

# Electricity Generation and Pollutants Removal of Landfill Leachate by Osmotic Microbial Fuel Cells with Different Forward Osmosis Membranes

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## Research

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# Abstract

In this study, thin-film composite with embedded polyester screen (TFC-ES), cellulose triacetate with a cast nonwoven (CTA-NW) and cellulose triacetate with embedded polyester screen (CTA-ES) were examined as the intermediate membranes in osmotic microbial fuel cells (OsMFCs). The reactors were fed with actual landfill leachate and the performance was studied in two operation modes: active layer facing draw solution (AL-DS) and active layer facing feed solution (AL-FS). The OsMFC with CTA-ES exhibited the best energy generation (maximum power density:  $0.44 \text{ W}\cdot\text{m}^{-2}$ ) and pollutant removal efficiency (ammonia nitrogen:  $70.12 \pm 0.28\%$ , total nitrogen:  $74.04 \pm 0.33\%$ ) in the AL-FS mode, which could be ascribed to the lowest internal resistance (236.75 ohm) and highest microbial richness. *Pseudomonas* was the highest proportion of microbial in OsMFCs. The results of this study has demonstrated the potential of OsMFCs for landfill leachate treatment.

## 1. Introduction

Landfill leachate contains a wide range of organics, inorganics, heavy metals and salts. It is generally characterized with a high concentration of ammonia and a low biodegradable organic matter content [1]. Untreated leachate causes serious hazardous impacts to the surrounding environment, and thus requires prompt and efficient action with suitable treatments [2, 3]. At present, Electro-Fenton Process, Sequencing Batch Reactor (SBR), Internal Circulation (IC) anaerobic reactor and Upflow Anaerobic Sludge Blanket (UASB) are commonly used to treat landfill leachate [4, 5]. Due to the complex composition of landfill leachate, these treatments alone are not able to achieve complete removal of the diverse organics from leachate, causing secondary pollution and further affecting the environment and human health [6, 7]. Hence, it is necessary to develop new technologies for the effective removal.

Microbial fuel cell (MFC) is a new method of generating electrical energy through microbially catalyzed organic oxidation [8]. Prior studies have shown that MFCs are capable to remove pollutants from landfill leachate at low energy consumption [9]. Compared with conventional leachate treatments, MFC can achieve the same or even higher removal performance, while generating energy and saving aeration costs [9]. Wu et al. [10] summarized the effects of different feed modes, cell structures and leachate loading rates on the energy recovery efficiency of MFCs, and identified chemicals and leachate characteristics that could potentially improve bioelectrochemical activity and energy production. These include high concentration of nitrogen and electrical conductivity [7], which could improve the electrical performance by reducing the internal resistance. By far, research has been focused on using MFCs to recover bioenergy and value-added products from leachate, but MFC has very limited effect on wastewater treatment. Developing a technology that can remove pollutants and generate energy and simultaneously extract clean water from liquid waste stream will be more competitive than existing wastewater treatment technologies [11]. Forward osmosis (FO) can extract clean water from wastewater, but it only concentrates wastewater without degradation of organic pollutants [12]. The combination of forward osmosis and MFCs can address their inherent problems and achieve synergetic benefits [13].

Zhang et al. [11] first used FO membrane as a separator to construct a new type of MFCs, and found that OsMFC had a higher electricity production than conventional MFCs under sequential batch and continuous operation. Werner et al. [14] constructed an air cathode microbial osmotic fuel cell (MOFC) and observed low internal resistance and high power density. In order to improve the treatment efficiency, Zhang and He [15] coupled an OsMFC with a microbial desalination cell (MDC), and the coupled system significantly improved the desalination efficiency as a combined result of the dilution in the OsMFC and the bioelectrochemical desalination in the MDC. Zhu et al. [16] studied the electrochemical properties of different MFCs with FO membrane, anion exchange membrane (AEM) and cation exchange membrane (CEM) as separators. It was found that the FO-MFC has lower internal resistance and a higher output voltage, probably due to higher salt concentration and higher proton flux. To comprehend the influence of membrane materials on OsMFC performance, Yang et al. [17] compared the performance of OsMFCs with FO membranes consist of polyamide (PA), cellulose triacetate (CTA) nonwoven (NW), and CTA embedded support (ES). The results exhibited that electricity generation performance of OsMFC with a CTA-ES membrane was the best. Wu et al. [18] had observed effects of power generation on RSF (reverse solute flux) of ten inorganic-based DS in OsMFCs. Na<sup>+</sup>-based and K<sup>+</sup>-based DS were considered to be most suitable DS for OsMFC owing to stable power generation and water flux, as well as significant RSF reduction. These studies have added a growing body of knowledge of the fundamentals of OsMFC. However, the applications of OsMFC in leachate treatment is still lacking.

In this work, the effects of three different FO membranes (TFC-ES, CTA-NW and CTA-ES) on OsMFC electricity generation and actual landfill leachate treatment were studied. The reactors were run in two modes: active layer facing feed solution (AL-FS) and active layer facing draw solution (AL-DS). The biomass on OsMFC electrode/membrane surface and in anolyte/catholyte were sampled, and the microbial communities were characterized using 16S rRNA amplicon sequencing. The particular aims of this research were to: (1) demonstrate feasibility of using OsMFC to treat actual landfill leachate; (2) investigate the OsMFCs performance affected by membrane material and membrane orientation; (3) analyze the microbial community at the different locations in the OsMFCs and identify the dominant taxa.

## 2. Materials And Methods

### 2.1. OsMFC set-up

The OsMFCs were made of plexiglass, and the effective volume of the anode and cathode chambers was 125 mL. The two chambers were separated by FO membranes (diameter 0.35 m, effective working area is  $9.6 \times 10^{-4} \text{ m}^2$ ). The anode and cathode electrodes were made of carbon felt (Physicochemical (Hong Kong) Ltd, China), and the projected area of both electrodes is  $8 \text{ cm}^2$  ( $1 \times 8 \text{ cm}$ ). In order to improve electricity production, the cathode carbon felt was heated at 600°C for 4 h before installation. Titanium wire was applied to link the electrodes and the resistance was 200 Ω. The cathode was externally

connected to a 1000 ml beaker for catholyte recirculation with a peristaltic pump (60 ml/min) to maintain the dissolved oxygen concentration. The structure of the OsMFC is shown in Fig. S1.

Anode chambers were inoculated with microorganisms from a MFC that had been running steadily for two years. FO membranes used in this experiment are three commercial membranes of TFC-ES, CTA-NW and CTA-ES (HTI AQP). After enrichment, the anolyte (feed solution) was changed to landfill leachate from a landfill in Songjiang, Shanghai. The characteristics of leachate employed are given in Table 1. NaCl solution (1 mol/L) were employed as the catholyte (draw solution). The OsMFCs were operated under a sequential batch mode. Samples were collected as soon as the cycles ends. Experiments were performed in a climatic cabinet (Shanghai Bielang Instrument Co., LTD) at  $36 \pm 3$  °C.

Table 1  
Water quality indicators of landfill leachate

Parameter	Unit	Conc.
pH	-	$8.35 \pm 0.03$
Conductivity	$\text{mS cm}^{-1}$	$25.40 \pm 0.20$
SS	$\text{mg L}^{-1}$	$896.00 \pm 4.00$
COD	$\text{mg L}^{-1}$	$2638.20 \pm 33.60$
TOC	$\text{mg L}^{-1}$	$716.00 \pm 2.50$
BOD <sub>5</sub>	$\text{mg L}^{-1}$	$790.00 \pm 5.00$
NH <sub>4</sub> <sup>+</sup> -N	$\text{mg L}^{-1}$	$1666.05 \pm 2.50$
TN	$\text{mg L}^{-1}$	$2015.90 \pm 6.44$
TP	$\text{mg L}^{-1}$	$3.27 \pm 0.04$

SS: Suspended solids; COD: Chemical oxygen demand; TOC: Total organic carbon; BOD<sub>5</sub>: Biochemical oxygen demand; NH<sub>4</sub><sup>+</sup>-N: Ammonia nitrogen; TN: Total nitrogen; TP: Total phosphorus.

## 2.2. System perform evaluation

The voltages of the OsMFCs were registered every 2 min via CTA2001A, (Wuhan LAND Electronic Co.Ltd). Both open circuit voltage (OCV) and operating voltage were collected. Current was calculated according to the Ohm's law ( $I = U/R$ , where  $U$  (V) is operating voltage, and  $R$  ( $\Omega$ ) is external resistance) and normalized to anode electrode area ( $I_A = I/A$ , where  $I$  (A) is current, and  $A$  ( $\text{m}^2$ ) is projected area of anode electrode) to obtain current density. Power output was also calculated using the Ohm's law ( $P = UI/A$ ). Polarization curve and the power density curve were measured with the steady-state discharge method. Briefly, the circuit was disconnected and stabilized overnight. The resistance was the decreased consecutively between 10000  $\Omega$  and 20  $\Omega$  with a rheostat (Shanghai Dongmao Electronic Technology

Co., LTD), and the voltages under different resistances were recorded. Total organic carbon (TOC) was gauged by a TOC detector (Vcph, Shimadzu, Japan). Ammonia nitrogen (NH<sub>4</sub><sup>+</sup>-N) was measured by Nessler's reagent spectrophotometry. Total phosphorus (TP) was measured using Molybdenum-antimony spectrophotometry. Total nitrogen (TN) was measured by spectrophotometry method (HJ-636-2012, China).

The mass change of the draw solution was measured with an electronic balance (ME104/02, Shimadzu, Japan) to figure water flux  $J_w$  (L/(m<sup>2</sup>·h)):

$$J_w = \Delta m / (A_m \times \Delta t) \quad (1)$$

Where  $\Delta t$  (h) is the operation time,  $\Delta m$  (g) is increased weight of DS during operation time,  $A_m$  (m<sup>2</sup>) is actual membrane surface area ( $9.616 \times 10^{-4}$  m<sup>2</sup>).

The reverse salt flux  $J_s$  (g/m<sup>2</sup>·h) was figured as below:

$$J_s = (V_t \times C_t - V_0 \times C_0) / (A_m \times \Delta t) \quad (2)$$

Where  $V_0$  (L) is original volume of feed solution,  $V_t$  (L) is final volume of feed solution,  $C_0$  (mg/L) is original salt concentration of feed solution,  $C_t$  (mg/L) is the final salt concentration of feed solution,  $\Delta t$  (h) is operation time,  $A_m$  (m<sup>2</sup>) is effective membrane surface area ( $9.616 \times 10^{-4}$  m<sup>2</sup>).

## 2.3. Microbial analysis

Samples were collected from anode carbon felt, membranes, anolyte and catholyte in the OsMFCs equipped with three different FO membranes (CTA-ES, CTA-NW and TFC-ES). Then, according to the manufacturer's (Shenggong Biotechnology Co., Ltd., Shanghai, China) instructions, DNA was extracted from samples using the Soil DNA kit. The first round of polymerase chain reaction (PCR) amplification was performed using the primers targeting the V3/V4 region of the bacterial 16S rRNA genes: 341F (CCCTACACGACGCTCTTCCGATCTG (barcode) CCTACGGGNGGCWGCAG) and 805R (GACTGGAGTTCCTTGGVACCCGAGAATTCCAGACTACHVGGGTATCTAATCC) [19, 20], followed by a second round of amplification with the same primer pairs. After amplification, gel electrophoresis was performed to detect the amplified products. A magnetic beads (Agencourt AMPure XP) with a volume ratio of 0.6 to the sample was selected for purification and recovery of DNA fragments longer than 400 bp. Using the Qubit 2.0 DNA analysis kit to quantify the concentrations of the recovered amplicon [21]. The amplicon was pooled at 10 ng DNA per sample, resulting in a final sequencing concentration of 20 pmol.

The RDP classifier is used to classify the sequences, classify each sample and each species unit, perform sequence abundance calculation, and construct a sequence abundance matrix of sample and species classification units.

The software used for Alpha diversity analysis is *mothur*, and its indicators include Shannon Index, ACE (Abundance-based Coverage Estimator) Index, Chao1 Index, Coverage, Simpson, etc.

## 3. Results And Discussion

### 3.1. OsMFCs performance with different FO membranes and operation modes

#### 3.1.1. Power generation

**Figure 1A** shows the electricity production of the OsMFCs with three different membranes under AL-FS mode. The voltage of ES-OsMFC remained high throughout the experiment, while that of the NW-OsMFC was high at the beginning, dropped rapidly in a first 2000 hr of operation, and remained relatively stable. In comparison, the voltage of the NW-OsMFC was the lowest. When the reactors reached steady state, the output voltages were 106.9 mV, 108.8 mV, and 153.5 mV for the reactors equipped with TFC-ES, CTA-NW, and CTA-ES, respectively. The high voltage output with the CTA-ES membrane might be due to the high water flux in that OsMFC, which accelerated ion transfer and consequently reduce internal resistance. Although the water flux with the TFC-ES membrane was also high, the growth of the anode bacteria might be limited due to the higher oxygen diffusion [17, 21]. It can be seen from **Fig. 1B** the electricity production of the three OsMFCs under the AL-FS mode was 148.7 mV, 87.4 mV and 79.8 mV, for ES-OsMFC, NW-OsMFC, and TFC-OsMFC, respectively. It was worth noting that the voltages of the NW-OsMFC and TFC-OsMFC under the AL-DS mode were 19.7% and 25.4% lower than those under the AL-FS mode, respectively, which might be due to more serious membrane fouling and faster drop of water flux on AL-DS mode [22].

The polarization curves and power density curves at the initial operation stage were shown in **Fig. 2(A-B)**. Under the AL-FS mode, the open circuit voltages of ES-OsMFC, NW-OsMFC, and TFC-OsMFC were 614.6 mV, 545.7 mV, and 551.8 mV, respectively, which were not significantly different from the open circuit voltage under AL-DS mode (590.7 mV, 548.8 mV, 551.2 mV). According to the slope of polarization curve [16], the internal resistance of ES-OsMFC, NW-OsMFC, and TFC-OsMFC under AL-FS mode were 236.75  $\Omega$ , 392.37  $\Omega$ , and 307.62  $\Omega$ , respectively, which were 28.26%, 22.78% and 20.23% lower than that under AL-DS mode. As a critical parameter in OsMFCs internal resistance is directly linked to power density [23, 24]. The maximum power density of the OsMFCs exhibited a trend in the following order: FS-ES-OsMFC ( $0.44 \text{ W}\cdot\text{m}^{-2}$ ) > FS-TFC-OsMFC ( $0.37 \text{ W}\cdot\text{m}^{-2}$ ) > DS-ES-OsMFC ( $0.33 \text{ W}\cdot\text{m}^{-2}$ ) > DS-TFC-OsMFC ( $0.30 \text{ W}\cdot\text{m}^{-2}$ ) > FS-NW-OsMFC ( $0.28 \text{ W}\cdot\text{m}^{-2}$ ) > DS-NW-OsMFC ( $0.24 \text{ W}\cdot\text{m}^{-2}$ ). The reason why NW-OsMFC generated the lowest current and maximum power density might be that the relatively large structural parameter (S) value led to the increase in mass transfer resistance, which weakened the power generation capacity of the system [17]. To achieve high power generation, FO membranes used in OsMFCs should not only maintain a good mass transfer rate, but also minimize oxygen diffusion, as the intruded oxygen can serve as an alternative electron acceptor to the anode bacteria and short-circuit the system.

## 3.1.2. Reverse salt flux and water flux

Reverse salt flux and water flux of reactor were also important indicators to evaluate the OsMFC performance. Figure 3 shows the reverse salt flux and water flux of three OsMFCs. Under the AL-FS mode, the order of reverse salt flux and water flux of the membranes were: CTA-ES (3.68 gMH) > TFC-ES (3.37 gMH) > CTA-NW (3.01 gMH), and CTA-ES (0.98 LMH) > TFC-ES (0.79 LMH) > CTA-NW (0.56 LMH), respectively. The ratios between water flux and reverse salt flux were thus  $0.27 \text{ L}\cdot\text{g}^{-1}$ ,  $0.18 \text{ L}\cdot\text{g}^{-1}$  and  $0.23 \text{ L}\cdot\text{g}^{-1}$ , respectively. Under the AL-DS mode, the order of reverse salt flux and water flux of membranes were: CTA-ES (4.28 gMH) > TFC-ES (4.28 gMH) > CTA-NW (4.25 gMH), and CTA-ES (1.02 LMH) > TFC-ES (0.84 LMH) > CTA-NW (0.71 LMH). The ratios between water flux and reverse salt flux were  $0.24 \text{ L}\cdot\text{g}^{-1}$ ,  $0.17 \text{ L}\cdot\text{g}^{-1}$  and  $0.20 \text{ L}\cdot\text{g}^{-1}$ , respectively. The reverse salt flux and water flux under the AL-FS mode were both smaller than that under the AL-DS mode, and CTA-ES in those two modes showed better performance than the other two membranes, which was consistent with the previous results (**Figs. 1 and 2**). Under AL-FS mode, draw side was diluted with the formation of internal concentration polarization (ICP), then reduced osmotic pressure difference in two sides of membrane. In the meantime, draw solute entered the membrane through the porous support layer, increasing the resistance over the membrane, which might be the reason for this difference [25]. However, microorganisms and macromolecular organic substances in the anolyte might block porous support layer, thus increasing membrane resistance. Therefore, the difference of water flux on AL-DS and AL-FS mode was not particularly significant.

## 3.1.3. Pollutant removal performance

In **Fig. 4**, the removal of TOC,  $\text{NH}_4^+\text{-N}$ , total nitrogen and TP by three OsMFCs under the two modes was very similar, with no obvious difference. All OsMFCs had a removal efficiency of more than 70% for TOC and total nitrogen, and more than 85% for TP. Once active layer of membrane faced anolyte (AL-FS mode), some of microorganisms in the anolyte deposited on the membrane surface, causing membrane clogging and thereby affecting the contaminant removal [26]. In AL-DS mode, the effective mass transfer driving force was large [27], and the pollutants formed a higher concentration gradient in support layer under concentrated concentration polarization [28], so that more pollutants reached the cathode. Therefore, the removal efficiencies of the OsMFCs under the two modes were similar in this experiment. However, the removal of ammonia nitrogen was not as efficient. Among the OsMFCs, DS-NW-OsMFC had the lowest removal efficiency for ammonia nitrogen, which was only  $52.43 \pm 0.41\%$ . In contrast, the OsMFCs under the AL-FS mode showed higher removal efficiencies for ammonia nitrogen than under the AL-DS mode. FS-ES-OsMFC achieved the highest ammonia nitrogen removal of  $70.12 \pm 0.28\%$ . It has been reported that, to maintain charge balance,  $\text{NH}_4^+\text{-N}$  in the anolyte migrates into the catholyte when  $\text{Na}^+$  diffused into the anolyte [29, 30]. In OsMFCs, the FO membrane surface carried more negative charge, which led to an increase in the bidirectional diffusion of  $\text{NH}_4^+$  and  $\text{Na}^+$  [31]. This might be the reason why OsMFCs were inefficient in removing ammonia nitrogen. Overall, the removal of various

pollutants in landfill leachate was satisfactory compared with that in the published literature [32], which proved that OsMFCs is a promising technology for landfill leachate treatment.

## 3.2. Microbial community structure on different FO membranes

### 3.2.1. Microbial diversity

The abundance and diversity of bacterial community could be revealed through diversity analysis. Table 2 listed the Alpha diversity indices of the microbial communities in the three OsMFCs. The ACE and Chao1 were indices that estimate number of operational taxonomic units (OTUs) in a community and were commonly used to estimate the total number of species. Table 2 showed that both the ACE index and the Chao1 index follow the same order: ES-OsMFC > NW-OsMFC > TFC-OsMFC. The Shannon and Simpson index are used to estimate the microbial diversity in a sample: a high diversity is reflected by a high Shannon index and a low Simpson index. As shown in Table 2, the ranking of the Shannon index was NW-OsMFC (5.09) > ES-OsMFC (4.73) > TFC-OsMFC (4.35). Correspondingly, the order of the Simpson index was NW-OsMFC (0.02) < ES-OsMFC (0.03) < TFC-OsMFC (0.05). Both indices indicated a highly diverse microbial community on the NW membrane. The diversity analysis results are reliable as indicated by the high coverage index of 0.99 for the three OsMFCs [33]. The rarefaction curve (Fig. S2) also indicates that NW-OsMFC had the highest number of microbial species, while TFC-OsMFC had the lowest number of species.

Table 2  
Species diversity of microbial communities on different membranes

Sample-ID	Seq-num	OTU	ACE	Chao1	Shannon	Simpson	Coverage
NW-OsMFC	62582	1526	1905.85	1822.93	5.09	0.02	0.99
ES-OsMFC	75625	1516	1909.36	1865.47	4.73	0.03	0.99
TFC-OsMFC	47491	1126	1527.06	1473.72	4.35	0.05	0.99

### 3.2.2. Microbial community composition

At the genus level, the community structure on the different membranes was similar, but the abundance of the genus was different (Fig. 5A). Genera belonging to *Proteobacteria* (*Pseudomonas*, *Thiopseudomonas*, *Marinobacterium*, *Arcobacter*, *Sulfurospirillum*, *Rhodopseudomonas*, *Desulfobulbus*, *Pusillimonas*, *Advenella*), *Firmicutes* (*Saccharofermentans* and *Tissierella*), *Bacteroidetes* (*Proteiniphilum*), and *Synergistetes* (*Aminobacterium*) were the dominant taxa on the membrane surface.

*Proteobacteria* is mostly anaerobic or facultative anaerobic gram-negative bacteria. It was widely distributed on the membrane surface, and the percentages in ES-OsMFC, NW-OsMFC and TFC-OsMFC were 40.11%, 47.21% and 68.11%, respectively. Many studies had shown that *Proteobacteria* exists extensively in MFC anodes [34–36], thus key genera are discussed in details below.

*Pseudomonas* is a heterotrophic bacterium under the  $\gamma$ -*proteobacteria* class, which uses organic matter as a energy source for anaerobic respiration [37]. *Pseudomonas* accounted for 6%, 13.56%, and 20.55% in the NW-OsMFC, ES-OsMFC, and TFC-OsMFC, respectively, and thus was speculated to be the major electroactive bacteria in the OsMFCs. It could also be seen from **Fig. S3** that *Pseudomonas* was most abundant on the three membranes. Pham et al. [38] found that *Pseudomonas* produced phenazine compounds for electron shuttling and improved MFC performance in mixed cultures. The abundance of *Marinobacterium* in the TFC-OsMFC (4.42%) was relatively higher than in the NW-OsMFC (1.14%) and ES-OsMFC (2.04%). *Marinobacterium* has been reported to be halophiles [39, 40]. Because the catholyte was 1 mol/L NaCl, the forward osmosis would cause reversely transported salts. The landfill leachate also contained a certain salinity, resulting in high salinity of the anolyte. *Arcobacter* belongs to the  $\epsilon$ -*proteobacteria* class whose bioelectrochemical activity has been reported [41, 42]. The percentage of *Arcobacter* in ES-OsMFC (9.54%) was higher than in NW-OsMFC (6.01%) and TFC-OsMFC (0.35%). This might be one of the reasons why ES-OsMFC had a better power generation effect (**Fig. 2**). Fedorovich et al. [43] found that *Arcobacter butzleri* ED-1 was an electrogenic microorganism that could efficiently use acetate as a carbon source. Due to the presence of *Saccharofermentans* in OsMFCs, the organic matter is degraded into acetic acid, which leads to better growth of *Arcobacter*. *Rhodopseudomonas* belongs to the  $\alpha$ -*proteobacteria* class, is a Gram-negative bacterium, which secretes a phenolic electron mediator with weak electrical energy and uses various carbon as an energy source to generate electricity [43–47]. *Rhodopseudomonas* in NW-OsMFC, ES-OsMFC and TFC-OsMFC were 3.8%, 4.43% and 2.86%, respectively. *Thiopseudomonas* as a denitrifying bacteria [45] showed a percentage of 1.58%, 1.57% and 10.05% in NW-OsMFC, ES-OsMFC and TFC-OsMFC, respectively.

*Firmicutes* have been reported to utilize complex organic matter to produce electricity [48]. The abundance of *Firmicutes* in the ES-OsMFC, NW-OsMFC and TFC-OsMFC were 28.85%, 24.23% and 11.80%, respectively, probably due to the presence of complex high organic in landfill leachate. In this phylum, *Saccharofermentans* are known to perform hydrolysis, fermentation, and acetogenesis [49]. Its abundance in NW-OsMFC, ES-OsMFC and TFC-OsMFC were 3.34%, 3.58% and 2.24%, respectively.

*Pseudomonas* [50], *Arcobacter* [51] and *Rhodopseudomonas* [52] are commonly found in bioelectrochemical systems and are speculated to be the main electrogenic bacteria in the OsMFCs. However, some well-known electroactive microorganisms (e.g., *Anaeromusa* [53], *Dechloromonas*, *Geobacter* [54], and etc.) were been found in this study, probably because the salt in the catholyte passed through the membranes and caused high anode salinity. In addition, landfill leachate as an anode substrate has a complex composition and high toxicity that may be inhibitory to those microorganisms.

## **3.3. Microbial community structure at different OsMFCs sites**

### **3.3.1. Microbial diversity**

It can be seen from Table 3 that the ACE index and Chao1 index are the highest in the anolyte (1928.77, 1875.12) compared to the TFC-ES membrane (1527.06, 1473.72), anode carbon felt (1579.99, 1513.01) and catholyte (222.52, 208.63). Similarly, the anolyte sample showed the highest Shannon index and the lowest Simpson index, suggesting that the anolyte community had high richness and diversity [55]. The same result could also be proven in the rarefaction curves (**Fig. S4**). As shown in Table 3, the coverage index of the four samples indicated that the sequencing results has captured the dominant taxa in the communities.

Table 3  
Species diversity of microbial communities on different OsMFCs sites

Sample-ID	Seq-num	OTU	ACE	Chao1	Shannon	Simpson	Coverage
Membrane	47491	1126	1527.06	1473.72	4.35	0.05	0.99
Electrode	63407	1241	1579.99	1513.01	4.74	0.03	0.99
Anolyte	64396	1536	1928.77	1875.12	5.09	0.02	0.99
Catholyte	64566	200	222.52	208.63	1.69	0.28	1.00

### 3.3.2. Microbial community composition

As shown in **Fig. 5B**, there were some differences in community structure for four samples. *Aliidiomarina*, *Halomonas*, *Pseudomonas*, *Rhodopseudomonas*, *Methylophaga*, *Thiopseudomonas*, *Marinobacterium*, *Desulfuromonas* (these genus belong to *Proteobacteria* phylum), *Saccharofermentans*, *Tissierella*, *Sporanaerobacter* (belong to the *Firmicutes* phylum) were the dominant species of four samples.

The *Proteobacteria* phylum was gain dominant in the communities, and the abundance of *Proteobacteria* on the TFC-ES membrane, anode carbon felt, in the anolyte, and catholyte were 68.11%, 36.02%, 36.52%, and 97.62%, respectively. *Aliidiomarina* was found to be significantly enriched in the catholyte with an abundance of 40.59% but not at other locations. This result was the same as shown in **Fig. S5**. *Halomonas*, a rod-shaped gram-negative bacteria that can survive in saline environments [56], was also abundant with 31.16% only in the catholyte. *Methylophaga* as an aerobic Gram-negative moderate halophilic genus that utilizes a single carbon sugar in the ribulose monophosphate pathway as a carbon source showed a high abundance of 14.97% in the catholyte [57]. The predominance of those taxa was correlated with the higher salinity in catholyte.

The abundance of *Pseudomonas* detected on the TFC-ES membrane, anode carbon felt, in the anolyte, and catholyte samples were 20.55%, 1.87%, 7.88% and 0.58%. A small amount of *Pseudomonas* was also found in the catholyte, probably because a part of the microorganisms permeated into the catholyte during the operation. The abundance of *Rhodopseudomonas* genus on the TFC-ES membrane, anode carbon felt, in the anolyte were 2.86%, 13.35%, 6.64%, respectively. The high abundance of *Rhodopseudomonas* on the carbon felt reflected its electroactive nature. *Desulfuromonas* can grow

through oxidizing acetate and reducing elemental sulfur [58]. The abundance of this taxa was as high as 5.11% on the carbon but low in membrane (0.11%) and anolyte (0.68%) and not detected in catholyte. Thiopseudomonas was observed relatively abundant on the carbon felt (1.32%) and in the anolyte (3.04%).

## 4. Conclusions

The ES-OsMFC showed the highest electricity production and most efficient pollutant removal under both operation modes. Under the AL-FS mode, ES-OsMFC achieved the highest power output of  $0.44\text{W}\cdot\text{m}^{-2}$  with  $76.63 \pm 0.28\%$  TOC removal, higher than the  $0.33\text{W}\cdot\text{m}^{-2}$  and  $74.06 \pm 0.28\%$  under the AL-DS mode. Sequencing analyses revealed that the ES-OsMFC had the highest microbial enrichment on the membrane, which might explain the satisfactory performance of the ES-OsMFC. *Pseudomonas* was the most abundant taxa on the membranes, and *Rhodopseudomonas* was the most abundant taxa on the carbon felt, both of which were likely to be the key electrogenic bacteria in the OsMFCs.

### Declarations

## Declarations

## Ethics approval and consent to participate

Not applicable

### Consent for publication

Not applicable

### Availability of data and materials

All data generated or analysed during this study are included in this published article and its supplementary information files.

### Competing interests

The authors declare that they have no competing interests in this section.

## Funding

Not Applicable

## Authors' contributions

Nan Jiang and Li Huang have conducted the experimental studies on osmotic microbial fuel cells for the treatment of Landfill leachate. Teng Cai and Jialing Song have supervised towards the experimental work on power generation and performance studies. Manhong Huang has expressed her suggestions and ideas on the chemical analysis and characteristics of the OsMFC. Shengyang Zheng, Jili Guo and Zhuang Kong helped revise the manuscript. All authors read and approved the final manuscript.

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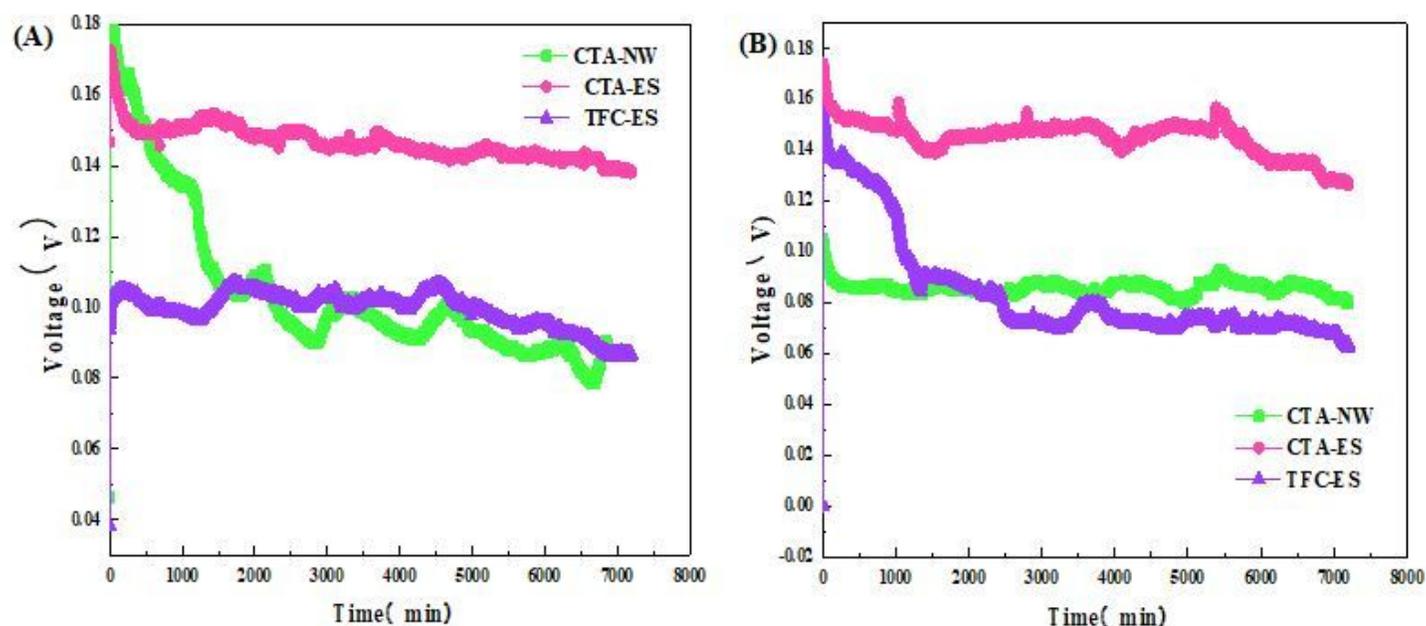
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## Figures



**Figure 1**

Voltage outputs versus operation time for OsMFCs fed with leachates under AL-FS mode(A), AL-DS mode(B)

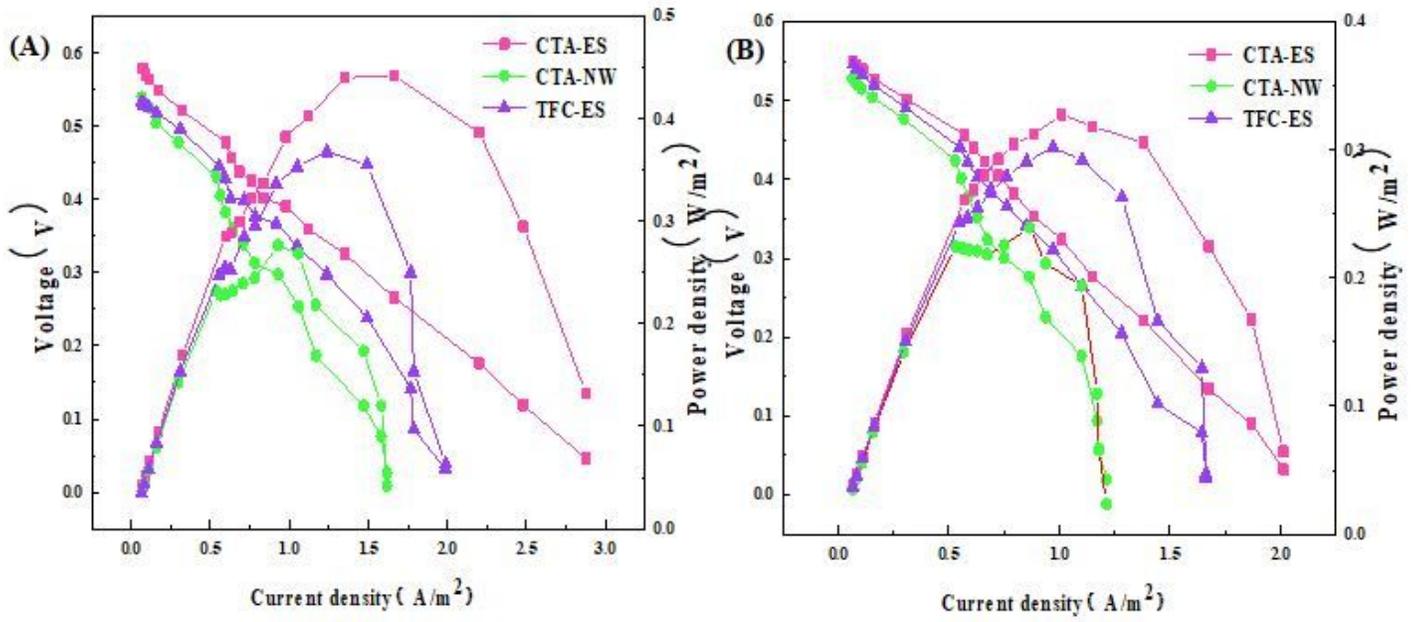


Figure 2

The power density curves and polarization curves of OsMFCs under AL-FS mode (A), AL-DS mode (B)

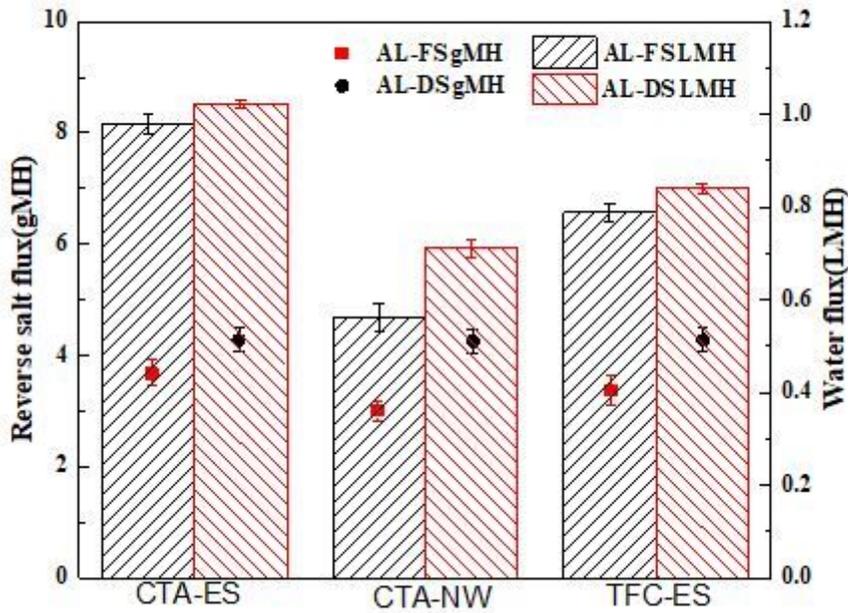
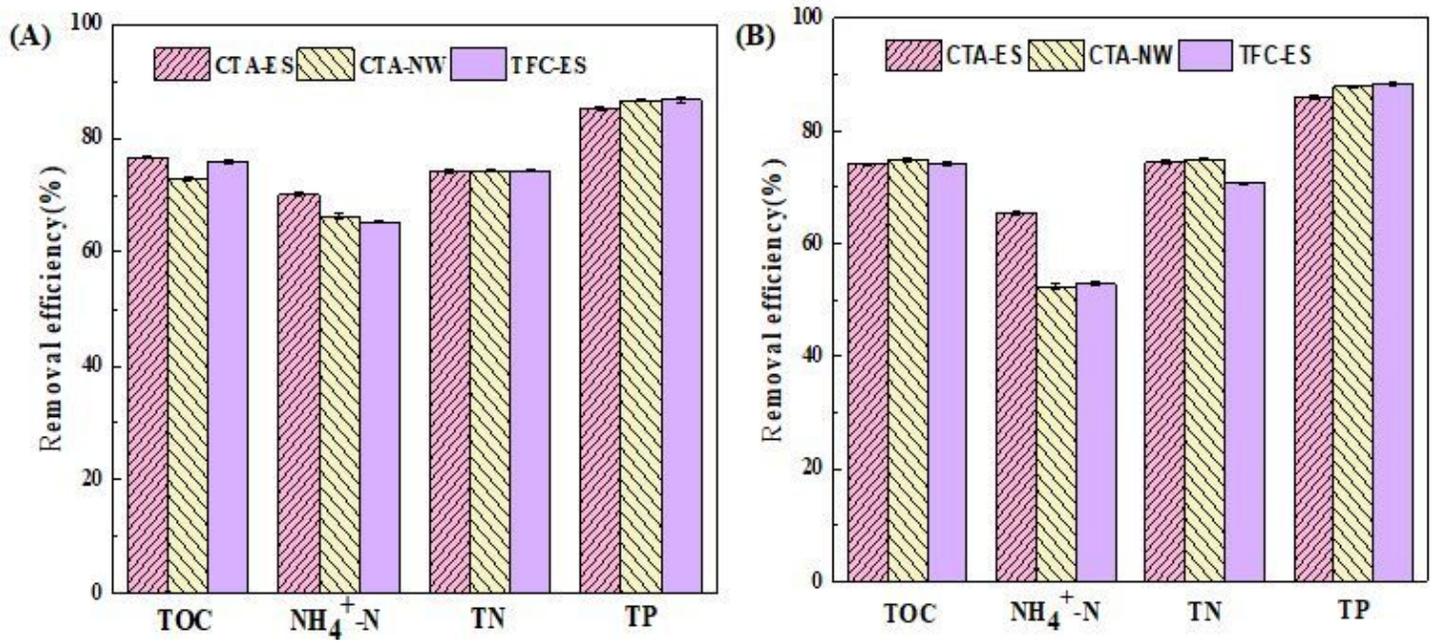


Figure 3

Water flux and reverse salt flux for OsMFCs under both modes



**Figure 4**

The removal efficiencies after treatment for OsMFC with different FO membrane in AL-FS mode (A), AL-DS mode (B)

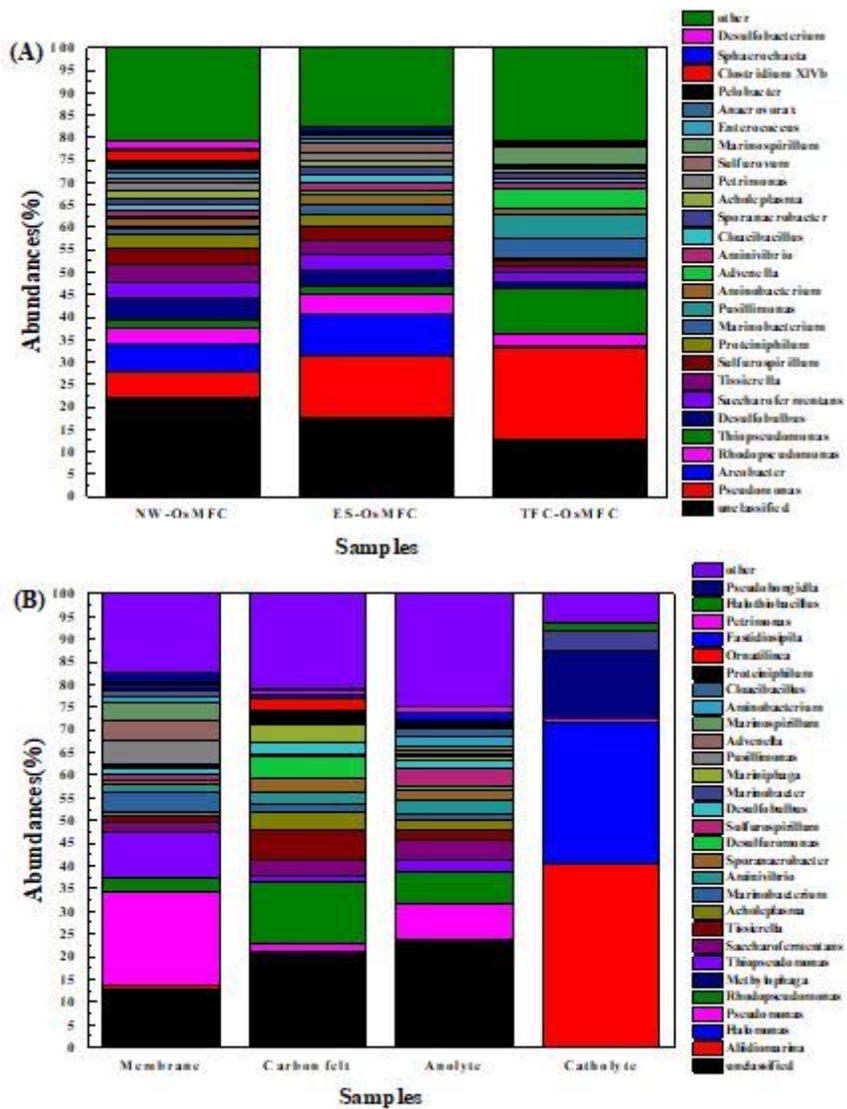


Figure 5

Distribution of microorganisms in each sample of different OsMFCs (A), different site (B) at Genus level

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