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A Numerical Study on the Effect of CO₂ Addition for Methane Explosion Reaction Kinetics in Confined Space

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Abstract

To explore the influence of the CO₂ volume fraction on methane explosion in a confined space over wide equivalent ratios, the explosion temperature, the explosion pressure, the concentration of the important free radicals, and the concentration of the disastrous gas generated after the explosion in a confined space were studied. Meanwhile, the elementary reaction steps dominating the gas explosion were identified through the sensitivity analysis. With the increase of the CO₂ volume fraction, the explosion time prolongs, and the explosion pressure and temperature decrease monotonously. Moreover, the concentrations of the investigated free radicals also decrease as the increase of the CO₂ volume fraction. For the disastrous gas, the concentration of the gas product CO increases and the concentrations of CO₂, NO, and NO₂ decrease as the volume fraction of CO₂ increases. When 7% methane is added with 10% CO₂, the increase rate of CO is 76%, and the decrease rates of CO₂, NO, and NO₂ are 27%, 37%, and 39%, respectively. If the volume fraction of CO₂ is constant, the larger the volume fraction of methane in the blend gas, the greater the mole fraction of radical H and the lower the mole fraction of radical O. For radical OH, its mole fraction first increases, and then decreases with the location of peak value of 9.5%, while the CO concentration increases with the increase of the methane concentration. For all the investigated volume fraction of methane, the addition of CO₂ reduces the sensitivity coefficients of each key elementary reaction step, and the sensitivity coefficient of reaction promoting methane consumption decreases faster than that of the reaction inhibit methane consumption, which indicates that the addition of CO₂ effectively suppresses the methane explosion.

Keywords: confined space; methane explosion; carbon dioxide; free radicals; sensitivity analysis

1. Introduction

Mine gas explosion accidents are one of the biggest factors, which endangers the safe production in coal mines. These accidents cause serious economic losses and casualties¹. In recent

years, with the continuous increase in coal production, the gas explosion accidents have occurred frequently^{2,3}.

To prevent the occurrence of gas explosions, many relevant researches had been conducted in the field of inert gas explosion suppression. In terms of the explosion suppression experiments, Lu et al. designed a device that can automatically eject nitrogen during the explosion process. The effects of injection pressure, injection timing, and nozzle arrangement on the explosion suppression function were studied. The results showed that successful explosion suppression can be achieved when the nitrogen pressure reaches or exceeds 0.3 MPa^{4,5}. Cao et al. studied the suppression effect of ultrafine mist on methane/air explosions. With the increase of ultrafine water/NaCl solution mist, the flame propagation speed, the maximum explosion overpressure, and the maximum pressure rising rate descended⁶⁻⁸. Based on the eddy dissipation concept combustion model, Wang et al. studied the mechanism and effect of ultrasonic water mist on suppressing gas explosion through experiments and EDC(Eddy-Dissipation Concept) combustion model⁹. Liang et al. investigated the influence of the nitrogen fraction in the blend of on the unstretched laminar flame propagation velocity, unstretched laminar combustion velocity, Markstein length, flame stability, and maximum combustion pressure. It was found that above parameters decrease distinctly with the increase of nitrogen fraction in the gas mixture¹⁰. Qian et al. obtained a fitting formula through experiments under different conditions, which can predict the explosion limit of methane at any ratio of N₂ to CO₂. They reported that the limit oxygen volume fraction decreases linearly with the increase in N₂ content in the mixture¹¹. Furthermore, some researches had been carried out to research the inhibition effect of N₂, CO₂ and N₂/CO₂ mixture on gas explosion, it was found that both N₂ and CO₂ can inhibit the gas explosion, and the inhibition effect on high concentration gas is better. At the same time, the higher the volume fraction of CO₂ in the mixed gas, the better the inhibition effect¹²⁻¹⁵. The above researches show that the inert gas can inhibit the explosion, to deeply understand the behavior, many simulation works are performed.

Luo et al. used the (DFT) B3LYP/6—31G methods of density functional theory and the GRI-Mech 3.0 to analyze the related elementary reactions. The results indicated that the NH₃ could achieve explosion suppression by competing the free radicals H and OH, and the reactant of O₂ with CH₄^{16,17}. Liang et al. and Wang et al. found that the increase of the water content in the mixed gas

can promote the generation of CO₂ but reduce the intensity of the gas explosion, and inhibits the generation of harmful gases, such as CO, NO, and NO₂^{18,19}.

Lu et al. suggested that the H₂O acts as the third body in the explosion process, which directly participated in the ternary collision reaction existing in the form of inert molecules. It would collide with the free radicals and the free atoms to destroy the chain carrier, which reduces the concentration of active centers in the chain reaction, and achieve the explosion suppression²⁰. Ren et al. modified the reaction mechanism of GRI-Mech 3.0 by assuming that the N₂, CO₂, and H₂O only participated in the inhibition process as the third body. The physical and chemical effects of the three inert gases on the laminar combustion velocity, adiabatic flame temperature, and net heat release rate under different methane equivalence ratios ($\Phi=0.8, 1.0$ and 1.2) were analyzed²¹. Jia et al. indicated that the N₂, CO₂, and H₂O reduced the sensitivity of the elementary reaction steps dominating the gas explosions and the inhibition effect of CO₂ and H₂O were better than that of the N₂^{1,2,22}. Li et al. pointed out that the addition of N₂, CO₂, and H₂O would strongly inhibit the generation of free radicals CH₃ and HCO. The inhibitory effect of CO₂ and H₂O is not only from their participation in the three-body collision reaction, but also from their participation in another chain reactions^{23,24}.

Though a number of experiments and simulation had been performed to investigate the suppression effect of inert gas on methane explosion, most of the previous studies focused only on the independent influences of different volume fractions of inert gas on methane explosion mechanism under stoichiometric ratio condition. Because the working condition of coal mine is complicated, and the inhibition effect may be different in different conditions. However, the influence of inert gases with different volume fractions on explosions over wide methane equivalence ratios has not been reported. Therefore, the influence of the CO₂ volume fraction on methane explosion in confined space under different methane equivalent ratios is investigated in the study to provide a theoretical basis for the improvement of the inert gas explosion suppression mechanism.

2. Mathematical model

2.1. Governing equation

The composition equation is as follows.

$$\frac{dY_i}{dt} = \nu w_i M_i \quad (i = 1, 2, \dots, k_g) \quad (1)$$

$$\dot{w}_i = \sum_{k=1}^{N_g} \nu_{ik} K_{fk} \prod_{j=1}^{k_g} [X_j]^{\nu_{jk}} \quad (j = 1, 2, \dots, k_g) \quad (2)$$

$$K_{fk} = A_k T^{b_k} \exp\left[\frac{-E_k}{RT}\right] \quad (k = 1, 2, \dots, N_g) \quad (3)$$

where Y_i , w_i , and M_i denote the mass fraction, chemical reaction rate, and molecular weight of the substance i , respectively, t is the time, ν , R , and T represent the specific heat capacity, gas constant, and temperature of the mixture, respectively, and N_g and k_g are the total number of reaction steps and groups, respectively. The total number of points is the reverse stoichiometric coefficient, forward stoichiometric coefficient, and the difference between the forward and reverse stoichiometric coefficients of substance i in elementary reaction k . Here, K_{fk} is the rate constant of the positive reaction in the elementary reaction j , $[X_j]$ is the molar concentration of component j , and A_k , b_k , and E_{ak} are the pre-exponential factors, temperature index, and reaction activation energy of the elementary reaction k , respectively.

The energy equation is

$$c_v \frac{dT}{dt} + V \sum_{i=1}^{k_g} e_i \dot{w}_i M_i = 0 \quad (4)$$

where c_v is the constant volume specific heat of the mixed gas, and e_i is the internal energy of component i .

2.2. Sensitivity analysis

Sensitivity analysis is a method to determine the sensitivity factors that have an important impact on the overall response from multiple uncertain factors²⁵.

Assuming a variable, it is expressed as

$$\frac{dZ}{dt} = F(Z, t, a) \quad (5)$$

where $Z = (Y_1, Y_2, \dots, Y_{k_g})^t$ is the mass fraction of each component, and $a = (A_1, A_2, \dots, A_{N_g})$ is the prefactor of each elementary reaction.

$$w_{l,i} = \frac{\partial Z_l}{\partial a_i} \quad (6)$$

where $w_{l,i}$ is the sensitivity coefficient, Z_l is the variable number l , and a_i is the preference factor of the reactions i .

As the derivation of Equation (6), one obtains

$$\frac{dw_{l,i}}{dt} = \frac{\partial F_l}{\partial Z} w_{l,i} + \frac{\partial F_l}{\partial a_i} \quad (7)$$

2.3 Reaction mechanism

The total chemical reaction formula of gas explosion is $\text{CH}_4 + 2(\text{O}_2 + 3.76\text{N}_2) \rightarrow \text{CO}_2 + 2\text{H}_2\text{O} + 7.52\text{N}_2 + 882.6\text{kJ/mol}$, GRI-Mech 3.0 is selected as the chemical reaction mechanism of methane combustion, the mechanism includes 53 species and 325 elementary reactions²⁶. Table 1 shows some key elementary reaction steps in the detailed mechanism of gas explosion chain reaction.

Table 1. Main reactions affecting the change of free radicals.

Reaction step	Elementary reaction
R32	$\text{O}_2 + \text{CH}_2\text{O} \rightleftharpoons \text{HO}_2 + \text{HCO}$
R38	$\text{H} + \text{O}_2 \rightleftharpoons \text{O} + \text{OH}$
R52	$\text{H} + \text{CH}_3(+\text{M}) \rightleftharpoons \text{CH}_4(+\text{M})$
R53	$\text{H} + \text{CH}_4 \rightleftharpoons \text{CH}_3 + \text{H}_2$
R57	$\text{H} + \text{CH}_2\text{O}(+\text{M}) \rightleftharpoons \text{CH}_3\text{O}(+\text{M})$
R98	$\text{OH} + \text{CH}_4 \rightleftharpoons \text{CH}_3 + \text{H}_2\text{O}$
R118	$\text{HO}_2 + \text{CH}_3 \rightleftharpoons \text{O}_2 + \text{CH}_4$
R119	$\text{HO}_2 + \text{CH}_3 \rightleftharpoons \text{OH} + \text{CH}_3\text{O}$
R155	$\text{CH}_3 + \text{O}_2 \rightleftharpoons \text{O} + \text{CH}_3\text{O}$
R156	$\text{CH}_3 + \text{O}_2 \rightleftharpoons \text{OH} + \text{CH}_2\text{O}$
R157	$\text{CH}_3 + \text{H}_2\text{O}_2 \rightleftharpoons \text{HO}_2 + \text{CH}_4$
R158	$2\text{CH}_3(+\text{M}) \rightleftharpoons \text{C}_2\text{H}_6(+\text{M})$
R161	$\text{CH}_3 + \text{CH}_2\text{O} \rightleftharpoons \text{HCO} + \text{CH}_4$
R170	$\text{CH}_3\text{O} + \text{O}_2 \rightleftharpoons \text{HO}_2 + \text{CH}_2\text{O}$

2.3. Simulation condition

To reveal the effect of carbon dioxide on the kinetic characteristics of the methane explosion over wide methane equivalent ratios, the explosion of different methane concentrations within the explosion limit was simulated by using a higher initial temperature instead of the high-temperature heat source ($>650^\circ\text{C}$)²⁷. In the present study, the methane explosion is simulated with the constant volume combustion bomb model, with the initial temperature of 1300 K, the initial pressure of 1 atm, and the reaction time of 0.02 s. The specific working conditions are presented in Table 2.

Table 2. Initial working conditions of methane explosion.

7 vol% CH_4 ($\varphi=0.72$)			9.5 vol% CH_4 ($\varphi=1$)			11 vol% CH_4 ($\varphi=1.18$)		
CO_2	O_2	N_2	CO_2	O_2	N_2	CO_2	O_2	N_2
0	19.53	73.47	0	19.005	71.495	0	18.69	70.31
2	19.11	71.89	2	18.585	69.915	2	18.27	68.73
4	18.69	70.31	4	18.165	68.335	4	17.85	67.15
6	18.27	68.73	6	17.745	66.755	6	17.43	65.57

8	17.85	67.15	8	17.325	65.175	8	17.01	63.99
10	17.43	65.57	10	16.905	63.595	10	16.59	62.41

3. Calculation results and analysis

3.1. Pressure and temperature

The variations of the pressure and temperature during the explosion process of 7% CH₄–air with different CO₂ additions are plotted in Figure 1. With the increase of the CO₂ volume fraction, the explosion time prolongs and the explosion pressure and temperature decrease monotonously. When the volume fraction of CO₂ increases from 0% to 10%, The maximum gas explosion pressure decreases from 2.12 MPa to 2.04 MPa with the decrease rates of 3.77%. The maximum temperature decreases from 2702.882K to 2591 K with the decline rates of 4.14%. These results indicate that the increase of the volume fraction of CO₂ would suppress the gas explosions.

Figure 1. Variation of explosion pressure and temperature with time under different CO₂ volume fractions at 7% CH₄: (a) explosion pressure and (b) explosion temperature.

Figure 2 further displays the influence of the CO₂ volume fraction on the maximum explosion pressure and explosion temperature with different methane volume fraction. As seen, the maximum explosion pressure and explosion temperature decrease with the increase of the CO₂ volume fraction under all the methane volume fraction. The larger the methane volume fraction, the greater the maximum explosion pressure decrease, and the better the suppression effect on the methane explosion. When the volume fraction of methane is 7%, 9.5%, 11%, the maximum explosion pressure of adding 10% CO₂ is reduced by 3.9% compared with the case with no addition in Figure 2(a). As Figure 2(b) shows, for methane with a volume fraction of 11%, the explosion temperature is more sensitive to changes in the CO₂ volume fraction than for 7% and 9.5% volume fractions. When

the volume fraction of methane is 7%, 9.5%, 11%, the explosion temperature of the addition of 10% CO_2 decreases by 4.2%, 5.3%, 6.2% compared with the case with no addition. The results indicate that the inhibitory effect of CO_2 addition on the methane explosions increases as the increase of the methane concentration.

Figure 2. Variation of explosion pressure and temperature with CO_2 volume fraction under different methane volume fractions: (a) explosion pressure and (b) explosion temperature.

3.2. Free radicals

The essence of gas explosion is a complex thermal chain reaction. When the mixed gas absorbs enough energy, the molecular chain breaks. Then, the number of free radicals H, O, and OH begin to rise sharply to form chemical reaction active center with high concentration of free radicals, which leads to the explosion. As shown in Figure 3, when the volume fraction of methane is 7% with no CO_2 addition, the maximum mole fraction of the free radicals H, O, and OH are 0.013, 0.016, and 0.021, respectively. Because the addition of CO_2 increases the probability of free radicals collision with the third body to form low-activity stable molecules, as the increase of the CO_2 volume fraction, the location of peak concentration of free radicals prolongs and the peak concentrations of the free radicals H, O, and OH decrease.

Figure 4 shows the effect of CO_2 addition on the peak concentration of radical H, O, and OH over $\phi=0.72, 1, 1.18$. It can be found that the CO_2 addition reduces the peak concentration of all the investigated radicals. The greater the methane volume fraction, the greater the decrease rate of radicals H and OH, and the smaller the decrease rate of radical O. When the volume fraction of CO_2 is constant, the increase of the volume fraction of methane leads to the increase of the maximum

mole fraction of radical $H\cdot$ and the decrease of the maximum mole fraction of radical O . For radical OH , its maximum mole fraction first increases and then decreases with the location of peak value of 9.5%. The larger the equivalence ratio of CH_4 , the less O_2 in the mixture, which increases the number of CH_4 molecules and decreases the number of O_2 molecules in the unit volume of the reactant. The concentration of radical H increases, and the concentration of radical O decreases. At the same time, with the increase of CH_4 concentration, the elementary reaction step R52: $H+CH_3(+M) \rightleftharpoons CH_4(+M)$, R11: $O+CH_4 \rightleftharpoons OH+CH_3$ tend to promote the consumption of CH_4 . It also explains the appearance of Figure 2.

Figure 3. Variation of free radicals concentration with time under different CO_2 concentrations at 7% CH_4 : (a) free radical H , (b) free radical O , and (c) free radical OH .

Figure 4. Variation of maximum mole fraction of free radicals with CO_2 volume fraction under different methane volume fractions: (a) free radical H , (b) free radical O , and (c) free radical OH .

3.3. Gas products

The disastrous gases, such as CO , CO_2 , NO , NO_2 , produced in the gas explosions process are the major cause of casualties²⁸. After adding CO_2 , the change of the mole fraction of disastrous gas with 7% CH_4 -air is shown in Figure 5.

As seen, with the increase of the CO_2 volume fraction, the mole fraction of CO is increased, whereas the mole fractions of CO_2 , NO , and NO_2 are decreased. This is caused by elementary reaction R31: $O_2+CO \rightleftharpoons O+CO_2$, R99: $OH+CO \rightleftharpoons H+CO_2$, R120: $HO_2+CO \rightleftharpoons OH+CO_2$, R132:

$\text{CH} + \text{CO}_2 \rightleftharpoons \text{HCO} + \text{CO}$, R153: $\text{CH}_2(\text{S}) + \text{CO}_2 \rightleftharpoons \text{CO} + \text{CH}_2\text{O}$. When CO_2 is added to the gas mixture, the initial concentration of CO_2 in the gas mixture increases, which causes the above reaction is easier to happen toward to the direction of CO_2 consumption, which results in a large amount of CO . Figure 5(a) reveals that the mole fraction of CO reaches its peak first, then it reacts with the excess oxygen to form CO_2 , and eventually tends to a stable value. Under working condition 1, after gas explosion, the mole fractions of CO , CO_2 , NO , and NO_2 are 0.0159, 0.0527, 0.0150, and 7.94×10^{-6} , respectively. Under working condition 6, after gas explosion, the mole fractions of CO , CO_2 , NO , and NO_2 are 0.0281, 0.0382, 0.0094, and 4.84×10^{-6} . the increase rate of CO is 76%, and the decrease rates of CO_2 , NO , and NO_2 are 27%, 37%, and 39%.

Figure 5. Variation of product concentration of some gases with time under different CO_2 volume fractions at 7% CH_4 : (a) CO , (b) CO_2 , (c) NO , and (d) NO_2 .

Table 3 lists the effect of CO_2 addition on the concentration of the disastrous gas under different methane volume fractions. It shows that, $\phi=0.72, 1, 1.18$, with the increase of the CO_2 volume fraction, the mole fraction of CO is increased, and the mole fractions of CO_2 , NO , and NO_2 are decreased accordingly in all the investigated conditions. When the volume fraction of CO_2 is constant, with the increase in methane volume fraction, the volume fractions of CO is increased, and

the volume fractions of CO₂, NO, and NO₂ are decreased. The above results indicate that the addition of CO₂ plays a positive role in inhibiting the formation of NO and NO₂ but promoting the formation of CO.

Table 3. Mole fractions of gas products under different working conditions.

Working condition	CO	CO ₂	NO	NO ₂
7% CH ₄	0.01590066	0.05270834	0.01503820	0.00000793779
7% CH ₄ + 10% CO ₂	0.02811000	0.03818010	0.00944985	0.00000484152
9.50% CH ₄	0.04258436	0.04812039	0.01105626	0.00000329051
9.5% CH ₄ + 10% CO ₂	0.06740572	0.01813410	0.00693919	0.00000190858
11% CH ₄	0.06146430	0.04155837	0.00759739	0.00000149968
11% CH ₄ + 10% CO ₂	0.09511225	0.00064950	0.00415820	0.00000070496

3.4. Key reactions

The key elementary reaction steps during the methane explosion under different conditions are shown in Figure 6. According to Figure 6(a), when 7% CH₄-Air explodes, the key reaction steps inhibiting CH₄ consumption are R53 and R158. Both reactions consume the free radicals H, O, and OH, which interrupt the chain reaction. The key reaction steps promoting CH₄ consumption are R118, R155, R157, R156, R38, R52, R119, and R85. These reactions promote the formation of free radicals, and enhance the chain reaction.

According to Figure 6(b), after the addition of 10% CO₂, the key elementary reaction steps inhibiting CH₄ consumption change from R53 and R158 to R158, R53, and R98. The key reaction step promoting CH₄ consumption change from R118, R155, R157, R156, R38, R52, R119, and R85 to R155, R156, R38, R32, R119, R161, and R170. The sensitivity coefficients of each elementary reaction step are decreased, and the time of the maximum sensitivity coefficient of each elementary reaction step prolongs; at the same time, the reduction amplitude of the coefficient to promote methane consumption is greater than to promote methane formation. This indicates that the change in methane concentration is affected by these reaction steps, the influence becomes weaker, and the addition of CO₂ inhibits the combustion of methane.

Figures 6(c) and (d) show that, when 9.5% CH₄-Air explodes, the key elementary reaction steps inhibiting CH₄ consumption are R158, R53, and R57, and the key elementary reaction steps promoting CH₄ consumption are R155, R156, R38, R32, R119, R161, and R170. When 10% CO₂ was added, the key elementary reaction steps promoting and inhibiting CH₄ consumption do not

change, and the sensitivity coefficient value is virtually unchanged. However, the time when the sensitivity coefficient of each elementary reaction step reaches the maximum value moves back. This means that for the methane explosion with a methane equivalence ratio of 1, the addition of CO_2 has little effect on the change in the methane concentration during the explosion, but inhibits the methane explosion.

As Figures 6(e) and (f) show, when 11% CH_4 -Air explodes, the key elementary reaction steps inhibiting CH_4 consumption are R158 and R53, and the key elementary reaction steps promoting CH_4 combustion are R118, R155, R156, R38, R32, R119, R161, and R170. When 10% CO_2 was added, the key elementary reaction steps inhibiting CH_4 consumption are R158, R53, and R57, and the key elementary reaction steps promoting CH_4 combustion are R155, R156, R38, R32, R119, R161, and R170. The key elementary reaction steps promoting and inhibiting CH_4 consumption are basically the same as those without CO_2 , but the sensitivity coefficients of each elementary reaction step are decreased, and the reduction amplitude of the coefficient of promoting CH_4 consumption is greater than inhibiting CH_4 consumption. This indicates that the addition of CO_2 inhibits the process of methane explosion to a certain extent.

Figure 6. Key reaction steps affecting the change in methane volume fraction: (a) 7% CH_4 0% CO_2 , (b) 7% CH_4 10% CO_2 , (c) 9.5% CH_4 0% CO_2 , (d) 9.5% CH_4 10% CO_2 , (e) 11% CH_4 0% CO_2 , and (f) 11% CH_4 10% CO_2 .

4. Conclusion

In this study, 2%, 4%, 6%, 8%, and 10% CO₂ were sequentially filled into a mixed gas with different methane concentrations. the explosion reaction time prolonged as the increase of CO₂ volume fraction and the maximum pressure and temperature of the methane explosion were significantly reduced compared with the case with no CO₂ addition. If the volume fraction of CO₂ is constant, with the increase of methane concentration, the inhibitory effect of CO₂ on methane explosion was increasingly effective.

In the fuel-lean, stoichiometric and fuel-rich conditions, the peak mole fraction of free radicals decreased with the increase of the CO₂ volume fraction. When the volume fraction of CO₂ is constant, as the volume fraction of methane increased, the maximum mole fraction of radical H increased, while the maximum mole fraction of radical O decreased. For radical OH, its maximum mole fraction first increased and then decreased with the location of peak value of 9.5%.

After 10% CO₂ was added to the 7% CH₄-Air, the mole fraction of CO increased by 76%, while the mole fractions of CO₂, NO, and NO₂ decreased by 27%, 37%, and 39%, respectively. The higher the volume fraction of CH₄, the more CO was produced after the addition of CO₂. Although the addition of CO₂ played a positive role in inhibiting the formation of NO and NO₂, it promoted the formation of CO.

The addition of CO₂ changed the key elementary reaction steps affecting CH₄ concentration, and the time of the maximum sensitivity coefficient of each reaction step prolonged. When CH₄ was in a fuel-lean, stoichiometric and fuel-rich conditions, the sensitivity coefficient of each key elementary reaction step was reduced, and the reduction amplitude of the coefficient promoting methane consumption was larger than inhibiting the consumption, indicated that the addition of CO₂ could inhibit CH₄ explosion.

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