Hence, the lithium ion sieve is known as  
 239 an adsorbent with excellent performance in extracting  $\text{Li}^+$ . Experimental data fit via  
 240 Langmuir and Freundlich models, which were calculated by Eqs. (5) and (6):

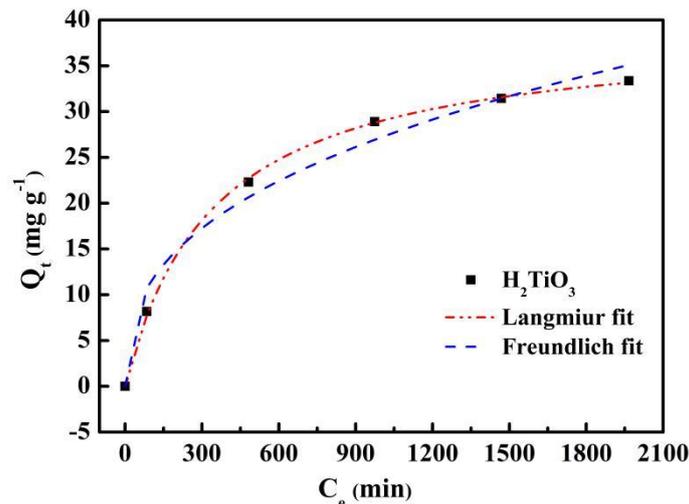
$$Q_e = \frac{K_L Q_m C_e}{1 + K_L C_e} \quad (5)$$

$$Q_e = K_F C_e^{1/n} \quad (6)$$

241 In the formula,  $Q_m$  ( $\text{mg} \cdot \text{g}^{-1}$ ) is expressed as the maximum amount of  $\text{H}_2\text{TiO}_3$  to  
 242  $\text{Li}^+$ .  $K_L$  ( $\text{L} \cdot \text{g}^{-1}$ ) corresponds to the Langmuir isotherm constant.  $K_F$  ( $\text{mg} \cdot \text{g}^{-1}$ )  
 243 corresponds to Freundlich isotherm direction constant,  $1/n$  corresponds to the effect of  
 244 concentration on the amount of adsorption,  $R_L$  is used as a separation factor to identify  
 245 the merits of  $\text{H}_2\text{TiO}_3$ , which the calculation formula of  $R_L$  is listed in formula (7):

$$R_L = \frac{1}{1 + C_m K_L} \quad (7)$$

246 In this formula,  $C_m$  is explained as the maximum initial concentration of  $\text{Li}^+$ .



247

248

Fig.7 Isotherm model fitting of on  $\text{H}_2\text{TiO}_3$  adsorbing  $\text{Li}^+$ .

249

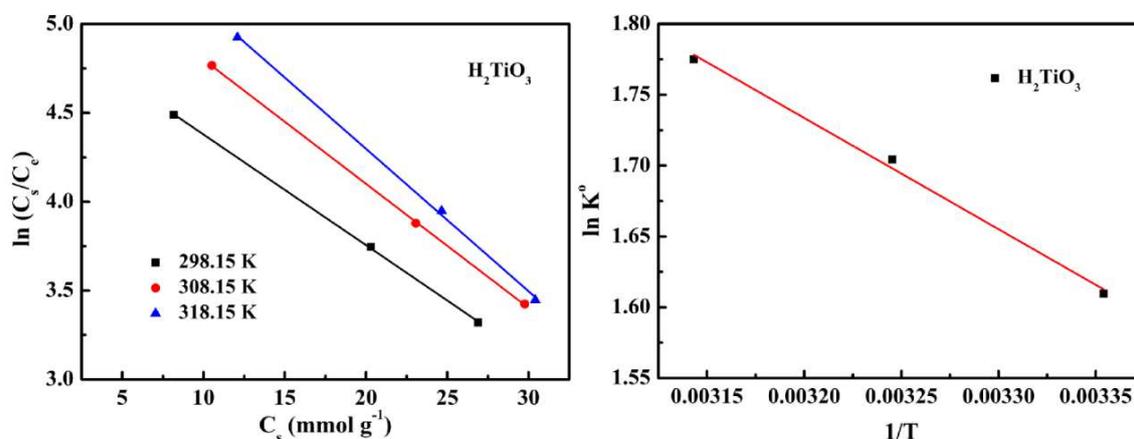
250

Table 2. Adsorption equilibrium constants of Langmuir and Freundlich models

Sorbents	Langmuir isotherm model			Freundlich isotherm model		
	$Q_m$ ( $\text{mg} \cdot \text{g}^{-1}$ )	$K_L$ ( $\text{L} \cdot \text{mg}^{-1}$ )	$R^2$	$K_F$ ( $\text{mg} \cdot \text{g}^{-1}$ )	$1/n$	$R^2$
$\text{H}_2\text{TiO}_3$	38.96	0.003	0.998	2.01	0.38	0.948

#### 252 4.4. Effect of temperature

253 Further, considering the influence of thermal motion characteristics on the  
 254 adsorption efficiency. Therefore, we explored the effect of  $\text{H}_2\text{TiO}_3$  on  $\text{Li}^+$  adsorption  
 255 at different temperatures (298.15 K, 308.15 K, and 318.15 K) through thermodynamic  
 256 experiments.  $\Delta G^\circ$  is calculated from the Gibbs free energy formula, and the change of  
 257  $Q_e$  with temperature was studied (Fig. 8 (a)).  $\Delta H^\circ$  and  $\Delta S^\circ$  are calculated by the  $\ln K^\circ$   
 258 equation, and the change of van't Hoff plot of  $\ln K^\circ$  to  $1/T$  was studied (Fig. 8  
 259 (b))(Zhang et al.). The results of the thermodynamic parameters of the ion sieve are  
 260 shown in Table 3. It can be observed that at a temperature of 298.15-318.15K, the  
 261 value of  $\Delta G^\circ$  is maintained at -3.85 to -4.73  $\text{kJ} \cdot \text{mol}^{-1}$ , and is always negative. It  
 262 indicates that as the temperature increases, the adsorption capacity will gradually  
 263 become higher. That is to say, the adsorption of  $\text{Li}^+$  is a spontaneous process. At the  
 264 same time,  $\Delta H^\circ$  is always positive, which can be explained as an endothermic  
 265 adsorption process, indicating that the  $\text{Li}^+$  adsorption effect will increase with  
 266 increasing temperature. Hence, we believe that the adsorption of  $\text{Li}^+$  on the ion sieve  
 267 is a spontaneous endothermic process.



268

269 Fig. 8 Thermodynamic properties of  $\text{Li}^+$  on  $\text{H}_2\text{TiO}_3$  at 298.15, 308.15, and 318.15 K

270

271

Table 3. Thermodynamic parameters for Li<sup>+</sup> adsorption

<i>Sorbents</i>	$\Delta H^{\circ}$ (kJ mol <sup>-1</sup> )	$\Delta S^{\circ}$ (J mol <sup>-1</sup> )	<i>T</i> (K)	<i>K<sup>o</sup></i>	$\Delta G^{\circ}$ (kJ mol <sup>-1</sup> )	<i>R</i> <sup>2</sup>
H <sub>2</sub> TiO <sub>3</sub>	6.54	35.31	298.15	5.00	-3.99	0.992
			308.15	5.50	-4.37	
			318.15	5.90	-4.70	

272

#### 273 4.5. Selective and reusability tests

274 Through selective experiments to determine whether H<sub>2</sub>TiO<sub>3</sub> has a specific  
 275 adsorption selectivity for Li<sup>+</sup>, we simulated salt lake brine for competitive adsorption  
 276 experiment, and tested the adsorption performance of H<sub>2</sub>TiO<sub>3</sub> to Na<sup>+</sup>, Mg<sup>2+</sup>, K<sup>+</sup>, Ca<sup>2+</sup>,  
 277 Li<sup>+</sup>. *K<sub>d</sub>* (mL·g<sup>-1</sup>) is the partition coefficient and *k* as the selectivity coefficient were  
 278 used as indicators to evaluate the selectivity of H<sub>2</sub>TiO<sub>3</sub>. According to the magnitude  
 279 of the comparison *K<sub>d</sub>* value, the adsorption selection performance of H<sub>2</sub>TiO<sub>3</sub> for Li<sup>+</sup>  
 280 can be judged. From the experimental results, we can clearly observe that when the  
 281 adsorption reaches equilibrium, the adsorption effect and partition coefficient (*K<sub>d</sub>*) of  
 282 Li<sup>+</sup> by H<sub>2</sub>TiO<sub>3</sub> are several times that of other metal ions. Based on this, it can be  
 283 determined that the lithium ion sieve H<sub>2</sub>TiO<sub>3</sub> specifically adsorbs Li<sup>+</sup>. The selectivity  
 284 of ion sieve for Li<sup>+</sup> K<sup>+</sup> Ca<sup>2+</sup> Na<sup>+</sup> Mg<sup>2+</sup> was assessed by distribution coefficient (*K<sub>d</sub>*,  
 285 mL g<sup>-1</sup>), which is listed in formula (8):

$$k_d = \frac{C_0 - C_f}{C_f} \times \frac{V}{m} \quad (8)$$

286 In this formula, *C<sub>0</sub>* is interpreted as the initial concentration of five ionic  
 287 solutions, and *C<sub>f</sub>* represents the final concentration of each ionic solution.

288 The industrial feasibility of lithium ion sieve was verified by adsorption cycle  
 289 experiment, so that the production cost was minimized. After each adsorption, the  
 290 eluent (0.1M HCl) desorbs the adsorbent. Such a process is called a cycle. The  
 291 experimental results are shown in Fig. 11. After 5 cycles, the capacity of the  
 292 adsorbent remained above 82% of the initial value. All these results confirm that  
 293 H<sub>2</sub>TiO<sub>3</sub> has a good cycle adsorption potential for Li<sup>+</sup>.

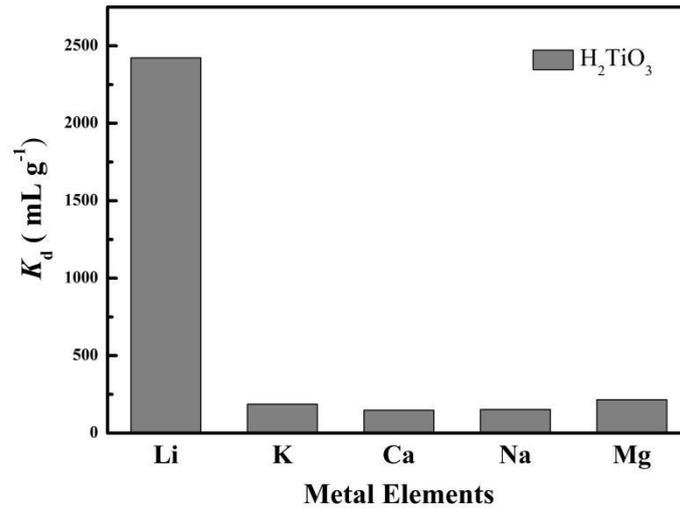


Fig.9  $K_d$  values of  $H_2TiO_3$  for a mixture of  $Na^+$ ,  $Mg^{2+}$ ,  $K^+$ ,  $Ca^{2+}$ ,  $Li^+$

Table 4.  $K_d$  and  $k$  values of  $H_2TiO_3$

Cation	$H_2TiO_3$		
	$C_f$ ( $mg \cdot L^{-1}$ )	$K_d$ ( $mL \cdot g^{-1}$ )	$k$
$Li^+$	14.609	2422.548	
$K^+$	48.059	40.388	0.017
$Ca^{2+}$	45.961	87.879	2.176
$Na^+$	47.634	49.670	0.565
$Mg^{2+}$	44.087	134.121	2.700

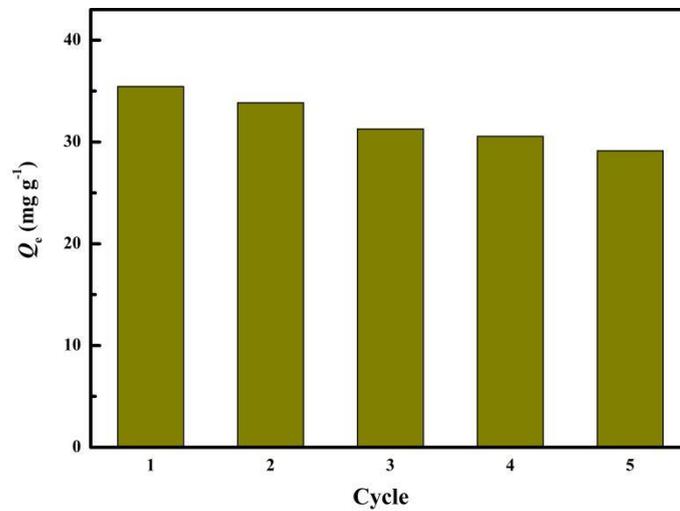


Fig.10 Regeneration of  $H_2TiO_3$  5 cycles.

#### 4. Conclusion

In this study, a lithium ion sieve with bacterial cellulose as a template was successfully prepared and used for the specific adsorption and separation of  $Li^+$  from seawater and salt lake brine. And it shows excellent periodicity and stability in

304 adsorption, elution and circulation experiments. At the same time, using bacterial  
305 cellulose as a biological template, the preparation of mesoporous titanium-based  
306 lithium ion sieve was realized. Compared with the previous methods of assembling  
307 lithium-ion sieve, the ion sieve prepared by using cellulose as biological template not  
308 only has a slightly higher adsorption capacity, but also has the mesoporous structure  
309 provided by bacterial cellulose, which provides more possibilities for future research.  
310 Therefore, we believe that the spinel-type titanium dioxide ion sieve prepared by this  
311 method has broad application prospects and is expected to be widely used.

## 312 **Acknowledgements**

313 This work was funded through National Natural Science Foundation of China  
314 [No.21808018, 21876015, 21878026]; Jiangsu Provincial Science and Technology  
315 Department Industry Foresight Plan [No. FZ20180422]; Natural science research  
316 project of colleges and universities in Jiangsu Province [No.18KJB610002] and  
317 Applied Basic Research in Changzhou [No. CJ20180055]. The authors also expressed  
318 their gratitude to other testers in this study.

## 319 **Declarations**

## 320 **Conflict of interest**

321 The authors declare that they have no conflict of interest.

## 322 **Ethical approval**

323 The article does not contain any experiments with human participants or animals  
324 performed by any of the authors.

## 325 **Informed consent**

326 Informed consent was obtained from all individual participants included in the st  
327 udy

## 328 **References**

- 329 Aimar A, Palermo A, Innocenti BJJ<sub>o</sub>HE (2019) The Role of 3D Printing in Medical Applications: A  
330 State of the Art 2019:1-10  
331 Argurio P, Tagarelli A, Molinari R (2019) A Study on Neodymium Recovery from Aqueous Solutions  
332 for Designing a New Generation of Sandwich Liquid Membrane

333 DING et al. (2018) Genesis of the Weiquan Ag-Polymetallic Deposit in East Tianshan, China: Evidence  
334 from Zircon U-Pb Geochronology and C-H-O-S-Pb Isotope Systematics v.92:222-244

335 Elik A, Topu G, Isik T, Baba A, Horzum N, De mir MM Investigation of Lithium Sorption Efficiency  
336 Using SWCNT Functionalized Electrospun Fiber Mats from the Hypersaline Geothermal  
337 Brine. In: Materials Science Forum, 2018.

338 Gao A, Sun Z, Li S, Hou X, Li H, Wu Q, Xi XJDT (2018) The mechanism of manganese dissolution on  
339 Li<sub>1.6</sub>Mn<sub>1.6</sub>O<sub>4</sub> ion sieves with HCl 47:3864-3871

340 Garay-Rodríguez L, Murcia-López S, Andreu T, Moctezuma E, Torres-Martínez L, Morante JRJC  
341 (2019) Photocatalytic Hydrogen Evolution Using Bi-Metallic (Ni/Pt) Na<sub>2</sub>Ti<sub>3</sub>O<sub>7</sub> Whiskers:  
342 Effect of the Deposition Order 9

343 Garcia, Eric, M., Taroco, Hosane, Recycling AJ (2018a) Water Electrolysis Anode Based on  
344 Stainless Steel Coated with Cobalt Recycled from Li-Ion Batteries 3:42-42

345 Garcia, Eric M, Taroco, Hosane A, Teixeira, Rodrigo GJR (2018b) Fast Electrochemical Method for  
346 Organic Dye Decolorization Using Recycled Li-Ion Batteries

347 Gebreslase GAJJoMS, Technology (2018) Review on Membranes for the Filtration of Aqueous Based  
348 Solution: Oil in Water Emulsion 08

349 Grágeda M, González A, Grágeda M, Ushak SJIJoER (2018) Purification of brines by chemical  
350 precipitation and ion-exchange processes for obtaining battery-grade lithium compounds

351 Gza B, Dt A, Mb AJAG (2020) Solvent extraction of lithium from simulated shale gas produced water  
352 with a bifunctional ionic liquid - ScienceDirect 123

353 Img A, Avv A, Vmv B (2021) Thermal dependency of Li<sup>+</sup> ion conductivity in Li<sub>2</sub>O-Fe<sub>2</sub>O<sub>3</sub>-Al<sub>2</sub>O<sub>3</sub>  
354 ceramics

355 Li M, Miao Y, Zhai X, Yin Y, Liu ZJM, design (2019) Preparation of and research on bioinspired  
356 graphene oxide/nanocellulose/polydopamine ternary artificial nacre 181:107961

357 Lihua et al. (2018) New Insights into the Application of Lithium-Ion Battery Materials: Selective  
358 Extraction of Lithium from Brines via a Rocking-Chair Lithium-Ion Battery System

359 Liu L, Feng X, Rahe C, Li W, Ouyang MJJoEC (2021) Internal short circuit evaluation and  
360 corresponding failure mode analysis for lithium-ion batteries

361 Ma L, Xi X, Wang K, Zhao LJRoCI (2018) Adsorption of Li by a lithium ion-sieve using a buffer  
362 system and application for the recovery of Li from a spent lithium-ion battery:1-19

363 Michel C, Barré Y, Guiza MB, Dieuleveult CD, Windt LD, Grandjean AJCEJ (2018) Breakthrough  
364 studies of the adsorption of Cs from freshwater using a mesoporous silica material containing  
365 ferrocyanide 339:288-295

366 Peng C, Liu F, Wang Z, Wilson BP, Lundstrom MJJoPS (2019) Selective extraction of lithium (Li) and  
367 preparation of battery grade lithium carbonate (Li<sub>2</sub>CO<sub>3</sub>) from spent Li-ion batteries in  
368 nitrate system 415:179-188

369 Romero VCE, Tagliazucchi M, Flexer V, Ca Lvo EJJJoTES (2018) Sustainable Electrochemical  
370 Extraction of Lithium from Natural Brine for Renewable Energy Storage 165:A2294-A2302

371 Sasaki K, Yu Q (2015) Synthesis of a Biotemplated Lithium Ion-Sieve Derived from Fungally Formed  
372 Birnessite. Advances in the Environmental Biogeochemistry of Manganese Oxides,

373 Song JF, Nghiem LD, Li XM, He TJESWR, Technology (2017) Lithium extraction from Chinese salt-  
374 lake brines: opportunities, challenges, and future outlook 3:593-597

375 Sw A, Yw A, Tao CA, Cl A, Yt BJCEJ Porous lithium ion sieves nanofibers: General synthesis strategy  
376 and highly selective recovery of lithium from brine water 379

377 Tomer VK, Malik R (2019) Hybridized Graphene for Chemical Sensing  
378 Wen Z, Mou Y, Song Z, Xie L, Wang Y, Jing CJPiC (2017) Adsorption Materials for Lithium Ion from  
379 Brine Resources and Their Performances  
380 Yang SS, Zhou ML, Wu JQ, Shen JN, Gao CJ Development and Adsorption Properties for a Novel  
381 Lithium Ion-Sieve. In: Materials Science Forum, 2016. pp 691-697  
382 Zeng X, Mathews JA, Li JJES, Technology (2018) Urban Mining of E-Waste is Becoming More Cost-  
383 Effective Than Virgin Mining 52:4835–4841  
384 Zhang, Zhang, Fusheng, Yongsheng, Zhongyu, Zheng, Xudong Dual-template docking oriented ionic  
385 imprinted bilayer mesoporous films with efficient recovery of neodymium and dysprosium  
386 Zhang LY, Shui Y, Zhao LL, Zhu P, You YHJC (2019) Preparation of Ni-Doped Li<sub>2</sub>TiO<sub>3</sub> Using an  
387 Inorganic Precipitation–Peptization Method 9:701  
388 Zhao D, Xue-Min DU, Wang SQ, Guo YF, Deng TLJJoSS, Industry C (2017) Research on Extraction  
389 from Salt Lake Brine with High Mg/Li Ratio  
390