

# Fabrication of Novel Bio-Adsorbent And Its Application For The Removal of Cu(II) From Aqueous Solution

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## Research Article

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1 **Fabrication of novel bio-adsorbent and its application for the removal of Cu(II)**  
2 **from aqueous solution**

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9

10 **Abstract**

11 As an eco-friendly adsorption material, hydroxyapatite (Ha) have received widely  
12 attention from researchers owing to their excellent biocompatibility and adsorption  
13 performance. However, the inconvenient in separating Ha powder from adsorbed  
14 processes following use has limited their application. Herein, a novel alginate-based  
15 composite beads encapsulation with cellulose and Ha (named HCA) was designed to  
16 remove Cu(II) from aqueous solution. Fourier-transform infrared spectroscopy (FTIR),  
17 X-ray diffraction (XRD), Scanning electron microscopy (SEM), and X-ray  
18 photoelectron spectroscopy (XPS) were used for characteristic analysis. The impacts  
19 of samples compositions, various Cu(II) concentration, adsorption equilibrium time,  
20 and regeneration performance on the adsorption process were investigated. The results  
21 suggested that beads exhibited their maximum adsorption capacity for Cu(II) was  
22 obtained to be 64.14 mg/g at pH=5 for 8 h, best fitted into Langmuir isotherm models  
23 and the pseudo-second-order kinetic model. In addition, the biocompatible beads not  
24 only increase the sorption sites, but also have good regenerability, would be a  
25 promising bio-adsorbent for heavy metal ion removal.

26 **Keywords** : Hydroxyapatite; Adsorption; Sodium alginate; Cellulose; Heavy Metal,  
27 bio-adsorbent.

28

## 29 **Introduction**

30 Attendant with the growth of global industrialization and urbanization, water  
31 environment such as lakes and river have been polluted by human-mediated activities.  
32 Emission of heavy metals has raised increasing concern, due to their toxicity,  
33 carcinogenicity, and non-biodegradable in living organisms. To address the problem  
34 of water pollution, many efficient strategies were used for the separation and  
35 purification of contained water, such as chemical precipitation(Ebrahimi et al. 2017),  
36 membrane filtration(Jiang et al. 2018), electrochemical treatment and  
37 adsorption-based separation (Shalla et al. 2019). Among these various techniques,  
38 adsorption is effective and widely used in water treatment because of the facile and  
39 low-cost operation (Joseph et al. 2019). Various adsorbents have been evaluated,  
40 including graphene oxide (GO), and metal organic frameworks (MOF) (Zhu et al.  
41 2019; Yap et al. 2020). However, the inconveniently in separating these powder  
42 materials after adsorption process limit their application for water treatment.

43 Sodium alginate (SA), a polyanionic polymer, can crosslink with divalent metal  
44 ions to form a stable framework with three-dimensional (3D) network structure,  
45 which can combined with nanomaterials to overcome the barrier in separation and  
46 recover of nanomaterials after adsorption process (Song et al. 2019). Futhermore,  
47 their surface with hydroxyl and carboxyl groups provide large amounts of bonding  
48 sites, which are conducive to capturing metal ions. For instance, Baigorria et al.  
49 introduced bentonite-composite polyvinyl alcoho into the network structure of  
50 composite hydrogel beads, forming adsorbents that are stable and with excellent

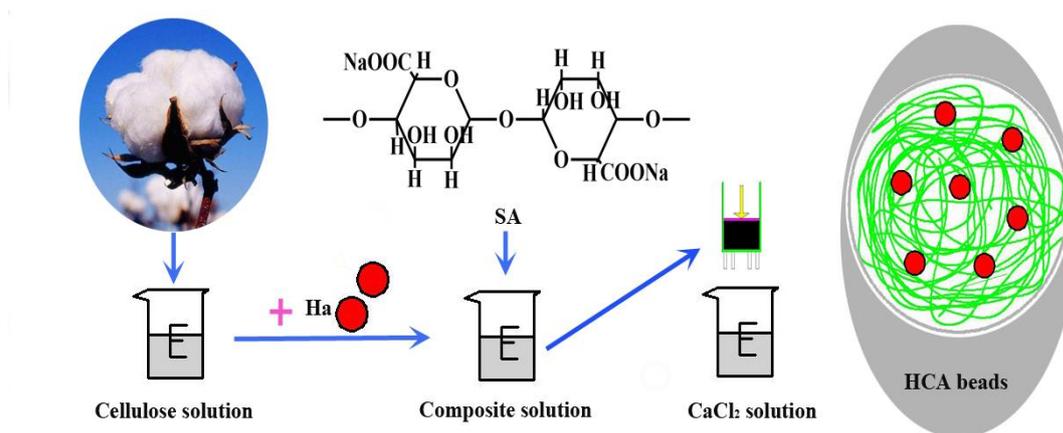
51 adsorption performance for As (Baigorria et al. 2020). Considering the  
52 interdependency of the physical and chemical properties of alginate-based hydrogels,  
53 the powder material encapsulated into the hydrogel network not only outstanding  
54 change its structure, but also could enhanced in environmental applications (Lva et al.  
55 2019). Accordingly, Ha is a natural mineral calcium apatite, which is the main  
56 component of hexagonal crystal of calcium, phosphorus and oxygen(Szczęś et al.  
57 2017). Due to its nontoxicity, high adsorption efficiency, high biocompatibility and  
58 cost-effective production, Ha may be an alternative material for heavy metal removal.

59 Recently, bioadsorbents have attracted more and more attention because of their  
60 non-toxic and biodegradable properties (Muya et al. 2016). Natural biopolymers (e.g.,  
61 cellulose, pectin and chitosan), as a biodegradable, abundant, and renewable resource,  
62 has attracted great attention for the design of sorbent materials from security concern.  
63 Cellulose is considered to be renewable polysaccharide and widely in the world. In  
64 the long run, non-poisonous, ecological, and abundant bio-polymers will be  
65 undoubtedly beneficial for supplying clean water for the human (Zhang et al. 2020).  
66 More important, Cellulose can form a stable network structure through physical  
67 crosslinking, which is helpful to provide more adsorption sites. In the past years, some  
68 researchers have employed cellulose composite beads to improve their adsorptive  
69 properties for heavy metal removal of from wastewater (Luo et al. 2016; Liu et al.  
70 2020 ).

71 Inspired by the advantages alginate and cellulose based material, we develop a  
72 nontoxic and eco-friendly bio-adsorbent for the removal of heavy metal ion (Cu(II))

73 from aqueous solution. The fabrication of the adsorbent was described in Scheme 1.  
 74 We hypothesized that if the good adsorption performance of Ha could be combined  
 75 with the good 3D porous performance of cellulose and alginate material, the difficulty  
 76 of separation of ha from water can be overcome, the adsorption performance of  
 77 hydrogel beads could be improved. The adsorbent performance was evaluated in view  
 78 of the adsorption kinetics, isotherms and thermodynamics. The outcomes of our study  
 79 suggest that the cross-linked HCA composite beads are a potential adsorbent for  
 80 efficient water purification.

81



82

83 Scheme 1. Schematic diagram for the characterization of HCA beads

## 84 2.Methods and Materials

### 85 2.1 Materials

86 Cellulose ( $\alpha$ -cellulose) was kindly obtained by Hubei Golden Ring Co.,Ltd.  
 87 (Xiangyang, China). Sodium hydroxide (NaOH), urea, sodium alginate, copper sulfate  
 88 pentahydrate ( $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$ ) and calcium chloride were provided by Sinopharm  
 89 Chemical Reagent Co., Ltd (Shanghai, China). Ha ( $\geq 97\%$ ,  $< 100\text{nm}$ ) was obtained  
 90 from Aladdin industrial corporation (Shanghai, China). Deionized (DI) water was

91 supplied from a TS-DI water filtration system.

## 92 2.2 Preparation of the cellulose solution (CS)

93 Cellulose (4g) was rapidly dissolved into NaOH/urea/H<sub>2</sub>O( 7:12:81, weight ratio)  
94 solution at low temperature condition (-12 °C) according to the reported method (Qi  
95 et al. 2009). The resulting solution stirring for 5 min, until to obtained the transparent  
96 CS.

## 97 2.3 Preparation of the HCA beads

98 Firstly, the Ha (0.1 g, 0.2 g, 0.4 g, 0.8 g and 1.6 g) and CS (0.2 g, 0.4 g, 0.8 g, 1.6  
99 g and 3.2 g) were added into SA solution (1%, w/v), respectively. The mass ratios  
100 (Ha:CS:SA) of mixed solution for (0.1:0.2:1) (0.2:0.4:1) (0.4:0.8:1) (0.8:1.6:1) and  
101 (1.6:3.2:1). Then, the mixture were stirred for 0.5 h to produce mixed solution evenly.  
102 Finally, the mixed solution was dropped into CaCl<sub>2</sub> solution (2%, 200 mL) using a 20  
103 mL syringe. After curing for 6 h, the obtained HCA beads were washed three times  
104 with deionized water.

## 105 2.4 Adsorption Investigation

106 To systematically study Cu(II) adsorption behaviors of HCA beads, adsorption  
107 experiments were conducted using Cu(II) as model heavy metal ions. An optimized  
108 dose of wet adsorption beads were added to 50ml of copper ion solution, the  
109 concentrations of the initial solutions were 100-500mg/L. Therein, it is ensured that  
110 adsorbents has well contact with the solution, the concentration of the adsorbed  
111 solution was determined by spectrophotometry (Apha 2005). the results were repeated  
112 for three times. Adsorption capacity was calculated using the following equation:

113 
$$q_e = \frac{(C_0 - C_e) V}{m} \quad (1)$$

114 The removal rate of Cu(II) by HCA was calculated from each step and defined  
115 as:

116 
$$\text{Removal (\%)} = \frac{C_0 - C_e}{C_0} \times 100\% \quad (2)$$

117  $q_e$  stands for the adsorption capacity of the bio-adsorbent for heavy metals  
118 (Cu(II)) (mg/g),  $V$  is volume of Cu(II) solution (L), and  $C_0$  and  $C_e$  are concentration  
119 of the initial and equilibrium, respectively.

## 120 2.5 Characterization methods

121 Fourier-transform infrared spectra (FTIR) of the product was performed on a  
122 spectrometer (Nicolet 6700). X-ray diffraction (XRD) test of sample was carried out  
123 by an XRD Rint-2000 diffractometer. The surface microstructure of the product was  
124 observed by a scanning electron microscopy (SEM) Nova Nano SEM 230 with an  
125 energy dispersive spectroscopy (EDS) for analyzing different elements. Elemental  
126 analysis of the materials was performed on X-ray photoelectron spectroscopy (XPS)  
127 ESCALAB 250Xi.

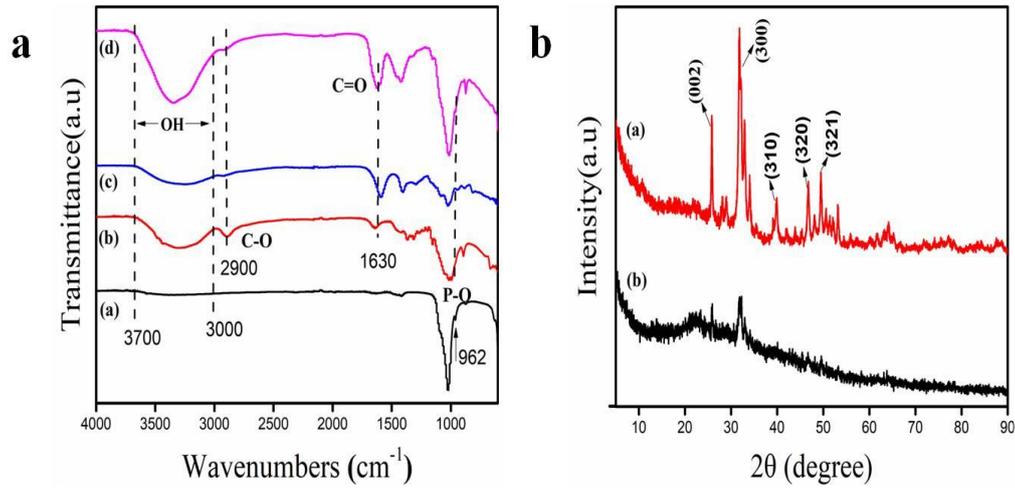
## 128 2.6 Regeneration experiment

129 To further investigate the reusability of HCA beads for Cu(II) adsorption, the  
130 desorption experiments were carried out with 0.1mol/L  $\text{Ca}(\text{NO}_3)_2$  solutions,  
131 0.01mol/L  $\text{HNO}_3$  and deionized water. After elution, the regenerated HCA beads was  
132 subsequently evaluated in adsorption experiments to study their recyclability.

## 133 3. Results and discussion

134 3.1. Characterization of the samples

135 3.1.1. FT-IR analysis

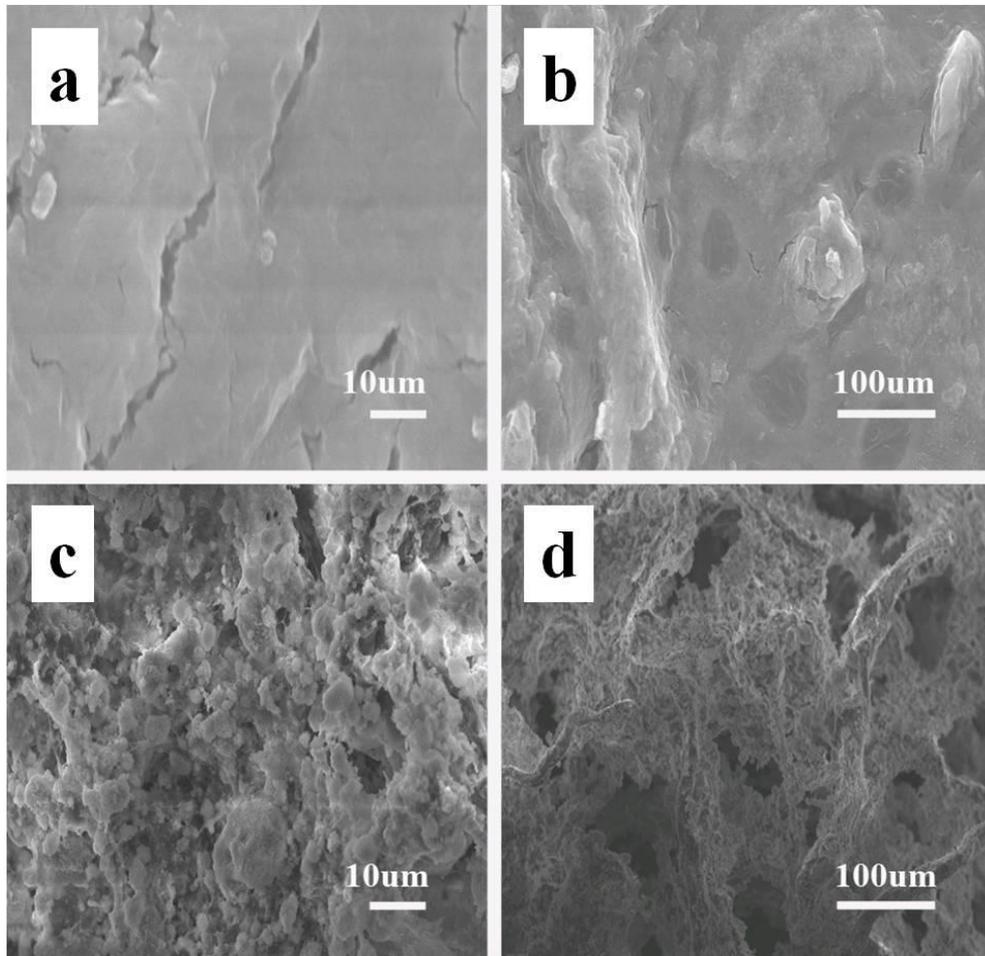


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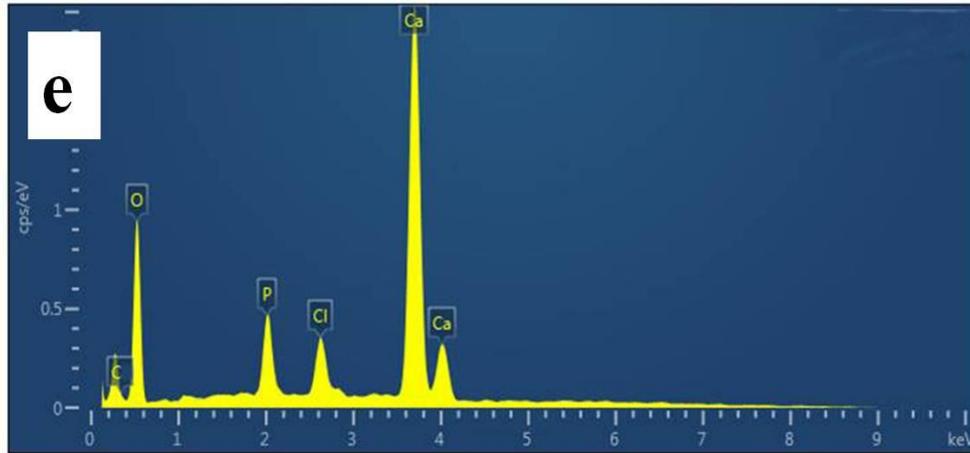
137 Fig. 1 . a: FTIR spectra of Ha (a), Cellulose (b), CA (c) and HCA(d). b: XRD patterns  
138 of Ha (a) and HCA (b)

139 To investigate the interaction between the Cellulose and Ha, CA and HCA, the  
140 prepared sample were characterized by FTIR spectra and XRD patterns. The results  
141 were presented in Fig. 1a and Fig. 1b. As shown in Fig. 1a, FTIR analysis show the  
142 characteristic absorbance of the Ha (a), CA (b), Cellulose (c) and HCA (d). The  
143 absorption peak at around 962 cm<sup>-1</sup> is derived from stretching modes of P-O in HCA  
144 composite beads (Zhang et al. 2019). After the Ha and Cellulose were introduced into  
145 CA, the asymmetric and symmetric stretching vibrations of the C=O bands shifted to  
146 1630cm<sup>-1</sup> (HCA) from 1640 cm<sup>-1</sup> (Cellulose) and 1590 cm<sup>-1</sup> (CA), which also  
147 provided evidence for the interaction between Cellulose and sodium alginate matrix.  
148 These new peak at 2900 cm<sup>-1</sup> was corresponding to the stretching vibration of C-O,  
149 which confirms the binding of cellulose and alginate chains on the HCA surface by  
150 the electrostatic force (Luo et al. 2016). A broad absorption peak at around 3600-3000

151  $\text{cm}^{-1}$  was derived from the stretching vibrations of hydroxyl groups in the HCA,  
152 suggesting the more stronger interaction among the alginate matrix. The XRD  
153 patterns of the obtained Ha (a) and HCA (b) are presented in Fig. 1b. The diffraction  
154 peaks (002), (300), (310), (320), and (321) can be indexed to  $\text{Ca}_5(\text{PO}_4)_3\text{OH}$  (JCPDS  
155 09-0432). For HCA composites, the intensities of diffraction peaks of Ha in the XRD  
156 pattern decline, indicating the exist of the Ha content in the as-prepared materials.  
157 3.1.2 SEM and EDS analysis



158

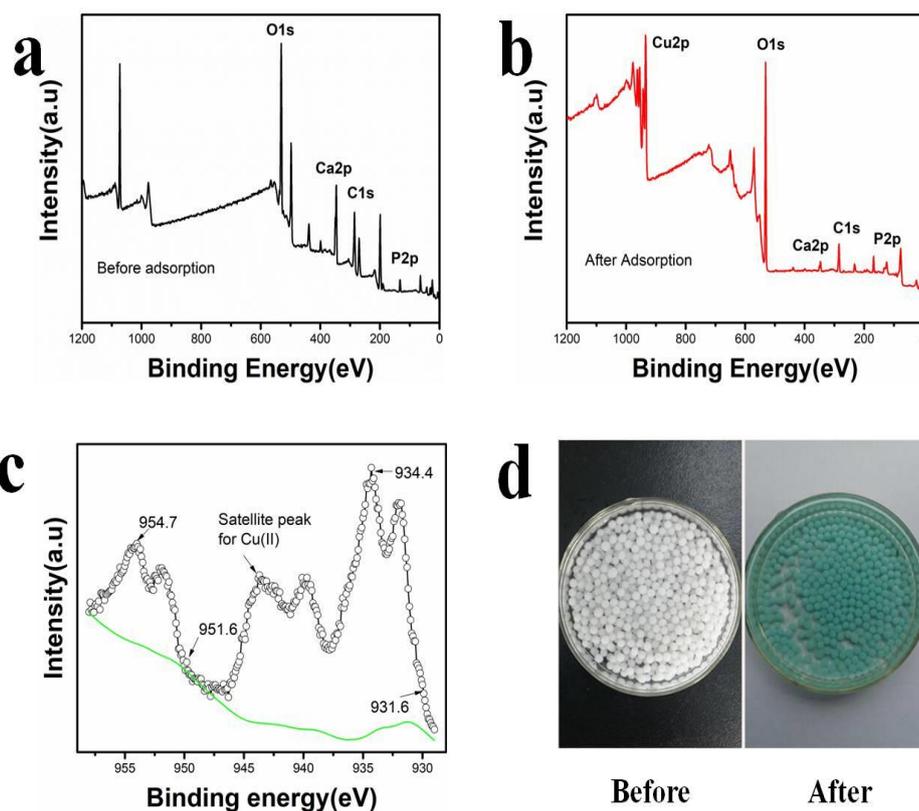


159

160 Fig. 2. SEM images of CA and HCA composite beads (a-d), EDS spectra of HCA (e).

161 As shown in Fig. 2(a-b) we can see that the morphological structure of CA with  
 162 smooth fracture surface, which may be caused by dehydration of the hydrogel beads.  
 163 For the HCA composite beads in Fig. 2(c-d), as expected, the surface showed an  
 164 irregular wrinkled structure, which would be conducive to the adsorption of heavy  
 165 metal ions. In addition, the composite beads appeared visible huge porous more  
 166 cavities significantly (Fig. 2d). Hence, the new structure could increase more active  
 167 sites, which was also beneficial for the adsorption of metal ions onto the HCA  
 168 material. In this way, the adsorption process of heavy metal ions Cu(II) not only occur  
 169 on the surface of the bead, but also interact with its internal active sites, thus the  
 170 adsorption sites can be maximized. In addition, the EDS analysis of HCA show that  
 171 the composite hydrogel beads is mainly composed of C, O, P, Cl and Ca elements (Fig.  
 172 2e), which demonstrated that Ha was successfully encapsulated into Cellulose and  
 173 alginate-based matrix.

174 3.1.3 XPS analysis



175

176 Fig. 3. The XPS survey spectra of HCA before and after Cu(II) adsorption

177 In order to study the changes of related elements before and after the adsorption  
 178 of adsorbent, the XPS spectra of Cu(II) adsorption before and after the modification  
 179 of HCA were analyzed(Fig. 3 a.b). The high resolution energy spectrum shows the  
 180 elemental composition of the HCA hydrogel beads, and the binding energy signals at  
 181 284.8 eV, 347 eV and 532 eV correspond to the C1<sub>s</sub> peak, Ca2<sub>p</sub> peak and O1<sub>s</sub> peak in  
 182 HCA, respectively (Zhang et al 2020). When Cu(II) was adsorbed, the characteristic  
 183 peak of Cu2<sub>p</sub> appeared, indicating that the heavy metal Cu(II) ion was successfully  
 184 adsorbed to the surface and/or interior of HCA. For the high-resolution Cu2<sub>p</sub> spectra  
 185 (Fig. 3c), the XPS peak binding energies of Cu 2<sub>p1/2</sub> and Cu 2<sub>p3/2</sub> are 951.6-954.7 eV  
 186 and 931.6-934.4 eV, respectively (Godiya et al 2019 ). In addition, the satellite peak is  
 187 located at the binding energy 944.3 eV (Zhang et al 2020), which also indicates that

188 Cu(II) exists on the surface of HCA hydrogel beads.

## 189 3.2 Adsorption studies

### 190 3.2.1 Adsorption kinetics of HCA beads

191 In order to further understand the adsorption process, the adsorption experiment  
192 was evaluated by the following kinetic model (Bo et al 2020).

193 The pseudo-first-order kinetic Eq. (5):

$$194 \quad \ln(q_e - q_t) = \ln q_e - k_1 t \quad (3)$$

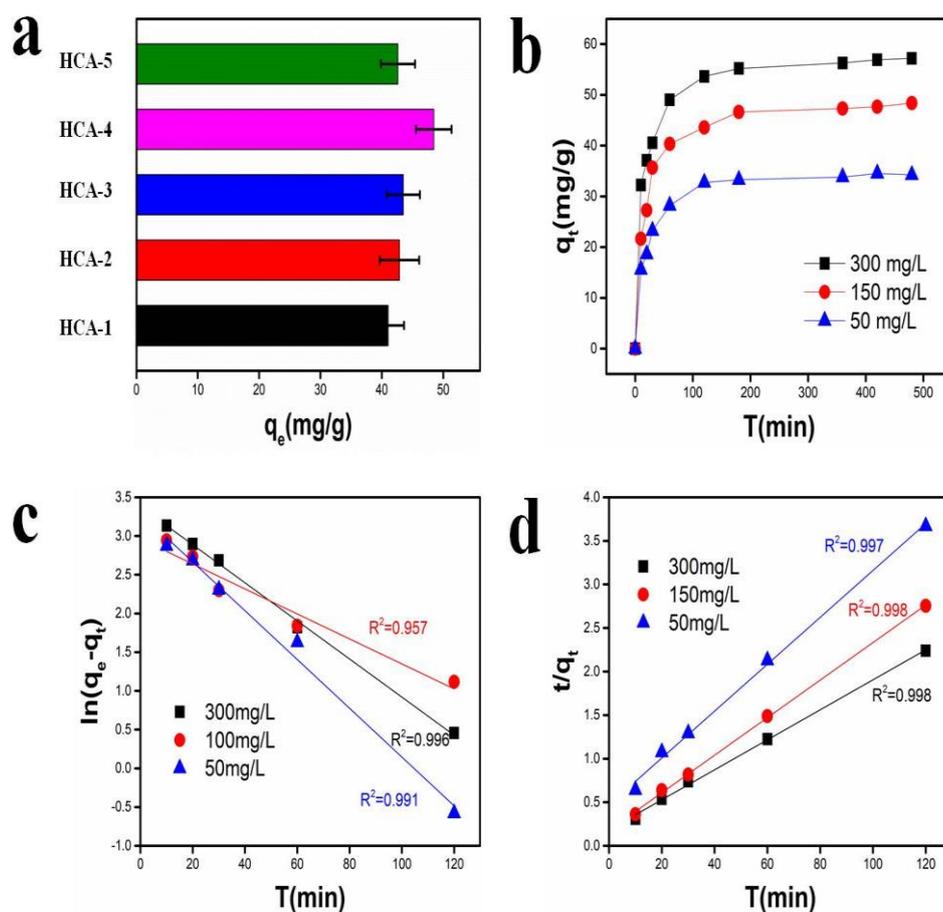
195 The pseudo second-order kinetic Eq. (6):

$$196 \quad \frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (4)$$

197 Where,  $q_e$  represents adsorption capacity of the equilibrium (mg/g), and  $q_t$   
198 represents the adsorption capacity at time  $t$  (min).  $k_1$  (L/min) and  $k_2$  (g/mg.min)  
199 represents adsorption rate constants.

200 Table 1 Compositions of the prepared HCA beads samples

Samples	HCA-1	HCA-2	HCA-3	HCA-4	HCA-5
HA	0.1%	0.2%	0.4%	0.8%	1.6%
CS	0.2%	0.4%	0.8%	1.6%	3.2%
SA	1%	1%	1%	1%	1%



201

202 Fig. 4. (a) Effect of the mass ratio of HCA contents for Cu(II) (Temperature: 293  
 203 K, pH=5). (b) fitting curves of adsorption kinetics. (c) pseudo-first-order model of  
 204 HCA beads. (d) pseudo-second-order model of HCA beads.

205 Table 1 shows the different mass ratios of the HCA samples with Ha, CS, and SA  
 206 in the preparation process. The influence of different mass ratios of Ha, CS, and SA  
 207 on the adsorption capacity was also investigated (Fig. 4a). As demonstrated above,  
 208 considering the adsorption capacity, the optimal mass ratio of Ha/CS/SA was  
 209 determined to be 0.8% : 1.6% : 1%. In order to investigate their adsorption properties.  
 210 HCA beads were placed in conical flask containing 50 mg/L, 150 mg/L, and 300  
 211 mg/L Cu(II) solution (50 mL, pH=5), respectively. The results are shown in Fig. 4b,

212 as the increase of Cu(II) concentration, the adsorption capacities of HCA beads  
213 obviously increased. The Cu(II) adsorption capacities of the HCA beads reach up to  
214 55.20 mg/g, better than those of other hydrogels materials (Zhang et al 2019, Wu et al  
215 2019). In addition, the experimental results show that the pseudo-second-order kinetic  
216 model (300mg/L :  $R^2=0.998$ , 150mg/L :  $R^2=0.998$ , 50mg/L :  $R^2=0.997$ ) can better fit  
217 the experimental data than the first-order kinetic model (300mg/L :  $R^2=0.996$ ,  
218 150mg/L :  $R^2=0.957$ , 50mg/L :  $R^2=0.991$ ) for Cu(II) adsorption. The calculated  
219 theoretical maximum adsorption capacity is closer to the real experimental value.  
220 Therefore, the above results show that the adsorption process of HCA for Cu(II) is  
221 more consistent with chemical adsorption (Pu et al 2018).

### 222 3.2.2 The isotherm study of HCA

223 In order to further evaluate the adsorption performance of HCA for Cu(II),  
224 Langmuir and Freundlich isothermal models are used to fit the adsorption  
225 experimental data. The formula of Langmuir and Freundlich adsorption isothermal  
226 model (Kim et al 2017) are:

227

$$228 \quad \frac{C_e}{q_e} = \frac{1}{bq_m} + \frac{C_e}{q_m} \quad (5)$$

$$229 \quad \ln q_e = \ln K_f + \ln C_e \quad (6)$$

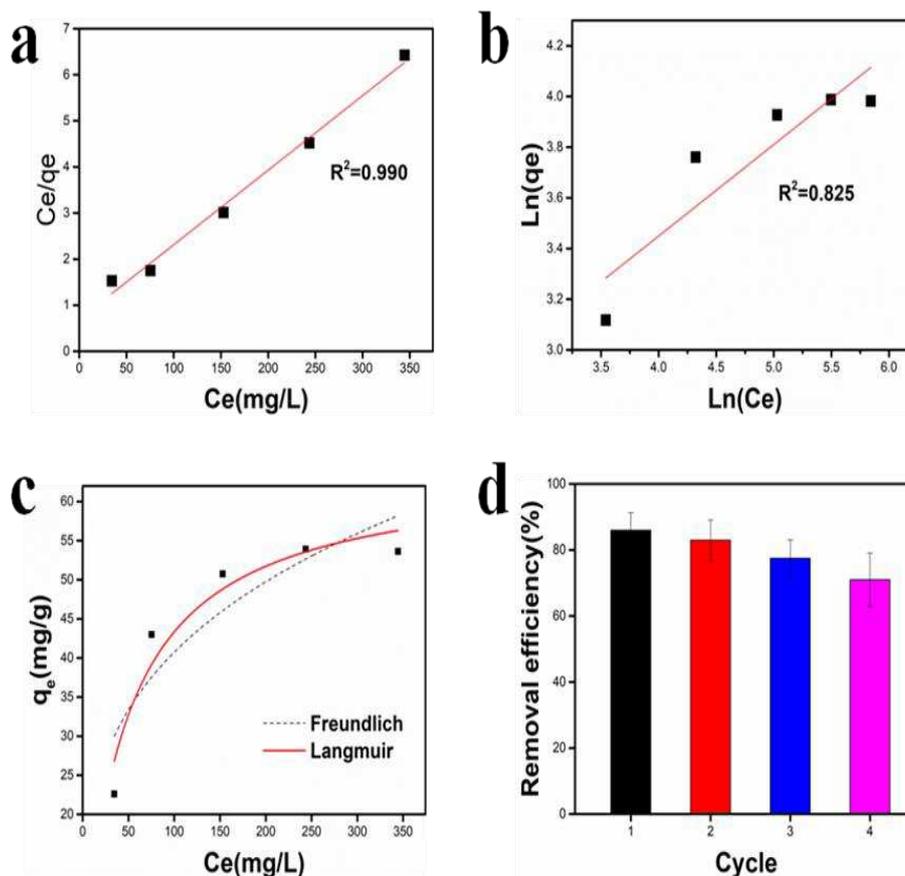
230  $K$  (L/mg) represent the Langmuir equilibrium adsorption constant,  $q_m$  represent  
231 the maximum uptake adsorption capacity (mg/g),  $C_e$  represent the concentration  
232 (mg/L), and  $q_e$  represent the equilibrium adsorption capacity (mg/g) of the two models.  
233  $n$  represent a heterogeneous factor.

234 The relevant parameters of Langmuir and Freundlich models are shown in Table  
 235 2. As you can see from the correlation coefficient  $R^2$ , the correlation coefficient of the  
 236 Langmuir sorption type ( $R^2=0.990$ ) is higher than that of the Freundlich sorption type  
 237 ( $R^2=0.825$ ), indicating that the adsorption type of Cu(II) on HCA beads are more  
 238 suitable for the Langmuir adsorption isotherm model. Therefore, the adsorption  
 239 performance of Cu(II) on HCA suggested a monomolecular layer adsorption plays an  
 240 key role (Hu et al 2018).

241 Table.2 Langmuir and Freundlich adsorption isotherm model parameters for the  
 242 adsorption of Cu(II) onto HCA at 293 K

T(K)	Langmuir			Freundlich		
	$q_m$ (mg/g)	$b$ (L/mg)	$R^2$	$K_f$	$n$	$R^2$
303	64.14	0.023	0.990	7.43	2.77	0.825

243



244

245 Fig. 5. (a) Langmuir models, (b) Freundlich models, (c) Langmuir isotherm and  
 246 Freundlich isotherm fitting curve, (d) Reusability of HCA beads for Cu(II) adsorption  
 247 (30 mg/L, 293 K).

#### 248 4. Recycling experiment

249 The regeneration of HCA beads adsorbents are highly important for further  
 250 evaluation of its practical application. The material was regenerated in 0.1 mol  
 251  $\text{Ca}(\text{NO}_3)_2$  and 0.01 mol/L  $\text{HNO}_3$  solution (Wang et al 2016, Oulguidoum et al 2021).  
 252 After cleaning with deionized water, the recycled samples were rinsed with distilled  
 253 water several times to remove trace salt, and then the adsorption test was carried out  
 254 to study their recycling performance. Fig. 5d shows the relationship between the  
 255 removal efficiency and the number of cycles. Specifically, after 4 cycles of

256 experiments, the removal efficiency decreased slightly, but still maintained a good  
257 removal efficiency. In conclusion, HCA microbeads not only show good reusability,  
258 but also can be separated by gravity, which has potential industrial applications.

## 259 **5. Mechanisms of Cu(II) removal**

260 The removal of Cu(II) is a complicated process, in which physics and chemistry  
261 adsorption might play a significant role. Specifically, (1) cation-exchange might  
262 participate in the adsorption process, namely calcium ions in hydrogel matrix  
263 definitely can be replaced with the free Cu(II) ions (Wang et al 2020). (2) The  
264 abundance of COO<sup>-</sup> and O-containing groups on the surface of beads can also easily  
265 coordinate with Cu(II) to form complexes (Zhang et al 2020). (3) Besides, Ha possess  
266 abundant hydroxyl functional groups, which all help are beneficial for Cu(II)  
267 adsorption from wastewater. Therefore, it can be further ascertained that HCA beads  
268 have a promising and star candidate for water decontamination.

## 269 **6. Conclusion**

270 In this study, eco-friendly, micro- and nanostructured and good recycling  
271 bio-adsorbent was fabricated via a green cross-linked technology for the removal of  
272 Cu(II). The stable surface structure of the adsorbent was confirmed by further FTIR,  
273 XRD, SEM and XPS characterization analysis. The adsorption performance were  
274 evaluated by using the batch adsorption experiment, and the maximum adsorption  
275 capacity of HCA for Cu(II) was 64.14 mg/g, The adsorption kinetics studies showed  
276 that the adsorption process for Cu(II) was mainly controlled by chemical adsorption,  
277 and Langmuir model fitted the adsorption parameter better. The adsorption-desorption

278 experiment was repeated for 4 times and still kept a high removal efficiency. In  
279 summary, The HCA beads with excellent adsorption performance is promising  
280 bio-adsorbent to applications for the removal of Cu(II) from wastewater.

#### 281 **Ethical approval and consent to participate**

282 Not applicable

#### 283 **Consent to publish**

284 Not applicable

#### 285 **Authorship contribution statement**

286 Dianjia Zhao: Conceptualization, Formal analysis, Methodology, Writing - original  
287 draft, Validation. Wenkang Ye: Investigation, Visualization, Validation Project  
288 administration. Wenxuan Cui: Software, Investigation, Data curation, Writing - review  
289 & editing.

#### 290 **Declaration of Competing Interest**

291 The authors declare that they have no known competing financial interests or personal  
292 relationships that could have appeared to influence the work reported in this paper.

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#### 298 **Data availability**

299 The datasets used and/or analyzed during the current study are available from the

300 corresponding author on reasonable request.

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### 398 **Highlights**

- 399 • A novel eco-friendly cross-linked HCA bio-adsorbent were prepared by a  
400 three-step method.
- 401 • The bio-adsorbent beads (HCA) showed excellent adsorption capacities for Cu(II),  
402 and the adsorption kinetics and isotherms were studied.
- 403 • Unlike traditional nanomaterials adsorbents, the spherical HCA beads, with a  
404 above diameter of 3-5mm, were easily separated after the adsorption process.
- 405 • The HCA bio-adsorbent can be easily regenerated and reused repeatedly for Cu(II)  
406 adsorption.